
Scheme-2 Reactor-1

Part-2, Case-4

$t_a = 900 \text{ sec}$, $t_m = 1200 \text{ sec}$
 $k_1 = 0.1$, $k_2 = 0.01$

$NB_t/NA_t = 1.06066$

Exponent $a = 1$
Exponent $b = 1$
Exponent $c = 1.5$
Exponent $d = 0.5$

$WA = 200$
 $WB = 53.0332$
 $NB_t = 2.82844$
 $V_t = 2.12652$
 $V_{at} = 0.526517$
Tot.Solv. = 2
 $SolA/(SolR+SolA) = 0.25$

$NA_0 = 2.66667$
 $NB_0 = 0$

Total input = 253.033 kg
Total output = 253.033 kg

Chemical Balance Error = 0.000237705 kg (% 9.39423e-07)

Solver: Explicit Runge-Kutta (4,5) Variable step (Dormand-Prince Pair)
Error tolerance: 0.1%

Final Concentrations with Step Size limited to 0.01

$NA \text{ (final)} = 0.0266753$
 $NB \text{ (final)} = 0.00445016$
 $NR \text{ (final)} = 2.45599$
 $NS \text{ (final)} = 0.183997$

Final Concentrations with Step Size limited to 0.1

$NA \text{ (final)} = 0.0266585$
 $NB \text{ (final)} = 0.00445394$
 $NR \text{ (final)} = 2.45598$
 $NS \text{ (final)} = 0.18403$



