
Scheme-8 Reactor-1

Part-2, Case-3

$t_a = 1800 \text{ sec}$, $t_m = 1200 \text{ sec}$
 $k_1 = 0.1$, $k_2 = 0.01$

$NB_t/NA_t = 1.42329$

Exponent $a = 0.5$
Exponent $b = 1.5$
Exponent $c = 1$
Exponent $d = 1$

$WA = 200$
 $WB = 71.1646$
 $NB_t = 3.79545$
 $V_t = 2.13558$
 $V_{at} = 1.03558$
 $Tot.Solv. = 2$
 $SolA/(SolR+SolA) = 0.5$

$NA_0 = 2.66667$
 $NB_0 = 0$

Total input = 271.165 kg
Total output = 271.166 kg

Chemical Balance Error = 0.00115903 kg (% 4.27427e-06)

Solver: Explicit Runge-Kutta (4,5) Variable step (Dormand-Prince Pair)
Error tolerance: 0.1%

Final Concentrations with Step Size limited to 0.001

$NA \text{ (final)} = 0.0266622$
 $NB \text{ (final)} = 1.62323e-05$
 $NR \text{ (final)} = 1.48458$
 $NS \text{ (final)} = 1.15543$

Final Concentrations with Step Size limited to 0.01

$NA \text{ (final)} = 0.0266618$
 $NB \text{ (final)} = 1.62325e-05$
 $NR \text{ (final)} = 1.48458$
 $NS \text{ (final)} = 1.15543$



