Adsorptive Removal of Iron Using SiO$_2$ Nanoparticles Extracted from Rice Husk Ash

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In this work, SiO$_2$ nanoparticles were prepared by the sol-gel method after sodium silicate was extracted from rice husk ash (RHA) under various experimental conditions such as types of acids, NaOH concentration, dissolved time, and temperature and used for removal of Fe$^{2+}$ ions from aqueous solutions. The extracted SiO$_2$ was morphologically and chemically characterized and showed a surface area of 78 m$^2$/g and uniform pores of 2.71 nm, offering high adsorption capacity for Fe$^{2+}$ ions. The influence of pH, contact time, and amount of adsorbent was studied in order to establish the best conditions for the Fe$^{2+}$ adsorption and removal. Furthermore, the adsorption data were fitted with an exponential shape curve for all the three variable parameters that affect the adsorption process. The best results were obtained for pH 5, 20 min contact time, and 0.5 g adsorbent dose. The loading adsorption capacity was 9 mg of Fe$^{2+}$ ions/g SiO$_2$ in the concentration range 0.1–1.0 mgL$^{-1}$. In addition, the synthesized SiO$_2$ with the size of around 50 nm can be used for specific heavy metal removal and drug delivery, after modification of the SiO$_2$ surface with various functional groups.

1. Introduction

In the past few decades, absorptive materials have been developed for removal of heavy metal ions including Hg$^{2+}$, Cu$^{2+}$, Pb$^{2+}$, Zn$^{2+}$, Cd$^{2+}$, and Fe$^{2+}$ from the environmental and biological system due to their toxicity [1–5]. Among all of the heavy metals mentioned, Fe$^{2+}$ ions widely existed in underground water and they are commonly used for household activity in the South of Viet Nam. Long-term drinking water containing high level of Fe$^{2+}$ ions may cause
kidney disease, cancer, and anemia along with metabolism disorders [6–12]. Until now, a great deal of effort has been developed for Fe\(^{2+}\) ion collection using various techniques, for instance, membrane technology, chemical precipitation coagulation, ion exchange, and electrolytic reduction [13–21]. However, it was known that these methods have several drawbacks such as long time for operation, low capacity for removal, and low thermal and mechanical stability [17, 19, 21]. Among these methods, the adsorption-based technique is a promising technique for removal of Fe\(^{2+}\) ions due to its high efficiency, easy operation, cost-effectiveness, and environmentally-friendly method. Therefore, several adsorbent materials for removal of Fe\(^{2+}\) ions have been widely investigated such as rice husk, activated carbon, fly ash, zeolites, and agricultural by-products [22–27]. It is worth to mention that silica dioxide (SiO\(_2\)) is a promising adsorptive material due to peculiar properties such as porous structure and large surface area. In addition, there are several methods to prepare silica nanoparticles (SNPs) from different agents such as synthesis of nanosilica via the precipitation method with the SNP size of around 50 nm [28, 29] and synthesis of SNPs based on the sol-gel method using rice husk with SNP size of 15 to 90 nm [30–33]. In Vietnam, the average rice husk produced was around 42 billion tons per year. After burning at high temperature, it became rice husk ash (RHA), which contained a very high amount of silica (approximately 90%). Note that the presence of silica in rice husk had been known since 1938 [34].

In this work, we presented the SNPs efficiency in Fe\(^{2+}\) ion adsorption, with SNPs extracted from RHA in brick-kiln industry. We used the sol-gel method for extraction of SNPs under certain controlled conditions such as acid, base, pH, and stirring speed. The physicochemical properties of SNPs were studied for applications of removal of Fe\(^{2+}\) ions. The SNPs synthesized could find potential applications including environment for removal of heavy metals and biomedicine for drug delivery.

2. Materials and Methods

2.1. Agents. Rice husk ash (RHA) was taken from brick-kiln industry. Hydrochloric acid (HCl), nitric acid (HNO\(_3\)), sulfuric acid (H\(_2\)SO\(_4\)), sodium hydroxide (NaOH), iron(II) sulfate, heptahydrate (FeSO\(_4\)\(\cdot\)7H\(_2\)O), hydroxylamine (H\(_2\)NO), and 1,10 phenanthroline (C\(_{12}\)H\(_8\)N\(_2\)) were purchased from Sigma-Aldrich. All agents were diluted in distilled water (DI water).

2.2. Methods

2.2.1. Extraction of SiO\(_2\) Nanoparticles. SNPs were extracted from RHA based on the sol-gel method. Figure 1 illustrates the procedure for extraction of SiO\(_2\) nanoparticles. The extraction process could be briefly described: Firstly, RHA of 2 g was collected from brick-kiln industry and then washed with DI water for removal of dirt. Secondly, RHA was soaked in the sodium hydroxide solvent under stirring at the speed of 400 rpm to generate sodium silicate. The RHA-induced sodium silicate was filtered to remove the nonreactive impurities. Finally, the sodium silicate solution obtained was cooled at room temperature and added to acid under vigorous stirring in order to initiate the hydrolysis-condensation reaction at pH 7. The gel obtained was then dispersed in ethanol, washed with DI water (three times), and dried at 110°C for 2 h to remove remaining surfactants. The SNPs synthesized were stored in a desiccator for further characterizations. In this work, the effect of acids, NaOH concentration, dissolved time, and temperature was studied.

2.2.2. Fe\(^{2+}\) Ion Adsorption Study. The adsorption of Fe\(^{2+}\) metal ions from aqueous solution was studied at room temperature. The influence of pH, adsorption time, and mass of adsorbed material was investigated. Consequently, the pH was changed from 3 to 7; adsorption time was set up from 5 to 25 min with increment of 5 min; and mass of SiO\(_2\) varied between 0.1, 0.5, 1.0, 1.5, and 2.0 g.

For Fe\(^{2+}\) ion adsorption measurement, a standard curve was plotted using the concentrations of Fe\(^{2+}\) solution in the range of 0.2, 0.4, 0.6, 0.8, and 1.0 ppm. The standard Fe\(^{2+}\) solution was generated by mixing FeSO\(_4\)\(\cdot\)7H\(_2\)O with 1 ml hydroxylamine hydrochloride, 5 ml phenanthroline, and acetate buffer solution (pH = 3.5). The standard solution generated was kept for 15 min and measured by using a UV-Vis spectrum analyzer. The adsorption capacity (C\(_{\text{cap}}\)) and the adsorption efficiency (E\(_{\text{eff}}\)) were estimated using the following equation, respectively:

\[
C_{\text{cap}} = \frac{C_{\text{in}} - C_{\text{fin}}}{m} V, \\
E_{\text{eff}} = \frac{C_{\text{in}} - C_{\text{fin}}}{C_{\text{in}}} \times 100\%,
\]

where \(C_{\text{in}}\) and \(C_{\text{fin}}\) are the initial concentration and concentration of equilibrium of Fe\(^{2+}\) ions in solution, respectively, \(m\) is the mass of the adsorbent used, and \(V\) is the volume of solution.

2.2.3. Physicochemical and Morphological Characterization. Five analytical techniques were used for physicochemical characterization of SiO\(_2\) extracted and adsorption of Fe\(^{2+}\) ions: energy dispersive X-ray spectroscopy (EDS) for the elemental composition of SiO\(_2\) extracted, transmission electron microscopy (TEM) for ultrastructural analysis; Fourier transform infrared spectroscopy (FT-IR) for characterization of functional groups in the range 4000–500 cm\(^{-1}\), ultraviolet-visible spectroscopy (UV-Vis) for determination concentration of solution, surface area measurement by the BET method, and pore size distribution by BJH (Micrometrics ASAP 2010).

3. Results and Discussion

In this work, we used 2 g of RHA for synthesis of nanosilica particles. To optimize the conditions for nanosilica synthesis, the effect of dissolved temperature, concentration of sodium hydroxide, concentration of acids, and dissolved
time was investigated. The stirring speed of 400 rpm was kept during all the process. Note that each square point in Figures 2 and 3 represents the average value of the three repeated experimental results.

3.1. Effect of Acids. The efficiency of SiO$_2$ extracted using different acids for neutralization is presented in Figure 2(a). We used three different acids including sulfuric acid, nitric acid, and hydrochloric acid with the same concentration of 3 M for precipitation. The results obtained showed that the extracted efficiency was 58%, 75%, and 76%, respectively. It should be noted that no significant difference was observed using HCl and HNO$_3$ for precipitation. The results were better than those of H$_2$SO$_4$, caused by slow gelation process of silica when sodium silicate reacted with H$_2$SO$_4$. Thus, HCl was chosen for further study. Herein, concentration of NaOH, temperature, stirring speed, and dissolved time was 3.5 M, 70°C, 400 rpm, and 120 min, respectively. Then, the effect of concentration of HCl was studied in the range from 1 to 5 M. The results showed the highest efficiency of 82%, due to increase in concentration of acids. In addition, the efficiency also depended on the amount of silicate in RHA. So, the optimizing concentration of HCl used was 4 M.

3.2. Effect of NaOH. In order to optimize the condition for nanosilica synthesis, an effect of NaOH concentration was investigated. The experiments were performed with NaOH concentration series of 2.0, 2.5, 3.0, 3.5, and 4 M; the dissolved time, concentration of HCl, temperature, and stirring speed were fixed at 120 min, 4 M, 70°C, and 400 rpm, respectively. The results showed that the concentration of NaOH was directly proportional to the efficiency. And, the efficiency of silica synthesized was obtained around 81% at NaOH concentration of 3.5 M as seen in Figure 2(b). This led us believe that the efficiency can be enhanced by controlling the other factors.

3.3. Effect of Dissolved Time. Based on the above results, the concentration of NaOH chosen was 3.5 M for further investigating dissolved time. Dissolved time of RHA in NaOH solution was set as a series of 60, 90, 120, 150, and 180 min.
Figure 2: Experimental results of SiO₂ nanoparticles extraction process. Effect of (a) acids, (b) sodium hydroxide, (c) dissolved time, and (d) temperature.

Figure 3: Continued.
Figure 2(c) shows that the amount of SiO₂ extracted was gradually increased. Efficiency increased from 70, 82, and 83% for the first, second, and third hours, respectively. The results showed that the amount of SiO₂ extracted was saturated at 120 min. This was because of the restricted amount of silicate on RHA under burning conditions in brick-kiln industry.

3.4. Effect of Temperature. The influence of temperature on the extraction of SiO₂ from RHA was illustrated in Figure 2(d). This study had been performed using the temperature range from 60 °C to 100 °C with an interval increment of 10 °C. The amount of SiO₂ extracted had increased with temperature and presented a maximum around 90 °C and remained until 100 °C. The maximum of extraction mass of SiO₂ was 1.66 g SiO₂ in this experiment, corresponding to 83% of efficiency. The efficiency was not higher than that of the other work, due to impurity of RHA in brick-kiln industry under variant conditions in comparison with RHA produced at laboratory with standard conditions [35].

The FT-IR spectrum showed strong adsorption bands at 1069 and 794 cm⁻¹ that corresponded to the symmetric and asymmetric Si-O-Si vibration as seen in Figure 4(a), respectively. After extraction of SiO₂, it was clear that the spectrum differs from the RHA, showing a deeper signal between 1069 and 794 cm⁻¹ due to increase in amount of SiO₂ extracted. In addition, an adsorption peak at 3450 cm⁻¹ was associated with the O-H bonds of the silanol groups. Moreover, the main elements consisted of Si, O, and Na with weight concentrations of 23, 75, and 2%, respectively. The small remaining Na was due to unperfect washing. The surface analysis of TEM showed that SiO₂ had a spherical shape with the diameter of around 50 nm. In addition, BET and BJH analyses of SiO₂ showed the specific surface area of 78 m²/g with a pore size of 2.7 nm. This led us to believe that the extracted SiO₂ could be used for removal of heavy metal applications.

The adsorption of Fe²⁺ ions by the synthesized SiO₂ was analyzed. Figure 3(b) shows the relation of the loading capacity (mg g⁻¹) and adsorption efficiency as a function of pH. At pH < 4, Figure 3(b) presents a low adsorption capacity due to competition between H⁺ ions and Fe²⁺ ions. For pH > 4, concentration of H⁺ decreased, offering the adsorption of Fe²⁺ ions. The adsorption phenomena could be explained by the charge of SiO₂ dependent on the pH of the surrounding medium. When the pH of the surrounding medium increased, negative charges on the surface of SiO₂ increased, leading to enhanced electrostatic interaction capacity between SiO₂ and Fe²⁺ ions as follows:

\[ 2(-\text{SiO}_2^-) + \text{Fe}^{2+} \rightarrow (-\text{SiO}_2)_2\text{Fe} \]  

The adsorption of Fe²⁺ ions on SiO₂ was found between pH 4 and 5. At pH > 5, the small change in adsorption of Fe²⁺ ions resulted from the precipitation of Fe²⁺ and small volume of the pore on SiO₂ surface. Furthermore, the removal of Fe²⁺ ions was also associated with contact time as seen in Figure 3(c). Results showed that the maximum adsorption efficiency occurred within 20 min with 0.5 g loading mass of SiO₂ and the maximum adsorption capacity was around 9 mg/g (efficiency of 99%). This result was better than other works using other adsorbents as depicted in Table 1 [36–38]. Note that the higher adsorption capacity would be caused by an increase in the number of active -OH sites on the SNPs surface as presented in Figure 4(a) as well as the surface area and the pore volume of the synthesized SiO₂.

We fitted the exponential shape curves of the form of \( q = q_o + a/[1 + \exp((b-x)/c)] \) to the measurement data in Figures 3(b)–3(d) to confirm the characteristic exponential shape of adsorption capacity with variable parameters including pH, time, and mass during adsorption.
process. Unlike the Langmuir and Freundlich isothermal model, this fitting equation could be used to estimate minimum possible adsorption capacity \( q_0 \) of the adsorbent. As shown in Table 2, the minimum possible adsorption capacity was 7.7, 7.8, and 0.5 mg/g for the case of time change (Figure 3(c)), mass change (Figure 3(c)), and pH change (Figure 3(b)), respectively. We saw that there was large difference in minimum possible adsorption capacity between pH with the other ones. This was due to the fact that there was competitive adsorption occurring between Fe\(^{2+}\) ions and H\(^+\) ions into SNPs at low pH as we already discussed based on equation (2). Moreover, the correlation coefficients \( R^2 \) were both higher than 0.95 indicating that the exponential adsorption data fit well into the model.

**Table 1: Comparison of iron adsorption capacity of SiO\(_2\) extracted from RHA with adsorbent materials in the references.**

<table>
<thead>
<tr>
<th>Adsorbent</th>
<th>Concentration range</th>
<th>Iron adsorption capacity (mg/g)</th>
<th>References</th>
</tr>
</thead>
<tbody>
<tr>
<td>SiO(_2)</td>
<td>0.1–1 ppm</td>
<td>9.0</td>
<td>This study</td>
</tr>
<tr>
<td>Coir fibers modifying</td>
<td>73–444 mg/L</td>
<td>7.5</td>
<td>[36]</td>
</tr>
<tr>
<td>hydrogen peroxide</td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Coir fibers</td>
<td>73–444 mg/L</td>
<td>2.8</td>
<td>[36]</td>
</tr>
<tr>
<td>Pine bark waste</td>
<td>55–111 mg/L</td>
<td>2.0</td>
<td>[37]</td>
</tr>
<tr>
<td>Cross-linked chitosan</td>
<td>3–9 ppm</td>
<td>64.1</td>
<td>[38]</td>
</tr>
</tbody>
</table>

**Table 2: Kinetic coefficients in iron adsorption.**

<table>
<thead>
<tr>
<th></th>
<th>Minimum adsorption capacity, ( q_0 ) (mg/g)</th>
<th>Fitting coefficients</th>
<th>( R^2 )</th>
</tr>
</thead>
<tbody>
<tr>
<td>Time</td>
<td>7.7</td>
<td>0.9</td>
<td>12.3</td>
</tr>
<tr>
<td>Mass</td>
<td>7.8</td>
<td>1.3</td>
<td>1.9</td>
</tr>
<tr>
<td>pH</td>
<td>0.5</td>
<td>7.9</td>
<td>4.2</td>
</tr>
</tbody>
</table>

**Figure 4:** Characterization of SiO\(_2\) extracted. (a) FT-IR spectrum of the RHA and extracted SiO\(_2\). (b) TEM image of SiO\(_2\) nanoparticles. (c) EDS elemental composition analysis of SiO\(_2\) nanoparticles. (d) SiO\(_2\) nanoparticles extracted from RHA.
The use of the synthesized silica nanoparticles may offer several benefits for drug delivery and adsorption of heavy metals in environment, as mentioned below. Firstly, silica nanoparticles can eliminate the toxicity in comparison with the other particles linked with magnetic nanoparticles or silver nanoparticles when they are introduced into human body for treatment. Secondly, the synthesis process of silica nanoparticles can also be applied for generation of an insulating layer to control electron tunneling between particles, which may be important in charge transfer or magneto-optics. Thirdly, surface modification via functional group immobilization is being pursued with great interest since it can provide unique opportunities to engineer the interfacial of solid substrates while retaining particles’ basic geometry. Moreover, the extracted SiO2 can be conjugated with various functional groups for specific target detection such as heavy metal ions (Pb²⁺, Cu²⁺, and Cr⁶⁺) for environmental applications. Finally, the area of synthesized SiO₂ can be increased by using cetyltrimethyl ammonium bromide (CTAB) to enhance capability for drug delivery and heavy metal adsorption.

4. Conclusion

We presented the extraction process of SNPs from RHA under different conditions like types of acids, NaOH concentration, dissolved time, and temperature. The results showed that the extraction efficiency was around 83% with purity of 98% and surface area of 78 m²/g. Moreover, the Fe²⁺ ion adsorption capacity of the SiO₂ extracted from RHA was studied under different conditions including pH, contact time, and adsorbent mass. We obtained a maximum loading adsorption capacity of 9 mg Fe²⁺/g SiO₂ at pH 5 with 20 min of contact time. The adsorption efficiency can be enhanced by modification of SiO₂ with functional groups. In addition, the synthesized SiO₂ with the size of around 50 nm can be used for biomedical applications such as drug delivery.

Data Availability

The data used to support the findings of this study are available from the corresponding author upon request.

Conflicts of Interest

The authors declare that there are no conflicts of interest.

Acknowledgments

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