Research Article

Preparation of Sulfur-Free Exfoliated Graphite by a Two-Step Intercalation Process and Its Application for Adsorption of Oils

Jun He, Laizhou Song, Hongxia Yang, Xiaohui Ren, and Lifei Xing

School of Environmental and Chemical Engineering, Yanshan University, Qinhuangdao 066004, China

Correspondence should be addressed to Laizhou Song; songlz@ysu.edu.cn

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The sulfur-free exfoliated graphite (EG) was prepared by a two-step chemical oxidation process, using natural flake graphite (NFG) as the precursor. The first chemical intercalation process was carried out at a temperature of 30°C for 50 min, with the optimum addition of NFG, potassium permanganate, and perchloric acid in a weight ratio of 1:0.4:10.56. Then, in the secondary intercalation step, dipotassium phosphate was employed as the intercalating agent to further increase the exfoliated volume (EV) of EG. NFG, graphite intercalation compound (GIC), and EG were characterized by scanning electron microscope (SEM), energy dispersive spectrometer (EDS), X-ray diffractometer (XRD), Fourier transform infrared spectrometer (FTIR), BET surface area, and porosity analyzer. Also, the uptakes of crude oil, diesel oil, and gasoline by EG were determined. Results show that perchloric acid and hydrogen phosphate are validated to enter into the interlayer of graphite flake. The obtained EG possesses a large exfoliated volume (EV) and has an excellent affinity to oils; thus, the material has rapid adsorption rates and high adsorption capacities for crude oil, diesel oil, and gasoline.

1. Introduction

Although the petroleum consumption has resulted in a great deal of damage to natural environment [1], it is still extensively employed as one of the major fossil fuels. The increasing need of petroleum promotes the transport of this fossil; consequently, oil spill accidents have occurred and posed a serious threat to organisms and human beings [2]. Thus, for the purpose of alleviating the pollution for ocean, rivers, and lakes in the emergency accident caused by oil spill, it is urgent to dispose oil pollutants using the high efficient technology. Generally, the adsorption technique can be exactly competent for the disposal of spilled oils, so suction felt, suction linoleum, foam materials, and some porous polymers have always been employed as the adsorbents. Unfortunately, these adsorbents have an undesirable affinity to oils, thereby weakening the absorption efficiencies of them [3, 4]. In order to alleviate the pollution caused by spilled oils, the exploitation of novel adsorbents with a high affinity to oil is very imperative. Compared with the above-mentioned adsorbents, exfoliated graphite (EG) has received tremendous attention in dealing with marine oil pollution due to its large adsorption capacity of oil and the noticeable disposal efficiency [5–8].

EG as a sort of versatile material is applied in various fields such as packing [9], sealing material [10], fire retardant [11], oil absorbing material [8], and electrode [12], due to its peculiar properties of flexibility, lubricity, and adsorption. There are three techniques applied to prepare the precursor of EG, namely, graphite intercalation compound (GIC)—gas phase intercalation, chemical oxidation, and electrochemical intercalation [13]. Among these three techniques, chemical oxidation [14] and electrochemical intercalation methods [15] are commonly used. Compared with electrochemical intercalation method, chemical oxidation method owns the merits of more convenience, lower cost, and higher stability of the products. EG with an exfoliated volume (EV) of 200–300 mL/g can be obtained via the conventionally chemical oxidation process using concentrated sulfuric acid and concentrated nitric acid as the oxidants and intercalating reagents [16, 17]. However, this process always releases sulfur dioxide and nitrogen oxide into the air. In this regard, the
fabrication process of EG with the friendly environmental characteristics should be developed [18, 19].

The aim of this research is to develop a fabrication process of EG without using concentrated sulfuric acid and nitric acid as oxidants and intercalating reagents and then evaluate its adsorption efficiency of oils. In this study, a two-step chemical oxidation process was proposed; herein, reagents of perchloric acid (HClO₄) and dipotassium phosphate (KH₂PO₄) were employed as intercalating agents in the first and second steps, respectively. Structures, crystallinities, components, and chemical groups of natural flake graphite (NFG), GIC, and EG were characterized by scanning electron microscopy (SEM), X-ray diffraction (XRD), energy dispersive X-ray analysis (EDS), and Fourier transform infrared spectroscopy (FTIR) techniques. Influences of intercalation temperature, reaction time, and additions of potassium permanganate (KMnO₄) and HClO₄ on EV of EG were analyzed. Also, the uptakes of crude oil, diesel oil, and gasoline by EG were determined.

2. Materials and Methods

2.1. Materials. The NFG with an average size of 500 μm was purchased from Qingdao Tianheda Graphite Co., Ltd. (Shandong, China), and the weight content of carbon is 99.5 wt.%. Analytical reagents of HClO₄ (70–72 wt.%) and KMnO₄ (99.5 wt.%), and KH₂PO₄ (99 wt.%) were provided by Jingchun Scientific Co., Ltd. (Shanghai, China); crude oil, diesel oil, and gasoline were obtained from China National Petroleum Corporation.

2.2. Preparations of GIC and EG. GIC was prepared by a chemical oxidation process as follows. Under the continuous stirring condition, 3 g of NFG and the amount of KMnO₄ (0.3–2.1 g) were added slowly into a glass beaker, where the amount of HClO₄ (9–27 mL) was previously added in this beaker. The addition of KMnO₄ should be controlled discretely to prevent the temperature of the mixture exceeding 80°C. After the one-step intercalation reaction, 50 mL of saturated KH₂PO₄ solution was added to the mixture, and the oxidation process continued for 1 h at a temperature of 40°C. Then, the mixed solution was filtered and the collected GIC was cleaned with distilled water until the pH value of the washing effluent was neutral. Lastly, the cleaned GIC was dewatered by a suction filtration process followed by drying in an oven at 65°C for 24 h.

The preparation process of EG was as follows: 1 g of GIC was first added to a crucible, and then the crucible was placed into a muffle furnace and heated with a temperature of 950°C for 15 s. During the heating treatment, the laminar structure of GIC sample was exfoliated, and EG sample was finally obtained.

2.3. Characterization. The morphologies of NFG, GIC, and EG were characterized by a Hitachi S–4800 scanning electron microscope (SEM, Hitachi, Japan); the chemical components of GIC and EG were determined by an energy dispersive spectrometer (EDS) equipped into the above-mentioned microscope. The crystalline structures of NFG, GIC, and EG were measured using a Rigaku D/max 2500 PC X-ray diffractometer (XRD, Rigaku, Japan) with Cu Kα radiation (λ = 1.5418 Å) at 40 kV and 30 mA. The X-ray diffraction patterns were recorded in the range of 2θ = 10–90°. After being blended with KBr, a Nicolet IS10 Fourier transform infrared (FTIR) spectrometer (Nicolet, America) was employed to detect chemical groups of the obtained GIC and EG samples; FTIR data were recorded in the range of 4000–500 cm⁻¹. BET surface area, pore volume, and average pore diameter of the fabricated EG were measured by mercury intrusion porosimetry using an Autopore IV 9500 analyzer (Micromeritics, USA).

The exfoliated volume (EV) was determined by exfoliating 1.0 g of GIC in a temperature of 950°C for 15 s and its volume was measured using a graduated cylinder. Then the volume was recorded, and this datum was considered to be EV value. In order to ensure the accuracy, measurements were carried out in triplicate, and the average value was adopted.

2.4. Adsorption Rate and Capacity of EG for Oils. Crude oil, diesel oil, and gasoline as the oil candidates were selected as the target pollutants to measure the adsorption rate and capacity of EG. Three portions of EG samples with the same weight were placed in different beakers; then the excessive target oil was added and the solution was stirred at a temperature of 25°C. The mixture of EG and oil was separated by 35-numbered mesh net. After the different adsorption time, the collected EG sample was statically placed to make the excessive oil completely dropping down. The adsorption time was set at 1, 2, 4, 5, 6, 8, 10, 20, and 30 min. The adsorption capacity in different time was obtained from the weight increase before and after adsorption. The adsorption capacity of oil at certain time was calculated via

\[ Q = \frac{M - m}{m}, \]  

where Q is the adsorption capacity of EG at certain time (g/g); M and m (g) are the weights of EG before and after the oil adsorption. In order to ensure the accuracy, measurements were carried out in triplicate, and the average value was adopted.

The regeneration ratio of EG (the ratio between the readesorbed oil amount and the initial adsorbed value) was assessed with 1 g addition of EG. EG and oil were separated through air pump filtration process; then the regenerated EG was used for oil adsorption; this process was repeated three times. The regeneration ratio is calculated by

\[ \text{regeneration ratio (n)} \times 100\% = \frac{Q_{n+1}}{Q_{n}}, \]  

where n is the times of cyclic regeneration.

3. Results and Discussion

3.1. Influence of Intercalation Temperature. The effect of intercalation temperature on EV was presented in Figure 1. As shown in Figure 1, EV of EG increases with the enhancement
in intercalation temperature, and then it reduces when the temperature was higher than 30°C. Thus, the temperature of 30°C can be identified as the optimum intercalation temperature. As the reaction time was 60 min and the mass ratio of NFG, KMnO₄, and HClO₄ was 1 : 0.4 : 10.56, the value of EV reaches the maximum value (420 mL/g).

It is well known that the preparation of GIC via the chemical oxidation technique is an exothermic process, so the low temperature can be favorable to the intercalating reaction. But a high reaction temperature (no more than 30°C) might be needed at the beginning, which will be valuable for the intercalating reagent entering into the laminar spacing of NFG. However, the intercalating temperature higher than 30°C will accelerate the volatilization of HClO₄. As a result, the amount of this agent entering the graphite interlayer reduces, thus resulting in a low EV.

3.2. Influence of Reaction Time. When the intercalating temperature and the mass ratio of NFG, KMnO₄, and HClO₄ were kept at 30°C and 1 : 0.4 : 10.56, respectively, the effect of reaction time on EV was analyzed and the results are shown in Figure 2. The value of EV increases from 310 to 420 mL/g as the reaction time elapsed from 10 to 50 min, and then it slightly decreases as time extends. When the reaction time was less than 50 min, the intercalating reaction cannot complete and the extended time will be helpful in destroying the edge layer of graphite by the oxidant. Thus, the prolonged time will guarantee more intercalating reagents entering into the laminar layer of graphite, which is beneficial to the achievement of high EV. This oxidation process is almost finished as the intercalating time is 50 min; then EV will decrease when the time was further prolonged because intercalating reagents will run away as time goes on. Therefore, the optimum reaction time of 50 min was ascertained for the preparation of EG.

3.3. Influence of KMnO₄ Addition. EV of EG increases significantly with the increase in KMnO₄ addition (from 0.1 to 0.4 g/g NFG) (Figure 3); then the EV change can be ignored as the addition of KMnO₄ ranges from 0.5 to 0.7 g/g NFG. The maximum EV with a value of 420 mL/g can be obtained with KMnO₄ addition of 0.4 g/g NFG. During the intercalating reaction, the concentration of KMnO₄ in HClO₄ could hardly maintain saturated when its addition is below 0.4; as a consequence, NFG cannot be oxidized sufficiently, and the value of EV will be low. However, the excessive dosage of KMnO₄ (>0.4 g/g NFG) will erode the edge layers of NFG and destroy its lamellar structure. The intercalating agents will not be readily inserted into interlayer spacing, thereby resulting in the decrease in EV (<420 mL/g). The optical addition in weight ratio of NFG and KMnO₄ is validated as 1 : 0.4.

3.4. Influence of HClO₄ Addition. The influence of HClO₄ concentration on EV was also investigated and the result is depicted in Figure 4. Firstly, EV considerably increases with the enhancement in addition of HClO₄ (5.28~10.56 g/g NFG); but when the dosage exceeded 10.56 g/g NFG, EV decreases slightly and stays at a stable value of 390 mL/g. At a low addition of HClO₄, despite the help of KMnO₄ to destroy
the lamellar structure of NFG, the amount of HClO\textsubscript{4} was not enough to guarantee that the interlayer spacing of graphite is filled as most possible. On the contrary, at the higher addition of HClO\textsubscript{4} (>10.56 g/g NFG), the excessive acid will dilute the concentration of KMnO\textsubscript{4}, thereby weakening the oxidation potential of this oxidant; this is unfavorable for the enhancement in EV. The optimal weight ratio between NFG oxidation potential of this oxidant; this is unfavorable for the enhancement in EV. The optimal weight ratio between NFG and KMnO\textsubscript{4} is 1:0.4:10.56; with these additions of the above two reagents, the measured EV value is 420 mL/g.

In summary, the optimal conditions for the preparation of EG with EV value of 420 mL/g are as follows: mass ratio of NFG : KMnO\textsubscript{4} : HClO\textsubscript{4} is 1:10.56; with these additions of the above two reagents, the measured EV value is 420 mL/g.

The tested XRD patterns of NFG, GIC, and EG are shown in Figure 7. The peak appearing at 2\(\theta\) = 26.42\(^\circ\) (Figure 7(a)) with a d-spacing of 3.37 Å for NFG is observed. For the sample of GIC, this peak with a d-spacing of 3.50 Å shifts to 25.40\(^\circ\) (Figure 7(b)). This can be due to the fact that KMnO\textsubscript{4} can easily oxidize the graphite layers, and the repulsion interactions between the layers increase, thereby resulting in the increase in the interlayer spacing. As a result, HClO\textsubscript{4} migrates into the graphite layers and expands the lamellar spacing along the c-axis direction, which leads to the peak intensity of GIC lower than that of NFG. The similarity of these two peaks mentioned above evidences the insufficient oxidation reaction. As for the XRD pattern of GIC, another peak at 2\(\theta\) = 30.02\(^\circ\) (Figure 7(b)) can be observed, suggesting that NFG is successfully intercalated by HClO\textsubscript{4}. Also, for the XRD pattern of GIC, it is easy to find that the reflection peak at 2\(\theta\) = 54.56\(^\circ\) is divided into two peaks (2\(\theta\) = 51.88\(^\circ\) and 56.94\(^\circ\)). This change can also be attributed to the oxidation reaction. Two diffraction peaks (2\(\theta\) = 26.44\(^\circ\) and 54.54\(^\circ\)) for EG are observed in Figure 7(c). It is worth noting that the two peaks are the same as those of NFG, but the peaks of NFG are more obvious than those of EG.

3.5. Characterization

3.5.1. SEM Analysis. Morphologies of NFG, GIC, and EG under the previously described conditions were characterized, and SEM micrographs of them are presented in Figure 5. It is clear that the interlayer spacing of NFG is compact and much smaller than that of GIC (Figure 5(a)). The change in interlayer spacing between these two samples can be due to the intercalation and exfoliation of NFG. After the oxidation treatment, the interlayer spacing of NFG is enlarged and its boundary layers are crimped (Figure 5(b)). The worm-like porous structure can be seen from the surface morphology of EG (Figures 5(c)–5(f)), and the pore size ranges from several microns to hundreds of microns. The slit-shaped gaps between the graphite platelets can also be identified; this can be due to the fact that the compounds in interlayers of GIC were decomposed and some micropores are formed during the exfoliation process. The presence of the micropores will be of benefit for guaranteeing an excellent adsorption property of the prepared EG.

3.5.2. EDS Analysis. The chemical components of GIC and EG were determined, and measured EDS spectra are displayed in Figure 6. The chloride (Cl) and phosphorus (P) elements can be identified on the surfaces of tested samples. For both GIC and EG, the determined elements (atomic weight) are shown in Table 1. Atomic weights of Cl and P in GIC are 8.03\% and 0.95\%, respectively. The existence of Cl and P may derive from the additions of HClO\textsubscript{4} and KH\textsubscript{2}PO\textsubscript{4}. Thus, it can be deduced that both HClO\textsubscript{4} and KH\textsubscript{2}PO\textsubscript{4} were inserted into the interlayer of NFG; this process is a prerequisite for the preparation of EG. But the content of Cl in EG decreases to 0.05\% and P cannot be detected. After the exfoliation treatment at 950\(^\circ\)C, the inserted agents were decomposed and the worm-like EG was obtained.

3.5.3. XRD Analysis. The tested XRD patterns of NFG, GIC, and EG are shown in Figure 7. The peak appearing at 2\(\theta\) = 26.42\(^\circ\) (Figure 7(a)) with a d-spacing of 3.37 Å for NFG is observed. For the sample of GIC, this peak with a d-spacing of 3.50 Å shifts to 25.40\(^\circ\) (Figure 7(b)). This can be due to the fact that KMnO\textsubscript{4} can easily oxidize the graphite layers, and the repulsion interactions between the layers increase, thereby resulting in the increase in the interlayer spacing. As a result, HClO\textsubscript{4} migrates into the graphite layers and expands the lamellar spacing along the c-axis direction, which leads to the peak intensity of GIC lower than that of NFG. The similarity of these two peaks mentioned above evidences the insufficient oxidation reaction. As for the XRD pattern of GIC, another peak at 2\(\theta\) = 30.02\(^\circ\) (Figure 7(b)) can be observed, suggesting that NFG is successfully intercalated by HClO\textsubscript{4}. Also, for the XRD pattern of GIC, it is easy to find that the reflection peak at 2\(\theta\) = 54.56\(^\circ\) is divided into two peaks (2\(\theta\) = 51.88\(^\circ\) and 56.94\(^\circ\)). This change can also be attributed to the oxidation reaction. Two diffraction peaks (2\(\theta\) = 26.44\(^\circ\) and 54.54\(^\circ\)) for EG are observed in Figure 7(c). It is worth noting that the two peaks are the same as those of NFG, but the peaks of NFG are more obvious than those of EG.

3.5.4. Analysis of FTIR Spectra. The determined FTIR spectra of GIC and EG are shown in Figure 8. The peaks at 3450
Table 2: BET results of EG.

<table>
<thead>
<tr>
<th>Sample</th>
<th>BET surface area (m²/g)</th>
<th>Total pore volume (mL/g)</th>
<th>Average pore diameter (µm)</th>
</tr>
</thead>
<tbody>
<tr>
<td>NFG</td>
<td>0.7</td>
<td>—</td>
<td>—</td>
</tr>
<tr>
<td>GIC</td>
<td>0.8</td>
<td>—</td>
<td>—</td>
</tr>
<tr>
<td>EG</td>
<td>245</td>
<td>37.5</td>
<td>22.1</td>
</tr>
</tbody>
</table>

Figure 5: SEM images of (a) sectional morphology of natural flake graphite, (b) sectional morphology of GIC, and (c–f) surface morphology of EG: the magnification of each image is listed as follows: (a) ×5000, (b) ×500, (c) ×100, (d) ×500, (e) ×2000, and (f) ×10000.

3.5.5. Analysis of BET and Pore Structure. The surface area of NFG and GIC is low because they are bulk materials with an average size of 500 µm and less of porosity. BET surface area, pore volume, and pore diameter for EG sample were measured, and results are summarized in Table 2. The results show the feature of EG sample, that is, high surface area and micron pore structure. The surface area of the prepared EG was calculated to be 245 m²/g, which is much higher than that of exfoliated graphite synthesized by microwave irradiation [8]. It is
worth mentioning that the micrometer level of average pore diameter of EG will be advantageous to significantly enhance the adsorption performance toward oils [25, 26].

3.6. Adsorption Capacity and Adsorption Rate of EG for Crude Oil, Diesel Oil, and Gasoline. Figure 9 displays dynamic adsorption behaviors of EG for crude oil, diesel oil, and gasoline. The maximum adsorption capacities are 123.3 g/g for crude oil, 76.5 g/g for diesel oil, and 61.4 g/g for gasoline. The adsorption rate is another important factor during adsorption process. The time to reach the equilibrium sorption capacity for each oil is 5, 2, and 2 min, respectively, reflecting rapid adsorption rates for these oils. These results indicate that the as-prepared EG will be competent for the application in oil spill accidents. Herein, the adsorption characteristics of EG toward the oil will be comprehensively investigated in the further research.

3.7. Cyclic Regeneration of EG. Table 3 exhibits cyclic regeneration abilities of EG after adsorbing the aforesaid three oils. The adsorption capacity of EG for each oil decreases slightly after regeneration, confirming that EG can be repeatedly applied as an effective adsorbent after the separation process by air pump filtration.

3.8. Mechanism of Adsorption. In the process of GIC sample preparation, HClO₄ is used as both an intercalation agent and oxidizing agent. The strong acidity, volatility, and oxidability of HClO₄ can lead to a high-temperature expansion and the formation of microns pores for EG sample, guaranteeing its
Table 3: Cyclic regeneration of EG for the three kinds of oils.

<table>
<thead>
<tr>
<th>Categories of oils</th>
<th>Adsorption capacity number 1/g</th>
<th>Adsorption capacity number 2/g</th>
<th>Adsorption capacity number 3/g</th>
<th>Regeneration ratio (1)/%</th>
<th>Regeneration ratio (2)/%</th>
<th>Average regeneration ratio/%</th>
</tr>
</thead>
<tbody>
<tr>
<td>Crude oil</td>
<td>45.6</td>
<td>40.3</td>
<td>34.5</td>
<td>88.38</td>
<td>85.61</td>
<td>86.99</td>
</tr>
<tr>
<td>Diesel oil</td>
<td>27.8</td>
<td>23.6</td>
<td>19.4</td>
<td>84.89</td>
<td>82.20</td>
<td>83.29</td>
</tr>
<tr>
<td>Gasoline</td>
<td>23.5</td>
<td>19.8</td>
<td>15.6</td>
<td>84.25</td>
<td>78.79</td>
<td>81.52</td>
</tr>
</tbody>
</table>

![Dynamic adsorption curves of EG for crude oil, diesel oil, and gasoline.](image)

Excellent adsorption properties toward oils. In addition, high BET surface area and large pore volume of EG will also ensure rapid adsorption rates and high adsorption capacities.

4. Conclusions

In this study, a facile two-step intercalation method is proposed to prepare the sulfur-free EG, using HClO₄ and KH₂PO₄ as the inserting agent and KMnO₄ employed as the oxidant. The oxidant can easily open the graphite layers and the inserting agent will move into the interlayer spacing to obtain the GIC sample. The optimum conditions for the preparation of GIC are as follows: the mass ratio of NFG, KMnO₄, and HClO₄ is 1:0.4:10.56; the reaction temperature and time are kept at 30°C and 50 min. EV of the prepared EG is 420 mL/g. The worm-like porous morphology, high BET surface area, and large pore volume of EG guarantee the excellent adsorption property toward oils. The maximum adsorption capacities of EG for crude oil, diesel oil, and gasoline are 123.3, 76.5, and 61.4 g/g, respectively.

Conflicts of Interest

The authors declare that there are no conflicts of interest regarding the publication of this paper.

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