Chemical Studies on the Removal of Iron from Crude Phosphoric Acid Using an Organosilicon Compound

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Abstract: A new adsorbent has been developed to reduce the concentration of iron in crude Egyptian phosphoric acid. This adsorbent has been formed by the treatment of silicate compound derived from clay mineral with π organic acceptor ligand to carry out the exchange of ions as well as complexation with iron. Several parameters (shaking time, temperature, sorbent mass, and batch factor) have been studied. The adsorption of iron from crude phosphoric acid was investigated. The various methods to characterize the adsorption of iron on organosilicon compound (OSC) were collectively evaluated in this study. According to the Langmuir model, the maximum monomolecular capacity (Qº) is 122 mg/g and 122 mg/g with Freundlich model for an initial iron concentration of 2.37% contained in crude phosphoric acid. Characterization studies such as x-ray diffraction, infrared spectroscopy and electron scanning microscope were investigated to substantiate the nature of iron-OSC complexes.

Keywords: Chemical studies, Organosilicon compound, Crude phosphoric acid and Adsorption.

Introduction

The wet-process involves reaction of phosphate rock with an acid (mainly sulfuric acid) to produce crude phosphoric acid which contains a variety of impurities, that vary according to the original of minerals. Many of these impurities particularly the solid ores are removed from the acid by techniques such as clarification. The presence of these impurities affects the quantity and the quality of the product. For this reason, about 95% of the acid produced by the wet-process is directly used as fertilizers and excluded from the use in non-fertilizer applications¹. Many research techniques have been investigated for purifying phosphoric acid, such as: liquid-liquid extraction²⁻⁹, solid–liquid extraction¹⁰, crystallization, concentration or
addition of additives\textsuperscript{11} and by membrane process\textsuperscript{12}. The use of these techniques were limited due to a number of disadvantages such as: i) limited efficiency; ii) high costs of organic solvents and resins (more often not regenerable); iii) difficulty in recovering all the solvent from both the raffinate and the purified acid, due to its granular structure, insolubility in acids, chemical stability, high mechanical strength, and its local availability at almost low cost. The advantages in the application of organosilicon compound (OSC) are: i) no need to regenerate them; ii) their low production costs and waste minimization. In this work, a new material is proposed to achieve the reduction of iron impurities from Egyptian crude phosphoric acid (P\textsubscript{2}O\textsubscript{5} = 40.2\%). The initial concentration of iron in crude phosphoric acid was 2.37\%. This technique is based on the adsorption of iron on the surface of the OSC. In this study, factors affecting the sorption process are investigated in the mode operation of batch process.

**Experimental**

The starting material for this work is a commercial wet-process phosphoric acid (P\textsubscript{2}O\textsubscript{5} = 40.2\%), which is kindly supplied by Abu-Zaabal Company, Cairo, Egypt. Some characteristics of the acid are given in Tables 1 & 2.

### Table 1. Physical characteristics of the crude phosphoric acid.

<table>
<thead>
<tr>
<th>Character</th>
<th>Value</th>
</tr>
</thead>
<tbody>
<tr>
<td>Optical density (Absorbance)</td>
<td>1.4</td>
</tr>
<tr>
<td>PH</td>
<td>0.6</td>
</tr>
<tr>
<td>Density</td>
<td>1.54 kg/L</td>
</tr>
<tr>
<td>Viscosity</td>
<td>13.6 CP</td>
</tr>
<tr>
<td>Electromotive force</td>
<td>450 mv</td>
</tr>
<tr>
<td>Total solids</td>
<td>2%</td>
</tr>
</tbody>
</table>

### Table 2. Chemical properties of the crude phosphoric acid.

<table>
<thead>
<tr>
<th>Component</th>
<th>Value, %</th>
<th>Component</th>
<th>Value, ppm</th>
</tr>
</thead>
<tbody>
<tr>
<td>P\textsubscript{2}O\textsubscript{5}</td>
<td>40</td>
<td>Cd</td>
<td>15</td>
</tr>
<tr>
<td>Fe\textsubscript{2}O\textsubscript{3}</td>
<td>2.2</td>
<td>Co</td>
<td>40</td>
</tr>
<tr>
<td>Al\textsubscript{2}O\textsubscript{3}</td>
<td>0.66</td>
<td>Cr</td>
<td>120</td>
</tr>
<tr>
<td>SiO\textsubscript{2}</td>
<td>0.98</td>
<td>Ni</td>
<td>42</td>
</tr>
<tr>
<td>F</td>
<td>0.85</td>
<td>Pb</td>
<td>20</td>
</tr>
<tr>
<td>MgO</td>
<td>0.5</td>
<td>Zn</td>
<td>200</td>
</tr>
<tr>
<td>CaO</td>
<td>0.3</td>
<td>V</td>
<td>35</td>
</tr>
<tr>
<td>SO\textsubscript{4}</td>
<td>1.3</td>
<td>As</td>
<td>7</td>
</tr>
<tr>
<td>FeO</td>
<td>0.19</td>
<td>Mn</td>
<td>800</td>
</tr>
<tr>
<td>Total Fe as Fe\textsubscript{2}O\textsubscript{3}</td>
<td>2.37</td>
<td>Na\textsubscript{2}O</td>
<td>450</td>
</tr>
<tr>
<td>Organic matter</td>
<td>0.51</td>
<td>K\textsubscript{2}O</td>
<td>200</td>
</tr>
<tr>
<td>U</td>
<td>55 (ppm)</td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

*Preparation of OSC*

Organosilicon compound was prepared by the following procedure. The silicon compound was derived from clay minerals using caustic soda and potassium thiosulfate with ratio 3:1:1.5 w/w. Potassium thiosulfate used as initiator for the polymerization of silicate. 2.5 g of the derived silicon mixed with 1 g of acetyl trimethyl ammonium bromide as inert electrolyte for enhancement of the adsorption process, in addition to 3 g of NaOH in 30 mL of water.
The mixtures were shook vigorously with 0.01 molar of a π acceptor ligand. The organosilicon compound obtained was washed several times with distilled water until pH becomes neutral. Some characteristics of the silicate compounds, OSC before and after adsorption of iron are given in Table 3. The π acceptor ligand is a poly dentate ligand which contains mainly thio, cyano and carboxylic ester groups as shown in IR spectrum. The reagents used in the chemical analysis are of analytical grade. Double distilled water was used in all preparations.

**Table 3.** Chemical composition of silicate compound, OSC before and after adsorption of iron

<table>
<thead>
<tr>
<th>Component</th>
<th>OSC after</th>
<th>OSC before</th>
<th>Silicate compound</th>
</tr>
</thead>
<tbody>
<tr>
<td>SiO₂</td>
<td>31.76</td>
<td>64.63</td>
<td>61.65</td>
</tr>
<tr>
<td>TiO₂</td>
<td>0.53</td>
<td>0.41</td>
<td>1.02</td>
</tr>
<tr>
<td>Al₂O₃</td>
<td>13.75</td>
<td>19</td>
<td>26</td>
</tr>
<tr>
<td>Fe₂O₃</td>
<td>48.36</td>
<td>1.5</td>
<td>6.74</td>
</tr>
<tr>
<td>CaO</td>
<td>0.51</td>
<td>0.27</td>
<td>0.59</td>
</tr>
<tr>
<td>K₂O</td>
<td>0.44</td>
<td>12</td>
<td>0.75</td>
</tr>
<tr>
<td>SO₃</td>
<td>0.34</td>
<td>0.36</td>
<td>1.22</td>
</tr>
<tr>
<td>MgO</td>
<td>3</td>
<td>1.21</td>
<td>2.12</td>
</tr>
<tr>
<td>Total</td>
<td>98.69</td>
<td>99.38</td>
<td>100</td>
</tr>
</tbody>
</table>

**Spectrophotometric determination of iron**

Iron was determined spectrophotometrically by complexation with 1,10 phenanthroline in the presence of hydroxylamine hydrochloride and in the presence of sodium acetate as a buffer solution as follows. In a 25 mL measuring flask to a micro sample containing iron, 2 mL of 10% hydroxylamine hydrochloride, 4 mL of sodium acetate (10%) and 5 mL of 1.10 phenanthroline was added to the mark and dissolved with distilled water. The absorbance was then measured at 512 nm using all constituents without iron as blank solution

**Qualitative analysis of OSC before and after adsorption of iron**

Identification of the OSC before and after adsorption of iron was carried out using the infrared (IR) recording spectrometer. To accomplish this, one mg of OSC before and after adsorption of iron was mixed with 200 mg of dried KBr. Compression disk was then made by compressing the mixture for 5 min at 20000 Lbs/cm². Analysis of the OSC before and after adsorption of iron by electron microscope was carried out according to the following method. A small quantity of each sample was shaken in a test tube with distilled water to obtain a suspension. A drop of this suspension was placed on a coated microscope slide. A further drop was spread on a clean glass slide and a direct platinum carbon replica formed. New tensile fracture surfaces were replaced with carbon and shadowed with gold palladium then electron microscope photos were taken.

**Adsorption studies**

In the present work the adsorption system was studied by batch process. The factors affecting the adsorption process, e.g. shaking time, batch factor, sorbent mass and temperature were studied. In all cases 10 mL of the crude acid was contacted with known weights of the adsorbate in a stoppered glass bottles. The conditions of each experiment were adjusted and the bottles were shaken using a thermostatic shaker to achieve equilibrium concentration. Each mixture was filtered and the samples were analyzed for organic matter and iron using UV-Vis spectrophotometer. The Langmuir isotherm is represented by the following equation:

\[
\frac{1}{q_e} = \left(\frac{1}{q_0}\right) + \frac{1}{b} \cdot \frac{1}{C_e}
\]  

(1)
Where \( C_e \) is the equilibrium concentration (mg/L), \( q_e \) is the amount adsorbed at equilibrium time (mg/g) and \( q^e \) and \( b \) are Langmuir constants related to adsorption capacity and energy of adsorption, respectively. These can be calculated from the \( 1/q_e \) vs. \( 1/C_e \) plot by the relationships:

\[
q^e = \text{intercept}^{-1} \quad \text{and} \quad b = \text{slope}^{-1} \times \text{intercept}.
\]

The favorable nature of adsorption can be expressed in terms of a dimensionless separation factor of equilibrium parameter, which is defined by:

\[
R_L = 1/(1 + bC_o)
\]

Where, \( b \) is the Langmuir constant and \( C_o \) is the initial concentration of the adsorbate in solution.

Freundlich equation is presented as:

\[
q_e = K_f C_o^{1/n}
\]

Rearranging gives:

\[
\log q_e = \log K_f + 1/n \log C_o
\]

Hence, a plot of \( \log q_e \) vs. \( \log C_o \) enables the constant \( K_f \) and exponent ‘n’ to be determined.

**Batch experiments**

The factors affecting the adsorption process, e.g. shaking time, batch factor and sorbent mass were studied. In all cases, 10 mL of green acid was contacted with fixed amount of OSC in stoppered glass bottles. The conditions of each experiment were adjusted and the bottles were shaken using a thermostatic shaker to achieve equilibrium concentration. Each mixture was filtered and the samples were analysed for iron using a Shimadzu model 160 A double-beam UV spectrophotometer. Matched 10 mm quartz absorption cells were used. In all cases, the difference between the initial concentration \( (C_o) \) and the equilibrium concentration \( (C_e) \) was calculated and used to determine the adsorptive capacity \( (q_e) \) as follows. \( q_e = V (C_o-C_e)/m \), where \( V \) is the total volume of solute solution (mL); \( m \) is the mass of sorbent used (g), \( C_o \) is the initial concentration of the solute (mg/L) and \( C_e \) is the residual concentration of the solute (mg/L). Adsorption isotherms of iron were determined by shaking various amounts OSC with constant volume of green acid (10 mL) until equilibrium is reached. The residual concentration was determined as described above.

**Results and Discussion**

**Effect of OSC dose**

Different weights of OSC were used at 25 °C. The OSC dose used covers the range from 0.5 to 12 g/L. The uptake percent of iron on the OSC plotted against the respective OSC dose in Figure 1 shows that the adsorption increases by increasing OSC dose till 12 g/L then become a constant because of the saturation of the active sits.
Effect of shaking time

Different shaking time intervals were studied in the range of (5-40) min., to study the uptake % of iron by OSC the results are represented in Figure 2. The results show that equilibrium is reached after 15 min. of shaking time.

![Figure 2. Effect of contact time on uptake % of iron by OSC.](attachment:image2)

Effect of temperature

The effect of temperature on the adsorption of iron by OSC was studied by varying the temperature in the range 30-70 °C. Plotting of uptake % values against the respective absolute temperature in Figure 3, confirm that the adsorption of iron on OSC may be chemical in nature where, the adsorption rate is improved when temperature increases.

![Figure 3. Effect of temperature on uptake % of iron by OSC.](attachment:image3)

Effect of $H_3PO_4$ volume to OSC mass ratio (v/m)

The effect of changing v/m ratio studied by increasing the weight of sorbent in the range 0.5-12 g, while fixing the volume at 1L. From the results shown in Figure 4, it was deduced that as v/m ratio decreases by increasing the sorbent weight the uptake percent increases. This may be related to the increase of sorbent of iron due to the increase of the available sites of sorbent.

Effect of organic matter concentration

The effect of organic matter impurities concentration in the crude phosphoric acid on the uptake of iron was studied by using two different concentrations of organic matter. From the data obtained it was found that the organic matter originally present in the crude phosphoric acid have no significant effect on the adsorption of iron by OSC.
Effect of the oxidation state of iron
The effect of iron oxidation state on its uptake % by OSC is studied. The results in Figure 5 show that ferrous ions are adsorbed more than ferri c ions. This could be explained by the presence of the π acceptor ligand which interact with iron via electron transfer from the ligand to ferrous ions then return back to the ligand throught π interaction.

Adsorption isotherms
Adsorption data for a wide range of adsorbate concentrations are most conveniently described by adsorption isotherm, which relate adsorption density qₑ to equilibrium adsorbate concentration in the bulk fluid phase, Cₑ as shown in Figure 6. The Langmuir isotherm\(^\text{14}\) was tested by plotting 1/ Cₑ vs. 1/ qₑ where, Cₑ (g/L) is the equilibrium concentration of the investigated metal ion, qₑ (g/g) is the metal ion concentration in the loaded solid phase as shown in Figure 7. The obtained linear relation indicates that the adsorption of iron obey langmuir isotherm. From the figure, qₑ max for iron was found to be 122.46 mg iron / g OSC and (b) for iron was 0.18 Freundlich isotherm\(^\text{15}\) is also tested by drawing a plot of log qₑ vs log Cₑ as shown in Figure 8. The adsorption of iron was found to follow the Freundlich isotherm. The fitting of the data to Freundlich isotherm suggests that adsorption is not restricted to one specific class of sites and assumes surface heterogeneity. From the slope and intercept of the plot, the Freundlich parameters are calculated,
Chemical Studies on the Removal of Iron

$K = 122.46 \text{ mg/g sorbent.}$

$1/n = 5.59$

and $n = 0.18$

The slope of Freundlich isotherm is more than 1, indicating a concentration independent adsorption of iron$^3$. 

**Figure 6.** General adsorption isotherm of iron by OSC.

$R^2 = 0.9665$

**Figure 7.** Langmuir adsorption isotherm of iron by OSC.

$R^2 = 0.9494$

**Figure 8.** Freundlich adsorption isotherm of iron by OSC.
Sorption mechanism

Sorption of iron onto OSC can be understood in terms of hydrophilic surface containing mainly K which works as ion exchanger for K ions and complex formation with deprotonated sulfide groups as a ligand as well as cyanide group coordinated with iron via charge transfer from iron to the \( \pi \) molecular orbital of cyanide group. Uptake of iron was shown to be accompanied by a stoichiometric replacement of K from the exchange sites. To substantiate the nature of OSC iron complexes, classical x-ray diffractometry, in conjunction with and complementary with infrared spectroscopy are investigated. Also electron scanning microscope is singularly suited for the study of OSC-iron interactions.

X-ray studies

X-ray diffractometry is one of the major tools in the study of metal complexes. Its usefulness is due to the relative ease with which one can determine whether adsorption only occurs on external mineral surfaces, or if the metal ions is capable of being adsorbed within the interlayer spaces. Furthermore, the orientation of the metal ion between lattice layers, whether parallel, normal or at an angle to the mineral plane, can be predicted from basal expansion, provided that interlayer adsorption is regular X-ray diffractograms of silicate compound, OSC and iron-O SC are depicted in Figures 9, 10 & 11 respectively. Interpretation of these diffractograms in terms of the basal spacings of OSC before and after sorption is given in Table 4. Comparison between OSC and iron-OSC complex reveals that the basal spacing of the studied OSC remains unchanged to some extent. Comparing c-spacing of OSC and their iron complexes indicates that applied treatments do not affect the characteristic diffraction peaks. These findings dictate that iron must have been adsorbed on external surfaces and edges of such material. Nevertheless, the slight contraction or expansion of c-spacing may suggest the possible entrapment of the iron species into the tunnels and channels of the OSC, which remained, more or less, unchanged. Also X-ray diffractograms of the iron-OSC shown in Figures 9 indicate the appearance of the characteristic iron peak (2.0091 Å) on the OSC after acid treatments which provide an evidence for the sorption of iron. Nevertheless, IR spectroscopy and electron microscopy will add further confirmation regarding to the type of bonding and morphology of sorbed metal ion.

\[ \text{Figure 9. X-ray diffraction of silicate compound.} \]
Infrared spectroscopy studies

The IR adsorption bands and the frequencies of vibrations are dependent on the mass of atoms, the restraining forces of the bonds and the geometry of structure. Consequently, the spectrum is sensitive to isomorphous substitutions in the mineral structures, as these affect both bond strengths and atom masses. The symmetry and regularity of structure determine the intensity and frequency of its vibrations\(^9\). So that the IR spectrum is often a sensitive indicator of the degree of order of a mineral. Therefore, IR spectrum of a mineral is a characteristic feature that permits the identification of mineral species. IR spectra can provide direct evidence on the chemical and physical processes that lead to adsorption on surface, and these reactions may, in turn, serve to differentiate the various types of surfaces present in heterogeneous systems as OSC. The IR spectrum of silicate compound shown in Figure 12 is characterized by the following absorption bands:
Figure 12. IR spectrum of silicate compound.

Two sharp bands at 3699 cm\(^{-1}\) and 3622 cm\(^{-1}\), indicating isomorphous substitution in the crystal lattice, the band mostly arises from OH coordinated to (Al, Fe) pair. A medium broad band at 3429 cm\(^{-1}\), indicating OH stretching vibrations, the broadening is a result of Al substitution for Si in the tetrahedral sheet. A medium broad band at 1635 cm\(^{-1}\) ascribed to deformation OH or absorbed water. Broad band at 1035 cm\(^{-1}\), mostly related to Si-tetrahedron in smectite clay minerals group. Three sharp bands at 528, 690 and 914 cm\(^{-1}\), due to Si-O stretching bands which are complicated by variations in Al substitution for Si, OH bending vibration causes a characteristic absorption at 914 cm\(^{-1}\) which indicates that only Al is present in octahedral sheet. Two medium sharp bands at 428 cm\(^{-1}\) and 466 cm\(^{-1}\), indicating water linked to Mg ions. A strong sharp band at 790 cm\(^{-1}\), most probably due to Al-tetrahedron I.R. spectra of the studied OSC minerals before and after sorption of iron are shown in Figures 13, 14.

Figure 13. I.R spectrum of OSC before adsorption.
Spectrum of OSC before sorption
A medium band at 1635 cm\(^{-1}\) ascribed to deformation OH or adsorbed water. Two weak bands at 501 and 586 cm\(^{-1}\) due to Si-O stretching bands which are complicated by variation in Al substitution for Si.\(^{20}\) A strange sharp band at 798 cm\(^{-1}\), most probably due to Al-tetrahedron. Weak band at 987 cm\(^{-1}\), mostly related to C-N stretching vibration. A weak broad band at 1107 cm\(^{-1}\), ascribed to C-S stretching.

Spectrum of OSC after sorption
To substantiate the effect of sorption on the I.R. spectra of the OSC, Figure 14 clarifies that the I.R. spectrum of iron-OSC differs from that of OSC in respect to: appearance of a new band at 459 cm\(^{-1}\) due to water associated with iron. Dislocation of the absorption bands at 798, 501, 586 and 1639 cm\(^{-1}\) to another values as they appear at 794, 493, 590 and 1635 cm\(^{-1}\). Dislocation of the absorption bands at 1107 and 2380 cm\(^{-1}\) to higher values as they appear at 1114 and 2403 cm\(^{-1}\) and this most probably due to the bonding between iron and the function groups corresponding to the absorption band (C-S and C≡N respectively). Dislocation of the absorption bands 3240 and 3413 cm\(^{-1}\) to a tower values as they appear at 3101 and 3379 cm\(^{-1}\) mostly due to water linked to iron and/or hydroxyl stretching vibrations. The relative intensity of some absorption bands is some what affected. For instance, the band at 1635 cm\(^{-1}\) displays apparent increase in its intensity. This behavior may be taken as an indication that iron is adsorbed on the external surface of these materials and its hydration shell contribute to such absorption band.

Electron Microscope studies
The above mentioned results of X-ray and I.R. spectrum of OSC and iron-OSC complex are supported by the electron micro graphs which reveals that the silicate compound is characterized by the platy morphology and relatively fine particle size. Photographing the OSC and OSC-iron complex in the electron microscope, showed the characteristic shapes of its grains in a very clear manner. Moreover the electron micro graphs reveal that the used OSC samples have heterogeneous surface. The electron micrographs of OSC-iron complex show that an aggregate mass that appears interwoven characterized by porous structure. The varieties identified in the micrographs are small and large pores. The small variety (≈ 1 nm) may contain more iron. Also, the complementary EDAX technique shows the silicate compound and OSC before and after adsorption of iron as shown in Figures 15, 16 & 17.
Figure 15. EDAX of silicate compounds.

Figure 16. EDAX of OSC before adsorption.

Figure 17. EDAX of OSC after adsorption.
Conclusions
Iron could be removed efficiently from phosphoric acid produced at Abu-Zaabal Company, Egypt, using organosilicon compound. The uptake of iron increases in reducing conditions. 12 g of OSC is optimal for the removal of about 60% of iron content of the acid. Optimization studies with separating funnel indicate that a time of 15 min is sufficient for reaching equilibrium. The uptake of iron is an endothermic process.

References