

Research Article

Magnesium Removal from an Aluminum A-332 Molten Alloy Using Enriched Zeolite with Nanoparticles of SiO₂

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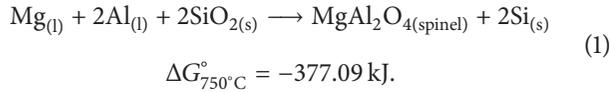
In order to improve the Mg removal from an A-380 molten alloy, mixtures of zeolite and SiO₂ nanoparticles (SiO_{2(NPs)}) were tested. Zeolite was enriched with 2.5, 5, 7.5, 10, or 12.5 wt-% of amorphous SiO_{2(NPs)}. The SiO_{2(NPs)} and zeolite were mixed for 30 min in ethanol for each experiment and then dried in a furnace at 80°C for 12 h. The enriched zeolites were analyzed by scanning electron microscopy, transmission electron microscopy, and N₂ gas adsorption analysis. The Mg removal was carried out injecting each mixture into the molten aluminum alloy at 750°C using argon. The Mg content of the molten alloy was measured after different periods of the injection time. Zeolites enriched with 2.5 and 5 wt-% of SiO_{2(NPs)} were demonstrated to be the better mixtures, removing Mg from an initial content of 1.6 to a final content of 0.0002 and 0.0101 wt-%, respectively, in 45 min of injection.

1. Introduction

Al-Si alloy is one of the aluminum casting alloys widely used in automotive industries due to its excellent microstructure, casting, and mechanical characteristics as is the A380 alloy. Abedi et al. [1] showed that magnesium can refine the size of primary $\alpha(\text{Al})$ phase and eutectic silicon. Vončina et al. [2] established the grain refining influence by Ce in A380 alloy. On the other hand, the increase of ultimate tensile strength and elongation in A380 alloy can be obtained by SDAS (secondary dendrite arm spacing) values ranging from 5.70 to 10 μm on the squeeze cast parts as shown by Murat Lus [3]. But it is noticeable that in the case of the A380 alloy for automotive use, the standard indicates a maximum of 0.1 wt-% of Mg because the presence of this element in the alloy increases its oxidation tendency [4]. However, when the alloy is produced from scrap, the resultant Mg content of

the alloy is higher than 0.1 wt-% and the excess of Mg needs to be removed. Vieira et al. [5] used the chlorine method and discuss bubble-formation theories and magnesium kinetic removal from aluminum scraps using chlorine and inert gas fluxing. In spite of that Neff and Cochran [6] showed that the kinetics of the magnesium removal as MgCl₂ is rapid, but the unreacted chlorine and the gaseous coproduct AlCl₃ can limit the environmental acceptability of the process. Electrochemical method and the incorporation of powder reagents (fluorides) are used for Mg removal [7]. Both have disadvantage: the first is not profitable because of the high cost of electricity and the second produces toxic wastes. As can be seen, the secondary aluminum industry has been focused on the development of processes that overcome the mentioned limitations. One option is represented by the use of purified silica-based powders because the generated products in the treatment are not pollutants. Reports on

literature establish the effect of SiO₂ on the Mg removal as presented by Muñoz et al. [8] and Escobedo et al. [9], which is performed according to the following:



However, silica requires supplementary processes for its concentration resulting in additional costs. Additionally, the kinetics of the Mg removal using silica is relatively slow [10]. However, in recent studies Muñoz et al. [8, 11] have demonstrated the feasibility of Mg removal from aluminum molten alloys by injecting zeolite (containing more than 50 wt-% of SiO₂) and silica using an inert carrier gas. On the other hand, nanotechnology has been applied in foundry processes to improve mechanical properties of some materials according to studies in Al alloy treatment with nano-SiC powders in order to improve toughness [12]. Li et al. [13] improved the tensile strength and toughness as well as wear resistance with the addition of SiC nanopowders in the performance of traditional cast iron. Therefore, the nanotechnology may be used for removing undesirable elements during the adjustment of the final chemical alloys composition. Zeolite, with its high porosity, is ideal to be impregnated with amorphous SiO_{2(NP's)}. Further, amorphous SiO_{2(NP's)} can act as chemical catalyst to remove magnesium of molten aluminum improving the efficiency of the process. Due to the fact that the surface structural defects (i.e., undercoordinated units) strongly increase with decreasing nanoparticle size, diffusion of atomic species to the surface of nanoparticles significantly increases as suggested by Huynh et al. [14] and Carmona-Muñoz et al. [15]. Therefore, such considerations are appropriate for impregnating the porous inner part of zeolite. It is noteworthy that the nanoparticles can increase the surface area of zeolite to reduce the time of magnesium removal from molten aluminum alloys.

The aim of this work was the study of the Mg removal from a molten aluminum alloy by using mixtures of zeolite and amorphous SiO_{2(NP's)} as Mg remover agents. The capacity of Mg agents was evaluated by comparing its effect with that corresponding to the pure zeolite.

2. Experimental Procedure

2.1. Raw Materials and Characterization of Zeolites without Amorphous SiO_{2(NP's)}. The mineral zeolite was crushed in a ball mill and classified obtaining powders with an average particle size smaller than 150 μm. The chemical composition of the minerals was determined by atomic absorption spectroscopy, inductively coupled plasma atomic emission spectroscopy, and gravimetric method. Amorphous SiO_{2(NP's)} (Aldrich, 99.99%) with size smaller than 10 nm were selected for this work. These nanoparticles were characterized by TEM.

2.2. Impregnation and Characterization of Zeolites with Amorphous SiO_{2(NP's)}. The impregnation of zeolite with amorphous SiO_{2(NP's)} was reached mixing the selected amount of

nanoparticles (2.5, 5, 7.5, 10, or 12.5 wt-%) with zeolite for 30 min in ethanol and drying the mixture in a furnace at 80°C for 12 h. Samples of the enriched zeolites were analyzed by TEM and SEM and their surface area was measured by Autosorb 1-C using liquid nitrogen adsorption.

2.3. Selection of the Al Alloy and Mg Removal by Injection. The selected alloy was the A-332 aluminum base alloy (Al-11.64Si-0.338Fe-2.05Cu-1.6Mg-1.54Ni). An induction electric furnace, equipped with a silicon carbide crucible of 12 kg of capacity and temperature control, was used to melt and hold the alloy. Injection equipment, with devices to measure and control the gas and powder flows, was used to introduce the powder mixtures into the melt. The injection lance (internal diameter of 6.98 mm) was made of graphite and covered externally with refractory material. The selected parameters for the submerged powder injection experiments were argon (ultrahigh purity) flow of 4.4 L/min, powder flow of 16.2 g/min, mass of aluminum alloy of 8 kg, and aluminum alloy treatment temperature of 750°C. The lance was submerged at the 85% of the depth of the melt. The variable in the experiments was the composition of the powder mixtures zeolite-SiO_{2(NP's)} to be injected (0, 2.5, 5, 7.5, 10, or 12.5 wt-% of SiO_{2(NP's)}). The mass of the powders to be injected was calculated considering the SiO₂ as the solid reagent and spinel and silicon as products according to the chemical reaction (1). For each experiment, samples of the melt were obtained every 10 min and the produced dross (oxidized material) was collected at the end of the experiment. The solidified samples were analyzed by spark atomic emission spectrometry to determine their chemical compositions and a sample of the dross was analyzed by XRD. Finally, the quantity of dross was weighted and the efficiency of process was calculated with

$$\eta(\%) = \frac{\text{Mg}_{(\text{start})} - \text{Mg}_{(\text{end})}}{\text{Mg}_{(\text{start})}} * 100, \quad (2)$$

where $\eta(\%)$ is efficiency, $\text{Mg}_{(\text{start})}$ is initial Mg content (wt-%), and $\text{Mg}_{(\text{end})}$ is final Mg content (wt-%).

2.4. Characterization of Reaction Products by DRX and SEM of Samples after the Magnesium Removal by Injection. In order to determine the reaction products of slags formed during the injection of enriched zeolite with different percentages of SiO_{2(NP's)}, the samples were characterized by X-ray diffraction (XRD). In the case of semireacted particles founded in the metallic samples, these samples were characterized and analyzed by SEM and EDX, respectively.

3. Results and Discussions

3.1. Raw Materials Characterization. Figure 1(a) shows a SEM image of a particle of pure zeolite (irregular morphology). Two zones can be observed: (1) a clear zone (labeled LZ) corresponding to the Carlsbad twins and (2) a dark zone (labeled DZ) containing mainly Si and O and Al, Ca, Na, and K traces (classical chemical composition of Feldspar's group).

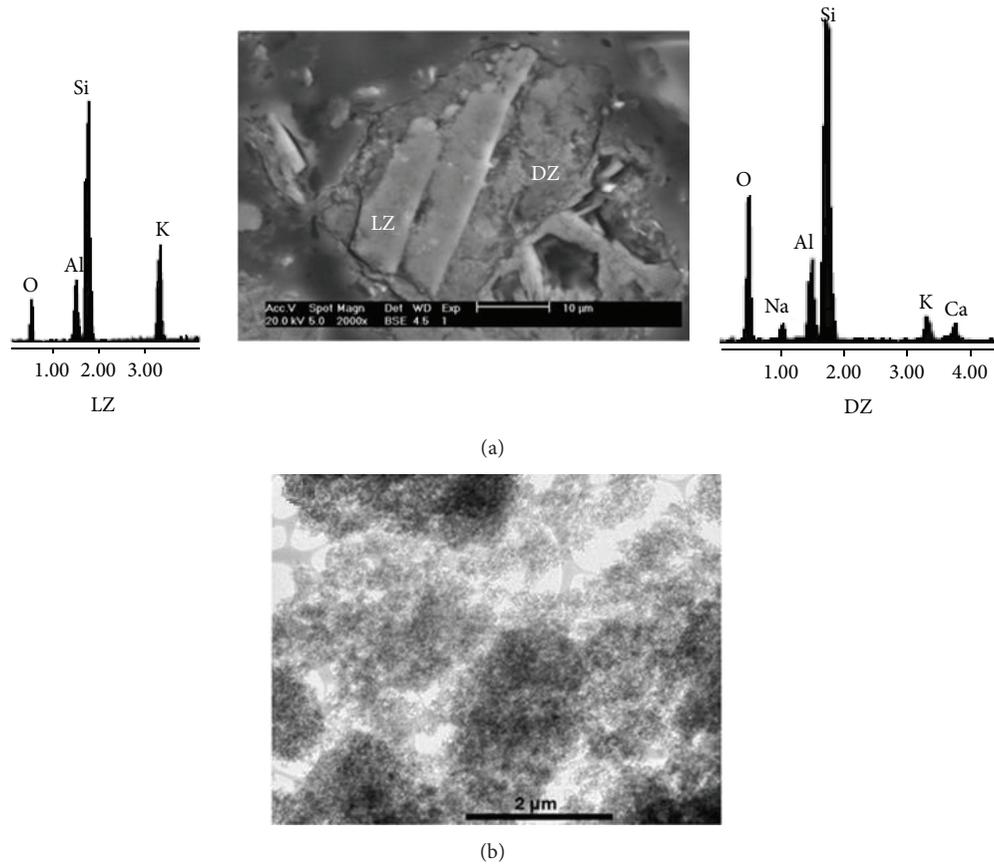


FIGURE 1: (a) SEM image of pure zeolite with Carlsbad twins and (b) TEM image of amorphous $\text{SiO}_2(\text{NPs})$ as received.

TABLE 1: Compounds identified by XRD.

Compound	Chemical formula
Heulandite	$\text{Ca}(\text{Si}_7\text{Al}_2)\text{O}_{18} \cdot 6\text{H}_2\text{O}$
Sanidine	KAlSi_3O_8

Table 1 shows the compounds identified in zeolite by XRD. Figure 1(b) shows a TEM image of pure nanoparticles. It is possible to observe agglomerates of nanoparticles of spherical morphologies. These nanoparticle characteristics allow high chemical reactivity because this kind of surfaces has a high specific surface energy.

3.2. Characterization of the Enriched Zeolites with Amorphous $\text{SiO}_2(\text{NPs})$. A sample of enriched zeolite (12.5 wt-% of $\text{SiO}_2(\text{NPs})$) was analyzed by SEM. Figures 2(a) and 2(b) show backscattered electron SEM images of the scanned area at high magnifications. Small agglomerates of less than $1 \mu\text{m}$ (Figure 2(b)) can be appreciated. Due to the size of the scanning spot, it is not appropriate to perform chemical analysis by EDX.

Examining other zones of the same sample, agglomerated particles of spherical morphology were observed (Figure 3). This fact can be due to the effects of sonication by ultrasound. The EDS analysis of the surface of the agglomerate shows that

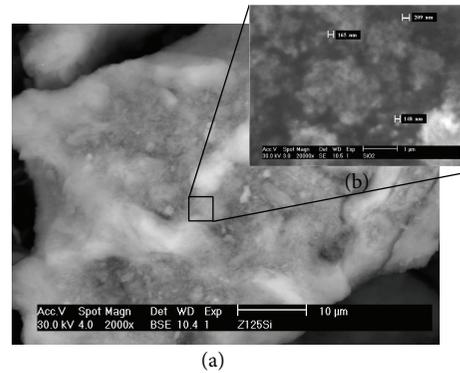


FIGURE 2: SEM images of (a) zeolite with 12.5% of $\text{SiO}_2(\text{NPs})$ and (b) $\text{SiO}_2(\text{NPs})$ agglomerates at high amplifications.

its chemical composition approaches SiO_2 . The advantage of such spherical morphology is that it increases the reaction kinetics due to its high surface energy.

Representative samples of enriched zeolite (2.5 and 12.5 wt-% of $\text{SiO}_2(\text{NPs})$) were analyzed by TEM. Studies such as that by Tomokazu and Hidekazu [16] suggest that by decreasing the silicoaluminates particle size ($<300 \mu\text{m}$), the rate of Mg removal decreases. However, this disadvantage can be avoided with the impregnation of $\text{SiO}_2(\text{NPs})$ on the

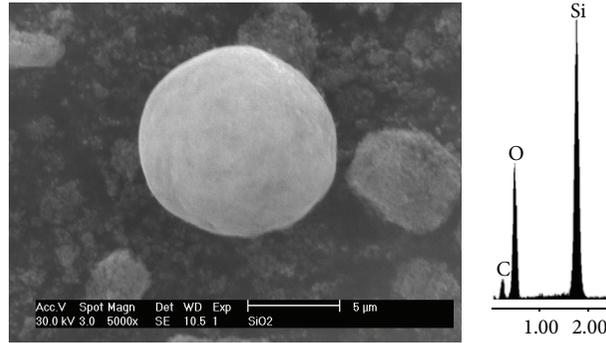


FIGURE 3: Secondary electron SEM image of a spherical particle rich in $\text{SiO}_2(\text{NPs})$.

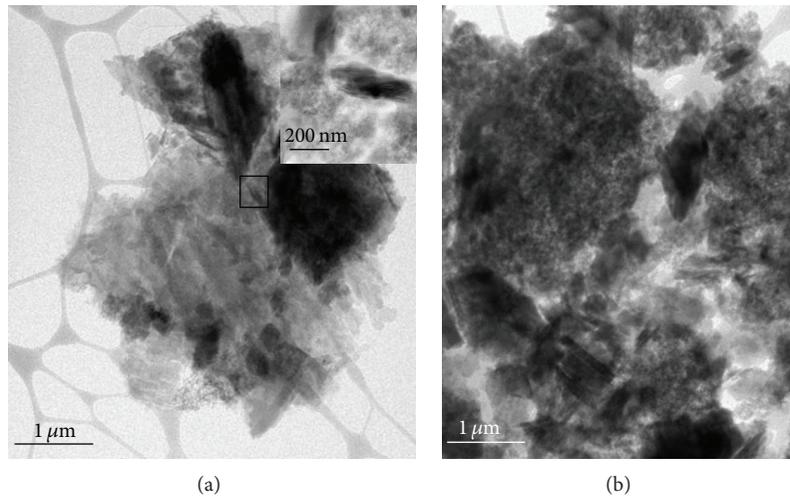


FIGURE 4: TEM images of enriched zeolites with $\text{SiO}_2(\text{NPs})$: (a) 2.5% and (b) 12.5%.

surface of the zeolite, changing in this way the surface area of the material. At high amplification, it is observed that the $\text{SiO}_2(\text{NPs})$ are immersed in a stretch gap approach to $1\ \mu\text{m}$ between zeolitic materials (dark zone) (Figure 4(a)). By contrast, the enriched zeolite with 12.5% of $\text{SiO}_2(\text{NPs})$ shows a high quantity of agglomerated nanoparticles (Figure 4(b)). Both surface aspects can affect the rate and time of Mg removal by injection.

The characterization of zeolite without and with 2.5, 5, 7.5, 10, and 12.5% of $\text{SiO}_2(\text{NPs})$ by Autosorb yielded important information that is necessary for understanding the role between the pores of zeolite and the $\text{SiO}_2(\text{NPs})$. As it can be seen in Table 2, the zeolite shows a pore size of 15 nm that is sufficient to get inside the $\text{SiO}_2(\text{NPs})$. These pores can be filled and enriched with nanoparticles with a size smaller than 15 nm. Likewise, the amorphous nature of nanoparticles can increase the rate of magnesium removal before a spinel shell is formed on the surface of zeolite. As a consequence, the zeolite acts as nanostructured transport medium. On the other hand, according to Table 2, the values of the surface area suggest the following aspects: in the zeolite with 2.5 to 5% of $\text{SiO}_2(\text{NPs})$ the nanoparticles are being introduced inside the pores and among spaces of the mineral, leading to a decrease in

the surface area. However, in the case of enriched zeolite with 7.5, 10, and 12.5% of $\text{SiO}_2(\text{NPs})$ the surface area increases. It means that the nanoparticles are agglomerated on the surface of zeolite because the pores are full of them. This is the reason of a higher amount of dross in the molten aluminum with 7.5, 10, and 12.5% of $\text{SiO}_2(\text{NPs})$ in comparison with that of the 2.5 and 5%.

3.3. Magnesium Removal by Injection of Zeolite without and with $\text{SiO}_2(\text{NPs})$. Figure 5 shows the reduction of the Mg content in the alloy as a function of the injection time. As it is seen in this figure when pure zeolite (without $\text{SiO}_2(\text{NPs})$) is injected, the final content of Mg in the alloy, after 70 min of injection, is 0.7 wt-% of Mg. The best result was obtained when zeolite + 2.5% $\text{SiO}_2(\text{NPs})$ was injected. In this case, the Mg content in the alloy was 0.1 wt-% after only 47 min of injection, which is in agreement with the standard, and the final Mg content, after 70 min of injection, reaches 0.0002 wt-%. Similar effects occur when zeolite + 5% $\text{SiO}_2(\text{NPs})$ is used (52 min of injection to reach 0.1 wt-% of Mg). By contrast, the Mg removal decreases when zeolite enriched with 7.5 to 12.5% of $\text{SiO}_2(\text{NPs})$ is used. In these cases, the target of 0.1 wt-% of Mg is not reached, even by injection for 70 min.

TABLE 2: Measurements of surface area of zeolite without and with amorphous $\text{SiO}_2(\text{NPs})$.

Material	$\text{Mg}_{(\text{end})}$ (wt-%)	$W_{(\text{oxidized material})}$ (kg)	η (%)	Area surface (m^2/g)	Pore size (nm)
Zeolite	0.5007	1.210	68.75	22.09	15
Zeolite: 2.5% $\text{SiO}_2(\text{NPs})$	0.0002	0.058	99.98	20.98	12
Zeolite: 5% $\text{SiO}_2(\text{NPs})$	0.0101	1.100	99.25	18.47	13
Zeolite: 7.5% $\text{SiO}_2(\text{NPs})$	0.0500	1.130	98.37	21.88	14.5
Zeolite: 10% $\text{SiO}_2(\text{NPs})$	0.1040	1.600	96.87	22.94	17
Zeolite: 12.5% $\text{SiO}_2(\text{NPs})$	0.1090	1.860	93.18	25.98	19.5

$\text{Mg}_{(\text{end})}$: final Mg content in the alloy.

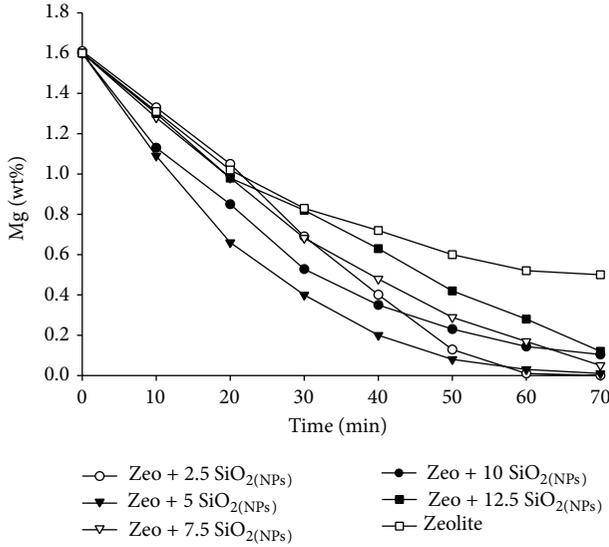
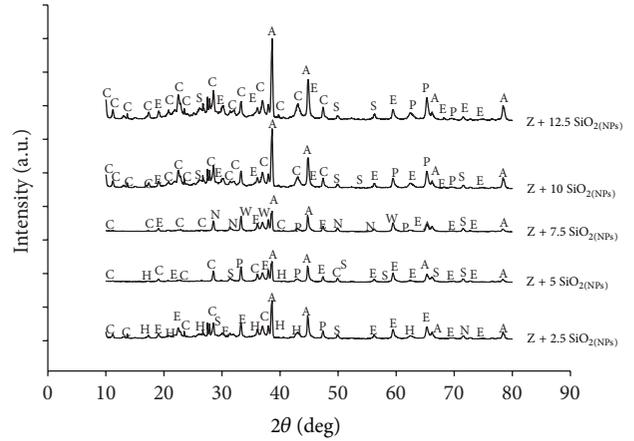


FIGURE 5: Mg removal from the alloy as a function of injection time using zeolite and zeolite with different percentages of $\text{SiO}_2(\text{NPs})$.

Comparatively, the $\text{SiO}_2(\text{NPs})$ enriched zeolite increases the efficiency of the chemical reaction to remove Mg due to the size and amorphous nature of the $\text{SiO}_2(\text{NPs})$. This suggests that the nanoparticles improve the surface energy of the zeolite and its amorphous nature becomes as chemical catalyst. It should be noted that the initial content of Mg in this research work is considerably high (1.6 wt-% Mg) with regard to that in other reports in the literature [4, 10] that starts from 1 wt-% of Mg using enriched zeolites with different percentages of SiO_2 as bulk. Likewise, removal times over 60 min in order to reach 0.1 wt-% of Mg in the alloy are as shown by Muñoz-Arroyo et al. [11]. This means that the Mg removal method using nanoparticles improves the efficiency of the process and decreases the removal time. Besides, the power consumption can be lower in the process of Mg removal.

3.4. Characterization of Reaction Products during the Magnesium Removal by Injection. The slags were analyzed by X-ray diffraction in order to found the products of the reaction between the enriched zeolite with $\text{SiO}_2(\text{NPs})$ and the elements of the molten bath (Figure 6). The XRD patterns of the slags show peaks corresponding to spinel, clinoptilolite, periclase, anorthite, and so forth. Elements such as aluminum



A = aluminum = Al

S = silicon = Si

E = spinel = MgAl_2O_4

C = clinoptilolite = $\text{Ca}_{8,16}\text{Si}_{36}\text{O}_{72} \cdot (\text{H}_2\text{O})_{21,8}$

P = periclase = MgO

H = anorthite = $\text{Ca}(\text{Al}_2\text{Si}_2\text{O}_8)$

N = nantroquite = CuCl

W = wurtzite = AlN

FIGURE 6: X-ray diffraction patterns of slags from the process where zeolite is with nanoparticles of SiO_2 .

and silicon were also detected and belong to the aluminum alloy. It is noticeable that in the slag from the zeolite with 7.5% $\text{SiO}_2(\text{NPs})$ were identified wurtzite and nantroquite. It is postulated that both compounds are formed from impurities of the base magnesium alloy that was used to adjust the content of magnesium in the Al-Si alloy.

The metallic specimens obtained during injection were analyzed by scanning electron microscopy to understand the kinetics of the magnesium removal. As can be seen, in Figure 7(a), a particular specimen that shows a semireacted particle of zeolite obtained in the samples treated with enriched zeolite with 5% nanoparticles injected for 20 min was found. According to the corresponding EDX spectra, the chemical composition of the shell is approaching the stoichiometry of spinel. Meanwhile, the center of the particle belongs to the chemical compositions of zeolite, as shown in Figures 7(b) and 7(c). During the magnesium removal, the

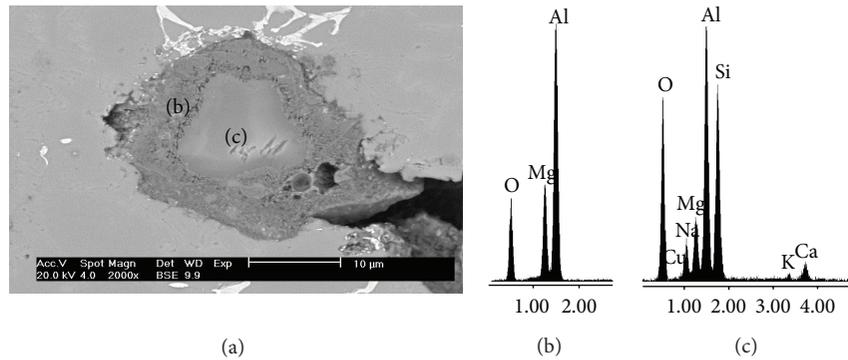


FIGURE 7: (a) Image of backscattered electron for a semireacted particle of enriched zeolite with 5% of SiO_2 nanoparticles, obtained after 20 minutes of injection; EDX of (b) shell and (c) center of particle.

reaction products form a shell on the surface of enriched zeolite with $\text{SiO}_2(\text{NPs})$. Hence, the reaction rate is slow due to the nature of the process; a shell of reaction products is formed on the particles and makes the mass transfer difficult.

On this viewpoint, it is postulated that the formation of a stable shell on the surface will be quickly formed as a stable diffusive barrier among dissolved Mg in the liquid bath of aluminum and shell on the zeolite (spinel) that reduces the removal kinetics. Finally, when nanoparticles are in contact among them, they tend to reduce their free energy reducing their surface energy. Then, at high temperature inside the molten bath, the nanoparticles coalesce (sintering of the nanoparticles) reducing substantially the reaction area. This is the reason why the efficiency of magnesium removal decreases and a higher amount of dross in the molten aluminum with 7.5, 10, and 12.5% of $\text{SiO}_2(\text{NPs})$ is formed.

4. Conclusions

The use of mineral zeolite enriched with 2.5 wt-% of $\text{SiO}_2(\text{NPs})$ provided higher Mg removal from the molten alloy than that obtained using pure zeolite. The kinetics of magnesium removal decreases as the percentage of $\text{SiO}_2(\text{NPs})$ increases, promoting the formation of a dross rich in intermetallic compounds.

The density, high surface area, and feasibility of ion exchange of the enriched particles allow better powder-liquid contact improving the process kinetics.

The methodology presented in this study is feasible to be applied on an industrial scale.

Conflict of Interests

The authors declare that there is no conflict of interests regarding the publication of this paper.

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