Research Article

A New Numerical Approach of MHD Flow with Heat and Mass Transfer for the UCM Fluid over a Stretching Surface in the Presence of Thermal Radiation

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Received 18 March 2013; Accepted 13 August 2013

Academic Editor: Tirivanhu Chinyoka

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This paper numerically investigates the magnetohydrodynamic boundary layer flow with heat and mass transfer of an incompressible upper-convected Maxwell fluid over a stretching sheet in the presence of viscous dissipation and thermal radiation as well as chemical reaction. The governing partial differential equations are transformed into a system of ordinary differential equations by using suitable similarity transformations. The resultant highly nonlinear ordinary differential equations are then solved using spectral relaxation method. The results are obtained for velocity, temperature, concentration, skin friction, and Nusselt number. The effects of various material parameters on the flow with heat and mass transfer and the dimensionless variables are illustrated graphically and briefly discussed.

1. Introduction

In the past few decades, the studies of boundary layer flows of Newtonian and non-Newtonian fluids of stretching surfaces have received great attention by virtue of their numerous applications in the fields of metallurgy, chemical engineering, and biological systems. These applications include geothermal reservoirs, wire and fiber coating, foodstuff processing, reactor fluidization, transpiration cooling, enhanced oil recovery, packed bed catalytic reactors, and cooling of nuclear reactors. The prime aim in extrusion is to keep the surface quality of the extricate. Coating processes demand a smooth glossy surface to meet the requirements for the best appearance and optimum properties. Sakiadis [1, 2] did pioneering work on boundary layer flow on a continuously moving surface. After that many investigators discussed various aspects of the stretching flow problem (see, e.g., Chiam [3], Crane [4], Liao and Pop [5], Khan and Sanjayanand [6], Abel and Mahesha [7], and Fang et al. [8], among others).

A number of industrial fluids such as molten plastics, artificial fibers, blood, polymetric liquids, and foodstuff exhibit non-Newtonian fluid behaviour. In many industrial processes, cooling continuous strips or filaments is done by drawing them through a quiescent fluid. It must be noted that during these processes, the strips are sometimes stretched or shrunk. Therefore the properties of the final product depend to a great extent on the rate of cooling. The rate of cooling can be controlled and the desired characteristics of the final product can be obtained by drawing the strips in electrically conducting fluids subjected to uniform magnetic fields.

In recent years, MHD flows of viscoelastic fluids above stretching sheets have also been studied by various researchers (Liu [9], Cortell [10], among others). This is the simplest subclass of viscoelastic fluid known as the second grade fluid. However, a non-Newtonian second grade fluid does not give meaningful industrial results for highly elastic fluids such as polymer melts, which occur at high Deborah number (Hayat et al. [11]). For theoretical results to become
of any industrial use, more realistic viscoelastic fluid models such as upper-convedted Maxwell model should be used in the analysis.

Alizadeh-Pahlavan et al. [12] investigated using a two- auxiliary-parameter homotopy analysis method for the problem of laminar MHD flow of an upper-convedted Maxwell fluid above a porous isothermal stretching sheet. Aliakbar et al. [13] analyzed the influence of Maxwell fluids above stretching sheets. Abel et al. [14] performed an analysis to investigate the influence of MHD and thermal radiation on the two-dimensional steady flow of an incompresible, upper-convedted Maxwell fluid. Motsa et al. [15] investigated the MHD boundary layer flow of an incompresible upper- convedted Maxwell fluid over a porous stretching surface. Hayat et al. [16] investigated MHD flow of a more realistic viscoelastic fluid model above a porous stretching sheet. Sadeghy et al. [17] among other researchers, the radiative heat flux, \( q_r \), is given by

\[
q_r = -\frac{4\sigma^*}{3K_s^2} \frac{\partial T^4}{\partial y},
\]

where \( \sigma^* \) is the electrical conductivity, \( B_0 \) is the uniform magnetic field, \( T \) is the temperature, \( c_p \) is the specific heat at constant pressure, \( k \) is the thermal conductivity, \( C \) is the concentration of the species diffusion, \( D \) is the diffusion coefficient of the diffusion species, \( \nu \) is the kinematic viscosity, \( \lambda \) is the relaxation time, and \( K_n \) denotes the reaction rate constant of the nth-order homogeneous and irreversible reaction. The appropriate boundary conditions are

\[
\begin{align*}
\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} &= 0, \\
u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + \lambda \left[ u^2 \frac{\partial^2 u}{\partial x^2} + v^2 \frac{\partial^2 u}{\partial y^2} + 2uv \frac{\partial^2 u}{\partial x \partial y} \right] &\equiv \nu \frac{\partial^2 u}{\partial y^2} - \frac{\sigma B^2_0}{\rho} u, \\
u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} &= \frac{k}{\rho c_p} \frac{\partial^2 T}{\partial y^2} + \frac{\mu}{\rho c_p} \left( \frac{\partial u}{\partial y} \right)^2 - \frac{1}{\rho c_p} \frac{\partial q_r}{\partial y}, \\
u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} &= D \frac{\partial^2 C}{\partial y^2} - K_n (C - C_{co})^n,
\end{align*}
\]

2. Mathematical Formulation

We consider the steady and incompressible MHD boundary layer flow with heat and mass transfer of an electrically conducting fluid obeying UCM model over a stretching sheet in the presence of thermal radiation. The flow is generating by the stretching of the sheet by applying two equal and opposite forces along the x-axis, keeping the origin fixed and considering the flow to be confined to the region \( y > 0 \). We assume that the continuous stretching sheet has a linear velocity, \( u = bx \), with \( b \) as the stretching rate and \( x \) being the distance from the slit. We impose a uniform magnetic field of strength \( B_0 \) along the y-axis, and the induced magnetic field is negligible. This assumption is valid on a laboratory scale under the assumption of small magnetic Reynolds number, and the external electric field is zero. We also assume that the boundary layer approximations are applicable to all momentum, energy, and mass equations. Although this theory is incomplete for viscoelastic fluids, but it is more plausible for Maxwell fluids as compared to other viscoelastic fluid models (Renardy [33]). Following Sadeghy et al. [17] among others, in a two-dimensional flow, the equation of continuity, the equation of motion, and the diffusion equations can be written as
where $\sigma^*$ and $K_s$ are the Stefan-Boltzmann constant and the Rosseland mean absorption coefficient, respectively. We assume that the temperature differences within the flow are sufficiently small such that

$$T^4 \approx 4T_{\infty}^3 T - 3T_{\infty}^4.$$  \hspace{1cm} (7)

Using (6) and (7) in the last term of (3) we obtain

$$\frac{\partial q}{\partial y} = -\frac{16\sigma^* T_{\infty}^3}{3K_s} \frac{\partial^2 T}{\partial y^2}. \hspace{1cm} (8)$$

2.1. Similarity Transformation. To make the problem amenable we introduce the following nondimensional quantities:

$$\eta = \sqrt{\frac{b}{\nu} y}, \quad \psi = \sqrt{b\nu x f(\eta)},$$

$$\theta (\eta) = \frac{T - T_{\infty}}{T_w - T_{\infty}},$$

$$\phi (\eta) = \frac{C - C_{\infty}}{C_w - C_{\infty}}.$$  \hspace{1cm} (9)

where $f(\eta)$ is the dimensionless stream function and $\eta$ is the similarity variable, $\theta$ is the dimensionless temperature, and $\phi$ is the mass concentration. The continuity equation is automatically satisfied through the variables. Then introducing the relations (9) into (2)-(3), we obtain the following nonlinear system of ordinary differential equations:

$$f''' + ff'' - f' - M^2 f' + \beta (2ff' f'' - f^2 f'''') = 0,$$  \hspace{1cm} (10)

$$\left(1 + \frac{4R}{3}\right) \phi'' + Pr (f\phi' - 2f' \theta) + Pr Ec f'' = 0,$$  \hspace{1cm} (11)

$$\phi'' + Sc \left[ f\phi' - 2f' \phi - \gamma \psi \phi' \right] = 0.$$  \hspace{1cm} (12)

Here $M^2 = \sigma R_b \rho b$ and $\beta = \lambda b$ are magnetic and elastic parameters, respectively, $Pr = \mu c_p / k$ is the Prandtl number, $Ec = b^2 / \nu_x T_s$ is the Eckert number, $R = 4\sigma^* T_{\infty}^3 / k K_s$ is the thermal radiation parameter, $\gamma = K_n C_0^{-1} b^{n-2} x^n / \nu^2$ is the chemical reaction parameter, and $Sc = D / \nu$ is the Schmidt number. The boundary conditions are

$$f(0) = 0, \quad f'(0) = 1, \quad \theta(0) = 1, \quad \phi(0) = 1,$$

$$f' \to 0, \quad \theta \to 0, \quad \phi \to 0, \quad \text{as} \quad \eta \to \infty.$$  \hspace{1cm} (13)

3. Method of Solution

The Successive Relaxation Method (SRM) begins by letting

$$p = f'$$  \hspace{1cm} (14)

so that $p' = f''$ and $p'' = f'''$. Consequently, (10) through (12) become

$$p'' + fp' - p^2 - M^2 p + \beta (2fp p'' - f^2 p'''') = 0,$$  \hspace{1cm} (15)

$$\left(1 + \frac{4R}{3}\right) \theta'' + Pr (f\theta' - 2f\theta) + Pr Ec p'' = 0,$$  \hspace{1cm} (16)

$$\phi'' + Sc \left[ fp\phi' - 2f\phi - \gamma \psi \phi' \right] = 0.$$  \hspace{1cm} (17)

Proceeding in a manner similar to the Gauss-Seidel method, (14) and (15) through (16) are replaced by the following recursive formulae:

$$f_{r+1} = p_r, \quad f_{r+1}(0) = 0,$$  \hspace{1cm} (18)

$$p_{r+1} = f_{r+1} p_r - p_r^2 - M^2 p_{r+1} + \beta (2f_{r+1} p_r - f_r^2 p_{r+1}) = 0,$$  \hspace{1cm} (19)

$$p_{r+1}(0) = 1, \quad p_{r+1}(\infty) = 0,$$  \hspace{1cm} (20)

$$\theta_{r+1} = \frac{1}{Pr} \left(1 + \frac{4R}{3}\right) \theta_{r+1}' + f_{r+1} \theta_{r+1},$$

$$\theta_{r+1}(0) = 1, \quad \theta_{r+1}(\infty) = 0,$$  \hspace{1cm} (21)

$$\phi_{r+1} = Sc \left[ f\phi_{r+1}' - 2p_{r+1} \phi_{r+1} - \gamma \psi \phi_{r+1}' \right] = 0.$$  \hspace{1cm} (22)

The Chebyshev spectral collocation method will be used to solve (18) through (21). First, we replace the semi-infinite interval [0, $\infty$) with the closed interval [0, $L$], where $L$ is sufficiently large. It is convenient to use the change of variable

$$\eta(\xi) = \frac{1 + \xi}{2} L$$  \hspace{1cm} (23)

to map the interval [0, $L$] on the $\eta$-axis onto the interval $[-1, 1]$ on the $\xi$-axis. On $[-1, 1]$ we form a computational grid $-1 = \xi_N < \xi_{N-1} < \cdots < \xi_0 = 1$, where

$$\xi_j = \cos \left( \frac{j\pi}{N} \right), \quad j = 0, 1, \ldots, N,$$  \hspace{1cm} (24)

are the Chebyshev collocation points. The derivative $h'(\xi_j)$ at each collocation point is evaluated using formula

$$h'(\xi_j) = \sum_{k=0}^{N} D_{jk} h(\xi_k)$$  \hspace{1cm} (25)

where $D$ is the Chebyshev differentiation matrix. Successive application of Chebyshev differentiation reveals the more general formula

$$\frac{d^p}{d\xi^p} h = D^p h.$$  \hspace{1cm} (26)
Chebyshev differentiation transforms (18) through (21) to discrete form:

\[ A_1 f_{r+1} = B_1, \quad f_{r+1}(\xi_N) = 0, \]
\[ A_2 p_{r+1} = B_2, \quad p_{r+1}(\xi_N) = 1, \quad p_{r+1}(\xi_0) = 0, \]
\[ A_3 \Theta_{r+1} = B_3, \quad \theta_{r+1}(\xi_N) = 1, \quad \theta_{r+1}(\xi_0) = 0, \]
\[ A_4 \Phi_{r+1} = B_4, \quad \phi_{r+1}(\xi_N) = 1, \quad \phi_{r+1}(\xi_0) = 0, \]

where

\[ A_1 = D, \quad B_1 = p_r, \]
\[ A_2 = D^2 + \text{diag}[f_r] D - M^2 I, \]
\[ B_2 = p_r^2 - \beta \left(2 f_{r+1} p_r - f_{r+1}'' p_r''\right), \]
\[ A_3 = \left(1 + \frac{4}{3} R\right) D^2 + \text{Pr} \left(\text{diag}[f_r] D - 2 \text{diag}[p_{r+1}]\right), \]
\[ B_3 = -\text{Pr Ec} p_r^2, \]
\[ A_4 = D^2 + \text{Sc} \left(\text{diag}[f_r] D - 2 \text{diag}[p_{r+1}]\right), \]
\[ B_4 = \text{Sc} \Phi_r^n. \]

Initial approximations needed to drive this iterative scheme must satisfy boundary conditions (13). Suitable choices are

\[ f_0(\eta) = 1 - e^{-\eta}, \quad p_0(\eta) = e^{-\eta}, \]
\[ \theta_0(\eta) = e^{-\eta}, \quad \phi_0(\eta) = e^{-\eta}. \]

4. Results and Discussion

In this section we give the SRM results for the main parameters that have significant effects on the fluid flow velocity and temperature. We remark that all the SRM results presented in this work were obtained using \( N = 50 \) collocation points, and also convergence was achieved after as few as five iterations. Also the infinity value \((\eta_\infty)\) was taken to be 50. It is also important to note that the magnetic field is taken quite strong by assigning large values of \( M \) to ensure the occurrence of steady flow near the sheet. Unless otherwise stated, the default values for the parameters are taken as \( M = 1, \beta = 0.1, R = 1, \)
\( \text{Pr} = 0.71, \text{Ec} = 0.1, \text{Sc} = 0.2, \gamma = 0.2, \) and \( n = 2. \)

In order to validate the numerical method, it was compared with the MATLAB routine \textit{bvp4c} which is an adaptive Lobatto quadrature iterative scheme. Table 1 presents a comparison between SRM approximate results and the \textit{bvp4c} results for selected default values of the magnetic parameter \( M \). It can be seen from this table that there is an excellent agreement between the results from the two methods. Analyzing Table 1 shows that an increase in the magnetic field strength leads to an increase in the skin-friction but a decrease to the Nusselt number. This is physically expected as application of a transverse magnetic field produces a drag force which then reduces the flow velocity but generates heat within the fluid.

Table 1: Comparison of the SRM results of \(-f''(0), -\theta'(0)\) with those obtained by \textit{bvp4c} for different values of the magnetic parameter.

<table>
<thead>
<tr>
<th>( M )</th>
<th>\textit{bvp4c}</th>
<th>SRM</th>
<th>\textit{bvp4c}</th>
<th>SRM</th>
</tr>
</thead>
<tbody>
<tr>
<td>0.0</td>
<td>1.42811186</td>
<td>1.42811186</td>
<td>0.57932373</td>
<td>0.57932373</td>
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<tr>
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<td>2.71897650</td>
<td>0.27809236</td>
<td>0.27809236</td>
</tr>
</tbody>
</table>

Table 2 gives a comparison of the SRM results to those obtained by the \textit{bvp4c} for different values of the elasticity parameter \( \beta \). We again observe that the results from the two methods agree very well giving confidence to the current proposed method. Increasing the fluid elasticity parameter leads to the increase in the skin friction coefficient but a decrease to the heat transfer coefficient. Figures 1 and 2 show the influence of the elasticity parameter \( \beta \) on the \( u \)-velocity and \( v \)-velocity profiles, respectively. From both these figures, we observe that an increase in the elasticity parameter results in the decrease in both velocity components and a decrease in the thickness of the momentum boundary layer.

Figures 3 and 4 depict the effects of the magnetic field parameter \( M \) on the \( u \)-velocity and \( v \)-velocity profiles, respectively. From these figures we clearly observe that increasing magnetism significantly reduces the thickness of the boundary layer, thereby reducing the velocity components. Physically, the application of the transverse magnetic field presents a damping effect on the fluid velocity by producing a drag force that opposes the fluid motion.

Figure 5 depicts the effect of increasing the elasticity parameter \( \beta \) on the temperature distribution. A decrease in the streamwise velocity component, \( u \), can result in a decrease in the amount of heat transferred on the surface sheet. Similarly, a decrease in the transverse velocity component, \( v \), means that the amount of fresh fluid which is extended from the lower-temperature region outside the boundary layer and directed towards the sheet is reduced, thereby reducing the rate of heat transfer. These two effects on the velocity components in the same direction reinforce each other. Thus, an increase in the elastic number increases the temperature distribution in the fluid as depicted in Figure 5.

Figure 6 represents the dimensionless temperature for different values of the magnetic field parameter \( M \). From this figure we clearly see that the temperature profiles increase with the increase of the magnetic field parameter. Thus the applied magnetic field tends to heat the fluid and thus reduces
Figure 1: Graph of the SRM solutions of the $u$-velocity for different values of $\beta$.

Figure 2: Effect of the $\beta$ on the $v$-velocity profile.

Figure 3: Influence of the magnetic parameter $M$ on the $u$-velocity profile.

Figure 4: The variation of the $v$-velocity component for different values of $M$.

Figure 5: Graph of the SRM solutions of the temperature distribution for different values of $\beta$.

The influence of thermal radiation on the temperature profiles is shown in Figure 8. It can be seen that the thermal boundary layer thickness increases as $R$ increases. This induces the decrease in the absolute value of the temperature gradient at the surface. Thus, the heat transfer rate at the surface decreases with increasing $R$, thereby causing the temperature profiles to increase.

Figure 9 depicts the effect of increasing the Prandtl number on the fluid temperature distribution. An increase in
the Prandtl number as expected is seen to reduce the fluid temperature above the sheet. This is because as the Prandtl number increases, the thermal boundary layer becomes thinner. Thus the rate of thermal diffusion drops, resulting in the fluid temperature dropping as well.

Figure 10 shows how the elastic parameter $\beta$ affects the concentration profiles. As the elasticity parameter reduces the flow velocity, it means that less fluid is taken away at any given point resulting in the concentration profiles increasing. The same phenomenon happens when the values of the magnetic parameter increase as can be clearly seen in Figure 11. The reduction of flow velocity as the result of increasing the strength of the magnetic field causes the fluid concentration to increase as less fluid is taken downstream at any given point.

Figure 12 presents the profiles of the concentration for selected default values of the chemical reaction parameter
\[ \eta \geq 0. \] It is observed from this figure that an increase in the values of chemical reaction parameter leads to a decrease in the concentration profiles. The concentration boundary layer becomes thin as the reaction parameter increases.

Figure 13 shows graphically the effect of increasing the reaction-order parameter \( n \). The effect of \( n \) is seen as to increase the fluid concentration.

5. Conclusion

The present work analyzed the MHD flow with heat and mass transfer within a boundary layer of an upper-convected Maxwell fluid above a stretching sheet in the presence of viscous dissipation, thermal radiation, and chemical reaction. Numerical results are presented in tabular/graphical form to elucidate the details of flow with heat and mass transfer characteristics and their dependence on the various physical parameters. The accuracy of the SRM is validated against the MATLAB in-built \( \textit{bvp4c} \) routine for solving boundary value problems.

(1) We observe that the flow velocity is decreased when the magnetic parameter increases. Also an increase in the elasticity parameter results in velocity decrements. However, both the temperature and concentration profiles are enhanced by increasing the values of the magnetic parameter as well as the elasticity parameter.

(2) The dimensionless temperature \( \theta \) increases with increase in the thermal radiation but decreases with increasing Prandtl number.

(3) The effect of the chemical reaction \( \gamma \) is to decrease the fluid concentration while the concentration profiles are increased as the order of reaction \( n \) is increased.

(4) It is shown that the skin-friction increases with an increase of the magnetic parameter and elasticity parameter, but the Nusselt number and Sherwood number (not shown for brief) are found to be decreased as these parameters are increased.

(5) Finally the Nusselt number increases with increasing values of the Prandtl number but decreases as thermal radiation increases.

Acknowledgments

The authors wish to acknowledge financial support from the University of Venda and NRF.

References


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