

Research Article

A Note on the Unsteady Incompressible MHD Fluid Flow with Slip Conditions and Porous Walls

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This work is concerned with the influence of uniform suction or injection on flow and heat transfer analysis of unsteady incompressible magnetohydrodynamic (MHD) fluid with slip conditions. The resulting unsteady problem for velocity and heat transfer is solved by means of Laplace transform. The characteristics of the transient velocity, overall transient velocity, steady state velocity and heat transfer at the walls are analyzed and discussed. Graphical results reveal that the magnetic field, slip parameter, and suction (injection) have significant influences on the velocity, and temperature distributions, which also changes the heat transfer behaviors at the two plates. The results of Fang (2004) are also recovered by keeping magnetic field and slip parameter absent.

1. Introduction

Navier-Stokes equations are the basic equations of fluid mechanics. Exact solutions of Navier-Stokes equations are rare due to their inherent nonlinearity. Exact solutions are important because they serve as accuracy checks for numerical solutions. Complete integration of these equations is done by computer techniques, but the accuracy of the results can be established only by comparison with exact solutions. In the literature, there are a large number of Newtonian fluid flows for which exact solutions are possible [1–6]. The effects of transverse magnetic field on the flow of an electrically conducting viscous fluid have been studied extensively in view of numerous applications to astrophysical, geophysical, and engineering problems [7–15]. If the working fluid contains concentrated suspensions, then the wall slip can occur [16]. Khaled and Vafai [3] studied the effect of the slip on Stokes and Couette flows due to an oscillating wall. However, the literature lacks studies that take into account the possibility of fluid slippage at the walls. Applications of these problems appear in microchannels or nanochannels and in applications where a thin film of light oil is attached to the moving plates or when the surface is coated with special coating such as a thick monolayer of hydrophobic

octadecyltrichlorosilane [17]. Yu and Ameel [18] imposed nonlinear slip boundary conditions on flow in rectangular microchannels. Erdogan [6] studied deeply the solution to the Stokes problem under nonslip conditions at the wall. Ayub and Zaman [19] studied the effects of suction and blowing for orthogonal flow impinging on a wall. Khan et al. [20] discussed the flow of Sisko fluid through a porous medium. Ariel et al. [21] considered the flow of elasticoviscous fluid with partial slip. Raptis et al. [22–25] studied steady and unsteady free convection and mass transfer flow through a porous medium. Penton [26] presented the transient solution for the flow due to the oscillating plate.

In this note, the flow of an incompressible, unsteady, viscous, MHD fluid with slip conditions is considered. Unsteady means time dependent flow, and we are looking for the effects of different parameters on flow with the variation of time. Unsteady and steady velocity profiles with mass transfer will be presented and solved exactly. There is mass injection from one plate and the same amount of suction on the other plate. The steady state temperature is also solved and discussed. When the fluid motion is set up from rest, the velocity field contains transients, determined by the initial conditions which gradually disappear in time. The effect of magnetic field and time on the transient

velocity and on overall transient velocity has been seen graphically for both injection and suction. The effect of slip parameter on steady state velocity for injection/suction is shown graphically. Steady state temperature profiles and heat transfer rate at the walls (Nusselt number at the walls) are also discussed for injection/suction for different Prandtl and Reynolds numbers. The results of Fang [1] are recovered by taking magnetic field parameter and slip parameter to be zero.

2. Theoretical Derivation

2.1. Transient Velocity Profiles. Consider an incompressible, viscous, unsteady flow problem, in which there is slip between the bottom wall and fluid and also between top wall and fluid. There are mass injection velocity v_w at the bottom wall and mass suction velocity v_w at the top wall; $v_w > 0$ corresponds to injection and $v_w < 0$ corresponds to suction. The governing equation for this problem can be obtained as [2]

$$\frac{\partial u(y,t)}{\partial t} + v_w \frac{\partial u(y,t)}{\partial y} = \nu \frac{\partial^2 u(y,t)}{\partial y^2} - Nu(y,t), \quad (1)$$

where $u(y,t)$ is the velocity of the fluid in the y -direction which is along the wall direction, y is the distance along y -axis, t is the time, $\nu = \mu/\rho$, $N = \sigma B_0^2/\rho$, μ is the dynamic viscosity, ν is the kinematic viscosity, ρ is the density of the fluid, σ is the electric conductivity of the fluid, B_0 is the applied magnetic field, and N is the MHD factor or parameter. For the boundary conditions we consider the existence of slip between the velocity of the fluid at the walls and speed of the walls:

$$\begin{aligned} u(0,t) - \lambda \frac{\partial u(y,t)}{\partial y} \Big|_{y=0} &= 0, \\ u(h,t) + \lambda \frac{\partial u(y,t)}{\partial y} \Big|_{y=h} &= U_0. \end{aligned} \quad (2)$$

Initial condition is

$$u(y,0) = 0, \quad (3)$$

where λ is the slip parameter ($\lambda = 0$ gives the usual no slip condition at the wall) and U_0 is the velocity at the upper wall. The problem exactly reduces to the problem of Fang [1] if we take $N = 0$, $\lambda = 0$. Equations (1), (2), and (3) can be made dimensionless by defining

$$U = \frac{u}{U_0}, \quad Y = \frac{y}{h}, \quad T = \frac{t}{\tau_c} = \frac{t\nu}{h^2}. \quad (4)$$

Then (1), (2), and (3) become

$$\frac{\partial U}{\partial T} + R_e \frac{\partial U}{\partial Y} = \frac{\partial^2 U}{\partial Y^2} - \bar{N}U, \quad (5)$$

$$U(0,T) - \bar{\lambda} \frac{\partial U(Y,T)}{\partial Y} \Big|_{Y=0} = 0, \quad (6)$$

$$U(1,T) + \bar{\lambda} \frac{\partial U(Y,T)}{\partial Y} \Big|_{Y=1} = 1, \quad (7)$$

$$U(Y,0) = 0, \quad (8)$$

where $\bar{N} = N(h^2/\nu)$, $\bar{\lambda} = \lambda/h$, and $R_e = v_w(h/\nu)$ (Reynolds number). Decomposing $U(Y,T)$ into two parts, say, transient part and a steady state part,

$$U(Y,T) = U_t(Y,T) + U_s(Y,T). \quad (9)$$

Then we have two separate problems and the steady state part will be

$$R_e \frac{dU_s}{dY} = \frac{d^2 U_s}{dY^2} - \bar{N}U_s, \quad (10)$$

$$U_s(0,T) - \bar{\lambda} \frac{\partial U_s(Y,T)}{\partial Y} \Big|_{Y=0} = 0, \quad (11)$$

$$U_s(1,T) + \bar{\lambda} \frac{\partial U_s(Y,T)}{\partial Y} \Big|_{Y=1} = 1. \quad (12)$$

The solution of (10) with BCs (11) and (12) can be obtained as

$$U_s(Y) = \frac{e^{aY} \left[(1 - \bar{\lambda}a) \sinh(b_1 Y) + \bar{\lambda}b_1 \cosh(b_1 Y) \right]}{e^a \left[(1 - \bar{\lambda}^2(a^2 - b_1^2)) \sinh(b_1) + 2\bar{\lambda}b_1 \cosh(b_1) \right]}, \quad (13)$$

where $a = R_e/2$ and $b_1 = \sqrt{R_e^2/4 + \bar{N}}$. When $\bar{\lambda} = 0$ (no slip) and $\bar{N} = 0$ (no magnetic field), then (13) becomes

$$U_s(Y) = \frac{e^{(R_e/2)Y} \sinh(R_e/2) Y}{e^{R_e/2} \sinh(R_e/2)} = \frac{1 - e^{R_e Y}}{1 - e^{R_e}}. \quad (14)$$

Equation (14) the result number (7) of Fang [1]. If there is no mass transfer at the walls, then $R_e = 0$, so $a = 0$ and $b_1 = \sqrt{\bar{N}}$, and (13) becomes

$$U_s(Y) = \frac{\sinh(\sqrt{\bar{N}}Y) + \bar{\lambda}\sqrt{\bar{N}} \cosh(\sqrt{\bar{N}}Y)}{(1 + \bar{\lambda}^2\bar{N}) \sinh(\sqrt{\bar{N}}) + 2\bar{\lambda}\sqrt{\bar{N}} \cosh(\sqrt{\bar{N}})}. \quad (15)$$

If there is no mass transfer at the walls and magnetic field is absent, then $R_e = 0$, $\bar{N} = 0$, and slip parameter $\bar{\lambda} = 0$ then (10), (11), and (12) will collapse into

$$\frac{d^2 U_s(Y)}{dY^2} = 0, \quad U_s(0) = 0, \quad U_s(1) = 1. \quad (16)$$

Its solution is $U_s(Y) = Y$, which is conventional Couette flow. When $R_e \rightarrow -\infty$, $\bar{N} = 0$, and $\bar{\lambda} = 0$, then (13) gives $U_s(Y) = 1$, except at the bottom wall (at the bottom wall $Y = 0$ and $U_s(0) = 0$). When $R_e \rightarrow \infty$, $\bar{N} = 0$, and $\bar{\lambda} = 0$, then (13) gives $U_s(Y) = 0$, except at the upper wall (at the upper wall $Y = 1$ and $U_s(1) = 1$). The transient part problem becomes

$$\frac{\partial U_t}{\partial T} + R_e \frac{\partial U_t}{\partial Y} = \frac{\partial^2 U_t}{\partial Y^2} - \bar{N} U_t, \quad (17)$$

$$U_t(0, T) - \bar{\lambda} \frac{\partial U_t(Y, T)}{\partial Y} \Big|_{Y=0} = 0, \quad (18)$$

$$U_t(1, T) + \bar{\lambda} \frac{\partial U_t(Y, T)}{\partial Y} \Big|_{Y=1} = 1, \quad (19)$$

$$U_t(Y, 0) = -U_s(Y). \quad (20)$$

The solution can be derived by using Laplace transformation techniques [27]. The Laplace transform pair is defined by

$$\bar{U}(Y, s) = L[U(Y, T)] = \int_0^\infty U(Y, T) e^{-sT} dT, \quad (21)$$

$$U(Y, T) = L^{-1}[\bar{U}(Y, s)] = \frac{1}{2\pi i} \int_{\lambda_1 - i\infty}^{\lambda_1 + i\infty} \bar{U}(Y, s) e^{sT} ds,$$

over that range of values of s for which the integrals exist. Here, s is a parameter, real or complex, L is the operator that transforms $U(Y, T)$ into $\bar{U}(Y, s)$, called Laplace transform operator, and L^{-1} is the inverse Laplace transform operator. The solution can be shown as

$$\begin{aligned} U_t(Y, T) = L^{-1} & \left[\left(e^{aY} \left((1 - \bar{\lambda}a) \sinh(bY) + \bar{\lambda}b \cosh(bY) \right) \right) \right. \\ & \times \left(e^a s \left(\left(1 - \bar{\lambda}^2 (a^2 - b^2) \right) \sinh(b) \right. \right. \\ & \left. \left. + 2\bar{\lambda}b \cosh(b) \right) \right)^{-1} \Big] - U_s, \end{aligned} \quad (22)$$

where $a = R_e/2$ and $b = \sqrt{R_e^2/4 + s + \bar{N}}$. In inverse Laplace transform of the above equation we have simple pole at $s = 0$ and infinite number of poles (located on the negative real axis) at $s_n = -(l_n^2 + a^2 + \bar{N})$, ($n = 1, 2, 3, \dots$), where $l_n = ib_n$, ($b_n = \sqrt{R_e^2/4 + s_n + \bar{N}}$) and are given by

$$\tan(l_n) = \frac{-2\bar{\lambda}l_n}{1 - \bar{\lambda}^2(a^2 + l_n^2)}. \quad (23)$$

The transient part velocity will be

$$\begin{aligned} U_t(Y, T) = \sum_{n=1}^{\infty} \text{Re } s \left[\bar{U}_t(Y, s) e^{sT} \right]_{s=s_n} \\ + \text{Re } s \left[\bar{U}_t(Y, s) e^{sT} \right]_{s=0} - U_s, \end{aligned} \quad (24)$$

where $\text{Re } s$ stands for residue and $\bar{U}_t(Y, s)$ is given by

$$\bar{U}_t(Y, s) = \frac{e^{aY} \left((1 - \bar{\lambda}a) \sinh(bY) + \bar{\lambda}b \cosh(bY) \right)}{e^a s \left(\left(1 - \bar{\lambda}^2 (a^2 - b^2) \right) \sinh(b) + 2\bar{\lambda}b \cosh(b) \right)}. \quad (25)$$

We have

$$\sum_{n=1}^{\infty} \text{Re } s \left[\bar{U}_t(Y, s) e^{sT} \right]_{s=s_n} = \sum_{n=1}^{\infty} \frac{G_1(l_n, Y)}{G_2(l_n)} e^{s_n T}, \quad (26)$$

where

$$\begin{aligned} G_1(l_n, Y) = e^{aY} & \left((1 - \bar{\lambda}a) \sin(l_n Y) \right. \\ & \left. + \bar{\lambda}l_n \cos(l_n Y) \right), \end{aligned}$$

$$\begin{aligned} G_2(l_n) = e^a s_n & \left(\bar{\lambda}(\bar{\lambda} + 1) \sin(l_n) \right. \\ & \left. - (1 + 2\bar{\lambda} - \bar{\lambda}^2 (a^2 + l_n^2)) \frac{\cos(l_n)}{2l_n} \right). \end{aligned} \quad (27)$$

The residue at $s = 0$ gives steady velocity

$$\begin{aligned} \text{Re } s \left[\bar{U}_t(Y, s) e^{sT} \right]_{s=0} \\ = \lim_{s \rightarrow 0} \left[s \bar{U}_t(Y, s) e^{sT} \right] \\ = \lim_{s \rightarrow 0} \left(e^{aY} \left((1 - \bar{\lambda}a) \sinh(bY) \right. \right. \\ \left. \left. + \bar{\lambda}b \cosh(bY) \right) e^{sT} \right) \\ \times \left(e^a \left(\left(1 - \bar{\lambda}^2 (a^2 - b^2) \right) \sinh(b) \right. \right. \\ \left. \left. + 2\bar{\lambda}b \cosh(b) \right) \right)^{-1}, \end{aligned} \quad (28)$$

$$\lim_{s \rightarrow 0} b = \lim_{s \rightarrow 0} \sqrt{\frac{R_e^2}{4} + s + \bar{N}} = \sqrt{\frac{R_e^2}{4} + \bar{N}} = b_1.$$

Therefore,

$$\begin{aligned} \text{Re } s \left[\bar{U}_t(Y, s) e^{sT} \right]_{s=0} \\ = \left(e^{aY} \left[(1 - \bar{\lambda}a) \sinh(b_1 Y) + \bar{\lambda}b_1 \cosh(b_1 Y) \right] \right) \\ \times \left(e^a \left[\left(1 - \bar{\lambda}^2 (a^2 - b_1^2) \right) \right. \right. \\ \left. \left. \times \sinh(b_1) + 2\bar{\lambda}b_1 \cosh(b_1) \right] \right)^{-1}. \end{aligned} \quad (29)$$

By using (13), we get

$$\text{Re } s \left[\bar{U}_t(Y, s) e^{sT} \right]_{s=0} = U_s. \quad (30)$$

The transient part velocity from (24) becomes

$$\begin{aligned}
 U_t(Y, T) &= \sum_{n=1}^{\infty} \frac{G_1(l_n, Y)}{G_2(l_n)} e^{s_n T}, \\
 U_t(Y, T) &= \sum_{n=1}^{\infty} \left[\left(e^{aY} \left((1 - \bar{\lambda}a) \sin(l_n Y) + \bar{\lambda} l_n \cos(l_n Y) \right) \right) \right. \\
 &\quad \times \left(e^a s_n \left(\bar{\lambda} (\bar{\lambda} + 1) \sin(l_n) \right. \right. \\
 &\quad \left. \left. - \left(1 + 2\bar{\lambda} - \bar{\lambda}^2 (a^2 + l_n^2) \right) \right. \right. \\
 &\quad \left. \left. \times \frac{\cos(l_n)}{2l_n} \right) \right]^{-1} e^{s_n T}. \tag{31}
 \end{aligned}$$

Therefore, the overall transient solution from (9) becomes

$$\begin{aligned}
 U(Y, T) &= \sum_{n=1}^{\infty} \left\{ \left(e^{aY} \left((1 - \bar{\lambda}a) \sin(l_n Y) + \bar{\lambda} l_n \cos(l_n Y) \right) \right) \right. \\
 &\quad \times \left(e^a s_n \left(\bar{\lambda} (\bar{\lambda} + 1) \sin(l_n) \right. \right. \\
 &\quad \left. \left. - \left(1 + 2\bar{\lambda} - \bar{\lambda}^2 (a^2 + l_n^2) \right) \right. \right. \\
 &\quad \left. \left. \times \frac{\cos(l_n)}{2l_n} \right) \right) \right\}^{-1} e^{s_n T} \\
 &+ \left(e^{aY} \left[(1 - \bar{\lambda}a) \sinh(b_1 Y) + \bar{\lambda} b_1 \cosh(b_1 Y) \right] \right) \\
 &\times \left(e^a \left[\left(1 - \bar{\lambda}^2 (a^2 - b_1^2) \right) \sinh(b_1) \right. \right. \\
 &\quad \left. \left. + 2\bar{\lambda} b_1 \cosh(b_1) \right] \right)^{-1}. \tag{32}
 \end{aligned}$$

To recover Fang [1] result number (13) we substitute $\bar{\lambda} = 0$, $\bar{N} = 0$, $a = R_e/2$, and $b_1 = R_e/2$ into (32), and we get

$$\begin{aligned}
 U(Y, T) &= \sum_{n=1}^{\infty} \left\{ \frac{\sin(l_n Y) e^{s_n T} e^{(R_e/2)Y}}{-e^{R_e/2} s_n \cos(l_n) / (2l_n)} \right\} \\
 &+ \frac{\sinh((R_e/2)Y) e^{(R_e/2)Y}}{e^{R_e/2} \sinh(R_e/2)}. \tag{33}
 \end{aligned}$$

Since $\bar{\lambda} = 0$, so (23) gives

$$\tan(l_n) = 0 \implies \sin(l_n) = 0 \implies l_n = \arcsin(0) = n\pi, \tag{34}$$

$$n = 1, 2, 3, \dots$$

Therefore $\cos(l_n) = \cos(n\pi) = (-1)^n$; also we have $l_n = ib_n$, ($b_n = \sqrt{R_e^2/4 + s_n + \bar{N}}$), but $\bar{N} = 0$, so

$$\begin{aligned}
 l_n &= i \sqrt{\frac{R_e^2}{4} + s_n} \implies n\pi = i \sqrt{\frac{R_e^2}{4} + s_n} \\
 &\implies n^2 \pi^2 = - \left(\frac{R_e^2}{4} + s_n \right) \\
 &\implies s_n = - \left(n^2 \pi^2 + \frac{R_e^2}{4} \right). \tag{35}
 \end{aligned}$$

Using $l_n = n\pi$, $\cos(l_n) = (-1)^n$, and $s_n = -(n^2 \pi^2 + R_e^2/4)$ into (33) we obtain

$$\begin{aligned}
 U(Y, T) &= \frac{2\pi e^{-(R_e^2/4)T} e^{(R_e/2)Y}}{e^{R_e/2}} \\
 &\times \sum_{n=1}^{\infty} \left\{ \frac{n(-1)^n \sin(n\pi Y) e^{-n^2 \pi^2 T}}{(n^2 \pi^2 + R_e^2/4)} \right\} \\
 &+ \frac{\sinh((R_e/2)Y) e^{(R_e/2)Y}}{e^{R_e/2} \sinh(R_e/2)}. \tag{36}
 \end{aligned}$$

Consider

$$\begin{aligned}
 &\frac{\sinh((R_e/2)Y) e^{(R_e/2)Y}}{e^{R_e/2} \sinh(R_e/2)} \\
 &= \frac{e^{(R_e/2)Y} (e^{(R_e/2)Y} - e^{-(R_e/2)Y})}{e^{R_e/2} (e^{R_e/2} - e^{-R_e/2})} \\
 &= \frac{(e^{R_e Y} - 1)}{(e^{R_e} - 1)} = \frac{(1 - e^{-R_e Y})}{(1 - e^{-R_e})}. \tag{37}
 \end{aligned}$$

So (36) becomes

$$\begin{aligned}
 U(Y, T) &= \frac{2\pi e^{-(R_e^2/4)T} e^{(R_e/2)Y}}{e^{R_e/2}} \\
 &\times \sum_{n=1}^{\infty} \left\{ \frac{n(-1)^n \sin(n\pi Y) e^{-n^2 \pi^2 T}}{(n^2 \pi^2 + R_e^2/4)} \right\} \\
 &+ \frac{(1 - e^{-R_e Y})}{(1 - e^{-R_e})}. \tag{38}
 \end{aligned}$$

Result number (13) of Fang [1] is exactly followed in (38).

2.2. Steady State Temperature. It is too difficult to exactly solve the transient energy equation with viscous dissipation for this problem by using $U(Y, T)$. We solve the steady state energy equation, which in dimensionless form is given by [1]

$$\begin{aligned}
 P_r R_e \frac{d\sigma}{dY} &= \frac{d^2 \sigma}{dY^2} + E_c P_r \left(\frac{dU_s}{dY} \right)^2, \\
 \sigma(0) &= 0, \quad \sigma(1) = 1, \tag{39}
 \end{aligned}$$

where $P_r = \nu/\alpha$ is the Prandtl number, $E_c = U_0^2/c_p(\theta_1 - \theta_2)$ is the Eckert number, θ_1 is temperature of the bottom fixed plate, θ_2 is temperature of the top moving plate, σ is dimensionless temperature ($\sigma = (\theta - \theta_1)/(\theta_2 - \theta_1)$), and U_s is the steady state velocity given by (13). The solution of (39) with BCs (35) for $P_r \neq 1$, is

$$\begin{aligned} \sigma(Y) = & \frac{(e^{P_r R_e Y} - 1)}{(e^{P_r R_e} - 1)} \\ & + E_c P_r M \left[\frac{(e^{P_r R_e Y} - 1)}{(e^{P_r R_e} - 1)} \right. \\ & \times \{N_1 (e^{2(a+b_1)} - 1) \\ & \quad + N_2 (e^{2(a-b_1)} - 1) - N_3 (e^{2a} - 1)\} \\ & + \{N_1 (1 - e^{2(a+b_1)Y}) \\ & \quad + N_2 (1 - e^{2(a-b_1)Y}) - N_3 (1 - e^{2aY})\} \left. \right], \end{aligned} \quad (40)$$

where

$$\begin{aligned} N_1 &= \frac{M_1}{L_1}, \quad N_2 = \frac{M_2}{L_2}, \quad N_3 = \frac{M_3}{L_3}, \\ L_1 &= 4(a + b_1)^2 - 2P_r R_e (a + b_1), \\ L_2 &= 4(a - b_1)^2 - 2P_r R_e (a - b_1), \quad L_3 = R_e^2 (1 - P_r), \\ M &= \frac{1}{\left[e^a \left\{ (1 - \bar{\lambda}^2 (a^2 - b_1^2)) \sinh(b_1) + 2\bar{\lambda} b_1 \cosh(b_1) \right\} \right]^2}, \\ M_1 &= \left(\frac{B_1 + b_1}{2} \right)^2, \quad M_2 = \left(\frac{B_1 - b_1}{2} \right)^2, \\ M_3 &= \left(\frac{B_1^2 - b_1^2}{2} \right), \\ B_1 &= (a - \bar{\lambda} (a^2 - b_1^2)). \end{aligned} \quad (41)$$

When viscous dissipation term is negligible, then energy equation (39) is

$$\frac{d^2 \sigma}{dY^2} - P_r R_e \frac{d\sigma}{dY} = 0, \quad \sigma(0) = 0, \quad \sigma(1) = 1. \quad (42)$$

Its solution is

$$\sigma(Y) = \frac{(e^{P_r R_e Y} - 1)}{(e^{P_r R_e} - 1)}. \quad (43)$$

So the first term in (40) is the solution of energy equation when viscous dissipation term is negligible and the second term in (40) is the temperature profile from viscous dissipation and MHD. It is found from (40) that the temperature

profile is linearly dependent upon the Eckert number. The Nusselt number at the walls will be $N_u = |d\sigma/dY|_w$. The Nusselt number for the bottom wall, $Y = 0$, is

$$\begin{aligned} N_{u_1} &= \left. \frac{d\sigma}{dY} \right|_{Y=0}, \\ N_{u_1} &= \left| \frac{P_r R_e}{(e^{P_r R_e} - 1)} \left[1 + E_c P_r M \left\{ N_1 (e^{2(a+b_1)} - 1) \right. \right. \right. \\ & \quad \left. \left. \left. + N_2 (e^{2(a-b_1)} - 1) \right. \right. \right. \\ & \quad \left. \left. \left. - N_3 (e^{2a} - 1) \right\} \right] \right. \\ & \quad \left. - 2E_c P_r M \left\{ N_1 (a + b_1) \right. \right. \\ & \quad \left. \left. + N_2 (a - b_1) - N_3 a \right\} \right|. \end{aligned} \quad (44)$$

The Nusselt number for the upper wall, $Y = 1$, is

$$\begin{aligned} N_{u_2} &= \left. \frac{d\sigma}{dY} \right|_{Y=1}, \\ N_{u_2} &= \left| \frac{P_r R_e e^{P_r R_e}}{(e^{P_r R_e} - 1)} \right. \\ & \quad \times \left[1 + E_c P_r M \left\{ N_1 (e^{2(a+b_1)} - 1) \right. \right. \\ & \quad \left. \left. + N_2 (e^{2(a-b_1)} - 1) \right. \right. \\ & \quad \left. \left. - N_3 (e^{2a} - 1) \right\} \right] \\ & \quad - 2E_c P_r M \left\{ N_1 (a + b_1) e^{2(a+b_1)} \right. \\ & \quad \left. + N_2 (a - b_1) e^{2(a-b_1)} - N_3 a e^{2a} \right\} \left. \right|. \end{aligned} \quad (45)$$

When $P_r = 1$, then the energy equation is

$$\begin{aligned} \frac{d^2 \sigma}{dY^2} - R_e \frac{d\sigma}{dY} &= -E_c M \left\{ M_1 e^{2(a+b_1)Y} \right. \\ & \quad \left. + M_2 e^{2(a-b_1)Y} - M_3 e^{2aY} \right\}, \\ \sigma(0) &= 0, \quad \sigma(1) = 1. \end{aligned} \quad (46)$$

The solution of (46) is

$$\begin{aligned} \sigma(Y) &= \frac{(e^{R_e Y} - 1)}{(e^{R_e} - 1)} \left[1 + E_c M \left\{ N_4 (e^{2(a+b_1)} - 1) \right. \right. \\ & \quad \left. \left. + N_5 (e^{2(a-b_1)} - 1) \right. \right. \\ & \quad \left. \left. - \frac{M_3}{R_e} e^{2a} \right\} \right] \\ & \quad + 2E_c M \left\{ N_4 (1 - e^{2(a+b_1)Y}) \right. \\ & \quad \left. + N_5 (1 - e^{2(a-b_1)Y}) + \frac{M_3 Y}{R_e} e^{2aY} \right\}, \end{aligned} \quad (47)$$

where

$$\begin{aligned} N_4 &= \frac{M_1}{L_4}, & N_5 &= \frac{M_2}{L_5}, \\ L_4 &= 4(a+b_1)^2 - 2R_e(a+b_1), \\ L_5 &= 4(a-b_1)^2 - 2R_e(a-b_1). \end{aligned} \quad (48)$$

The Nusselt number in this case is

$$\begin{aligned} N_{u_1} &= \left| \frac{R_e}{(e^{R_e} - 1)} \right. \\ &\quad \times \left[1 + E_c M \left\{ N_4 (e^{2(a+b_1)} - 1) \right. \right. \\ &\quad \quad \left. \left. + N_5 (e^{2(a-b_1)} - 1) \right. \right. \\ &\quad \quad \left. \left. - \frac{M_3}{R_e} e^{2a} \right\} \right] \\ &\quad - 2E_c M \left\{ N_4 (a+b_1) \right. \\ &\quad \quad \left. \left. + N_5 (a-b_1) - \frac{M_3}{R_e} \right\} \right|, \\ N_{u_2} &= \left| \frac{R_e e^{R_e}}{(e^{R_e} - 1)} \right. \\ &\quad \times \left[1 + E_c M \left\{ N_4 (e^{2(a+b_1)} - 1) \right. \right. \\ &\quad \quad \left. \left. + N_5 (e^{2(a-b_1)} - 1) \right. \right. \\ &\quad \quad \left. \left. - \frac{M_3}{R_e} e^{2a} \right\} \right] \\ &\quad - 2E_c M \left\{ N_4 (a+b_1) e^{2(a+b_1)} \right. \\ &\quad \quad \left. \left. + N_5 (a-b_1) e^{2(a-b_1)} - \frac{M_3}{R_e} a e^{2a} \right\} \right|. \end{aligned} \quad (49)$$

It is worth recalling in the vicinity of (40) that when $\bar{\lambda} = 0$, $\bar{N} = 0$, then result number (18) of Fang [1] can be derived.

3. Graphs and Discussion

In this part we discuss the variation of the transient part velocity U_t , overall transient velocity U , and steady state velocity U_s with distance from the wall Y for different values of Reynolds number R_e , magnetic field parameter \bar{N} , slip parameter $\bar{\lambda}$, and time T .

Figures 1 and 2 show the variation of transient part velocity U_t with distance from the wall Y for several values of magnetic parameter \bar{N} , by keeping $\bar{\lambda}$ and T fixed. Figure 1 shows that when there is mass suction $R_e < 0$ at the

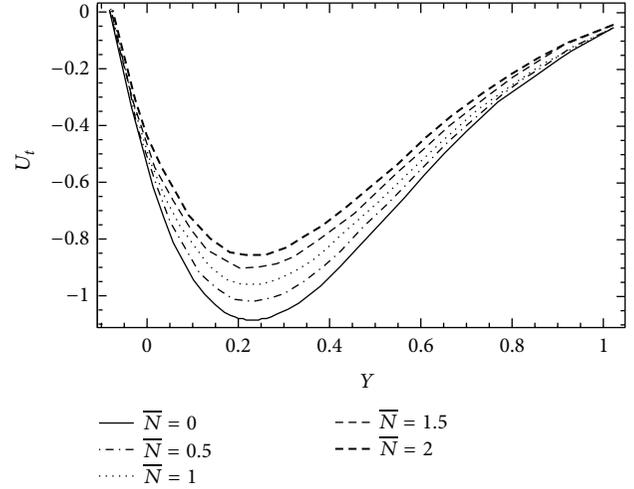


FIGURE 1: Variation of U_t with Y for several values of \bar{N} with $R_e = -5$, $\bar{\lambda} = 0.1$, and $T = 0.05$.

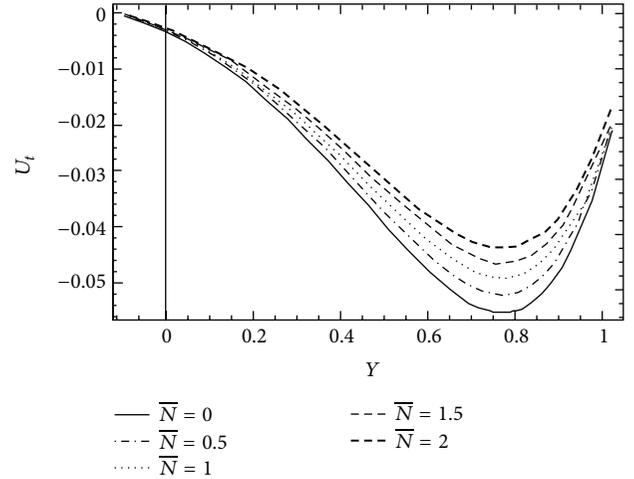


FIGURE 2: Variation of U_t with Y for several values of \bar{N} with $R_e = 5$, $\bar{\lambda} = 0.1$, and $T = 0.05$.

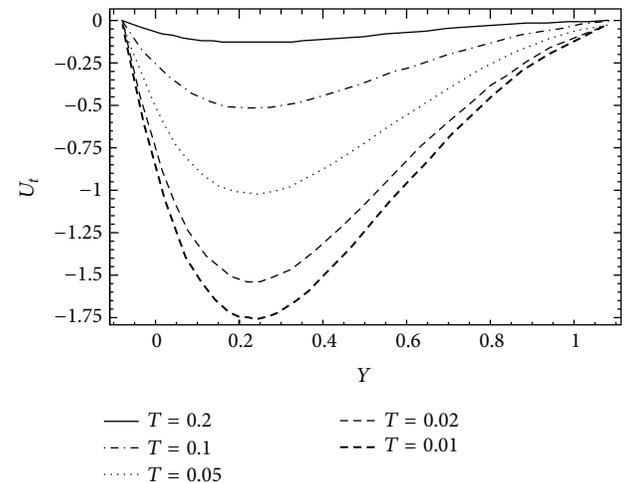


FIGURE 3: Variation of U_t with Y for several values of T with $R_e = -5$, $\bar{\lambda} = 0.1$, and $\bar{N} = 0.5$.

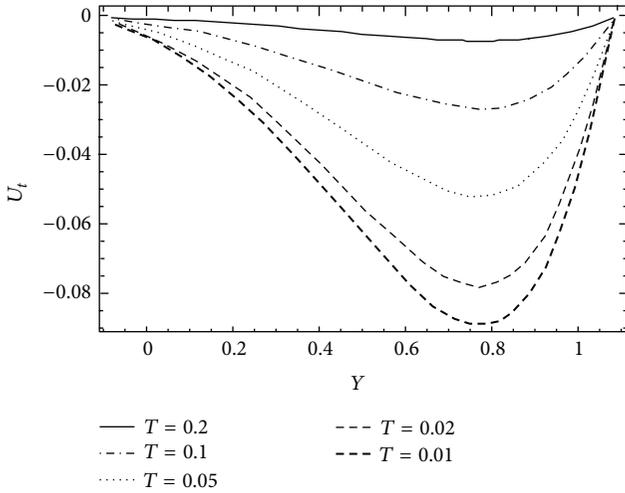


FIGURE 4: Variation of U_t with Y for several values of T with $R_e = 5$, $\bar{\lambda} = 0.1$, and $\bar{N} = 0.5$.

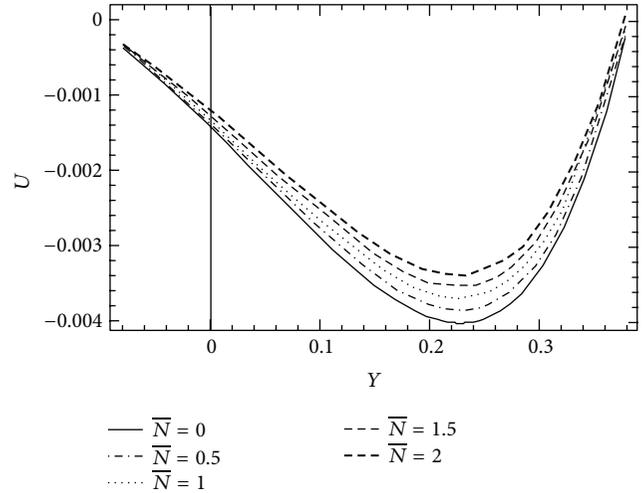


FIGURE 6: Variation of U with Y for several values of \bar{N} with $R_e = 5$, $\bar{\lambda} = 0.1$, and $T = 0.05$.

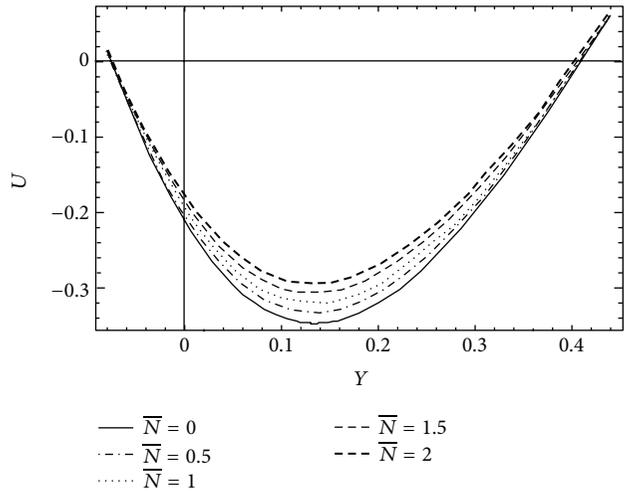


FIGURE 5: Variation of U with Y for several values of \bar{N} with $R_e = -5$, $\bar{\lambda} = 0.1$, and $T = 0.05$.

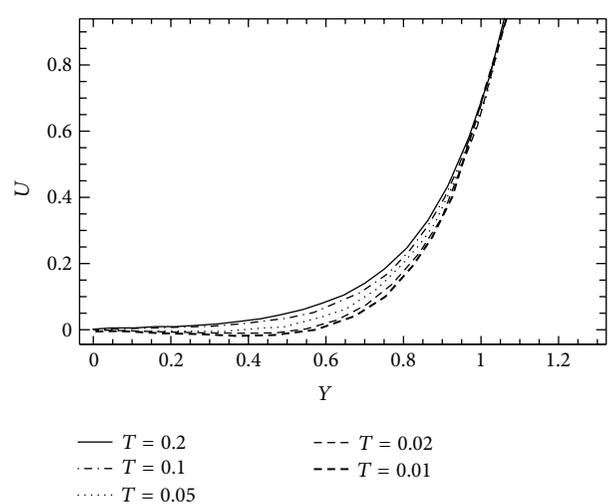


FIGURE 7: Variation of U with Y for several values of T with $R_e = 5$, $\bar{\lambda} = 0.1$, and $\bar{N} = 0.5$.

top wall, with increase in magnetic field, transient part velocity decreases in magnitude. Figure 2 shows that when there is mass injection $R_e > 0$ at the bottom wall, with increase in magnetic field, transient part velocity U_t decreases and will become weaker as compared to the case of suction. From Figure 3 it is observed that for suction at top wall and for fixed values of $\bar{\lambda}$, \bar{N} transient part velocity U_t decreases in magnitude with increase in time. Figure 4 shows that for injection at bottom wall and for fixed values of $\bar{\lambda}$, \bar{N} transient part velocity U_t decreases in magnitude with increase in time. From Figures 3 and 4 it is seen that the transient part velocity will decay with time, which is consistent with what we expected. From Figures 3 and 4 it is clear that, after a certain time, the transient part velocity will die away and velocity will become developed. Figures 5 and 6 indicate variation of overall transient velocity U with Y for fixed values of $\bar{\lambda}$ and T . Figure 5 shows that, for $R_e = -5 < 0$,

with increase in magnetic parameter \bar{N} , overall transient velocity U decreases. Figure 6 shows that, for $R_e = 5 > 0$, with increase in magnetic parameter \bar{N} , overall transient velocity U decreases but weaker. The overall transient velocities for $R_e = 5$ at different times are depicted in Figure 7. Figure 7 shows that for mass injection at the bottom wall, overall transient velocity U increases with time.

Figures 8 and 9 illustrate the variation of steady state velocity U_s with Y for several values of slip parameter $\bar{\lambda}$ and for fixed value of \bar{N} . Figure 8 shows that, for suction at the top wall with increase in slip parameter $\bar{\lambda}$, steady state velocity U_s increases. Figure 9 shows that, for injection at the bottom wall with increase in slip parameter $\bar{\lambda}$, steady state velocity U_s decreases.

Now we discuss the variation of the steady state temperature distribution σ with distance from the surface Y for

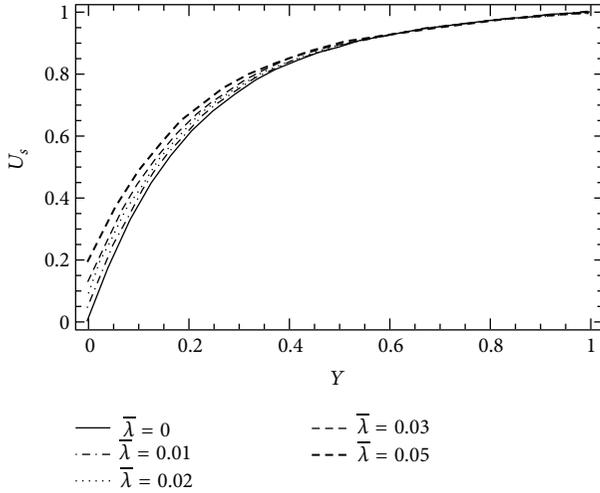


FIGURE 8: Variation of U_s with Y for several values of $\bar{\lambda}$ with $R_e = -5$, $\bar{N} = 0.5$.

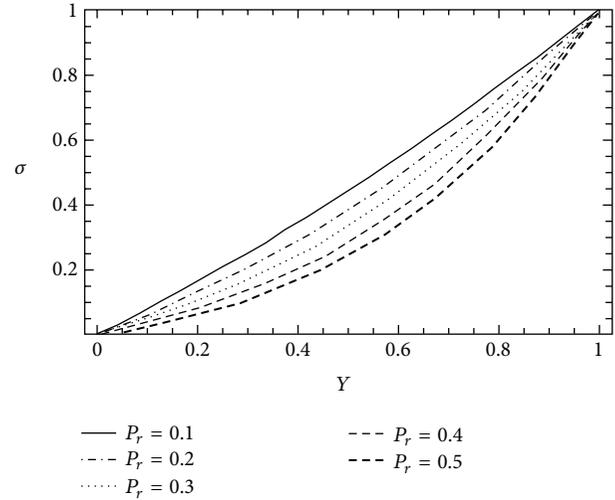


FIGURE 10: Variation of σ with Y for several values of P_r with $R_e = 5$, $E_c = 2$, $\bar{N} = 0.5$, and $\bar{\lambda} = 0.1$.

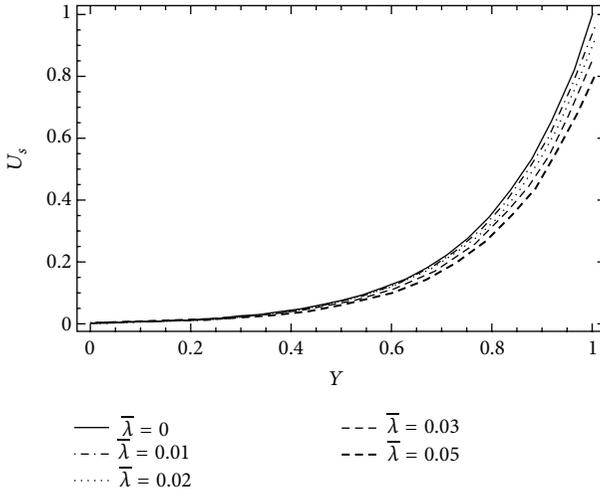


FIGURE 9: Variation of U_s with Y for several values of $\bar{\lambda}$ with $R_e = 5$, $\bar{N} = 0.5$.

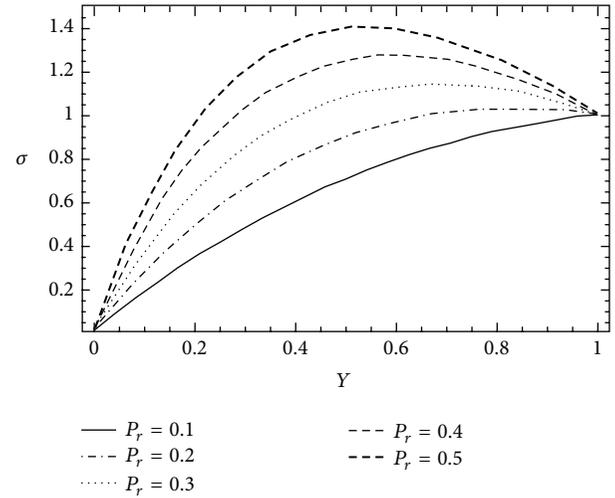


FIGURE 11: Variation of σ with Y for several values of P_r with $R_e = -5$, $E_c = 2$, $\bar{N} = 0.5$, and $\bar{\lambda} = 0.1$.

different values of five dimensionless parameters: Reynolds number R_e , Prandtl number P_r , Eckert number E_c , slip parameter $\bar{\lambda}$, and magnetic parameter \bar{N} . Variation of the Nusselt number at walls for different Prandtl numbers is also discussed. Figures 10 and 11 elucidate the variation of steady state temperature distribution σ with Y for several values of P_r and for fixed values of E_c , $\bar{\lambda}$, and \bar{N} . Figure 10 shows that for $R_e = 5 > 0$, (injection) temperature σ at a point decreases with increase in P_r . Figure 11 shows that, for $R_e = -5 < 0$, (suction) temperature σ with increase in P_r increases at a point. Comparison of Figures 10 and 11 shows that, for mass suction at the bottom wall, the maximum temperature will exist in the fluid because of viscous dissipation.

Figures 12 and 13 illustrate the variation of Nusselt numbers at the bottom wall with R_e , for fixed values of E_c , $\bar{\lambda}$, and \bar{N} and for several values of P_r . Figure 12 shows that

when there is mass suction at the bottom wall, heat transfer rate N_{u_1} increases with increase in P_r . Figure 13 shows that when there is mass injection at the bottom wall, heat transfer rate N_{u_1} decreases with increase in P_r . Figures 14 and 15 depict the variation of Nusselt numbers at the top wall with R_e , for fixed values of E_c , $\bar{\lambda}$, and \bar{N} and for several values of P_r . Figure 14 shows that when there is mass suction at the top wall, heat transfer rate N_{u_2} increases in magnitude with increase in P_r . Figure 15 shows that when there is mass injection at the top wall, heat transfer rate N_{u_2} increases with increase in P_r .

4. Final Remarks

In this study exact solutions for the velocity field and temperature field in the presence of magnetic field, porosity,

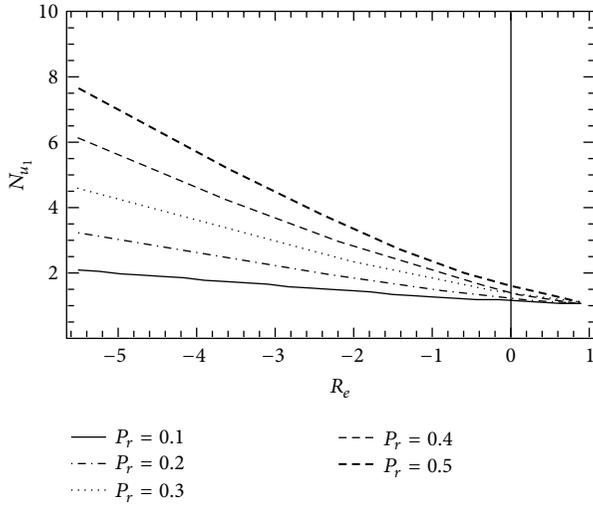


FIGURE 12: Variation of N_{u_1} with $R_e : -5.5 \rightarrow 0.9$ for several values of P_r with $E_c = 2$, $\bar{N} = 0.5$, and $\bar{\lambda} = 0.1$.

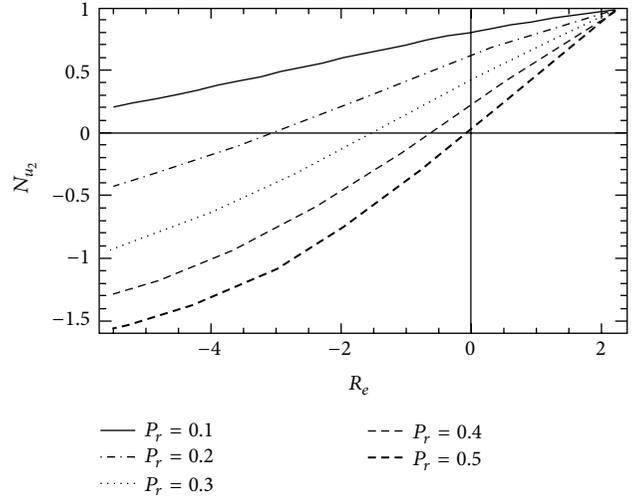


FIGURE 14: Variation of N_{u_2} with $R_e : -5.5 \rightarrow 2.2$ for several values of P_r with $E_c = 2$, $\bar{N} = 0.5$, and $\bar{\lambda} = 0.1$.

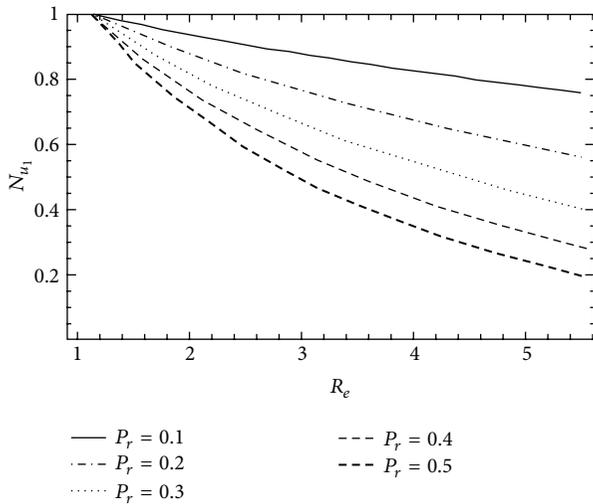


FIGURE 13: Variation of N_{u_1} with $R_e : 1 \rightarrow 5.5$ for several values of P_r with $E_c = 2$, $\bar{N} = 0.5$, and $\bar{\lambda} = 0.1$.

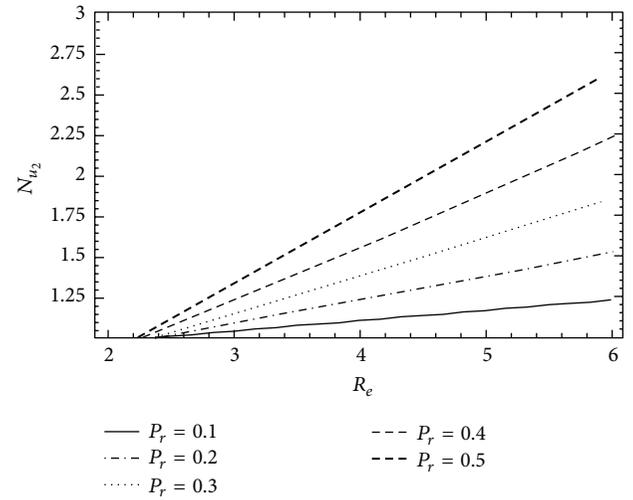


FIGURE 15: Variation of N_{u_2} with $R_e : 2 \rightarrow 6$ for several values of P_r with $E_c = 2$, $\bar{N} = 0.5$, and $\bar{\lambda} = 0.1$.

and slip parameter are constructed. A uniform magnetic field is applied transversely to the flow. The expressions of the velocity field and temperature field for flow subjected to the slip conditions between the two parallel plates and fluid are obtained by means of Laplace transform. The so-obtained solutions, depending on the initial and the boundary conditions, are presented as sum of the steady state transient solutions. The results of Fang [1] are also recovered by taking $\bar{\lambda} = 0$, $\bar{N} = 0$. Graphical results for mass transfer reveal that it has significant influence on the velocity distribution, temperature distribution, and heat transfer rate at the walls. The current analysis will be useful in dealing with real engineering problems.

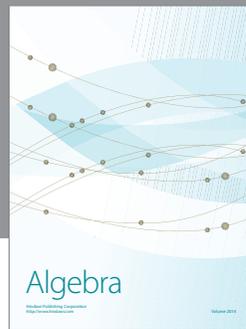
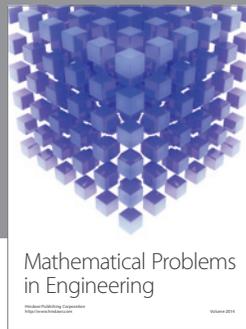
Conflict of Interests

The authors declare that there is no conflict of interests regarding the publication of this paper. The authors do not have a direct financial relation with the commercial identity mentioned in the paper that might lead to a conflict of interests for any of them.

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