
Scheme-3 Reactor-1

Part-2, Case-3

$t_a = 1800 \text{ sec}$, $t_m = 1200 \text{ sec}$
 $k_1 = 0.1$, $k_2 = 0.01$

$NB_t/NA_t = 1.72223$

Exponent $a = 1$
Exponent $b = 1$
Exponent $c = 0.5$
Exponent $d = 1.5$

$WA = 200$
 $WB = 86.1117$
 $NB_t = 4.59262$
 $V_t = 2.14306$
 $V_{at} = 1.04306$
 $Tot.Solv. = 2$
 $SolA/(SolR+SolA) = 0.5$

$NA_0 = 2.66667$
 $NB_0 = 0$

Total input = 286.112 kg
Total output = 286.114 kg

Chemical Balance Error = 0.00195698 kg (% 6.83991e-06)

Solver: Explicit Runge-Kutta (4,5) Variable step (Dormand-Prince Pair)
Error tolerance: 0.1%

Final Concentrations with Step Size limited to 0.001

$NA \text{ (final)} = 0.0266606$
 $NB \text{ (final)} = 6.64627e-13$
 $NR \text{ (final)} = 0.687389$
 $NS \text{ (final)} = 1.95262$

Final Concentrations with Step Size limited to 0.01

$NA \text{ (final)} = 0.0266603$
 $NB \text{ (final)} = 6.64913e-11$
 $NR \text{ (final)} = 0.687388$
 $NS \text{ (final)} = 1.95262$



