Research Article

Fluorometer Controlled Apparatus Designed for Long-Duration Algal-Feeding Experiments and Environmental Effect Studies with Mussels

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Experimental feeding and growth studies on filter-feeding organisms often rely on constant algal concentrations maintained over extended periods of time. Here we present a fluorometer controlled apparatus (FCA) designed for feeding experiments with suspension-feeding mussels at naturally low chlorophyll \( a \) concentrations above 0.5 \( \mu g L^{-1} \). The principle used is feedback regulation of the algal concentration based on continuous monitoring of the fluorescence intensity of chlorophyll \( a \) in water pumped through the apparatus from an aquarium with mussels. The filtration rate is monitored continuously as the rate of change of measured volume of an algal stock added to the aquarium for keeping a constant algal concentration. As an example, the FCA has been used to study the filtration rates of blue mussels (\( Mytilus edulis \)) at algal concentrations both near and above the incipient saturation level for reduced filtration activity. As another example to put the FCA into perspective as a reliable method for environmental effect studies, the apparatus has been used to demonstrate the acute effect of changing salinity on the filtration rate of \( M. edulis \).

1. Introduction

Bioenergetic and feeding-behavioural studies on filter-feeding organisms may often rely on supply of feed algae maintained at constant concentrations over extended periods of time. In the case of the blue mussel (\( Mytilus edulis \)) algal concentrations below a lower critical level [1–5] and above an upper critical saturation concentration (about 6 \( \mu g \) chlorophyll \( a \) (chl \( a \) L\(^{-1} \); see minireview by Riisgård et al. [6]) lead to partial shell closure and reduced filtration rate.

The feeding behaviour of \( Mytilus edulis \) was studied by Riisgård et al. [6] using the so-called steady-state method (e.g., [7]) at different well-defined but relatively high algal concentrations eventually leading to reduced filtration rate. Thus, the upper algal concentration at which the mussel exploits its filtration capacity over an extended period of time was identified by stepwise raising the steady-state algal concentration, and the threshold concentration for incipient "saturation reduction" of the filtration rate was found to be between 5,000 and 8,000 (\( Rhodomonas salina \)) cells mL\(^{-1} \), equivalent to 6.3 and 10.0 \( \mu g \) chl \( a \) L\(^{-1} \), respectively [6]. However, the steady-state method can only be used to ensure a constant algal concentration between the lower and upper critical algal concentration where the filtration rate is constant [7]. Therefore, a more sophisticated feedback-controlled apparatus is needed for maintaining a well-defined algal concentration in feeding and growth experiments with mussels at algal concentrations above the threshold concentration for incipient saturation reduction where filtration rate is not constant. Likewise, such an apparatus may have advantages in, for example, studies where changing environmental conditions, such as varying salinity of the ambient water, cause reduced valve-opening degree and thus reduced filtration rate.

The steady-state method has restricted previous long-term feeding and growth experiments with mussels to be conducted at algal concentrations below the saturation concentration [6, 8–11]. Other mussel studies, however, have been restricted to very high algal concentrations (e.g., [12–15]), presumably due to limited sensitivity of the feedback control systems. Most of the described control systems are based on measurements of turbidity, and low sensitivity of photoelectric cells seems to have been the major drawback.
in continuous automatic-recording apparatus [12, 13, 15–17]. The sensitivity of the detector was improved by Hornbach et al. [18], who used a fiber-optic colorimeter with possible adjustment of the light pathway according to the particle concentration for clearance rate measurements, or even more sophisticated by Breteler and Lann [19], who used an electronic particle counter as sensing unit. Furthermore, fluorescence where the emission of light of specific algal pigments after excitation is detected was used by Gallager and Mann [20] for measurements of grazing activity of mollusk larvae. More recently, Rico-Villa et al. [21] presented a flow-through rearing system for oyster larvae using a fluorescence sensor for monitoring the ingestion rate of the larvae.

Here, we present a new fluorometer controlled apparatus (FCA) designed not only for running long-duration feeding experiments with mussels fed algal cells at naturally occurring chl a concentrations but also for studying how varying salinity (and other environmental factors) may affect the filtration rate of mussels. The principle used is feedback regulation of the algal concentration, based on continuous monitoring of the fluorescence intensity of chl a in water samples pumped through the apparatus from the experimental aquarium with mussels. The filtration rate is monitored continuously by measurement of the volume of an algal stock added to the aquarium for keeping the algal concentration constant. As an important example of the applicability we have used the FCA for a detailed investigation of the feeding rate of Mytilus edulis at algal concentrations near and above the upper incipient saturation level. Another example dealing with the acute effect of changing salinity on the filtration rate of M. edulis puts the FCA into perspective as a reliable method for environmental effect studies.

2. Materials and Methods

2.1. Description of Fluorometer Controlled Apparatus (FCA). The apparatus maintains a defined concentration in an aquarium with filter-feeding mussels and a constant through-flow by adding concentrated algal suspension to replace the amount of algal cells removed (Figure 1). The volume of algal suspension added to the aquarium is determined by the filtration activity of mussels and by the wash-out of algal cells with the through-flow caused by a constant input of particle-free seawater which ensures a good water quality. Water from the aquarium with mussels is continuously recycled through a silicon tube to the fluorometer (10-AU Fluorometer, Turner Design) containing a flow-through cuvette which enables a continuous measurement of the algal concentration (Figure 1(a)). The specific wavelengths for excitation (430 nm) and emission (680 nm) are chosen for the characteristic pigment (chl a) of the algal strain (Rhodomonas salina) used as feed. The analog output of the fluorometer is connected via an A/D converter to a computer (Figure 1(b)). A program written in Microsoft C#.net creates a pulse with modulation (1 pulse every 6 s and a duty cycle from 0 to 100% in step of 0.1 s) of the digital output Port B0 on the PMD-1208 as a function of the measured algal concentration in the tank. Port B0 is connected to a driver circuit to switch a standard USB mains relay (Figure 1(b)). Correlation between fluorescence intensity and algal concentration is given by a calibration row. If the algal concentration is below a defined level the mains relay starts a peristaltic pump that pumps a suspension of concentrated algae from the stock into the aquarium to keep the algal concentration constant. Measured and average data are displayed in a TextBox every sec. Average of the data is recorded in a ListBox with an arbitrary TimeStamp. The data are recorded as a text file.

2.2. Filtration Rate of Mussels. When using the clearance method, to cross-check the filtration rates estimated from the FCA, the dosing pump of the FCA maintaining a constant algal concentration in the aquarium was stopped and filtration rates were measured as the volume of water that was cleared of suspended particles per unit of time. The reduction in the number of particles as a function of time was followed either by measuring the fluorescence or by taking water samples (10 mL) at fixed time intervals and measuring the particle concentration with an electronic particle counter (Elzone 5380) in the aquarium with mussels and well-mixed seawater to which were added algal cells (Rhodomonas salina, diameter about 6.7 μm). These are 100% efficiently retained by the gills of the mussels (i.e., cell diameter larger than 4 μm [22]) therefore clearance rate equals filtration rate. The clearance rate (F_CR) was determined from the exponential decrease in algal concentration as a function of time using the usual clearance formula (e.g., [23–25]):

\[ F_{CR} = \frac{V_b}{n}, \]  

where \(C_b\) is the terminal and initial concentrations of particles, \(V\) is the water volume in aquarium, and \(n\) is the number of mussels. A control experiment without mussels showed that sedimentation of algal cells was insignificant.

When using the FCA presented here, filtration rates were estimated by means of the following equation [11]:

\[ F = \frac{P \times (C_a - (P + F_l) \times C_a)}{C_a \times n}, \]

where \(P\) is the pumping rate of algal-dosing pump, calculated from the total volume of algal stock suspension (TV) added to the aquarium per unit of time (t), that is, \(P = \frac{\Delta (TV)}{dt}\); \(n\) is the number of mussels, \(C_a\) is the algal concentration in stock suspension, \(C_a\) is the algal concentration in well-mixed aquarium, and \(F_l\) is the flow-through rate of bio-filtered seawater measured as volume of collected out-flow water over a known time period.

2.3. Experimental Mussels. Blue mussels, Mytilus edulis, were collected in Kerteminde Fjord, Denmark, and acclimated for one week in the laboratory at the Marine Biological Research Centre (University of Southern Denmark) prior to the experiments. The mussels were kept in aerated flow-through tanks supplied with seawater from the fjord inlet until they were transferred to the experimental aquarium.
All experiments were performed at 12.0 ± 0.3°C and 21.8 ± 1.2 psu. Dry weight of soft parts (90° C, 24 h) and shell length were determined for a representative group of at least 10 muscles.

3. Results

A number of test experiments were conducted to evaluate the performance of the FCA. The following conversion factor was used: \( 1 \mu g \text{ chl a L}^{-1} = 1/(1.4 \times 10^{-3}) \sim 700 \) (Rhodomonas sp.) cells mL\(^{-1}\) which is in agreement with Clausen and Riisgård [10]. All experiments, with and without mussels were performed in prior bio-filtered (by mussels) seawater to ensure that no non-chl a containing particles could mask the results. The bio-filtered seawater was regularly checked for particles using a particle counter (Elzone 5380). After each experiment mussels were allowed to empty their digestive system overnight.

3.1. Maintaining Constant Algal Concentrations. The FCA was tested for its ability to maintain different algal (Rhodomonas salina) concentration levels in an aquarium diluted by a constant through-flow of biofiltered seawater. After initial addition of algal cells to the aquarium to reach a certain high concentration (around 8,000 cells mL\(^{-1}\)), the dosing pump was stopped and through-flow seawater was allowed to reduce the concentration to lower levels. During the test period, the fluorometer controlled additions of \( R. \text{salina} \) to the aquarium were recorded in order to measure the total volume (TV) of algal stock suspension added. In one case, the constant through-flow of seawater was monitored by means of the fluorometer to follow the exponential decrease in the algal concentration in order to compare the estimated washing-out rate ("clearance rate") with the actual through-flow rate.

From Figure 2 it appears that the FCA precisely maintains different algal concentration levels down to around 400
Rhodomonas salina cells mL$^{-1}$ (equivalent to 0.5 μg chl α L$^{-1}$) over an extended period of time (>12 h) in an experimental aquarium ($V = 15.4$ L) without mussels. Similar fluorescence intensities of a suspension with a known algal concentration measured prior to the experiment and afterwards revealed that no microbrial growth on the glass wall of the photoelectric cell of the fluorometer, interfering with measurements, occurred. Between 6 and 9 h a constant through-flow of bio-filtered seawater (12 L h$^{-1}$) caused an exponential decrease in the algal concentration, and from the exponent (0.75 h$^{-1}$) in the shown equation for the exponential curve fit it can be calculated that the decrease in algal concentration is equivalent to a washing-out rate of (0.75 × 15.4 =) 11.6 L h$^{-1}$ which is close to the actual through-flow rate.

3.2. Determination of Clearance Rate. The ability of the FCA to determine the clearance rate was tested both without and with mussels in the aquarium. First, the exponential decrease in algal concentration in the well-mixed aquarium, caused by the flow-through of seawater diluting the algal concentration, was measured by fluorescence in order to make a semi-ln plot of the decreasing algal concentration in order to estimate the washing-out rate = “clearance rate” ($F_{CR}$) from (1). Next, the decrease in algal concentration in the aquarium caused solely by filtering mussels (i.e., no through-flow of water) was measured using both an electronic particle counter (Elzone 5380) and the fluorometer to lay down the slopes of regression lines expressing the filtration rate of the mussels compare (1).

Figure 3(a) shows two examples of exponential decrease in algal concentration in the experimental aquarium caused solely by flow-through of seawater with rates of 2.1 and 1.2 L h$^{-1}$, respectively. Using (1) and slopes of regression lines in the semi-ln plots, it can be calculated that the washing-out rates (“clearance rate”) were (0.14 × 15.4 =) 2.2 and (0.06 × 15.4 =) 0.9 L h$^{-1}$, respectively, in reasonably good agreement with the actual flow-through rates. Figure 4(b) shows the exponential decrease in algal concentration in the aquarium caused solely by filtering mussels (mean ± S.D. shell length = 28.0 ± 1.3 mm). Using (1) and the slope of the regression lines it is estimated that the filtration rate of mussels exposed to 40,000 cells mL$^{-1}$ was (0.0024 × 15.4 × 60/8 =) 0.3 L h$^{-1}$ ind$^{-1}$, irrespective of the method used for measuring the algal concentration. At 40,000 cells mL$^{-1}$ where appearance of excreted products was seemingly high, no difference between measurement of exponential decrease in algal concentration using the FCA and the electronic particle counter was seen within at least 90 min (Figure 3(b)).

3.3. Test of Design. The FCA method for calculation of filtration rate using the dosing-pump rate ($P$) in (2) was tested for different number of mussels in the experimental aquarium. In Figure 4 it is seen that the TV of an algal stock added to the aquarium to maintain a constant algal concentration of 4,380 cells mL$^{-1}$ progressively responded (Figure 4(a)) from 15, 9, and 3 mussels as the $P$ of algal stock decreases while the measured mean filtration rates of 15, 9, and 3 mussels of 0.61, 0.60, and 0.55 L h$^{-1}$ ind$^{-1}$, respectively, are almost identical (Figure 4(b)). This indicates that the experiment was properly designed and water was sufficiently mixed by the 4 air stones to ensure instantaneous mixing of the exhalant water in the whole water volume of the aquarium which is a prerequisite for using both (1) and (2).

3.4. Filtration Activity of Mussels. The filtration rate of different sized mussels was measured by means of the FCA according to (2) in experiments performed under “optimum conditions” (i.e., fully open mussels). Furthermore, to highlight the applicability of the FCA near saturation levels and above, the saturation-caused reduction of the filtration rate of mussels exposed to different relatively high Rhodomonas salina concentrations (about 6,000, 7,000, 8,000, 9,000, 10,000, 12,000, 20,000, and 36,000 cells mL$^{-1}$) was studied for up to 24 h. Additionally, to study the filtration rate at saturation conditions over a long period an experiment was performed on 4 groups of mussels (Table 1) exposed to different Rhodomonas salina concentrations are shown in Figure 5. Initially, the mussels were exposed to a relatively low algal concentration (about 2,300 cells mL$^{-1}$) to stimulate the mussels to fully open their valves and to exploit their filtration rate capacity which was used as a reference when the algal concentration was subsequently increased to different higher algal concentrations that were maintained during the following about 12 to 24 h. During the initial period with “optimum conditions” (open triangles, Figure 5) the filtration rate ($F$, L h$^{-1}$) of the mussels increased with increasing shell length ($L$, mm) according to $F = 0.0024L^{2.01}$ (Figure 6) and was in good agreement.
Figure 3: Test of fluorometer controlled apparatus (FCA). (a) Two examples of exponential decrease in algal concentration ($C_0 = \text{around 40,000 cells mL}^{-1}$) in experimental aquarium ($V = 15.4 \text{ L}$) caused by flow-through of biofiltrated seawater ($\square$, 2.1 and $\bigcirc$, 1.2 L h$^{-1}$) diluting the algal concentration measured by fluorescence. The slopes of the regression lines in the semi-ln plot express the flow-through rate, compare (1). (b) Exponential decrease in algal concentration in aquarium caused only by filtering mussels (mean ± S.D., shell length = 28.0 ± 1.3 mm). The algal concentration was measured using both an electronic particle counter ($\bullet$) and the FCA ($\square$). The slopes of the regression lines express the filtration rate of the mussels ($n = 8$, $\square$ and $\bullet = 0.3 \text{ L h}^{-1}$), compare (1).

Figure 4: Test of fluorometer controlled apparatus (FCA). Measurement of filtration rate with a varying number of mussels placed in the experimental aquarium. (a) Total volume of algal suspension added ($TV, \bullet$) when an algal stock suspension ($0.72 \times 10^6$ cells mL$^{-1}$) is used for keeping the algal concentration in the aquarium constant ($4,380 \pm 590$ cells mL$^{-1}$). Initially, 15 mussels (mean ± S.D., shell length = 21.1 ± 1.5 mm) were used; later after 1.5 h the number of mussels was reduced to 9, and further after 3 h to 3 mussels. (b) Calculated filtration rate ($F, \bigcirc$) based on recorded dosing-pump rate of algal stock ($P, \bullet$) at the end of each period according to (2).

with the relationship found by Kiorboe and Møhlenberg [26] who used the “suction method” and a mixture of suspended bottom material and the unicellular algae *Phaeodactylum tricornutum*, namely, $F = 0.0012L^{2.14}$, and recently by Riisgard et al. [25] who used the “clearance method” and found the equation to be $F = 0.001L^{2.262}$. These findings, along with the present supplementary measurements by means of the clearance method (Figure 5), inspire confidence that the FCA provides reliable measurements of the filtration rate. During the next period with increased algal concentrations, the filtration rate gradually decreased along with reduced valve opening irrespectively of the size of mussels (Figure 5). The decrease in filtration rate ($F_{24}$, L h$^{-1}$) with time ($t = 24$ h) in most of the experiments could be described by an exponential function: $F_{24} = c \times \exp(-d \times t)$, where the coefficients $c$ and $d$ (Table 1) were obtained from curve-fits (Figure 5). At 6,400 cells mL$^{-1}$ the filtration rate was within 24 h reduced to 48% and between 6,800 and 10,900 cells mL$^{-1}$ to about
Figure 5: *Mytilus edulis*. Mean individual filtration rate ($F$, ▲) measured by the fluorometer controlled apparatus (FCA) in 4 groups of mussels (Group I = (a) and (b); Group II = (c), (d), (e), (f), and (g); Group III = (h), (i), (j), (k), and (l); Group IV = (m), see Table 1). The mussels were initially exposed to a relatively low algal (*Rhodomonas salina*) concentration (△, about 2,300 cells mL$^{-1}$) to measure the maximum filtration rate, whereupon the algal concentrations were increased to different higher levels as indicated in the subfigures ($C$, cells mL$^{-1}$). Supplementary, filtration rates were regularly measured by the clearance rate method (○, (l)).
TABLE 1: Mytilus edulis. Filtration rate \( (F_0) \) initially measured by the fluorometer controlled apparatus (FCA) on 4 groups of mussels under optimum conditions (about 2,300 cells mL\(^{-1}\)), and estimated filtration rate \( (F_{24}) \) of the same mussels after \( t = 24 \) h exposure to different constant algal \( (Rhodomonas salina) \) concentrations \( (C, \text{ cells mL}^{-1}) \). The coefficients \( c \) and \( d \), and coefficient of determination \( (R^2) \) were obtained from exponential curve-fits according to the equation \( F_0 = c \times \exp(-d \times t) \) for data shown in Figure 5 \#). Condition index \( (CI) = W \) (g dry weight of soft parts)/\( L \) (cm).

<table>
<thead>
<tr>
<th>Group</th>
<th>Shell length (L)</th>
<th>Dry weight (W)</th>
<th>Condition index (CI)</th>
<th>#</th>
<th>C ((\times 10^3 \text{ cells mL}^{-1}))</th>
<th>c</th>
<th>d</th>
<th>(R^2)</th>
<th>(F_0) ((\text{L h}^{-1}))</th>
<th>(F_{24}) ((\text{L h}^{-1}))</th>
<th>(F_{24}/F_0) (%)</th>
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<tr>
<td>I</td>
<td>15.3 ± 0.4 mm</td>
<td>0.014 ± 0.002 g</td>
<td>3.9 ± 0.7 g cm(^{-3})</td>
<td>A</td>
<td>2.4 ± 0.2</td>
<td>78 ± 0.4</td>
<td>0.28</td>
<td>0.03</td>
<td>0.1</td>
<td>0.1</td>
<td>20</td>
</tr>
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<td></td>
<td></td>
<td></td>
<td></td>
<td>B</td>
<td></td>
<td>10.9 ± 0.6</td>
<td>0.64</td>
<td>0.13</td>
<td>0.9</td>
<td>0.1</td>
<td>20</td>
</tr>
<tr>
<td>II</td>
<td>30.4 ± 1.0 mm</td>
<td>0.219 ± 0.028 g</td>
<td>6.2 ± 0.5 g cm(^{-3})</td>
<td>C</td>
<td>2.3 ± 0.2</td>
<td>6.8 ± 0.5</td>
<td>2.48</td>
<td>0.08</td>
<td>0.9</td>
<td>0.6</td>
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<tr>
<td></td>
<td></td>
<td></td>
<td></td>
<td>D</td>
<td></td>
<td>7.9 ± 0.5</td>
<td>2.09</td>
<td>0.01</td>
<td>0.3</td>
<td>1.6</td>
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<td></td>
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<td></td>
<td></td>
<td>E</td>
<td></td>
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<td>0.7</td>
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<td></td>
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<td></td>
<td></td>
<td>F</td>
<td></td>
<td>9.6 ± 0.8</td>
<td>1.75</td>
<td>0.02</td>
<td>0.3</td>
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<td>III</td>
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<td>7.7 ± 0.6 g cm(^{-3})</td>
<td>G</td>
<td>2.3 ± 0.3</td>
<td>6.4 ± 0.4</td>
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<td>0.04</td>
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<td>H</td>
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<td>6.8 ± 0.3</td>
<td>1.73</td>
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<td></td>
<td>I</td>
<td></td>
<td>12.3 ± 1.4</td>
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<td></td>
<td>19.7 ± 2.9</td>
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<td>0.6</td>
<td>0.3</td>
<td>10</td>
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<tr>
<td></td>
<td></td>
<td></td>
<td></td>
<td>K</td>
<td></td>
<td>36.1 ± 4.6</td>
<td>3.49</td>
<td>0.19</td>
<td>0.3</td>
<td>0.3</td>
<td>10</td>
</tr>
<tr>
<td>IV</td>
<td>45.1 ± 0.1 mm</td>
<td>0.212 ± 0.022 g</td>
<td>2.3 ± 0.2 g cm(^{-3})</td>
<td>L</td>
<td>2.2 ± 0.1</td>
<td>7.9 ± 0.9</td>
<td>3.53</td>
<td>0.06</td>
<td>0.7</td>
<td>0.9</td>
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<tr>
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<td></td>
<td></td>
<td>M</td>
<td></td>
<td>9.7 ± 1.1</td>
<td>3.49</td>
<td>0.07</td>
<td>0.8</td>
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20% of their maximum filtration rate previously measured at low algal concentration. Further, mussels exposed to 19,700 cells mL\(^{-1}\) reduced their filtration rate to 10% of maximum after 24 h (Table I). Filtration rates in experiments A, D, F, I and K (Table I and Figure 5) could not be described properly by an exponential curve fit \( (R^2 < 0.5) \) though all measured filtration rates were below maximum (Figure 5). Mussels in experiment D, however, did not reduce their filtration rates to the same extent as found for mussels in other experiments. But it remains clear that further reduction of the filtration rate may take place during prolonged exposure to high algal concentrations. Thus in an experiment with mussels exposed to 8,160 cells mL\(^{-1}\), the filtration rate became reduced to about 12% after 48 h and then remained constantly low during the following 10 d (Figure 7). In this case, the filtration rate as a function of exposure time \( (t) \) could be described by the equation: \( F = F_{\text{red}} + (F_0 - F_{\text{red}}) \exp(-t/\tau) \), where \( F_0 \) is the maximum filtration rate, \( F_{\text{red}} \) is the constantly low filtration rate after initial 48 h saturation reduction, and \( \tau \) is the time constant for exponential decrease after incipient saturation reduction.

Algal concentration controlled by the FCA usually varied within 5 to 15% of a mean value in experiments performed for 15 h (Table I) and greatest variation within 22% of a mean algal concentration of 3,310 cells mL\(^{-1}\) was found for the experiment in Figure 7 performed for 10 d. Measured filtration rates varied within 5 to 15% of a mean, and only once a variation of 40% was found (Table I, Group 1 at 2,400 cells mL\(^{-1}\)).

3.5. Effect of Changing Salinity. The effect of changing salinity on the filtration rate of Mytilus edulis was studied in 4 experiments using 3 different groups of mussels (Table 2). In these experiments either concentrated seawater or demineralized water was flowing through the aquarium with 20 small (29.6±0.4 mm) mussels at a constant rate to increase or reduce salinity which was measured continuously and recorded on a computer. In Figure 8 is shown a typical example of an experiment. It is seen that the filtration rate is unaffected by decreasing salinity down to about 10 psu whereupon the mussels began to close their valves along with cessation of the filtration activity. However, when the salinity was subsequently increased, the normal filtration rate was soon afterwards restored. It was found that the changing rate of the filtration rate was strongly influenced by the salinity changing rate; the faster the salinity was either reduced or increased,
Figure 6: *Mytilus edulis*. (Mean ± S.D.) individual filtration rates of mussels measured by the fluorometer controlled apparatus (FCA) when exposed to about 2,300 cells mL\(^{-1}\) during the initial period of experiments shown in Figure 5 as a function of mean shell length (L). Group I = ●; II = ○; III = ▲; IV = △ (Table 1).

The FCA maintained a constant algal concentration in an experimental aquarium with mussels and gave reliable and continuously recorded filtration rates and was used for studying the filtration behaviour of mussels at different algal concentrations near and above the critical saturation level, that is, between 5,000 and 8,000 *Rhodomonas salina* cells mL\(^{-1}\), equivalent to 6.3 and 10.0 μg chl a L\(^{-1}\), respectively [6]. Thus, using the FCA we were able to narrow down the lower algal concentration at which *Mytilus edulis* eventually

4. Discussion

The FCA maintained a constant algal concentration in an experimental aquarium with mussels and gave reliable and continuously recorded filtration rates and was used for studying the filtration behaviour of mussels at different algal concentrations near and above the critical saturation level, that is, between 5,000 and 8,000 *Rhodomonas salina* cells mL\(^{-1}\), equivalent to 6.3 and 10.0 μg chl a L\(^{-1}\), respectively [6]. Thus, using the FCA we were able to narrow down the lower algal concentration at which *Mytilus edulis* eventually...
Table 2: *Mytilus edulis*. Variation in filtration rates ($\Delta F$) of mussels at different salinity changing rates ($\Delta S$). Experiments were performed at a mean algal concentration ($3,770 \pm 690 Rhodomonas salina$ cells mL$^{-1}$) with three groups of mussels. Number of mussels used in each experiment was 20 and the mean shell length was 29.4 ± 0.4 mm. For further explanation, see Figure 8.

<table>
<thead>
<tr>
<th>Experiment #</th>
<th>Group #</th>
<th>$-\Delta S$ (psu h$^{-1}$)</th>
<th>$+\Delta S$ (psu h$^{-1}$)</th>
<th>$-\Delta F$ (mL min$^{-1}$ h$^{-1}$)</th>
<th>$+\Delta F$ (mL min$^{-1}$ h$^{-1}$)</th>
</tr>
</thead>
<tbody>
<tr>
<td>I</td>
<td>2</td>
<td>-0.69</td>
<td>-</td>
<td>-1.41</td>
<td>-</td>
</tr>
<tr>
<td>II</td>
<td>1</td>
<td>-0.69</td>
<td>0.96</td>
<td>-2.99</td>
<td>4.17</td>
</tr>
<tr>
<td>III</td>
<td>1</td>
<td>-2.20</td>
<td>1.82</td>
<td>-2.09</td>
<td>3.17</td>
</tr>
<tr>
<td>IV</td>
<td>3</td>
<td>-0.18</td>
<td>0.55</td>
<td>-0.35</td>
<td>2.84</td>
</tr>
</tbody>
</table>

Table 3: *Mytilus edulis*. Salinity changing rates ($\Delta S$) and simultaneous filtration changing rates ($\Delta F$) of mussels in all experiments (see Table 2 and Figure 8).

<table>
<thead>
<tr>
<th>Group</th>
<th>$\Delta S$</th>
<th>$\Delta F$</th>
</tr>
</thead>
<tbody>
<tr>
<td>I</td>
<td>-0.69</td>
<td>-1.41</td>
</tr>
<tr>
<td>II</td>
<td>-0.68</td>
<td>-2.99</td>
</tr>
<tr>
<td>III</td>
<td>-2.20</td>
<td>-2.09</td>
</tr>
<tr>
<td>IV</td>
<td>-0.18</td>
<td>-0.35</td>
</tr>
</tbody>
</table>

reacts by partial valve closure and reduced filtration rate to be between 6,000 and 7,000 $R. salina$ cells mL$^{-1}$ (Table 1, Figure 5) equivalent to 8.5 to 10.0 $\mu$g chl $a$ L$^{-1}$ (cf. M&M), which is higher than what is usually found in the water column in nature [27–36] and much higher than the chl $a$ concentration which is higher than what is usually found in the water column [27–36].

However, in eutrophic and turbid tidal estuaries the chl $a$ concentration may frequently exceed the critical saturation concentration (see below).

The duration time before reduced filtration rate occurred was influenced by extent of increase in algal concentration in the experimental aquarium. Thus, the larger the change in algal concentration was appeared the faster the incipient reduction, in filtration rate, as previously reported for *Mytilus edulis* [6, 39], for the ascidian *Ciona intestinalis* [40], and for the suspension-feeding polychaete *Sabella penicillus* [41]. Additionally, the higher the algal concentration, the faster also the reduction of filtration rate, which is confirmed by the high positive value of the correlation coefficient ($0.782$) between values of $c$ and $d$ in Table 1. It should be emphasized, however, that it is not only the concentration of a certain algal species that determines the incipient reduction in filtration rate, but also the size (volume) of the algal cells used is crucial for the number of cells that can be ingested before the gut capacity is exceeded. Thus, Riisgård et al. [6] found that the total number of $6.9 \mu$m diameter *Rhodomonas salina* cells that can be ingested by small (21.5 mm shell length) *M. edulis* before incipient saturation amounts to $1.4 \pm 1.7 \times 10^6$ cells, equivalent to a total volume of 2 mm$^3$. However, filtration rates and responses to monospecies, cultured algae under laboratory conditions, may not accurately reflect in situ filtration where a wide spectrum of changing environmental factors may influence the feeding behaviour [6, 42]. Natural seston consists of a broad mixture of plankton, bacteria, detritus, and inorganic materials and extrapolating from laboratory to field concentrations of chl $a$ should be done with caution when discussing "critical saturation concentrations." Therefore further test of the FCA including natural seston, perhaps spiked with $R. salina$, may be relevant in future studies.

The FCA has opened up for new detailed information on the filtration-reduction course during the first hour and up to 10 days following incipient saturation (Figures 5 and 7). In this context it is possible to reinterpret the filtration rate data obtained by Navarro and Winter [13] who performed experiments with *Mytilus chilensis* using the automatic recording apparatus described by Winter [12] and high algal (*Dunaliella marina*) concentrations of 15,000, 25,000, and 40,000 cells mL$^{-1}$. The low specific filtration rates of 1.55, 1.05, and 0.79 L h$^{-1}$ g$^{-1}$ found by Navarro and Winter [13] may be compared to the specific rate of 7.37 L h$^{-1}$ g$^{-1}$ measured in *Mytilus edulis* by Riisgård and Møhlenberg [15] using a photoaquarium method and to 7.45 L h$^{-1}$ g$^{-1}$ measured by Møhlenberg and Riisgård [22] using the "suction method". Because the filtration rate experiments conducted by Navarro and Winter [13] "were carried out over 24 h," it seems likely that only saturation-reduced rates were recorded. In most of our experiments with *M. edulis* the filtration rate decreased to about 20% of the maximum rate when the mussels were exposed to algal concentrations between 6,800 and 10,900 *Rhodomonas* cells mL$^{-1}$. At higher algal concentrations (Table I, Group 3 at 19,700 and 36,100 cells mL$^{-1}$) the filtration rate after 24 h was further reduced to 10% of maximum. The reduction in filtration rate could not be described by exponential curvefits ($R^2 < 0.5$) in experiments A, D, F, I, and K (Table I and Figure 5). The reason why mussels in experiment D behaved differently from mussels in other experiments remains unexplained. A reduction of filtration rate has previously been found for *M. edulis* fed *Phaeodactylum tricornutum* at 15,000 to 40,000 cells mL$^{-1}$ [39, Figure 3(a) therein] whereby the filtration rate was reduced to about 25% of maximum after 300 min irrespective of the algal concentration, indicating "no regulation of filtration rate to ambient algal concentration" [39]. Winter [12] found a further reduction of filtration rate by 50% in *M. edulis* when the algal concentration was increased from 20,000 to 40,000 *Dunaliella marina* cells mL$^{-1}$. Kiørboe et al. [43] suggested "that *M. edulis* depends on suspended bottom material to exploit fully its clearance potential," but Clausen and Riisgård [10] showed that this may not be a prerequisite for mussels to achieve maximum growth. In turbid
macrotidal waters, such as the Western Scheldt Estuary [44] and the Marsdiep in the western Wadden Sea [45], *M. edulis* may frequently be exposed to high concentrations of chl *a* and suspended matter, and in such situations it remains unknown to what degree *M. edulis* may exploit its filtration rate capacity while also coping with cleaning of the gills and sorting of particles of food value, particularly phytoplankton, and particles without food value, particularly silt [2, 24, 26, 46–50]. Finally, it should also be mentioned that other environmental factors in nature may influence the filtration rate, for example, flow-induced inhibition of filtration rate due to high ambient current velocity and turbulence (e.g., [51, 52]), salinity changes (e.g., [53, 54]), and toxic algae [55, 56].

By passively controlling of the valve gape of *Mytilus edulis* Jørgensen et al. [57] found that the oxygen consumption rate was relatively uninfluenced until the filtration rate was reduced to about 20% of the maximum, but at further reduced filtration rates the oxygen consumption dramatically decreased. This indicates that in the present long-term experiment (Figure 7) where *M. edulis* reduced its filtration rate to about 12% the oxygen consumption may have been affected. Until recently it remained unknown if *M. edulis* is able to regulate its ingestion rate to ensure optimal growth during food-saturated conditions and partial valve closure or if optimal growth depends on unrestrained oxygen consumption (i.e., no reduction of respiration due to valve closure). Thus, using the FCA set-up Riisgård et al. [58] have run controlled growth experiments at constant algal concentrations both below and above the food-saturation levels (*C* *sat*). From nearly constant filtration rates measured at algal concentrations below *C* *sat* the filtration rate decreased with increasing algal concentrations above *C* *sat* to only 10% of previous rate. The ingestion rate (*I = F × C*) increased linearly below *C* *sat*, but the weight specific growth rates decreased sharply above *C* *sat* and a survey of naturally occurring phytoplankton biomass in the sea showed that this is generally below *C* *sat*. Hence, Riisgård et al. [58] concluded that mussels may generally feed at optimal rates depending on the concentration of phytoplankton exceeding the minimal biomass below which the mussels cease filtering.

The present study on the effect of changing salinity on the filtration rate of mussels (Figures 8 and 9) has demonstrated that the FCA set-up may also be useful in acute environmental effect studies on mussels. Obviously, the FCA set-up is not limited to mussels but may be extended to oysters, scallops, and other species of filter-feeding zoobenthos (ascidians, polychaetes, bryozoans, sponges, etc.). The very precise conditions in laboratory studies like the present are never fully encountered in the natural environment and FCA-measured filtration rates should be compared—"intercalibrated"—with in situ type studies. For a wide application the FCA needs to be further tested with cells of various sizes, morphologies, and fluorescence properties, and it should also be tested how the FCA performs with mixed-species assemblages that may be difficult to maintain consistently for extended time periods. However, the examples and tests made in the present study demonstrate a significant potential of the FCA system.

Conflict of Interests

The authors declare no competing interests.

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