Research Article

Effect of Transient Nicotine Load Shock on the Performance of Pseudomonas sp. HF-1 Bioaugmented Sequencing Batch Reactors

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Bioaugmentation with degrading bacteria can improve the treatment of nicotine-containing tobacco industrial wastewater effectively. However, the transient and extremely high feeding of pollutants may compromise the effectiveness of the bioaugmented reactors. The effect of transient nicotine shock loads on the performance of Pseudomonas sp. HF-1 bioaugmented SBRs were studied. The results showed that, under 500–2500 mg/L of transient nicotine shocks, all the reactors still could realize 100% of nicotine degradation in 4 days of recovery, while the key nicotine degradation enzyme HSP hydroxylase increased in expression. Though the dramatic increase of activities of ROS, MDA, SOD, and CAT suggested that transient nicotine shock loads could induce oxidative stress on microorganisms in activated sludge, a decrease to control level demonstrated that most of the microorganisms could resist 500–1500 mg/L of transient nicotine shock under the protection from strain HF-1. After 8 cycles of recovery, high ROS level and low TOC removal in high transient shock reactors implied that 2000–2500 mg/L of transient nicotine shock was out of its recovery of strain HF-1 bioaugmented system. This study enriched our understanding on highly efficient nicotine-degrading strain bioaugmented system, which would be beneficial to tobacco waste or wastewater treatment in engineering.

1. Introduction

Nicotine is the main addictive component in tobacco and is the primary toxic compound in tobacco waste [1]. In fact, more than 60 tons of tobacco wastewater is discharged to produce only 1 ton of cigarettes [2]. Approximately, more than 500 billion tons of nicotine-containing wastewater is discharged globally each year [3]. As is known to all, nicotine can easily permeate different kinds of cell membrane even the blood-brain barrier [4], which is carcinogenic, teratogenic, and mutagenic [5]. Nicotine-containing tobacco wastewater treatment has attracted widespread attention.

With the isolation of highly efficient nicotine-degrading microorganisms, bioaugmentation has been well-developed [6–9]. In our previous study, we used Pseudomonas sp. HF-1 and Acinetobacter sp. TW to colonize in activated sludge for bioaugmentation, respectively. Both of these systems were operated excellently, with nearly 100% of nicotine degradation and more than 80% of chemical oxygen demand (COD) removal [1, 10]. Compared to the traditional activated sludge technology, bioaugmentation with highly efficient degrading bacteria is a powerful way to treat nicotine-containing tobacco wastewater.

For better development of bioaugmentation in nicotine-containing tobacco wastewater treatment, we did considerable amount of analysis both on traditional and on bioaugmented activated sludge systems. Actually, higher than 250 mg/L of nicotine can induce oxidative stress and inhibit bacterial activities when there were no nicotine-degrading bacteria in the activated sludge [11]. However, in the bioaugmented system, nicotine was rapidly degraded by highly efficient nicotine-degrading bacteria and the toxicity from nicotine on the bacterial community was minimized [1]. Highly efficient degrading strain played an important role in their good performance of bioaugmented systems [12, 13].
As the main toxicant in tobacco wastewater, nicotine takes a dominant part in inducing oxidative stress. With the increasing of nicotine concentration in wastewater, the content of reactive oxygen species (ROS) increased accordingly [14]. After bioaugmentation and acclimation, ROS was maintained in the reasonable range and the system was stably operated [10, 11]. Notably, stable operation is an ideal laboratory model. In the engineering operation, bioaugmented systems have to confront the nicotine load shock. Because of the changes of raw materials and production process in the cigarette manufacture, it could be up to 1000 mg/L of nicotine, which is 4 times the normal feed on our Pseudomonas sp. HF-1 bioaugmented system. Though a lot of studies investigated the performance of bioaugmented system in stable pollutant load, few studies give us the information about the operation under the shock of pollutant load. Shock tolerance is very important in the application of bioaugmented system in engineering.

In this study, reactor performance was investigated under different nicotine load shock. Besides, community structure and activities of nicotine-degrading strain were traced. In addition, oxidative stress was monitored by measuring four popular biomarkers ROS, malondialdehyde (MDA), catalase (CAT), and superoxide dismutase (SOD). This systematic report will give us the insight about how bioaugmented system confronts nicotine shock. It also will give us more information for future application of this technology in the tobacco wastewater treatment.

2. Materials and Methods

2.1. Experimental Set-Up. Experiments were conducted in six identical sequencing batch reactors (SBRs) named R1, R2, R3, R4, R5, and R6, with 1L of working volume. All the reactors were maintained at room temperature (28 ± 2°C) throughout the whole period of this experiment. An air pump through diffuser was employed to maintain 3–5 mg/L of dissolved oxygen (DO). Activated sludge with strain HF-1 colonization was inoculated into each reactor with a biomass of 3.9 ± 0.06 gSS/L. The reactors were operated on a 24 h cycle, and each cycle included 5 min influent filling, 10 min effluent withdrawal, 30 min settling and aeration for the rest of the time. After settling, effluent was discharged at 50% of volumetric exchange ratio.

Activated sludge with strain HF-1 colonization was cultured as follows: the activated sludge from Qige wastewater treatment plant (Hangzhou, Zhejiang, China) was used as the endogenous seed. Strain HF-1 was inoculated into the seed activated sludge. After stopping inoculating for 7 days, reverse-transcription-PCR was amplified to detect the colonization of strain HF-1 [15]. Once the colonization of strain HF-1 in activated sludge was successful, the activated sludge was used as the inoculating activated sludge for the set-up of the above-mentioned six identical reactors.

The tobacco wastewater to feed all reactors was prepared as follows: nicotine-containing tobacco waste collected from China Tobacco Zhejiang Industrial Co. Ltd. was mixed with distilled water. Then, the mixture was filtered and diluted for the SBR treatments. In the present study, the behavior of reactors was monitored under five different transient shock loads. Initially, reactors were operated with nicotine concentration of 250 mg/L at 24 h hydraulic retention (HRT) for 5 days to uniform the six identical reactors. To evaluate the effect from shock loads, the final concentration of nicotine in these reactors sharply reached 500 mg/L (2-fold), 1000 mg/L (4-fold), 1500 mg/L (6-fold), 2000 mg/L (8-fold), and 2500 mg/L (10-fold) in R2, R3, R4, R5, and R6, respectively. Reactor R1 feeding with 250 mg/L nicotine was used as a control.

2.2. Evaluation of Reactor Performance. Influent and effluent were sampled and analyzed for nicotine and total organic carbon (TOC) through the period of operation. Nicotine concentration was analyzed by WATERS high performance liquid chromatography (HPLC) using an X Bridge C-18 column (5 μm i.d., 4.6 × 250 mm). The mobile phase consisted of 0.1% triethylamine and methanol (40:60, v/v) was applied at a flow rate of 1 mL/min. And nicotine was detected at 254 nm. The TOC concentration was determined using a TOC analyzer (Shimadzu, Japan).

2.3. Detection of Strain HF-1 in Activated Sludge. Total RNA from the 6th and 14th d activated sludge was extracted using the Bioteke soil RNA isolation kit (Bioteke, Beijing, China). Then, total RNA was treated with DNase I (RNase-free) at a concentration of 1 U/μg for 30 min at 37°C to remove contaminating DNA. The RNA was reversely transcribed to cDNA by using the TransGene RT-PCR kit. Quantitative real-time PCR was carried out to quantify bacteria strain HF-1 in activated sludge. The 16S rRNA gene was used as a housekeeping gene, whose primer pair is 338F (5′-CCTACGGGAGGCAGCAG-3′) and 518R (5′-ATTACCGCGGCTGCTGG-3′). The specific hsp gene of strain HF-1 was amplified to quantify the amount of strain HF-1 in activated sludge, whose primer pair is hsp S (5′-ATACTGGCCGAAACAATACC-3′) and hsp A (5′-CCTCCAGAAAAGGAGAAC-3′). Real-time PCR was performed in a 10 μL reaction mixture system containing 5 μL of SYBR Green Supermix (Bio-Rad Laboratories Inc., Hercules, CA), 0.2 μL of each primer (10 μM), 1 μL cDNA (approximately 5 ng), and 3.6 μL sterile H2O. Real-time PCR conditions were as follows: 95°C for 3 min, followed by 40 cycles of 95°C for 20 s, 58°C for 20 s, and 72°C for 20 s. At the end, melt curve analysis was performed by the addition of a final step, starting at 65°C and going to 95°C; the signal was monitored every 5 s with a 0.5°C temperature increment. The relative abundance of strain HF-1 was normalized by hsp gene expression against the 16S rRNA through 2−ΔΔCt method [16].

2.4. Bacterial Community Analysis. PCR as well as denaturing gradient gel electrophoresis (PCR-DGGE) was used to analyze bacterial community in the reactors on 14th d. DNA was extracted from activated sludge samples using Bioteke sludge DNA isolation kit (Bioteke, China). PCR was performed with primers targeting bacterial 16S rRNA gene (P338F with GC-clamp and P518R). DGGE analyses were conducted with a Bio-Rad DCode system (Hercules, CA) using a 10% (wt/vol) polyacrylamide gel and a denaturing
gradient from 40 to 60%. The gels were run at 90 V and 60°C for 20 min, followed by 160 V and 60°C for 6.5 h. The gels were visualized by silver staining [17] and photographed using a gel imaging instrument. DGGE were analyzed using Quantity One software (version 4.6.2, Bio-Rad). A clustering analysis was performed using the unweighted pair group method with arithmetic means (UPGMA) [18].

2.5. Toxicity Assay. Activated sludge was collected on 4th d, 6th d, and 14th d by centrifugation at 12000 rpm for 10 min. Each sample was washed three times with phosphate buffer solution (PBS) and resuspended in 2 mL of PBS [13]. Then, the suspension was ultrasonically disrupted on ice for 99 cycles (with 3 s of working and 5 s of cooling between burst) by using a sonifier (Sonics, USA). Subsequently, the suspension was centrifuged at 12000 rpm and 4°C for 20 min and the supernatant was collected for toxicity assay.

The total protein content in the supernatant was determined by a modified Bradford method [19]. The activity of ROS was analyzed using the commercial ROS ELISA Kit purchased from the Chunxiang Biotechnology Co. Ltd. (Shanghai, China). The activities of MDA, SOD, and CAT were detected using the spectrophotometric protocols with kits A003, A001, and A007 purchased from the Nanjing Jiangcheng Bioengineering Institute (Jiangsu, China).

2.6. Statistical Analysis. All data were presented as mean ± standard error. One-way analysis of variance (ANOVA) was performed using SPSS software (version 19.0). The levels of significance were tested at \( p < 0.05 \).

3. Results and Discussion

3.1. Performance of the Reactors. The experiment lasted for 14 d. The efficiency of nicotine as well as TOC removal of all the reactors was routinely monitored (Figure 1). Before nicotine shock loads (from day 5 onwards), all reactors were efficient at pollutant removal with 100% of nicotine degradation and nearly 80% of TOC removal. There was no significant difference between all the reactors.

On the 5th day, we performed the nicotine shock. Final nicotine concentration in R2, R3, R4, R5, and R6 was 500, 1000, 1500, 2000, and 2500 mg/L, respectively. In order to evaluate the effect of nicotine shock on reactor performance, nicotine degradation and TOC removal were calculated as follows: nicotine degradation (%) = \( \frac{[\text{nicotine}_{\text{before cycles}} - \text{nicotine}_{\text{after cycles}}]}{[\text{nicotine}_{\text{before cycles}}]} \times 100\% \); TOC removal (%) = \( \frac{[\text{TOC}_{\text{before cycles}} - \text{TOC}_{\text{after cycles}}]}{[\text{TOC}_{\text{before cycles}}]} \times 100\% \).

Though the decline of nicotine and TOC removal efficiencies in R2–R6 was observed at the beginning of nicotine shock, all of the systems could be recovered after several days of nicotine shock. As seen in Figure 1, nicotine degradation in R2, R3, R4, R5, and R6 could be totally recovered within 2, 3, 4, 4, and 4 d after 2-fold, 4-fold, 6-fold, 8-fold, and 10-fold nicotine shock, respectively. *Pseudomonas* sp. HF-1 could express high nicotine tolerance even in complicated activated sludge environment.

Compared to nicotine degradation, it took a longer time to recover the TOC removal. TOC removal in R2, R3, and R4 could be recovered within 2, 3, and 4 d after 2-fold, 4-fold, and 6-fold shock, respectively. However, TOC removal in R5 and R6 was hard to be recovered under 8-fold and 10-fold shock. After 7 d, TOC was still lower than 70% of removal. Under 2000–2500 mg/L of nicotine shocks, native bacteria in activated sludge were possibly suffered.

3.2. Strain HF-1 in the Reactors. Quantitative real-time PCR was used to estimate the dynamic changes of the relative abundance of strain HF-1 with different concentrations of nicotine shock [10]. Gene *hsp*, which encodes HSP hydroxylase, is one of the key nicotine-degrading genes in strain HF-1 [20–22]. The more the copies of gene *hsp* are detected, the more the strain HF-1 exists in activated sludge [1]. In our preliminary study, gene *hsp* could not be detected in the original activated sludge obtained from Qige Treatment Plant.

As seen in Figure 2, compared with the control reactor R1, a sharp increase was noticed in all experimental groups (R2–R6) after shock loads (6th d). The activity of HSP hydroxylase in R3–R6 with 1000–2500 mg/L nicotine shock loads was significantly higher than R2 with 500 mg/L nicotine shock loads. After being recovered for 8 cycles, the activity returned but was still significantly higher than R1. These results could well explain why all reactors could recover nicotine degradation within 4 days even up to 2500 mg/L of nicotine load shock. With the sharp increasing of nicotine, more strain HF-1 reproduced to degrade nicotine. After rapidly degrading nicotine, the amount of strain HF-1 decreased due to limitation of nicotine. A good fitness of strain HF-1 to nicotine could bring a bright prospect to the development of bioaugmentation in tobacco wastewater treatment.

3.3. Bacterial Community of the Reactors. The activated sludge on the 14th d was sampled from each reactor and analyzed by PCR-DGGE. As shown in Figure 3, bands in the DGGE profile were similar in their amounts and sites. This suggested that the structures of bacterial communities in different reactors were similar. The transient shock loads of nicotine from 500 to 2500 mg/L would not change the microbial species present in activated sludge greatly.

According to the clustering analysis of DGGE pattern, R5 and R6, with 8-fold and 10-fold shock, were assembled together. For the DGGE pattern analysis, the density of band was taken into account to evaluate the bacterial abundance. As mentioned before, TOC removal was hard to be recovered under 8-fold and 10-fold shock. These might implicate that, under 8-fold and 10-fold shock, the activity of bacterial communities was suffered. Actually, when the population of microorganisms is lower than a certain abundance, it is hard to be detected by PCR-DGGE [23]. Thus, some other strategies should be developed to analyze the bacterial community within such short period.

3.4. Oxidative Stress in the Reactors. Toxic and hazardous compound is responsible for ROS produce, which is capable
Figure 1: Effect of nicotine shock on pollutant removal in SBRs treating tobacco wastewater. Reactor R1 was the control without nicotine shock load; reactors R2 to R6 were with the nicotine shock load of 500, 1000, 1500, 2000, and 2500 mg/L, respectively.

Figure 2: Changes of the activity of HSP hydroxylase in the reactors with different nicotine shock loads. Reactor R1 was the control without nicotine shock load; reactors R2 to R6 were with the nicotine shock load of 500, 1000, 1500, 2000, and 2500 mg/L, respectively. Different letters represent significant differences between reactors ($p < 0.05$).
of destroying the balance between oxidation and antioxidation in cells [24]. The change of ROS content is shown in Figure 4(a). Before nicotine shock loads, the contents of ROS in all reactors were almost the same and close to 20 U/mg prot. After nicotine shock, the content of ROS in the reactors with more than 1000 mg/L nicotine loads went up sharply. After recovery for 8 cycles, the ROS value in most of the reactors (R2–R4) returned to the initial level. However, the ROS value in R5-R6 was still higher than the initial level.

Meanwhile, we detected the content of MDA, which is the product of membrane lipid peroxidation [25]. The change of MDA content is shown in Figure 4(b). Before nicotine shock loads, the content of MDA in all reactors was almost the same and close to 4 mol/mg prot. A dramatic increase in MDA content was observed in the reactors with 1000, 1500, 2000, and 2500 mg/L nicotine shock loads, reaching levels that were 1.2-, 1.4-, 2-, and 2.4-fold higher than the one observed in the control reactor R1, respectively. The results were in accordance with the content of ROS. These results indicated that oxidative stress was induced when nicotine shock was higher than 1000 mg/L.

After the influent concentrations of nicotine returned to 250 mg/L and performed for 8 cycles, the content of MDA decreased below the control level in 14th d. However, the ROS value in R5-R6 was still higher than the initial level. ROS could produce a variety of oxidative stress, including lipid peroxidation, DNA damage, and inactivation of many enzymes [11, 26]. Though lipid peroxidation was recovered, other kinds of oxidative stress could put the native microorganisms into suffering longer, which is possibly one of the main reasons for nonrecovery of TOC removal. Thus, compared to other biomarkers for oxidative damage like MDA, the content of ROS is one of the direct and convincing biomarkers.

SOD and CAT are two main kinds of antioxidant enzymes in organisms, which could eliminate a certain amount of ROS quickly. The change in SOD and CAT activities of all reactors was evaluated and presented in Figures 4(c) and 4(d). The SOD activity in reactors R2, R3, and R4 with nicotine concentration of 500, 1000, and 1500 mg/L almost had no change after shock loading, while the SOD activity in reactors R5 and R6 with 2000 and 2500 mg/L reached up to 45.6 and 49.3 mol/mg prot, respectively. Meanwhile, after nicotine shock loads, the activities of CAT in R2, R3, R4, R5, and R6 were significantly higher than those on day 4. This suggested that both SOD and CAT played important roles in eliminating ROS induced by nicotine. Compared to SOD, CAT played a longer role in eliminating ROS. In the complicated system, we do not recommend using SOD and CAT as biomarkers.

4. Conclusions

The bioaugmented activated sludge system with strain HF-1 has a good performance to deal with nicotine shock. It took 2, 3, 4, 4, and 4 d to recover under 500, 1000, 1500, 2000, and 2500 mg/L of nicotine shock, respectively. The nicotine shock would not damage the ability of nicotine degradation of strain HF-1. On the contrary, it would stimulate the activity of HSP hydroxylase, which is key enzyme for nicotine degradation. Though a dramatic increase of ROS, MDA, SOD, and CAT suggested that nicotine shock induced oxidative stress on microorganisms in activated sludge, their decrease to control level demonstrated that activated sludge could resist 500–1500 mg/L of transient nicotine shock with protection from strain HF-1. However, under 2000–2500 mg/L nicotine shock, native microorganisms would be damaged by extremely high ROS in systems. Due to diversity oxidative stress on native microorganisms, MDA, SOD, and CAT were not suitable for biomarker under transient nicotine shock. Comparatively, as the direct reflection on oxidative stress, ROS could be selected as biomarker under transient nicotine shock.
Figure 4: The oxidative stress in the reactors with different nicotine shock loads. Reactor R1 was the control without nicotine shock load; reactors R2 to R6 were with the nicotine shock load of 500, 1000, 1500, 2000, and 2500 mg/L, respectively. (a) ROS; (b) MDA; (c) SOD; and (d) CAT.
Abbreviations

BOD: Biochemical oxygen demand
CAT: Catalase
COD: Chemical oxygen demand
DO: Dissolved oxygen
HPLC: High performance liquid chromatography
HRT: Hydraulic retention time
HSP: 6-Hydroxy-3-succinoylpyridine
MDA: Malondialdehyde
PCR-DGGE: Polymerase chain reaction and denaturing gradient gel electrophoresis
ROS: Reactive oxygen species
SBR: Sequencing batch reactor
SOD: Superoxide dismutase
TOC: Total organic carbon.

Competing Interests

The authors declare that there is no conflict of interests regarding the publication of this paper.

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References


