

Research Article

Copper Removal from Electroplating Wastewater by Coprecipitation of Copper-Based Supramolecular Materials: Preparation and Application Study

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Received 16 November 2015; Revised 17 January 2016; Accepted 14 February 2016

Academic Editor: Ewa Schab-Balcerzak

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This paper describes an experimental study for the removal of copper ions from electroplating wastewater. Different metal ions are added to the wastewater to remove copper ions by coprecipitation and the copper-based supramolecular materials with layered structures are obtained. It is found that the best results are obtained with the addition of $-Mg^{2+}-Al^{3+}$ mixture with ratio of 3 : 1, pH ≈ 10 , and aging for 1 d at 60°C. With these conditions, the residual copper in the electroplating wastewater satisfies national emission standards and wastewater handling capacity of up to 30 mL can be achieved. The properties of the copper-based supramolecular materials prepared under these optimal conditions are characterized. The results show that the materials have a layered structure and good thermal and structural stability and achieve a saturated adsorption of iodide ions of 41.23 mg/g.

1. Introduction

Electroless plating of metal coatings onto nonmetallic surfaces by means of chemical deposition can provide protection and improve the performance of the plated surface in various technical applications [1–3]. The coating produced by electroless copper plating exhibits excellent adhesion, corrosion resistance, reliability, heat resistance, and electromagnetic shielding, and the process has the advantage of producing an even coating. In addition, the chemical plating technique is applicable to the treatment of surfaces that are not electrically conducting [4–6].

Both the electroplating process itself and the cleaning of the coating produce a considerable amount of waste. In particular, electroplating wastewater contains a wide range of copper compounds, in addition to Fe^{3+} , Zn^{2+} , Cd^{2+} , Ni^{2+} , Cr^{3+} , and many other heavy metal ions. Not only do these represent a waste of resources, but as environmental pollutants they are hazardous to human and animal health [7–9]. But from the development of electroplating wastewater

treatment technology in recent decades, 80% of electroplating wastewater is using chemical methods to deal with the copper in electroplating wastewater at home and on-abroad. In addition, electrolysis, ion exchange, adsorption, and membrane separation method are used. Contemporary copper is widely used, and many kinds of copper-containing wastewater are produced. According to the nature of electroplating wastewater and concentration of copper in wastewater, the different methods of removal of copper in wastewater have been applied. The high copper concentration electroplating wastewater dealt with neutralization and electrolysis, while the low copper concentration electroplating wastewater can use the restore method or methods to mix. Copper is an essential trace element in the diet, but excessive intake can have toxic effects. For copper electroplating enterprises, the emission limit specified in the Chinese national standards is ≤ 0.5 mg/L [10].

Supramolecular materials are based on supramolecular chemistry, which has had wide applications in a number of areas of materials science and technology [11–14]. In recent

years, there has been great progress in the use of supramolecular materials in molecular devices and as liquid crystals, biomaterials, and nanomaterials [15–18].

In the study reported here, copper in electroplating wastewater is removed by a coprecipitation method by which copper-based supramolecular materials with layered structures are formed. The method was used in electroplating wastewater by adding a certain concentration of metal ions (such as Mg^{2+} , Al^{3+}); then layered double hydroxides (LDHs) formed by reaction between added metal ions and Cu^{2+} in waste in which board consists of liquid waste of copper ions and metal ions plus. Content of copper ion from waste was reduced and simultaneously the layered material formatted which structure between the layers is made up of calcium carbonate and hydroxyl anion. After high temperature roasting, losing structure interlayer anions and structure layer board of hydroxyl reserves layer board structure. So the layered structure material has strong adsorption for anion. The preparation and properties of these materials are investigated with regard to the use of this method in environmental protection.

2. Experimental

2.1. Instruments and Reagents. An inductively coupled plasma optical emission spectrometer (ICP-OES710ES, Varian), a constant-temperature electric drying oven (DHG-9101.1SA), an electronic analytical balance (Sartorius), and an atomic absorption spectrometer (AA7000) were used.

The reagents used were $\text{Mg}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$, $\text{Al}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$, Na_2CO_3 , NaOH , $\text{CuCl}_2 \cdot 2\text{H}_2\text{O}$, HCl , $\text{Ca}(\text{NO}_3)_2 \cdot 4\text{H}_2\text{O}$, $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$, $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$, KI , H_3PO_4 , HCOOH , and Br_2 . All were analytically pure.

2.2. Electroplating Wastewater Composition. The copper electroplating wastewater used in the experiment was provided by the manufacturer and the stock solution was diluted 20 times. Determination of the metal content of the wastewater by ICP-OES revealed that the concentrations of Cu were 8.8 g/L, as shown in Table 1 together with the concentrations of the other main elements present.

2.3. Experimental Procedure

2.3.1. Determination of Residual Copper Content of Wastewater. The copper content was determined by flame atomic absorption spectrometry (AAS) with the instrument parameters shown in Table 2.

2.3.2. Coprecipitation Method for Removal of Copper from Wastewater. A standard procedure was used for the preparation of copper-based supramolecular materials. Firstly, 0.13 mol/L $\text{Al}(\text{NO}_3)_3$ and 0.40 mol/L $\text{Mg}(\text{NO}_3)_2$ were prepared in a 100 mL beaker. Afterwards, 15 mL electroplating wastewater and 30 mL deionized water were added. The mixture was transferred to a constant-voltage funnel and slowly dripped into an aqueous solution of Na_2CO_3 (0.25 mol/L, 90 mL) under constant stirring. NaOH (0.1 mol/L) was then added to adjust the pH to 10. The resulting mixture was stirred

TABLE 1: Main element content of electroplating wastewater.

Element	Na	K	Ca	Mg	Al	Fe	Cr	Zn	Cu	Ni	Cd
Content (g/L)	0.36	0.36	0.25	0.05	0.86	0.23	0.06	8.4	8.8	11.3	29.9

for 30 minutes and left to aging for 1 d at 60°C. The copper content in the supernatant was determined by AAS. Finally, the mixture was filtered and the precipitate was washed with distilled water, dried, and roasted for 3 h at 400°C in a muffle furnace.

2.3.3. Adsorption Determination

UV-Spectrophotometric Determination of Iodide. 1 mL solution was sampled and placed in a 50.00 mL volumetric flask, to which deionized water (10 mL) and bromine water (2 drops) were added, followed by shaking and standing for 5 min. Formic acid (1.0 mL) was then added and the mixture was shaken until it was colorless. Phosphate (2.0 mL) was then added and the mixture was shaken again. Finally, an aqueous solution of KI (1 mL) was added, and then the mixture was diluted and shaken. When the reaction was allowed to proceed for 30 min, the absorbance was determined at 350 nm.

3. Results and Discussion

3.1. Comparison of Removal Rates of Copper from Electroplating Wastewater and Optimization of Experimental Conditions. According to the GB21900-2008 standard concerning the emission of pollutants from electroplating, the copper concentration in electroplating wastewater must not exceed 0.5 mg/L. As described in Section 2.3.1, the residual concentration of the copper in the electroplating wastewater was determined in order to evaluate the effects of different experimental conditions.

3.1.1. Effects of Different Metal Ions on Removal of Copper. According to the Jahn-Teller effect, layered double hydroxides (LDHs) from copper alone are not stable owing to the high copper content in electroplating wastewater, and accordingly, there is less precipitation. In order to increase the total amount of precipitation, other metal ions were required. Figure 1 shows the effect of the addition of different metal ions on the residual concentration of Cu^{2+} in the supernatant after coprecipitation. The results show that the addition of Ca^{2+} , Fe^{2+} , Zn^{2+} , or Mg^{2+} - Al^{3+} reduced the concentration of copper ions in the electroplating wastewater. It is clearly observed that the addition of Mg^{2+} - Al^{3+} gives the most effective removal of copper with a residual copper concentration of 0.46 mg/L. Such a lower concentration is in conformity with national emission standards.

The total coprecipitate was characterized by X-ray diffraction (XRD), as shown in Figure 2. The coprecipitates that formed with electroplating wastewater, or electroplating wastewater and Ca^{2+} , Fe^{2+} , Zn^{2+} , and Mg^{2+} , showed no

TABLE 2: Instrument parameters for AAS.

Element	λ/nm	Gas	Slit/nm	Current/mA	Flame
Cu	324.75	Air-C ₂ H ₂	0.2	3.0	Lean combustion

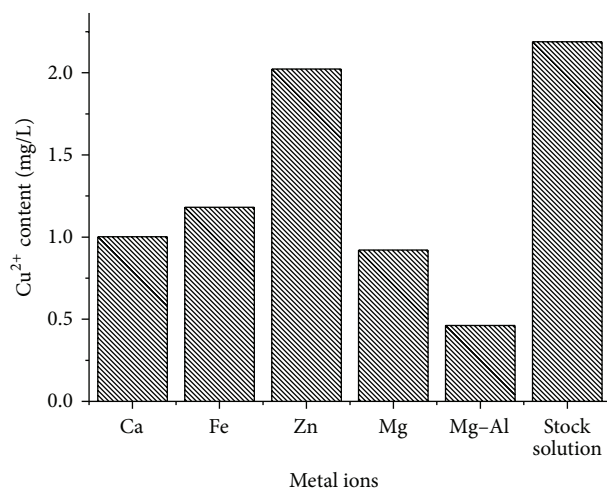


FIGURE 1: Effects of different metal ions on removal of copper.

peculiarities in their XRD peak sand that could be assumed to be ordinary sediments. In contrast, the coprecipitate that formed with electroplating wastewater and Mg²⁺-Al³⁺ showed characteristics representing a typical LDHs stratified structure, with a sharp diffraction peak at low angle 2θ [19]. In addition, the material absorption peak was in line with the 37-0630 map, matching the characteristics of Cu₆Al₂(OH)₂·16CO₃·4H₂O. These results indicated the formation of copper-containing layered metal hydroxides (Cu-Mg-Al LDHs), copper generated cupric hydroxides which constitute the layered structure of supramolecular materials layer board together with magnesium and aluminum. They also show that the addition of Mg²⁺-Al³⁺ provides the best route to copper removal via the formation of supramolecular materials with layered structures.

3.1.2. Effects of Mg²⁺/Al³⁺ Ratio on Removal of Copper. According to the results shown in Figure 3, when the ratio of Mg²⁺ to Al³⁺ was increased to 3 : 1, the residual concentration of the copper in the electroplating wastewater was about 0.2 mg/L, in conformity with national emission standards. When the ratio of Mg²⁺ to Al³⁺ is 3/1, the lowest copper concentration was observed for the fact that most copper is incorporated into the LDH layers with the formation of Cu-Mg-Al LDHs.

3.1.3. Effects of pH on Removal of Copper. It is found that the increasing pH can promote the formation of coprecipitation and hence increasing the removal of copper. As shown in Figure 4, the amount removed reached the highest with increasing pH to 10, beyond which no significant increase was

observed. Therefore, a value of pH 10 is chosen for further study.

3.1.4. Effects of Aging Temperature on Removal of Copper. Two parallel samples (samples 1 and 2) were prepared under the same conditions but with different temperatures (room temperature of 40°C or 60°C). The results in Figure 5 show that, compared with aging at room temperature, aging at 60°C and aging at 40°C led to a greater amount of copper being removed as a result of the more rapid and efficient crystallization of Cu-Mg-Al LDHs at 60°C. Thus, the optimal aging temperature is 60°C.

3.1.5. Effects of Aging Time on Removal of Copper. Again, two parallel samples (samples 1 and 2) were prepared and subjected to aging for different times. The results in Figure 6 show that longer aging leads to better crystallization of the Cu-Mg-Al LDHs. An aging time of 1 d is enough to assure that residual Cu²⁺ concentration in the electroplating wastewater is in accordance with the national emission standards.

3.2. Maximum Handling Capacity of Electroplating Wastewater. Wastewater dosages were selected as 5, 15, 25, 35, 45, or 50 mL. As shown in Figure 7, when more than 30 mL of wastewater was added, the effect of removal of copper was gradually reduced until residual Cu²⁺ in the wastewater was no longer in accordance with national emission standards. This is a consequence of the layer between the Cu-Mg-Al LDHs becoming saturated with water so that no more copper can be incorporated. Thus, the maximum handling capacity of electroplating wastewater is 30 mL.

3.3. Material Performance

3.3.1. Thermal Stability. As shown in Figure 8, the thermogravimetry-differential scanning calorimetry (TG-DTA) graph exhibits three absorption peaks. The first is at 134.4°C, with a weight loss of 9.70%; this represents removal of surface adsorption and interlayer water molecules. The second peak is at 352.8°C, with a weight loss of 15.19%; this probably represents the emergence of interlayer anions. The final peak is 551.7°C, with a weight loss of 10.52%; this represents dehydroxylation of the layers. The DTA curve has a strong endothermic peak at 354.8°C. At this temperature, the low-angle diffraction peak in the XRD pattern of the Cu-Mg-Al LDHs disappears, indicating destruction of the original layered structure.

3.3.2. Structural Stability. As shown in Figure 9, at lower solution pH, there is greater desorption of copper from the copper-based supramolecular material as a result of delamination. However, the amount of copper released into the solution is still in conformity with national emission standards.

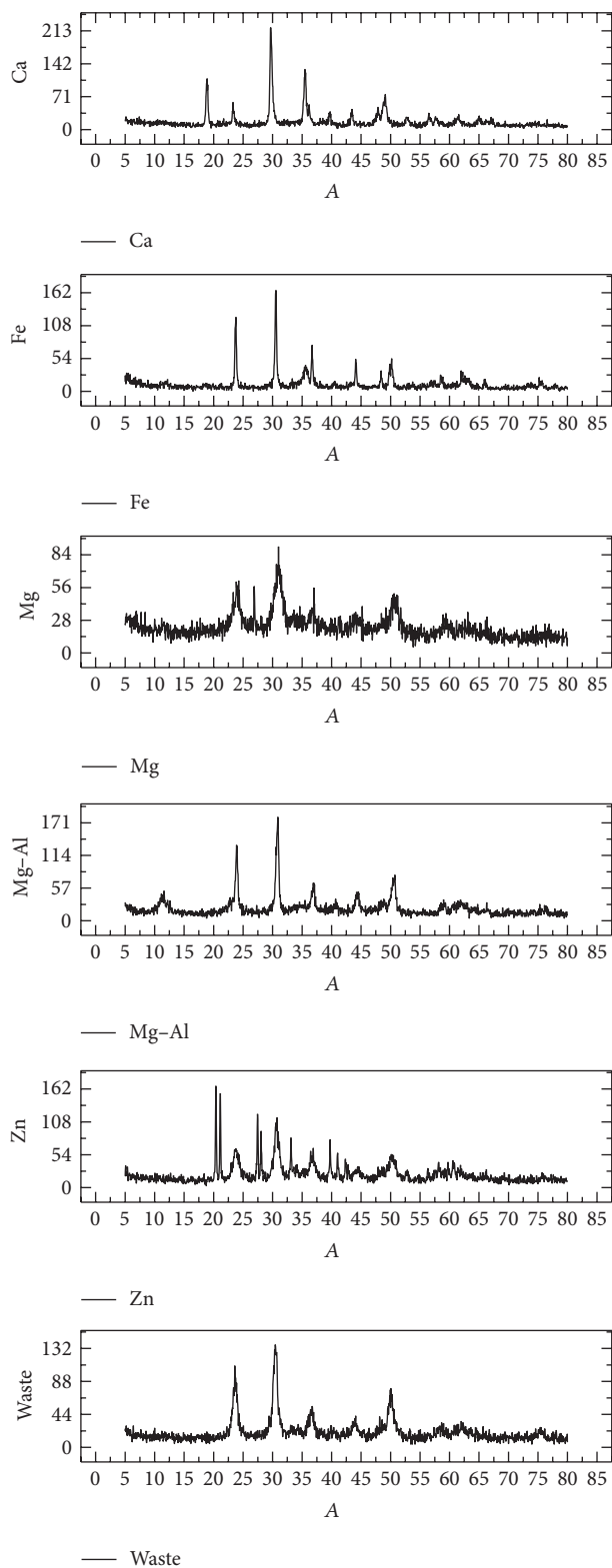


FIGURE 2: XRD patterns of copper-based metal-containing LDH materials.

At a solution pH close to neutral, hardly any copper is released. The result shows that Cu–Mg–Al LDHs exhibit strong structural stability and there is little risk of desorption causing secondary pollution.

3.3.3. Adsorption Capacity to Iodide. For adsorption testing, Cu–Mg–Al LDHs material was dried, roasted for 3 h at 400°C in a muffle furnace, and then ground to powder. Samples of 0.1 g Cu–Mg–Al LDHs were placed in a 50 mL Erlenmeyer

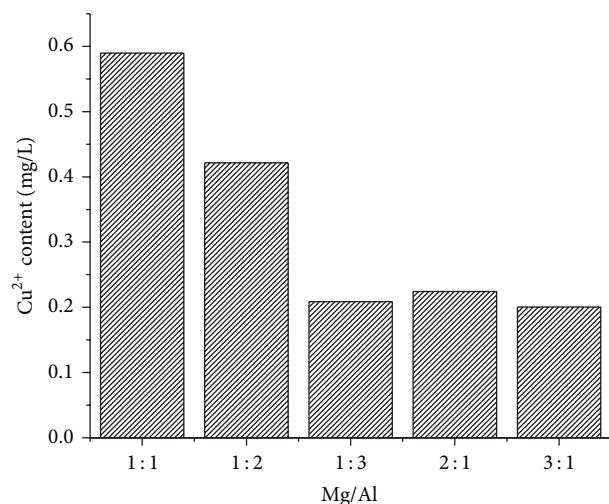


FIGURE 3: Effect of magnesia-alumina molar ratio on removal of copper.

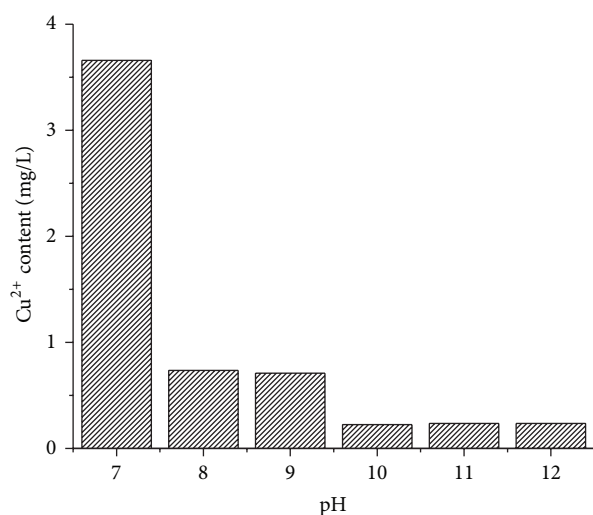


FIGURE 4: Effect of pH on removal of copper.

flask together with 25.00 mL of different concentrations of iodide solution and the mixture was shaken for 1 h at 35°C. The remaining iodide ion concentration in the solution was then determined as described in Section 2.3.3 and the adsorption ratio was calculated. As shown in Figure 10, with increasing I⁻ concentration in the initial solution, the adsorption capacity gradually increases. For an initial I⁻ concentration of 800 mg/L, the adsorption equilibrium was achieved and adsorption capacity was 41.23 mg/g. Cu-Mg-Al LDHs showed good adsorption properties for I⁻, which could be explained by penetration of I⁻ into the layered structure of the Cu-Mg-Al LDHs and also by the occurrence of a specific redox reaction between Cu in the Cu-Mg-Al LDHs and I⁻, producing CuI and indirectly enhancing the adsorption capacity for I⁻.

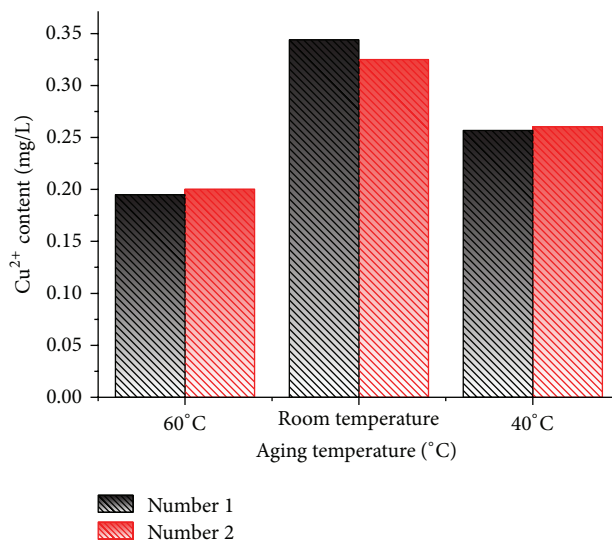


FIGURE 5: Effect of aging temperature on removal of copper.

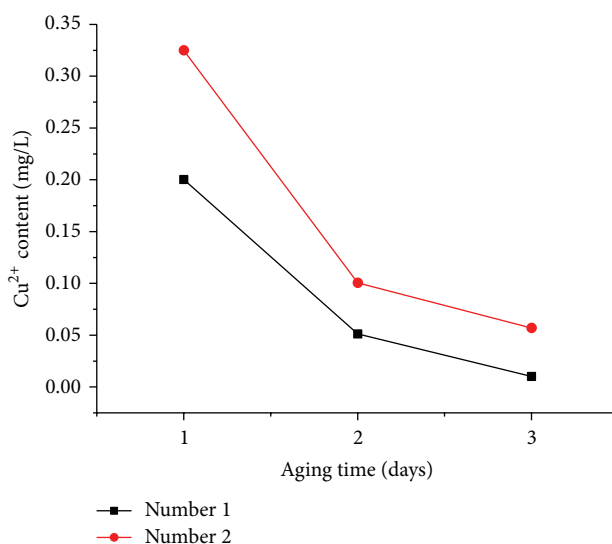


FIGURE 6: Effect of aging time on removal of copper.

4. Conclusion

This study reveals that Mg²⁺-Al³⁺ coprecipitation is effective at reducing the content of copper in electroplating wastewater so that the residual copper is in conformity with national emission standards. The copper is removed as Cu-Mg-Al LDHs formed by reaction between Mg²⁺-Al³⁺ and Cu²⁺. The Cu-Mg-Al LDHs have typical layered structures, good thermal and structural stability, and good adsorption capacity for I⁻. The results of this study are significant for environmental pollution control applications, and further investigations will consider whether the method can be applied to other inorganic metal ions and to the treatment of organic liquid wastes.

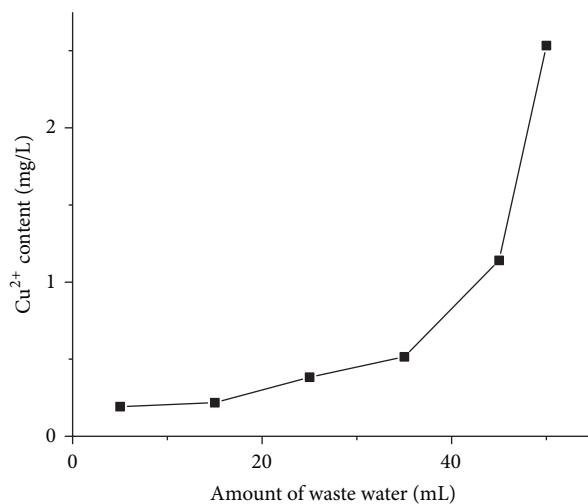
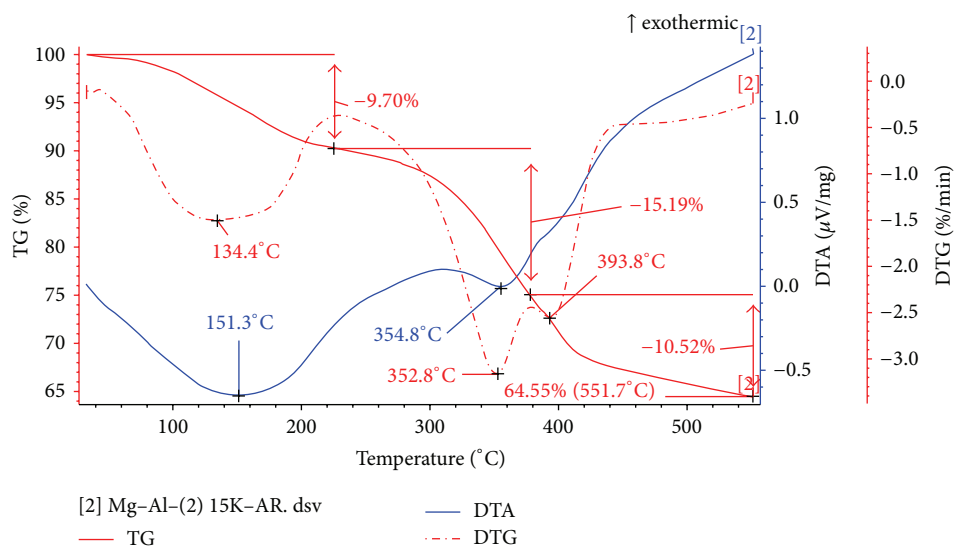


FIGURE 7: Maximum treatment of electroplating wastewater containing copper.



[2] Mg-Al-(2) 15K-AR. dsv

— TG

— DTA

- - - DTG

FIGURE 8: TG-DTA curve of copper-based supramolecular materials.

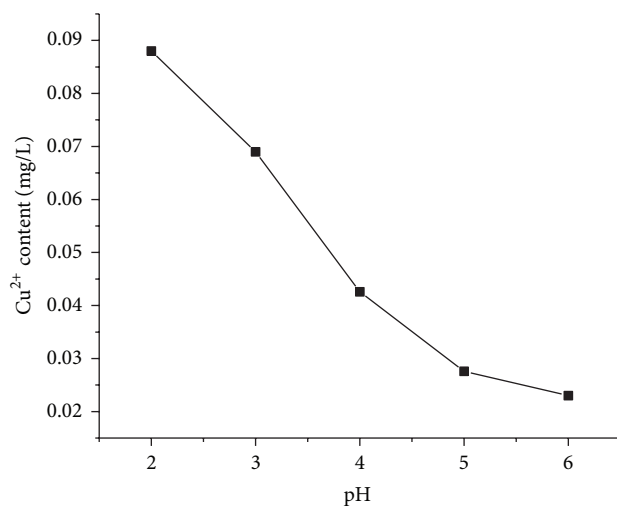


FIGURE 9: Desorption curve of copper in copper-based supramolecular materials.

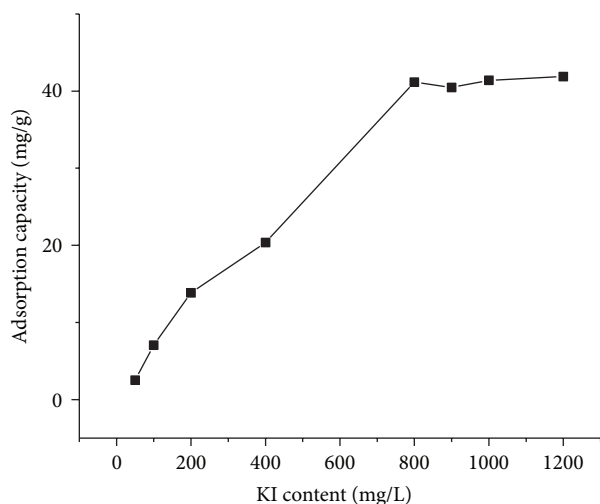


FIGURE 10: Iodide adsorption capacity of Cu-Mg-Al LDH material as a function of initial iodide content.

Conflict of Interests

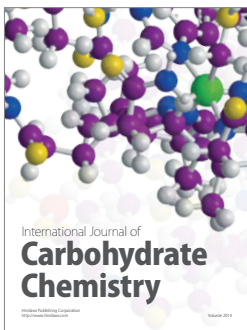
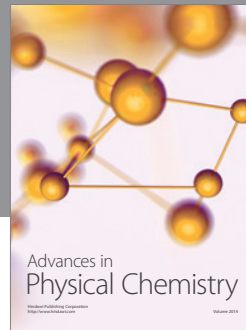
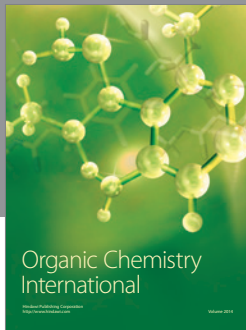
The authors declare that there is no conflict of interests regarding the publication of this paper.

Acknowledgment

This work was financially supported by the Science and Technology Department of Sichuan Province (no. 2015GZ0243).

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