

## Research Article

# High-Temperature (1700–1800°C) Electrochemical Preparation of Metallic Ti from Rutile: A Pathway of Step-by-Step Electrodeoxidization

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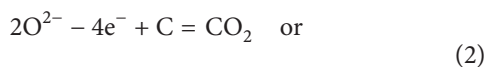
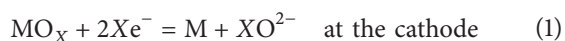
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The mechanism of producing metallic titanium by electrochemically reducing rutile ( $\text{TiO}_2$ ) at high temperatures was studied. First, the oxygen was successfully electroremoved from  $\text{TiO}_2$  at temperatures 1700, 1750, and 1800°C in molten  $\text{CaF}_2$  under a stable electrolytic potential of 2.5 V. Second, the electrodeoxidization process was studied with cyclic voltammetry (CV) tests at 1750°C. It was found that the electrochemical reduction for preparing metallic Ti from  $\text{TiO}_2$  at the high temperatures can be divided into several steps. In other words, the oxygen in  $\text{TiO}_2$  was electro-removed as a step-by-step pathway ( $\text{TiO}_2 \rightarrow \text{Ti}_4\text{O}_7 \rightarrow \text{Ti}_3\text{O}_5/\text{Ti}_2\text{O}_3 \rightarrow \text{TiO} \rightarrow \text{Ti}$ ) at different electrolytic potentials. It unraveled the mechanism of electrochemical reduction of  $\text{TiO}_2$  at the high temperatures, which is helpful for monitoring the reduction procedure.

## 1. Introduction

Titanium and its alloys play an essential role in industry because of their excellent properties of high ratio of strength/weight, fine plasticity, and superior corrosion-resistance [1]. Although Ti has an attractive future in industry, it cannot be widely used due to the high cost and complex production procedure. Until now, the mainly used commercial procedure for Ti production is Kroll process [2], but the Kroll process needs large energy and long time. In the recent decade, FFC Cambridge process was proposed and considered to be an effective alternative method of direct electrochemical reduction of rutile ( $\text{TiO}_2$ ) to Ti [3, 4]. In this process, the cathode of  $\text{TiO}_2$  pellets was immersed into molten  $\text{CaCl}_2$  and reduced to Ti electrochemically at 900°C under the electrolytic potentials of 2.8–3.2 V. The electrolytic reactions given by this process can be summarized as the following equations:



This process has two main advances compared with the traditional Kroll method: first, FFC process is a one-pot technique, thereby less time and less energy are spent; second, it can be applied to produce other metals or alloys by this electrochemical reduction method. For example, until now, many metals and alloys, such as, Cr, Si, Nb, Ni, Zr and Ni-Mn-Ga, Ti-W, and Nb-Si, were produced from their oxides by the electrochemical reduction method [5–14]. However, the most critical challenge to sabotage broad industrial applications of FFC process is low current efficiency and slow reaction rate. For example, the current efficiency was between 30% and 50% in most cases; in only a few experiments it can reach 80% [15]. Moreover, only the  $\text{TiO}_2$  contacted with the wrapped electrode wires could be completely deoxidized to metallic Ti after electrochemical reduction for several tens of hours [3]. Perovskite phase ( $1.49 < \text{O}/\text{Ti} < 1.89$ ) still exists in the areas which are not directly contacted with the electrode wires [16]. The incomplete and time-consuming electrolysis is attributed to relatively lower electrochemical reduction activity at lower experimental temperatures (850–950°C). Moreover, the produced metallic Ti could be covered on the surface of the  $\text{TiO}_2$ , which would seal the free pathways for oxygen releasing, leading to the termination of the electroreduction process [17, 18].

Recently, elevating electrochemical reduction temperature is considered to be an effective method to increase the efficiency of electrochemical reduction of  $\text{TiO}_2$  to produce metallic Ti [19]. Not only was the reaction rate increased by elevating reaction temperature, but also the current efficiency was remarkably rocketed up to 90% [19]. In addition, the electrochemical reduction method at high temperatures ( $>1500^\circ\text{C}$ ) was even used for alloys production, especially for some superalloys [14, 20]. Therefore, the electrochemical reduction method at the high temperatures might be widely used in the future for the production of Ti and other metals or alloys in industry. However, taking the Ti production by high-temperature electrolysis as an example, the mechanism is still unclear. It should be pointed out that the mechanism of electrochemical reduction at high temperature is critical for producing metals or for extracting alloys directly from their oxides.

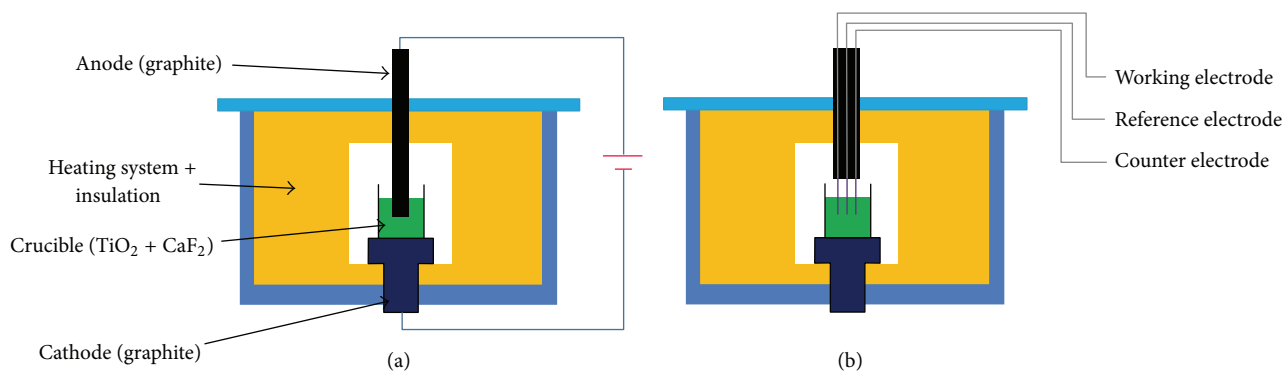
In this paper, it is the first time to study the mechanism of the electrochemical reduction of  $\text{TiO}_2$  to Ti at high temperatures ( $1700\text{--}1800^\circ\text{C}$ ). By the cyclic voltammetry (CV) measurement and thermodynamic analysis, we have proven that the electrochemical reduction of  $\text{TiO}_2$  has a step-by-step pathway. At an applied experimental temperature, the electrochemical reduction process was dependant on the applied reduction potential.

## 2. Experimental

**2.1. Materials Preparation.** In our experiments,  $\text{CaF}_2$  is used as electrolyte instead of  $\text{CaCl}_2$  because the electrolytic temperatures are high [19]. As it is known, the electrolyte can be decomposed if the potential applied is high enough. According to the thermodynamic data in [29], we can calculate that the electrochemical decomposition potential of the  $\text{CaCl}_2$  is lower than 2.2 V if the electrolysis temperature goes up to  $1700^\circ\text{C}$ . The electrochemical decomposition potential of  $\text{CaF}_2$ , however, is still higher than 4.5 V even in our experimental temperatures ( $1700\text{--}1800^\circ\text{C}$ ). In electrolysis, because of unavoidable IR drop, we should select an electrolyte ( $\text{CaF}_2$ ) with a high electrochemical decomposition potential to ensure the fine stability of electrolyte. In this work,  $\text{CaF}_2$  ( $\geq 99.0\%$ , Chengde Optical & Electrical Materials Ltd., Hebei, China) was prepared as in the following steps: first,  $\text{CaF}_2$  powders were die-pressed into small cylindrical pellets under the pressure of 30 MPa; second, the pellets were dried at  $70^\circ\text{C}$  in an oven overnight; third, the pellets were pulverized to small grains with an average size less than 5 mm.  $\text{TiO}_2$  pellets were prepared from rutile  $\text{TiO}_2$  powders ( $\geq 99.6\%$ , Chengde Optical & Electrical Materials Ltd., Hebei, China) with an identical method as that used in preparation of the  $\text{CaF}_2$  pellets. Then the  $\text{TiO}_2$  pellets were pulverized to smaller grains of size less than 1 mm. Graphite crucibles (inner diameter: 9.0 cm, height: 18.0 cm, and wall thickness: 1.0 cm) were flushed with industrial ethanol ( $>95\%$ , Beijing Keshi Co. Ltd., Beijing, China) for 3–5 times until the inner surfaces were almost free of graphite powders. At last, the  $\text{TiO}_2$  grains were placed in the graphite crucible and then covered with  $\text{CaF}_2$  grains. Each crucible had about 200 g of  $\text{TiO}_2$  and 2000 g of  $\text{CaF}_2$ .

**2.2. Potentiostatic Electrolysis.** The  $\text{CaF}_2$  was used as electrolyte in both  $\text{TiO}_2$  electrolysis and subsequent cyclic voltammetry (CV) measurements. As a cathode, a graphite crucible with  $\text{TiO}_2$  and  $\text{CaF}_2$  was placed in a temperature-controlled furnace made by China Iron & Steel Research Institute Group, as shown in Scheme 1(a). A graphite anode rod (diameter: 6.0 cm) was hung by an electromotor, which can move up and down vertically to ensure that the graphite rod can contact with the molten electrolyte during the electrolysis. KGHF-1000 A/6 V rectifier, made by Beijing Chunshu Electric rectifier Ltd., Beijing, China, was equipped with the furnace to supply a direct current for the electrolysis. The furnace was vacuumed, and then argon ( $\geq 99.9\%$ ,  $\text{O} \leq 10$  ppm,  $\text{H}_2\text{O} \leq 15$  ppm, and  $\text{N}_2 \leq 5$  ppm) was pumped into the furnace as soon as possible. Purged with the argon for 20 min, all valves of the furnace were turned off. Then the argon flow was kept at a rate of  $1.0\text{--}1.5\text{ L min}^{-1}$ , and the inlet and outlet valves were adjusted to maintain a gas pressure in the furnace around 0.01 MPa larger than the ambient pressure to further prevent air ingress. Heated the furnace to  $500^\circ\text{C}$  with a ramping rate of  $20^\circ\text{C min}^{-1}$  and then raised the temperature to  $1450^\circ\text{C}$  at an average rate of  $10^\circ\text{C min}^{-1}$ . Kept at  $1450^\circ\text{C}$  for 30 min to ensure the electrolyte  $\text{CaF}_2$  was completely melted in the crucible. Then the temperature continued to rise up to the experimental temperatures of  $1700\text{--}1800^\circ\text{C}$  with a heating rate of  $10^\circ\text{C min}^{-1}$ . Consequently, the potential was set to 2.5 V for electrolysis. It should be pointed out that preelectrolysis in this experiment was not applied as it was in other experiments [3–5, 21, 22]. Residual water and redox in the molten  $\text{CaF}_2$  were much less than those in the molten  $\text{CaCl}_2$ , which would be proven by the stable electrolytic current with only mild vibration during electrolysis in the first few minutes. After electrolysis and consequent cooling to room temperature, the graphite crucible was taken out of the furnace. The samples after electrochemical reduction at different high temperatures were obtained by smashing the graphite crucibles.

**2.3. CV Measurement.** In this work, three-electrode system was used in the CV tests and its design was shown in Scheme 1(b). A Mo wire (diameter: 1.0 mm) and a graphite tablet ( $4\text{ mm} \times 10\text{ mm} \times 50\text{ mm}$ ) worked as a quasireference and a counter electrode respectively. The working electrode was  $\text{TiO}_2$  slices ( $2\text{ mm} \times 10\text{ mm} \times 40\text{ mm}$ ), which were wrapped with a Mo wire (diameter: 0.5 mm). The three electrodes were linked to a CHI 604C Electrochemical System (Shanghai Chenhua Inc., Shanghai, China) with the Mo wires (diameter: 0.5 mm). For fixing the Mo wires, three holes were punched along the axial direction of a graphite rod (diameter: 6.0 cm), which had the same size as the rod used in electrolysis process. Thus, the three electrodes can be hung at the bottom of the graphite rod and move up and down together with the rod. The heating process was the same as that used in the former electrolysis. After reaching the experimental temperature, three electrodes were inserted into molten  $\text{CaF}_2$  simultaneously by pushing down the graphite rod for CV measurements.



SCHEME 1: (a) Schematic of electrolytic cell for  $\text{TiO}_2$  electrolysis; (b) design of three-electrode system for cyclic voltammetry (CV) tests.

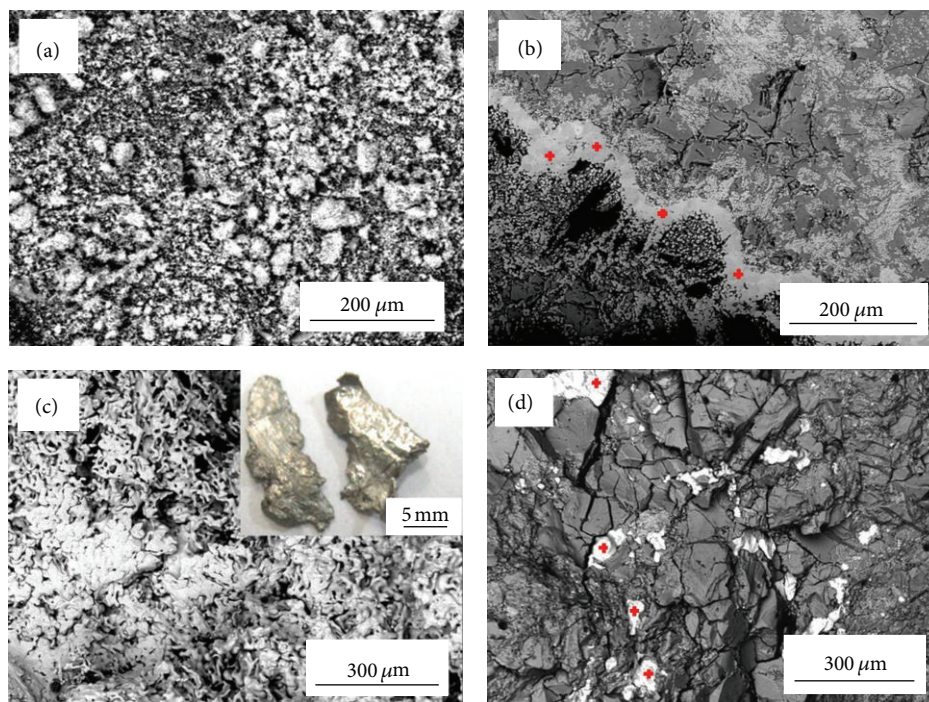


FIGURE 1: (a) SEM image of  $\text{TiO}_2$  powders before electrolysis; SEM images of the samples after electrolysis at (b) 1700°C, (c) 1750°C, and (d) 1800°C, respectively. The inset in (c) shows two selected pieces of metallic Ti slices after electrolysis at 1750°C. Red crosses in (b) and (d) mark the areas for EDX measurement.

**2.4. Characterizations of Morphology and Composition.** Micrograph and composition analyses were performed with a VEGA\LMU SEM system equipped with a CCD camera, from TESCAN. EDX equipment was purchased from OXFORD, and the analysis software was INCA.

### 3. Results and Discussion

Figure 1(a) shows the morphology of pure  $\text{TiO}_2$ , which were sintered and pulverized into small particles before electrolysis. Most of the particles had a size smaller than 100  $\mu\text{m}$ . Absolutely, the sample before electrolysis was pure  $\text{TiO}_2$  by EDX measurement in Table 1. As shown in Figure 1(b), after

electrochemical reduction at 1700°C, a bright S-shaped stripe was formed at the bottom of graphite crucible. Left downside areas of the S-shaped stripe, which was close to the bottom of graphite crucible, had large dark areas of graphite. Many scattered small bright areas were located at the right upside of the S-shaped stripe. With EDX measurement of these bright areas in Table 1, the Ti content increased to 75.3 at % but the O content decreased to 9.4 at %, compared with the pure  $\text{TiO}_2$ . However, the S-shaped stripe still had some Ca and F. Clearly, they were from electrolyte  $\text{CaF}_2$ . Figure 1(c) shows the sample after electrochemical reduction at 1750°C. Dozens of metallic Ti were obtained by smashing the crucible after electrolysis, among which two selected pieces were shown in the inset of Figure 1(c). Each piece was about 1.5 g in weight. The EDX



TABLE 1: EDX results of samples before and after electrolysis at different temperatures.

Samples	Ti [at. %]	O [at. %]	Ca [at. %]	F [at. %]
Pure TiO <sub>2</sub> <sup>a</sup>	33.2	66.8	—	—
1700°C <sup>b</sup>	75.3	9.4	5.4	9.9
1750°C <sup>c</sup>	100.0	—	—	—
1800°C <sup>b</sup>	91.3	—	3.6	5.1

—Not obtained by EDX.

<sup>a</sup>The sample of pure TiO<sub>2</sub> was measured by EDX before electrolysis.

<sup>b</sup>EDX measurement was taken from the areas in Figures 1(b) and 1(d), respectively. Content of each element was the average value in the four randomly selected areas marked in Figures 1(b) and 1(d), respectively.

<sup>c</sup>EDX result was obtained by surface scanning over the area in Figure 1(c).

results in Table 1 show that the samples obtained after electrolysis at 1750°C were pure metallic Ti. Given that the electrolytic temperatures used in our experiments were just below the melting point of TiO<sub>2</sub> (1843°C) [23], the oxygen ions were easily moved out from TiO<sub>2</sub> crystal lattice. This sample had a porous structure as shown in the SEM image in Figure 1(c). Simultaneously, the porosity structure can supply more free pathways to enhance oxygen ions transport. It should be pointed out that even at lower electrolytic temperatures, the porous structure was also demonstrated [18, 19]. After electrolysis at 1800°C, shown in Figure 1(d), many bright white areas were scattered in grey areas. By checking with the EDX, the large grey areas were electrolyte CaF<sub>2</sub>, while the white spots were rich in Ti (91.3 at %) as well as a small amount of Ca and F from electrolyte CaF<sub>2</sub>. It demonstrates that the O in TiO<sub>2</sub> was completely removed. However, there are two distinct differences between the sample electrolyzed at 1800°C and that electrolyzed at 1750°C. First, the bright spots, which were rich in Ti, did not aggregate to large pieces of metallic Ti; second, some Ca and F were still contained. This was probably the consequence of intense fluctuation of molten CaF<sub>2</sub> during electrolysis, which resulted from large electrolytic current and high fluidity of electrolyte at high temperatures [24, 25].

Figure 2 shows the chronoamperometric plots of the electrolysis at three different temperatures. Each chronoamperometric plot had a current peak in the first 20–40 min and then decreased to a steady current plateau, which continued for 3–4 hr. The current plateau was almost flat, which indicated that the electrolytic process was stable. Then the electrolytic current dropped to the background current sharply in 5 min. The current behavior can be explained by a three-phase-interline (3PI) mechanism proposed by Deng et al. [26]. Briefly, the electrochemical reduction of insulating solid oxides can proceed at the place of 3PI, linking the conductor, oxide and electrolyte. As reaction persisting, the metal/oxide/electrolyte 3PI propagates, leading to metallization on the 3PI interface initially and then into the interior of oxide preforms until the reduction is completed [5, 6, 27]. Therefore, upon commencing the reduction, total length of the 3PI increased as the current raised. Once the current reached the maximum, the 3PI started to decrease to a steady status, leading to the formation of the current plateaus. Meanwhile, the reaction proceeded into the interior of the oxide until the oxide was completely electroreduced.

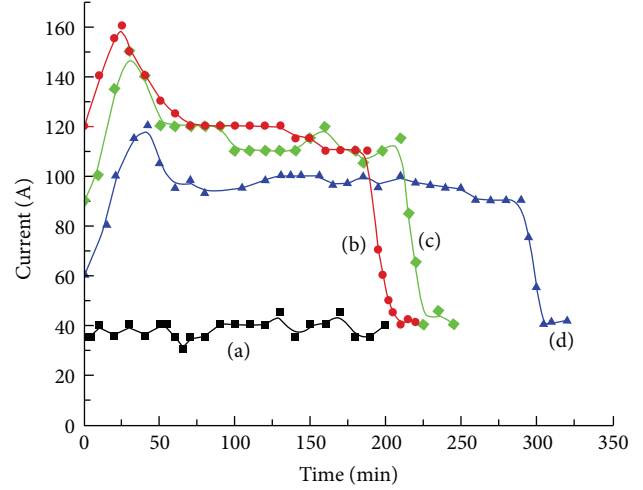
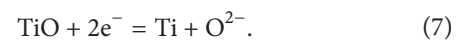
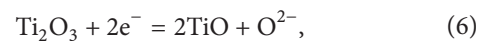
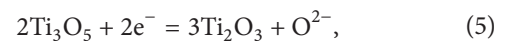
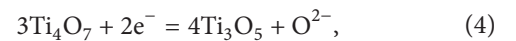
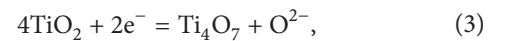


FIGURE 2: Chronoamperometric plots under constant electrolytic potential of 2.5 V at (b) 1800°C, (c) 1750°C, and (d) 1700°C. Plot (a) is a blank  $I-t$  curve, obtained under 2.5 V at 1750°C (only electrolyte CaF<sub>2</sub> in the electrolytic graphite crucible).

Thus, the higher the temperature during the electrolysis, the higher the rate of the 3PI propagation, and the earlier the current peak appeared. In addition, the initial electrolytic current peak and current plateau became higher and the total electrolytic time was shortened as the temperature increased.

The design of the three electrodes, shown in Scheme 1(b) and the inset of Figure 3(a), was used for CV tests to demonstrate the electrochemical reduction process of TiO<sub>2</sub>. Figure 3 shows the CV curves at 1750°C with and without TiO<sub>2</sub> slices as working electrode in molten CaF<sub>2</sub>, respectively. Herein, the equilibrium potential of Ca<sup>2+</sup>/Ca (Ca<sup>2+</sup> + 2e<sup>-</sup> ↔ Ca; Ca<sup>2+</sup> and Ca are in standard status) is defined as the reference potential ( $E_{Ca^{2+}/Ca}^{\theta} = 0$ ) as described in the other literature [3, 22, 28]. In Figure 3(a), with the potential becoming positive, oxidation currents increased rapidly to form a peak c1, which was the consequence of Ti dissolution [3]. If the working electrode was changed to a piece of Mo foil without TiO<sub>2</sub> slices, only two current plateaus of c2 and c3 would appear in both positive and negative potential directions, as shown in Figure 3(b). The difference between these two CV curves was a family of current peaks (a1–a5) shown in Figure 3(a). Apparently, these peaks were attributed to many electrochemical reactions. Moreover, we found that many types of titanium oxides existed in the Ti-O binary phase diagram due to different O ratios [23]. According to the O ratios in TiO<sub>2</sub>, the reduction process can be divided into many steps, which were shown in (3)–(7):



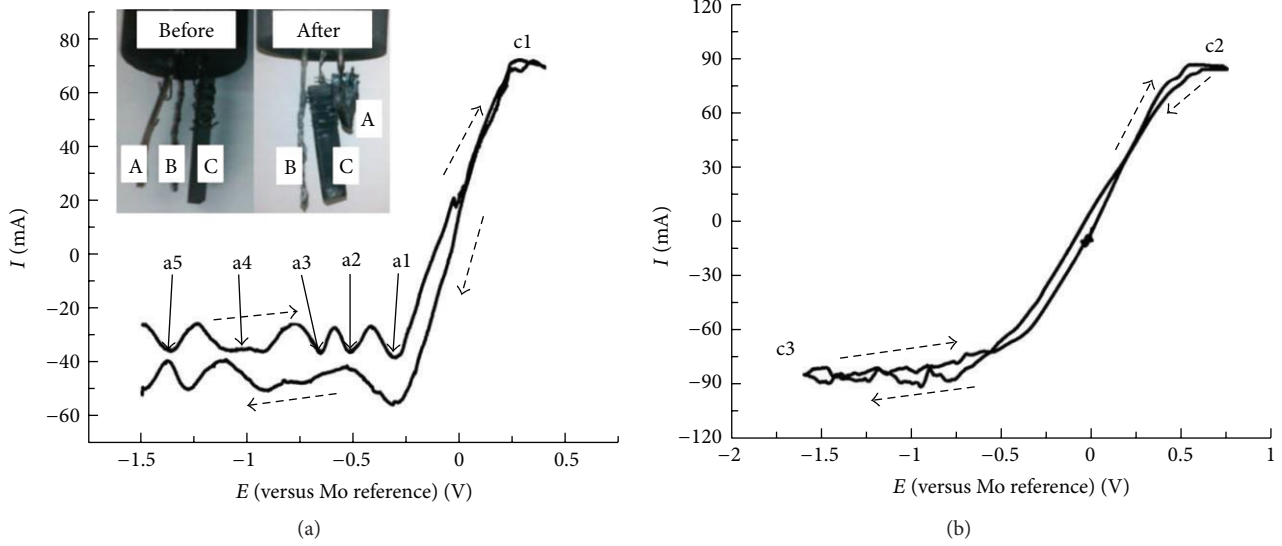


FIGURE 3: CV curves obtained at 1750°C. (a) A  $\text{TiO}_2$  slice (from oxidizing Ti foil at 1300°C for 1.5 hr) wrapped with Mo wire as working electrode (the inset of (a) shows the design of three electrodes (working electrode (A), reference electrode (B), and counter electrode (C)) before and after CV test at 1750°C); (b) only Mo foil as working electrode. The scan rate was  $20 \text{ mV s}^{-1}$ .

According to the thermodynamic data [29], we can obtain the plots of the electrolytic potential against temperature ( $E$ - $T$ ), as shown in Figure 4. The theoretical reduction potentials of  $\text{TiO}_2$ ,  $\text{Ti}_4\text{O}_7$ ,  $\text{Ti}_3\text{O}_5$ ,  $\text{Ti}_2\text{O}_3$ , and  $\text{TiO}$  at 1750°C were located at  $-1.30 \text{ V}$ ,  $-1.08 \text{ V}$ ,  $-0.96 \text{ V}$ ,  $-0.69 \text{ V}$ , and  $-0.23 \text{ V}$ , respectively. As what we have discussed above, the current peaks of the CV curve in Figure 3(a) have indicated a series of reactions during the electrochemical reduction process of  $\text{TiO}_2$ . Obviously, the peaks a5 ( $-1.28 \text{ V}$ ), a3 ( $-0.65 \text{ V}$ ), and a1 ( $-0.27 \text{ V}$ ) in Figure 3(a) were consistent with the theoretical potentials of electrochemical reduction of  $\text{TiO}_2$ ,  $\text{Ti}_2\text{O}_3$ , and  $\text{TiO}$ , respectively. Therefore, it can be concluded that these three peaks resulted from reactions (3), (6), and (7). Besides, a broad peak (a4) ranged from  $-0.9 \text{ V}$  to  $-1.13 \text{ V}$ , indicating many reactions in this potential range. From the Ti-O binary phase diagram [23], there are a series of phases named Magnéli phases ( $\text{Ti}_n\text{O}_{2n-1}$  ( $n \geq 4$ )) with an O ratio between  $\text{Ti}_2\text{O}_3$  and  $\text{TiO}_2$ . Definitely, the  $\text{Ti}_4\text{O}_7$  is one of the Magnéli phases. As shown in Figure 4, the titanium oxide with a higher oxygen ratio will have a higher electrochemical reduction potential and vice versa. Therefore, the electrochemical reduction potentials of the Magnéli phases are among  $\text{Ti}_2\text{O}_3$  and  $\text{TiO}_2$ . Besides, the reduction potential of the  $\text{Ti}_3\text{O}_5$  should also be located between  $\text{Ti}_2\text{O}_3$  and  $\text{TiO}_2$ . Thereby, the broad peak a4 was composed of reduction peaks of a series of Magnéli phases ( $\text{Ti}_4\text{O}_7$  is the typical oxidation) and  $\text{Ti}_3\text{O}_5$ . Besides, one point should be highlighted here: the electrochemical reduction potentials of reactions (4) and (5) are very close to each other, as shown in Figure 4. This also indicates why the current peaks can be largely overlapped and merged to one broad peak (a4 in Figure 3(a)). People might question why there is another current peak a2 appeared at  $-0.51 \text{ V}$  since no more Ti-O phases exist between  $\text{TiO}$  and  $\text{Ti}_2\text{O}_3$  in the Ti-O binary phase diagram [23]. In fact,  $\text{TiO}$  can easily form  $\text{CaTiO}_3$  or other higher perovskite phases

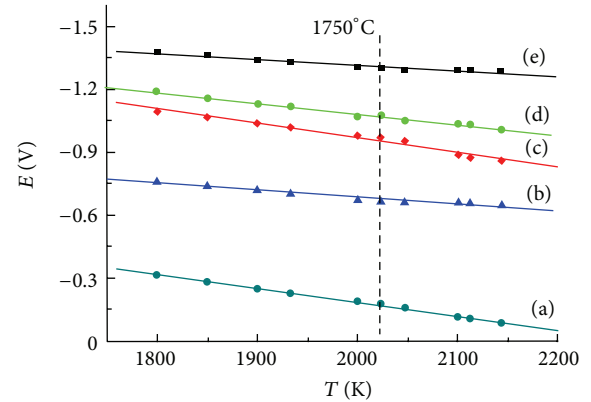
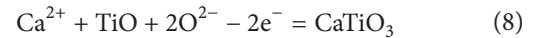


FIGURE 4: Plots of electrochemical reduction potentials of Ti oxides against temperatures: (a)  $\text{TiO} + 2\text{e}^- = \text{Ti} + \text{O}^{2-}$ ; (b)  $\text{Ti}_2\text{O}_3 + 2\text{e}^- = 2\text{TiO} + \text{O}^{2-}$ ; (c)  $2\text{Ti}_3\text{O}_5 + 2\text{e}^- = 3\text{Ti}_2\text{O}_3 + \text{O}^{2-}$ ; (d)  $3\text{Ti}_4\text{O}_7 + 2\text{e}^- = 4\text{Ti}_3\text{O}_5 + \text{O}^{2-}$ ; (e)  $4\text{TiO}_2 + 2\text{e}^- = \text{Ti}_4\text{O}_7 + \text{O}^{2-}$ . The vertical dashed line indicates the electrochemical reduction potentials of different Ti oxides at 1750°C.

( $\text{Ca}_\delta\text{TiO}_\chi$  ( $\chi/\delta \geq 2$ )) with  $\text{Ca}^{2+}$  and  $\text{O}^{2-}$  in molten electrolyte as reaction (8) [16, 22]:



Based on the thermodynamic data [29], we can infer that reduction potentials of this series of perovskite phases range from  $-0.36 \text{ V}$  to  $-0.58 \text{ V}$ . Therefore, some  $\text{TiO}$  will react with  $\text{Ca}^{2+}$  and  $\text{O}^{2-}$  at high temperatures to form  $\text{CaTiO}_3$  or other higher perovskite phases, which will lead to the peak a2. The remaining  $\text{TiO}$  will continue the electrochemical reduction process to be reduced to metallic Ti, leading to the current peak a1 as discussed above.

## 4. Conclusions

Generally,  $\text{TiO}_2$  was successfully electrochemically reduced to metallic Ti at high temperatures (1700–1800°C). The best result was shown by electrolysis at 1750°C; pure metallic Ti pieces were obtained. In addition, we have measured the procedure of the electrolytic reaction at 1750°C. It was found that the electrochemical reduction was separated into several steps. The oxygen in the  $\text{TiO}_2$  was electroremoved as a step-by-step pathway ( $\text{TiO}_2 \rightarrow \text{Ti}_4\text{O}_7 \rightarrow \text{Ti}_3\text{O}_5/\text{Ti}_2\text{O}_3 \rightarrow \text{TiO} \rightarrow \text{Ti}$ ) at different applied reduction potentials. This mechanism of electrochemical reduction can be helpful in controlling the production procedure of Ti in industry. Also, it can be used for producing Ti alloys by electrochemical reduction method at high temperatures.

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