
Scheme-8 Reactor-1

Part-3, Case-2

$t_a = 450 \text{ sec}$, $t_m = 1200 \text{ sec}$
 $k_1 = 0.1$, $k_2 = 0.002$

$NB_t/NA_t = 1.07794$

Exponent $a = 0.5$
Exponent $b = 1.5$
Exponent $c = 1$
Exponent $d = 1$

$WA = 200$
 $WB = 53.8971$
 $NB_t = 2.87451$
 $V_t = 2.12695$
 $V_{at} = 1.02695$
 $Tot.Solv. = 2$
 $SolA/(SolR+SolA) = 0.5$

$NA_0 = 2.66667$
 $NB_0 = 0$

Total input = 253.897 kg
Total output = 253.897 kg

Chemical Balance Error = 0.000242852 kg (% 9.56497e-07)

Solver: Explicit Runge-Kutta (4,5) Variable step (Dormand-Prince Pair)
Error tolerance: 0.1%

Final Concentrations with Step Size limited to 0.001

$NA \text{ (final)} = 0.0266116$
 $NB \text{ (final)} = 0.00252469$
 $NR \text{ (final)} = 2.40812$
 $NS \text{ (final)} = 0.231935$

Final Concentrations with Step Size limited to 0.01

$NA \text{ (final)} = 0.0266086$
 $NB \text{ (final)} = 0.00252481$
 $NR \text{ (final)} = 2.40812$
 $NS \text{ (final)} = 0.231937$



