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# Scheme-3 Reactor-1

Part-2, Case-4

$t_a = 900 \text{ sec}$ ,  $t_m = 1200 \text{ sec}$   
 $k_1 = 0.1$ ,  $k_2 = 0.01$

$NB_t/NA_t = 1.65467$

Exponent  $a = 1$   
Exponent  $b = 1$   
Exponent  $c = 0.5$   
Exponent  $d = 1.5$

$WA = 200$   
 $WB = 82.7336$   
 $NB_t = 4.41246$   
 $V_t = 2.14137$   
 $V_{at} = 0.541367$   
Tot.Solv. = 2  
 $SolA/(SolR+SolA) = 0.25$

$NA_0 = 2.66667$   
 $NB_0 = 0$

Total input = 282.734 kg  
Total output = 282.735 kg

Chemical Balance Error = 0.00178084 kg (% 6.29867e-06)

Solver: Explicit Runge-Kutta (4,5) Variable step (Dormand-Prince Pair)  
Error tolerance: 0.1%

Final Concentrations with Step Size limited to 0.001

$NA \text{ (final)} = 0.0266737$   
 $NB \text{ (final)} = 1.3386e-12$   
 $NR \text{ (final)} = 0.867527$   
 $NS \text{ (final)} = 1.77247$

Final Concentrations with Step Size limited to 0.01

$NA \text{ (final)} = 0.0266732$   
 $NB \text{ (final)} = 1.33872e-10$   
 $NR \text{ (final)} = 0.867524$   
 $NS \text{ (final)} = 1.77247$



