Research Article

Study the Migration Process of Chemical Substances through the Packaging/Food Interface during Microwave Treatment

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The diffusion of chemical substances from packaging into food endangers people’s health. The migration amount of the chemical substances increases with the time and temperature, but the diffusion process for different kinds of packaging materials differs much. Most recently, the research community showed a renewed interest on the diffusion process of chemical substances through packaging/food interface during microwave treatment. In this study, the diffusion coefficient model is suggested and then the migration process is studied based on Fick’s diffusion law. The results are finally compared with the experimental data, showing good agreement.

1. Introduction

Mathematical modeling is widely applied for studying the complex migration process of chemical substances from packaging into food [1–3]. The experiment methods as well as the modeling tools are studied thoroughly [4]. However, few works were reported on modeling the diffusion process during microwave treatment [5–7] though food is often microwave-heated directly inside the polymer package, which may accelerate the migration process. It is desirable to derive a mathematical model for the migration process of chemical substances from packaging into food during microwave treatment.

2. Mathematical Modeling

To derive the mathematical model, some assumptions are suggested: (1) the contaminant is well distributed in the packaging, while there is no contamination in the food initially; (2) the contaminant transfers through food/packaging interface with no block; (3) the migration process is unidirectional from packaging into food; and (4) the partition factor of the contaminant is taken as 1 at the interface of packaging and food.

By applying Fick’s second law of diffusion [8], the diffusion of chemical substances can be described as

\[
\frac{\partial C}{\partial t} = D(t) \frac{\partial^2 C}{\partial x^2},
\]

(1)

where \( C \) is the concentration of a migrant in a food contact polymer at time \( t \) at a distance \( x \) from the origin of the \( x \)-axis (for single-sided contact) and \( D \) is the diffusion coefficient in the polymer.

The initial condition and boundary conditions are given separately in (2) and (3)–(4):

\[
C = C_0, \quad 0 < x < L_p, \quad t = 0,
\]

(2)

\[
\frac{\partial C}{\partial x} = 0, \quad x = 0, \quad t > 0,
\]

(3)

\[
C = 0, \quad x = L_p, \quad t > 0,
\]

(4)

where \( C_0 \) represents initial concentration of contaminant in packaging and \( L_p \) defines the thickness of polymer.
Apply the variable separation approach (VSA), and set
\[ C(x, t) = X(x)T(t). \] (5)

The following equations are obtained:
\[ T = \exp \left( -\lambda^2 \int_0^t D(t) \, dt \right), \] (6)
\[ X = A \sin \lambda x + B \cos \lambda x. \]

From (6), we can get
\[ C = \sum_{m=1}^{\infty} \left( A_m \sin \lambda_m x + B_m \cos \lambda_m x \right) \exp \left( -\lambda^2 \int_0^t D(t) \, dt \right). \] (7)

Substituting (2)–(4) into (7) leads to
\[ \frac{C}{\pi} = 4C_0 \sum_{n=0}^{\infty} \frac{(-1)^n}{2n + 1} \exp \left( -\frac{(2n + 1)^2 \pi^2}{4L_p^2} \int_0^t D(t) \, dt \right) \times \cos \left( \frac{(2n + 1) \pi x}{2L_p} \right), \] (8)
from which the migration amount of chemical substances can be calculated by
\[ M_{F,t} = \int_0^t AD(t) \frac{2C_0}{L_p} \sum_{n=0}^{\infty} \exp \left( -\frac{(2n + 1)^2 \pi^2}{4L_p^2} \int_0^t D(t) \, dt \right) \, dt. \] (9)

And as suggested in [9], the relationship between the temperature and time during microwave treatment can be approximately modeled by a linear equation,
\[ T(t) = k_1 t + k_2. \] (10)

The relationship between the absorbed power and the temperature variation can be written as
\[ P_{\text{absorb}} = cm \Delta T. \] (11)

Substituting (10) into (11) leads to
\[ T(t) = \frac{P_{\text{absorb}}}{cm} + T_0, \] (12)
where \( c \) and \( m \) are separately the specific heat and mass of the food, respectively; \( T_0 \) is the initial temperature of the food.

By introducing the Arrhenius' law, the diffusion coefficient is related to the temperature as in [10]
\[ D(t) = D_0 \exp \left( -\frac{E}{RT} \right). \] (13)

\[ \text{Figure 1: Comparison of the experiment data and model results for migration of antioxidant 1076 from HDPE film into olive oil with microwave input power of 200 W.} \]

Substituting (12) into (13) and replacing \( D(t) \) in (9) lead to
\[ M_{F,t} = \int_0^t AD_0 \exp \left( -\frac{E}{R ((Pt/cm) + T)} \right) \frac{2C_0}{L_p} \times \sum_{n=0}^{\infty} \exp \left( -\frac{(2n + 1)^2 \pi^2}{4L_p^2} \int_0^t D_0 \exp \left( -E/R ((Pt/cm) + T) \right) \, dt \right) \times \left( 4L_p^2 \right)^{-1} \, dt. \] (14)

Here, \( A \) is the contact area between polymer packaging and food. \( E \) defines the activation energy of polymer, and \( R \) defines the molar constant of chemical substance.

### 3. Results and Discussion

The suggested model previously mentioned provides us with a new mathematical method for studying the diffusion process of chemical substances from packaging into food. To check the accuracy of the proposed method, the migration experiment of antioxidant 1076 from HDPE film into the fatty food stimulants (olive oil) through single contact is conducted and compared with the theoretical prediction. The contact area between polymer packaging and food (\( A \)) is 45 cm². The volume of fatty food stimulants is 25 mL (\( m \) equals 20 g), the parameter \( c \) in (14) for the studied mixture is 2000 kJ/kg. The initial concentration of contaminant in polymer (\( C_0 \)) is 4.5 mg·cm⁻³. The thickness of the film (\( L_p \)) is 45 μm. \( D_0 \) is 10⁻⁴ cm²/s. And the microwave input power is
200 W. It can be seen clearly from Figure 1 that the migration amount increases sharply with the growth of treatment time, and similar conclusion is suggested by the proposed model. Moreover, good agreement can be seen between the experiment data and the model results.

4. Conclusions

The diffusion process of chemical substances from packaging into food during microwave treatment was studied. A mathematical model was suggested and compared with the experiment results, showing good agreement. The results show that the migration process was accelerated during microwave treatment and the strong dependence nature of migration amount on input power and treatment time was revealed. The proposed mathematical model provides the research community with a useful tool for predicting the migration process. It should be pointed out that the suggested temperature-dependent model is valid only for single-layer packaging and the migration process is unidirectional from packaging into food.

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References
