
Scheme-3 Reactor-1

Part-2, Case-5

$t_a = 900 \text{ sec}$, $t_m = 1200 \text{ sec}$
 $k_1 = 0.1$, $k_2 = 0.01$

$NB_t/NA_t = 1.66762$

Exponent $a = 1$
Exponent $b = 1$
Exponent $c = 0.5$
Exponent $d = 1.5$

$WA = 200$
 $WB = 83.3812$
 $NB_t = 4.447$
 $V_t = 2.14169$
 $V_{at} = 1.54169$
 $Tot.Solv. = 2$
 $SolA/(SolR+SolA) = 0.75$

$NA_0 = 2.66667$
 $NB_0 = 0$

Total input = 283.381 kg
Total output = 283.383 kg

Chemical Balance Error = 0.00181543 kg (% 6.40632e-06)

Solver: Explicit Runge-Kutta (4,5) Variable step (Dormand-Prince Pair)
Error tolerance: 0.1%

Final Concentrations with Step Size limited to 0.001

$NA \text{ (final)} = 0.0266576$
 $NB \text{ (final)} = 1.18478e-12$
 $NR \text{ (final)} = 0.833022$
 $NS \text{ (final)} = 1.80699$

Final Concentrations with Step Size limited to 0.01

$NA \text{ (final)} = 0.026657$
 $NB \text{ (final)} = -1.1849e-10$
 $NR \text{ (final)} = 0.833019$
 $NS \text{ (final)} = 1.80699$



