
Scheme-4 Reactor-1

Part-2, Case-3

$t_a = 1800 \text{ sec}$, $t_m = 1200 \text{ sec}$
 $k_1 = 0.1$, $k_2 = 0.01$

$NB_t/NA_t = 1.73318$

Exponent $a = 0.5$
Exponent $b = 1.5$
Exponent $c = 0.5$
Exponent $d = 1.5$

$WA = 200$
 $WB = 86.6591$
 $NB_t = 4.62182$
 $V_t = 2.14333$
 $V_{at} = 1.04333$
 $Tot.Solv. = 2$
 $SolA/(SolR+SolA) = 0.5$

$NA_0 = 2.66667$
 $NB_0 = 0$

Total input = 286.659 kg
Total output = 286.661 kg

Chemical Balance Error = 0.0019862 kg (% 6.92878e-06)

Solver: Explicit Runge-Kutta (4,5) Variable step (Dormand-Prince Pair)
Error tolerance: 0.1%

Final Concentrations with Step Size limited to 0.001

$NA \text{ (final)} = 0.0266599$
 $NB \text{ (final)} = 5.83347e-13$
 $NR \text{ (final)} = 0.658197$
 $NS \text{ (final)} = 1.98181$

Final Concentrations with Step Size limited to 0.01

$NA \text{ (final)} = 0.0266593$
 $NB \text{ (final)} = -5.83596e-11$
 $NR \text{ (final)} = 0.658196$
 $NS \text{ (final)} = 1.98181$



