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Research Article

Influence of Processing Conditions on the Thermal Stability and Mechanical Properties of PP/Silica-Lignin Composites

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Functional silica-lignin dual fillers were obtained via mechanical grinding of the components (Syloid 244 silica and kraft lignin). Of particular importance here is the fact that lignin is a natural polymer and particularly that it is a waste by-product of paper production, whose recycling is highly desirable. The product underwent comprehensive dispersive-morphological and thermal analysis. SiO_2 -lignin hybrid fillers were also used in polypropylene-based composites, extruded via corotating a twin screw machine with different screw speeds. The thermogravimetric data obtained for the extrudates confirmed that the application of the lignin into PP produces a significant char residue. Addition of silica to lignin via this new hybrid formulation has a positive effect on the thermal stability of PP/silica-lignin composites, which can be seen even when observing the temperature for the maximum rate of weight reduction. Tensile test results show that the addition of silica by means of dual filler incorporation improves the mechanical parameters in comparison with pure PP and PP/lignin composite.

1. Introduction

The continued growth of research in advanced materials engineering and polymer technology yields the possibility of carrying out interdisciplinary work related to obtaining innovative and functional hybrid materials. Currently, it is important for economic and environmental reasons to use natural polymers as organic precursors that are derived from broadly defined biomasses or other sources. Particularly, noteworthy are the systems with silica, which represents a popular, relatively inexpensive inorganic filler or support, and biopolymers, for example, lignin [1–3] and its derivatives, including lignosulfonates [4, 5].

Reports in the literature indicate the possible use of lignocellulosic materials, including pure lignin, as fillers in a wide group of polymers. These include both highly polar (poly(ethylene terephthalate), PET, poly(ethylene oxide), PEO) [6, 7] and hydrophobic (polypropylene, PP) [8–10] polymer matrices. Studies have also been carried out with

polylactide (PLA) [11–14] and poly(vinyl chloride) [15, 16]. The latter showed better compatibility of PVC with lignin for unplasticized material than for the plasticized form.

The use of lignin as a polymer filler depends largely on its thermal stability. Thermal decomposition of the biopolymer depends mainly on the type of lignin, the temperature of the process, and the heating rate [17]. According to the available sources, the thermal decomposition of lignin takes place in the temperature range between 200 and 500°C [17–20].

Below 150°C the physically bound water evaporates, and then further degradation of the biopolymer chain occurs, which takes place in two stages [18]. The first starts at relatively low temperatures, approximately 200–275°C, and is connected to the thermal decomposition of lignin, involving the formation of new bonds as a consequence of cross-linking reactions. The highest stage of decomposition of lignin takes place at a temperature of ~400°C, where it creates aromatic hydrocarbons, phenolics, and compounds containing phenolic groups [17]. The thermal stability of lignin is therefore

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relatively high at plastic processing temperatures, so it can be used as a material for increasing the stability of the product [19]. The mass loss of lignosulfonate (lignin derivative) was significant and reached 60% relative to the initial mass of the sample [4]. The thermogravimetric curve recorded for lignosulfonate exhibits two characteristic stages. The first, below 200°C, results from endothermic water desorption from the sample. The second, more severe mass loss (~40%), starting at a temperature of about 200°C, reflects the gradual degradation and consequent fragmentation of the compound. The results are in agreement with data given by Brebu et al. [21] and Lemes et al. [22].

Other frequently used biopolymers that also widely occur, often as waste, are chitin, chitosan, and cellulose. Chitin is a biopolymer with relatively high thermal stability, even at 380°C [23–25]. However, the thermal degradation of chitin is dependent on several factors including acetylation, degree of crystallinity, and size of crystallites, and it is also strongly related to the origin of the material. Deacetylation decreases the thermal stability of chitin, and thus chitin has higher thermal stability than chitosan. Nam et al. [25] proved that thermal decomposition of chitin nanofibers follows a singlestep degradation process, although chitosan nanofibers with a deacetylation degree (DD) greater than 50% exhibited a two-step mechanism. This thermal property is the driving force for developing new chitin-based materials and chitin processing routes at high temperatures using the principles of hydrothermal synthesis and extreme biomimetics [26].

In turn, literature data indicate that the thermal stability curve of chitosan presents two significant decreases in weight. The first, at ~90°C, associated with a weight loss of ~6% of the sample, is due to the evaporation of physically bound water on the surface [27, 28]. The second, starting at approximately 245°C and ending at approximately 580°C, involves ~80% decrease in the mass of the sample. This decrease is related to the thermal degradation of the polymer chain of chitosan. The question of thermal stability is crucial when planning future-oriented processing of this material in industry [29].

A number of studies have also been carried out with cellulose [30]. TGA curves show three stages of degradation of cellulose. The first of these, at 200–300°C, is associated with a partial disintegration of biopolymer and water loss (a weight loss of about 4%). In a further step, at a temperature of 300–360°C, the sample undergoes a weight loss of about 55% [31, 32]. The last stage, with a sample weight loss of about 29%, occurs gradually at 360–440°C. The second stage which is of rapid loss plays a key role in defining the stability and fire retardancy of cellulose [31].

Many studies have been focused on lignin precursors as a factor in char formation during polymer burning, together with the addition of inorganic filler, but no one has combined these two materials as a single hybrid (duo) filler. Therefore, the objective of this study is to determine the influence of the presence of silica and lignin in a dual phase-like filler on the thermal degradation of polypropylene during melt-compounding. Additionally, the impact of the filler on processing degradation, as a function of extrusion parameters (screw speed), will be discussed. The effect of processing degradation on the composite's performance will be evaluated

based on rheology (MFR), mechanical properties, and thermogravimetric measurements.

2. Materials and Methods

2.1. Materials. The organic component kraft lignin was supplied by Sigma-Aldrich, USA. The properties of the lignin are described in detail in our previously published papers [33, 34]. For the production of silica-lignin hybrid fillers, the commercial silica Syloid 244 from W.R. Grace & Co., USA, was used. The polymer matrix used was isotactic polypropylene (iPP) (Basell Orlen Polyolefins Sp. z o.o., Moplen HP 500 N, Poland).

2.2. Preparation of Hybrid Materials Based on Silica and Lignin. Silica-lignin fillers were produced via a grinding and mechanical-alloying-like method. To combine the SiO_2 and lignin, a mechanical process was used whereby the initial powders (kraft lignin and silica Syloid 244) were ground and simultaneously mixed using a Pulverisette 6 Classic Line planetary ball mill (Fritsch, Germany). This process was described in detail in our previously published work [33].

Three types of hybrid fillers were prepared, differing by their lignin content. SiO_2 -lignin hybrid fillers were produced with the ratio of precursors equal to 5:1, 2:1, and 1:1.

2.3. Physicochemical Characteristics of Fillers

2.3.1. Dispersive-Morphological Properties. Dispersive characteristics of pure precursors and silica-lignin hybrid fillers were determined with the use of a Zetasizer Nano ZS and Mastersizer 2000, both made by Malvern Instruments Ltd. (UK), employing the methods of dynamic light scattering (DLS) and laser diffraction, respectively. Measurements of particle size were repeated at least three times for each sample.

Information on grain morphology, particle shape, character of agglomerations, and dispersion was obtained from scanning electron microscope (SEM) images (Zeiss EVO40, Germany). Prior to the testing, the samples were coated with Au for a time of 5 seconds using a Balzers PV205P coater.

2.3.2. Thermogravimetric Analysis. Thermogravimetric analysis was performed using a Jupiter STA449 F3 (Netzsch, Germany). Samples weighing approximately 10 mg were placed in an ${\rm Al_2O_3}$ crucible and heated at a rate of 10° C/min from 30 to 1000° C in a nitrogen atmosphere, at a flow rate of $40 \, {\rm cm}^3$ /min.

2.4. Preparation of PP/Silica-Lignin Composites via Extrusion. Isotactic polypropylene (iPP) was supplied by Basell Orlen Polyolefins Sp. z o.o. (Moplen HP 500 N) and had a melt flow rate (MFR) of 12 g/10 min at 230°C. The processing of PP/silica-lignin composites was conducted into two steps. First, each of the three types of silica-lignin hybrid fillers (differing in lignin content) was mixed separately with PP in a molten state using a twin screw extruder. All samples and their composition are described in Table 1.

Next, the pelletized composites were shaped into dog bone samples using an injection molding technique. At the beginning of the extrusion process, the main components

TABLE 1: Formulations of PP-based composites.

| Sample notation | Composition (wt.%) | | | |
|--|--------------------|--------------|-------------------|--|
| Sample notation | Polypropylene | Kraft lignin | Silica Syloid 244 | |
| PP | 100.0 | _ | _ | |
| PP/lignin | 90.0 | 10.0 | _ | |
| PP/SiO ₂ -lignin (1:1, w/w) | 90.0 | 5.0 | 5.0 | |
| PP/SiO ₂ -lignin (2:1, w/w) | 90.0 | 3.3 | 6.6 | |
| PP/SiO ₂ -lignin (5:1, w/w) | 90.0 | 1.7 | 8.3 | |

were preweighed and mixed in granular (PP) and powder states (silica-lignin hybrid fillers) in a rotating container. In the next operation, the prepared batches were dried in an air-circulating oven at 80° C for 12 h. After drying, all mixed compounds were fed into a corotating twin screw extruder (Zamak 16/40 EHD) with a barrel temperature of $155-185^{\circ}$ C. The plasticizing unit has screws with a diameter of 16 mm and an L/D ratio of 40 and is equipped with four kneading disc blocks and mixing elements. The screw configuration and detailed information about screw sections and the design of the mixing elements are supplied in Figure 1.

During extrusion, all composites as well as virgin polypropylene were extruded under four different screw rotation speeds: 100, 200, 300, and 400 rpm. The extrudates were cooled under dry conditions in atmospheric air to prevent any moisture absorption. Next, the extrudates were reground using a laboratory grinder (SC-1411 Shini), operating at a low rotor speed of 30 rpm to prevent overheating and further organic phase decomposition via high shear stress concentration.

Finally, the neat PP and the compounds were injection-molded into dumbbell-shaped specimens using an ENGEL 80/25 HLS injection molding machine, at a mold temperature of 30° C. The barrel temperature was set as 175° C, 180° C, 185° C, and 190° C (nozzle). The injection speed was low, at 50 mm/s. The injection speed used was sufficient for cavity filing and probably did not cause any overheating of the polymer phase and degradation of macromolecules by extended shear forces.

For tensile test bar preparation, a cavity mould with a thickness of 3 mm was used. The main dimensions of the utilized specimens were 115 mm total length, 25 mm gauge length, and 6 mm width.

2.5. Polymer Composite Testing. The mass melt flow rate of all extrudates was evaluated using the melt indexer Dynisco Polymer, TEST 4004, under 2.16 kg and a temperature of 230°C.

For TGA analysis, only the samples obtained with screw speeds of 100 rpm and 400 rpm were selected. Extrudates were directly tested by thermogravimetric analysis using a TG 209 FI LIBRA analyzer (Netzsch, Germany) in a nitrogen atmosphere. The heating rate was 10°C/min and the nitrogen flow rate was 60 cm³/min. The temperature ranged from 30 to 700°C.

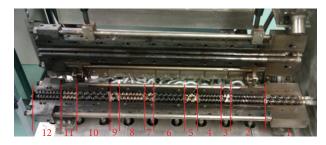


FIGURE 1: View of the opened plastisizing unit with screws working in a corotating mode. Zone 1: feed area (32 mm screw stroke), zones 2, 4, 6, 8, and 11: transporting sections, zones 3, 5, 7, and 9: kneading and mixing elements, zone 10: degassing unit, and zone 12: metering section (16 mm screw stroke). Compression factor = 2.

Tensile properties (yield strength, tensile strength, elongation, and modulus) were determined using an Instron 4481 universal testing machine at a crosshead speed of 50 mm/min, at room temperature, in accordance with ISO 527-1, 2. The samples were not conditioned prior to testing, because for polyolefins the influence of moisture on mechanical properties is negligible.

3. Results and Discussion

3.1. Dispersive-Morphological Properties and Thermal Stability of Silica-Lignin Hybrid Fillers. Syloid 244 reveals the presence of primary particles with diameters close to 100 nm, which show a tendency to form aggregates ($<1\,\mu$ m) and agglomerates ($>1\,\mu$ m). Silica exhibits different dispersive-morphological properties (see Table 2 and Figure 2(a)).

As follows from the data presented in Table 2, with the increasing content of lignin in the hybrid filler, the number of larger particles increases. This tendency is evident for the hybrid fillers based on Syloid 244 silica. The parameters from the Mastersizer 2000 describing the percentage contribution of particles of certain diameters show an increase. It should be noted that the commercial kraft lignin used in the study contains particles of sizes representing a wide range, which indicates the possibility of formation of large agglomerate structures. The presence of primary particles and secondary agglomerates is also confirmed by SEM images.

Figures 2(a) and 2(b) present the SEM images of silica and lignin, respectively, while Figures 2(c)–2(e) show images of silica-lignin hybrids obtained with the use of different weight ratios of biopolymer to silica.

Thermal stability measurements for the silica, lignin, and inorganic-organic materials were also performed. Figure 3 shows the TGA curves obtained for the precursors and the resulting silica-lignin dual fillers. Syloid 244 silica shows high thermal stability: a mass loss was observed at 100°C associated with the loss of water physically bound with the precursor. In the case of lignin, the thermogravimetric curve shows a clearly larger mass loss in comparison with silica. The TGA curve recorded for lignin indicates a significant mass loss of about 65% relative to the initial mass of the sample. The

Table 2: Dispersive characteristic of pure precursors (silica and lignin) and silica-lignin hybrid fillers.

| | Dispersive properties | | | | |
|---------------------------------|---|--|--------|--------|--|
| Sample | Particle size distribution from Zetasizer Nano ZS (nm) | Particle diameter from Mastersizer 2000 (μ m) | | | |
| | Tarticle size distribution from Zetasizer Ivano Z5 (IIII) | d(0.1) | d(0.5) | d(0.9) | |
| Syloid 244 + kraft lignin (1:1) | 106-295; 1990-5560 | 2.8 | 9.2 | 20.0 | |
| Syloid 244 + kraft lignin (2:1) | 91–220; 1990–4800 | 2.7 | 9.0 | 19.9 | |
| Syloid 244 + kraft lignin (5:1) | 79–122; 1720–4150 | 2.8 | 8.7 | 19.5 | |
| Syloid 244 | 39–295; 1720–2670 | 2.0 | 7.2 | 18.1 | |
| Kraft lignin | 1990-5560 | 5.0 | 12.5 | 38.6 | |

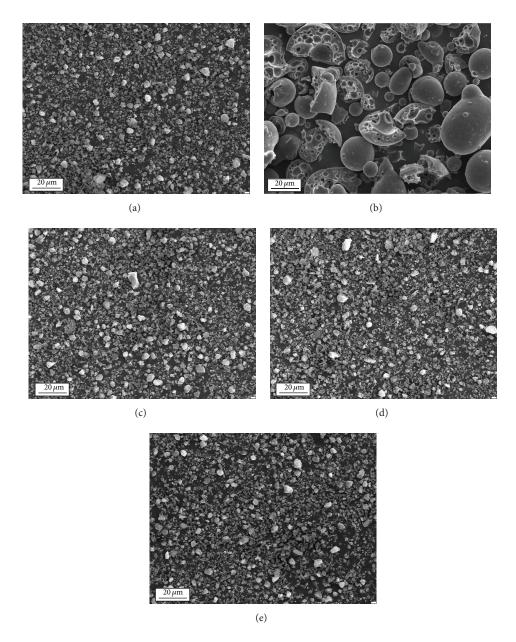


Figure 2: SEM images of silica Syloid 244 (a), kraft lignin (b), and silica-lignin hybrid fillers with weight ratio equal to 1:1 (c), 2:1 (d), and 5:1 (e).

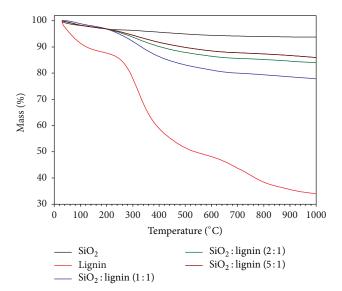


FIGURE 3: Thermal degradation curves versus temperature for pure silica and lignin as well as for silica-lignin hybrid fillers.

individual steps of the mass loss at particular temperatures for lignin are presented in Table 3.

Figure 3 also presents the TGA curves obtained for the prepared silica-lignin hybrid fillers. The final hybrid materials show rather greater thermal stability than is exhibited by pure lignin. The thermal analysis showed that the higher the content of lignin in the product, the poorer its thermal stability. Moreover, with an increase in lignin content, the TGA curves become more similar to those of pure lignin, and the mass loss is larger. The promising TGA results obtained at this stage of the study suggest that the silica-lignin products may be used as a new generation of polymer dual fillers.

3.2. Thermogravimetry Analysis of Composites. Figure 4 shows the basic thermal degradation curves, measured in nitrogen, as a function of increasing temperature, obtained for extrudates extruded at 100 rpm screw speed. We can see in this figure that the mass loss for pure PP is much more rapid than that for the composite with lignin at temperatures up to 430°C. Next, the curve for PP shows visible thermal degradation below 470°C without char formation. On the other hand, for the composite with lignin, we observe a curve with char yield formation. This feature is connected with the aromatic chemical structure of lignin, which may give a very high char yield, which is still high even at 700°C [35]. Other curves obtained from the blends with hybrid fillers with silica-lignin ratios of 1:1 and 5:1 possess higher thermal stability, up to 450°C, than the other tested materials. This may be connected with the relatively high surface area of the silica filler. The presence of silica in polymer matrices leads to the formation of an interlayer zone at the filler surface and thus the immobilization of polymeric chains on the filler surface. This feature increases the thermal stability of the polymeric phase. Surprisingly, the sample with a silica-lignin ratio of 2:1 in the hybrid structure exhibits markedly lower thermal stability.

Table 3: The individual steps of the mass loss in relation to particular temperatures for lignin.

| Stage | Mass loss (%) | Temperature (°C) | Reason/cause |
|-------|------------------|---------------------|---|
| 1 | 12 | 20-150 | Desorption of physically bound water with the product surface |
| 2 | 40 | 150-550 | Thermal decomposition of lignin macromolecule |
| 3 | 13 | 550-1000 | Fragmentation combined with the final thermal decomposition of the compound |

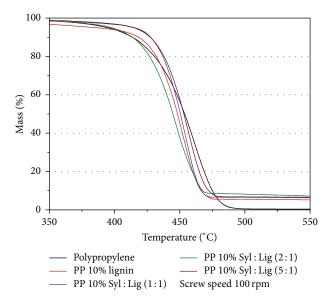


FIGURE 4: Thermal degradation curves versus temperature for pure PP and its blends with lignin and hybrid fillers, after extrusion with 100 rpm of screw speed.

In addition, Figure 5 shows curves obtained for the same materials but processed under higher shear forces, with a screw speed of 400 rpm. It can be clearly noted that the thermal decomposition T_D , the temperature at which half of the initial mass of the sample is lost, is especially low for polypropylene filled with lignin. This composite has a degradation temperature approximately 20°C lower than that of the other tested materials, previously treated in the extruder under the same conditions.

Table 4 summarizes the TGA and DTG experimental data, including the thermal degradation temperatures at which 5% and 50% of the initial mass are lost ($T_{D.5\%}$ and $T_{D.50\%}$) and the percentage of char produced at 700°C for all examined samples. Also, the temperature for the maximum rate of weight loss, $T_{\rm MR}$, is given in Table 4. We can see that pure PP degrades completely without any char formation, with the residual of the original sample mass being only 0.3%.

The thermal behavior of the composite with lignin is different. The tested samples revealed a significant char residue (4.19 wt.% and 3.17 wt.% for samples extruded at

PP/SiO₂-lignin (5:1)

| Sample | Screw speed | T _{D5%} (°C) | $T_{D50\%}$ (°C) | T_{MR} (°C) | Char (wt.%) |
|-----------------------------------|-------------|-----------------------|------------------|------------------------|-------------|
| PP | _ | 397 | 453 | 445 | 0.30 |
| PP/lignin | 100 rpm | 387 | 448 | 454 | 4.19 |
| PP/SiO ₂ -lignin (1:1) | | 415 | 450 | 455 | 5.80 |
| PP/SiO ₂ -lignin (2:1) | | 398 | 445 | 447 | 7.00 |
| PP/SiO ₂ -lignin (5:1) | | 423 | 456 | 460 | 6.17 |
| PP/lignin | | 377 | 440 | 446 | 3.17 |
| PP/SiO ₂ -lignin (1:1) | 400 rpm | 415 | 453 | 457 | 6.08 |
| PP/SiO ₂ -lignin (2:1) | | 420 | 452 | 454 | 3.61 |

454

423

Table 4: Comparison of the thermal decomposition temperatures of PP/silica-lignin composites under different extrusion conditions char wt.% formed during the test.

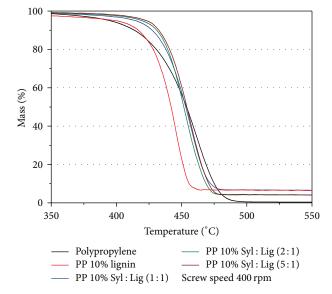
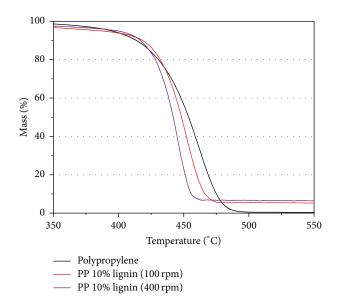


FIGURE 5: Thermal degradation curves versus temperature for pure PP and its blends with lignin and hybrid fillers, after extrusion with 400 rpm of screw speed.



456

3.77

FIGURE 6: Thermal degradation curves versus temperature for pure PP and its blends with lignin after extrusion with 100 and 400 rpm of screw speed.

100 rpm and 400 rpm resp.). Lignin has a thermal degradation temperature about 50°C less than that of PP, and it produces a very high quantity of char in an inert atmosphere (see Figure 3). This property was also confirmed by Canetti et al. [36]. When polypropylene/lignin composites start to degrade, the charring aromatic radicals from lignin [37] reduce the PP degradation rate (T_{MR}) and produce char as a protective coat (see Figure 6).

Based on these results, it is clear in our opinion that thermal decomposition of polypropylene with kraft lignin is greatly influenced by the shear rate during extrusion. Without silica protection, the heat (additionally generated by intermolecular friction) and shear forces cause some negative effects on the lignin structure and lead to a very low thermal decomposition temperature ($T_{D\ 50\%}$). This effect is also seen in the decrease in the temperature of maximum rate of weight loss ($T_{\rm MR}$) for PP/lignin composites. Based on this finding, treating thermoplastic composites with lignin under a very high screw speed is not recommended. For the remainder

of the tested samples, in general, the char yield increases with an increase in the quantity of inorganic additive. Some deviations were observed for the sample of PP/silica-lignin (1:1) at 400 rpm screw speed and may have their source in the degree of homogeneity of the composite samples. Moreover, the addition of an inorganic component such as silica generally increased the initial thermal decomposition temperature ($T_{D\ 5\%}$) by about 15–20°C, with a significant char yield (see Figure 7).

3.3. Mechanical Parameters and Melt Flow Rate Index. Melt mass flow rate is presented in Figure 8. For composite PP/lignin, for every extrusion step, a gradual increase in the MFR index is observed. This is a result of the thermomechanical degradation of PP macromolecules and the lignin filler. For composites with the hybrid filler, an unexpected increase in flow rate is observed in samples processed at 100 rpm and 400 rpm screw speed. This is probably the result of poor homogeneity in the composites. For the composites with the

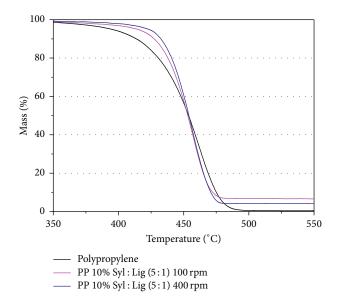


FIGURE 7: Thermal degradation curves versus temperature for pure PP and its blends with hybrid filler containing 20% of lignin, made with 100 and 400 rpm of screw speed respectively.

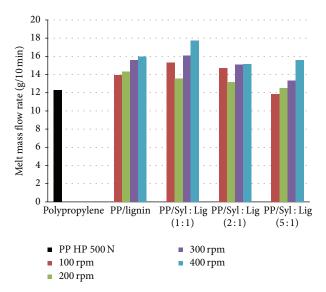


FIGURE 8: Mass melt flow rate for all tested materials versus applied screw speed.

highest amount of silica, the thermomechanical degradation processes during extrusion are hidden or limited by the interaction between the large BET surface area $(244\,\mathrm{m}^2/\mathrm{g})$ and polymer molecules. These interactions occur due to the formation of an oriented layer on the filler particle and the consequent reduction in Brownian motion of the molecules.

The variations in tensile strength, Young's modulus, and elongation at break as a function of lignin and hybrid filler content are shown in Figures 9–11.

The tensile strength is observed to increase slightly with the addition of filler. As a rigid filler, having a high BET surface area, the silica is also a reinforcing agent. Surprisingly,

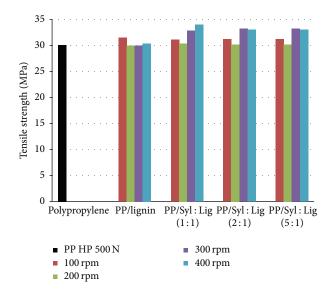


FIGURE 9: Tensile strength obtained during static uniaxial deformation versus applied screw speed.

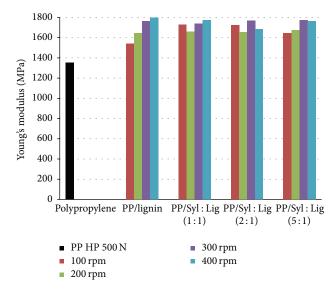


FIGURE 10: Young modulus obtained during static uniaxial deformation versus applied screw speed.

application of the highest screw speed results in visible positive changes in both tensile strength and stiffness of the composites. The explanation of these phenomena may be connected with the better dispersion of the filler achieved during extrusion at the highest screw speed. Fine filler particles embedded in the polymer may create a higher volume of the matrix at the intermediate layer created by the filler and may also act as a nucleating agent (especially in the case of hybrid fillers containing silica).

By contrast, there was a significant reduction in the strain at break. This may be due to the introduction of a rigid filler with particles on the macroscale. These particles are unable to deform, and under high elongation some voids appear at the filler-polymer interphase. This may lead to crack

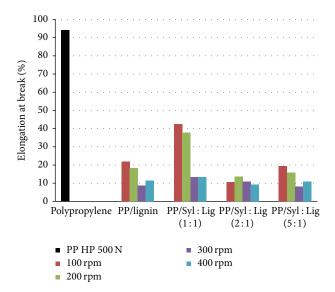


FIGURE 11: Elongation at break obtained during static uniaxial deformation versus applied screw speed.

formation and reduction in matrix plasticity. Moreover, the rapid decrease in elongation at break appeared at a rather high loading level of particular fillers. Very similar results were observed by Hu et al. [38] in polyethylene filled with 40% kraft lignin. Those authors tried to overcome this unfavorable effect by the addition of compatibilizers, mainly EVA, MAPE, and SEBS. The addition of EVA to the composite formulation enabled an increase in the elongation at break by 67%, and this was the best achieved result. In our work, we achieved an increase in the elasticity by more than 100% for composites with hybrid filler (kraft lignin combined with silica in a ratio of 50:50 wt.%) processed at 100 rpm and 200 rpm screw speed.

For future applications, we also believe that this unfavorable property can be limited by the use of block or random PPE copolymer as a polymer matrix. Usually, the presence of polyethylene macromolecules gives more flexibility and much higher plasticity to composite systems.

4. Conclusions

Advanced silica-lignin hybrid fillers have been obtained using as precursors Syloid 244 silica and kraft lignin. The tested hybrid components, as well as SiO₂-lignin dual fillers, have been thoroughly characterized by the determination of their dispersive-morphological properties and thermal stability. With the increasing content of lignin in the hybrid filler, the number of larger particles increases. This tendency is evident for the hybrid fillers based on Syloid 244 silica. The final hybrids show rather greater thermal stability than what is exhibited by pure lignin. The thermal analysis showed that the higher the content of lignin in the product, the poorer its thermal stability.

In addition, the novel hybrid so-called "dual phase fillers" were tested as a precursor in the retention of thermal degradation of polymer composites with lignin in polypropylene.

The presence of silica in the blend is able to bring about a significant shift in the initial degradation temperature, which corresponds to 5% weight loss of the polypropylene/lignin systems. Thus, the processing of green polymer composites via extrusion with relatively high screw speed could be protected by a fraction of active silica with a high BET surface area. As we demonstrated, the new type of dual phase silicalignin fillers has a positive impact on the main mechanical parameters. We noted a very positive effect of combining silica with kraft lignin, in the form of a sharp increase in elongation at break compared with composites filled with lignin. This may be connected with better dispersion of dual phase filler particles, together with thermal ageing protection of the lignin phase.

Conflict of Interests

The authors declare that there is no conflict of interests regarding the publication of this paper.

Acknowledgment

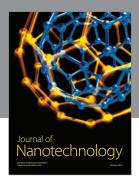
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