Influence of the Inner and Outer Secondary Air Ratios on the Combustion Characteristic and Flame Shape of a Swirl Burner with a Prechamber

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The swirl burner with a prechamber was used in a 14 MW pulverized-coal combustion experiment to investigate the influence of inner and secondary air ratios (ISA/OSA) on the combustion characteristic and flame shape in this work. The temperatures and species concentrations in the prechamber were measured via the flue gas analyzer and thermocouples. The flame shape beyond the prechamber outlet was captured by using a high-speed camera. The results showed that the combustion efficiency was increased and low nitrogen combustion was achieved by adopting the swirl burner with a prechamber. The high temperature corrosion and slagging phenomenon did not occur in the prechamber. The influence of ISA/OSA on temperature and species concentration profiles at different areas in the prechamber was different. The flame shape size exhibited an inflection point with increasing ISA/OSA. Considering, comprehensively, the temperature peak, near wall temperature, oxygen-free zone, CO concentration, flame length, flame diameter, and divergence angle, the case of ISA/OSA = 1:2 had great processing on combustion efficiency and NOx emission. Thus, ISA/OSA = 1:2 was selected as the optimized case under experiment conditions.

1. Introduction

Pulverized-coal (PC) combustion is one of the maximum coal application approaches. Combustion efficiency and pollutant emissions are the two key factors that restrict the development of PC combustion technology. In order to improve the economic efficiency and ease the pressure on environmental protection, large low nitrogen and high effective combustion technologies [1–5] are developed, such as air staging, fuel staging, flue gas recirculation, fuel rich/lean combustion, and preheating combustion. Achieving these technologies usually depended on the burner or furnace. For the swirl burner, the inner recirculation zone can be formed to keep combustion stable, which is generally applied to the PC boiler. Combining with the abovementioned technologies, the swirl burner has the ability of improving the combustion efficiency and achieving low nitrogen combustion. Flow characteristic analysis is a significant approach to understand and optimize the combustion characteristic of a swirl burner. Li et al. [6] experimentally investigated the gas-particle flow characteristic of an axial swirl burner (LNASB). The air field, gas-particle flow and combustion characteristic of the swirl burner (CFR) were researched by Chen et al. [7, 8]. Also, Zhou et al. [9] numerically analyzed that flame stability and the NOx formation mechanism depend on the flow and combustion characteristic of the swirl burner (HT-NR3). Thus, the influences of the swirl burner different variable (such as operating conditions and burner structure) on PC combustion were investigated by the flow and combustion characteristic. For all swirl burners without an adjustable structure, operating conditions [10–15] had significantly impacted on the flow and combustion characteristic. On the influence of the ISA or OSA ratio, Liu et al. [16] researched the position and size of the recirculation zone for LNASB, and the combustion characteristic was discussed in a 600 MW supercritical boiler; some dissertations [17–19] in China, respectively, studied the air flow and combustion characteristic for the CFR swirl.
burner, and Jing et al. [13] discussed the gas-particle flow characteristic. Xue et al. [14] investigated carbon burnout and NOx emission with different experimental coals for a radially biased swirl burner. Jiang et al. [20] experimentally researched how to avoid high temperature corrosion by ISA opening of a swirl burner in an opposed wall fired ultra-supercritical boiler. The abovementioned literatures indicated that the relationship between ISA and OSA of a swirl burner had a significant influence on PC combustion.

The swirl burner with a prechamber structure was used to solve the combustion difficult problem on inferior coal by enhancing the recirculation zone and particle concentration. With developing stable combustion technologies [21, 22] and high temperature corrosion and slagging occurring frequently, application of the prechamber structure gradually decreased. At present, a swirl burner with a prechamber appeared in an industrial boiler combining with low nitrogen combustion technologies. Jiangetal. [23] numerically investigated the combustion characteristic of the swirl burner with a double-cone prechamber in an industrial boiler; combining with deep air staging, Wang et al. [24] discussed the NOx emission of an industrial boiler. Chi et al. [25] also studied the combustion characteristic of a swirl burner with a prechamber. However, the influence of the ratio of ISA and OSA (ISA/OSA) on the flow and combustion characteristic for a swirl burner with a prechamber was less researched. Gong et al. [26] researched the influence of ISA/OSA for a swirl burner with a prechamber, but ISA and OSA were not provided at the same burner outlet.

In our present work, the influence of ISA/OSA had been investigated on the air flow and combustion characteristic for a swirl burner with a prechamber, but the primary air and PC was reverse flow in the prechamber. Therefore, we decided to experimentally research the influence of ISA/OSA on the combustion and flame characteristic for a swirl burner with a prechamber, in which primary air and PC were normal flow.

2. Experiment and Methods

The 14 MW pilot scale PC combustion experiment system was built in our work. Combining with measurement devices and methods, the data of temperature and species concentration in the prechamber and flame shape beyond the prechamber outlet were obtained to analyse the influence of ISA/OSA.

2.1. Pulverized-Coal Combustion Experiment System

Figure 1 shows the schematic diagram of the experiment system, which consisted of the coal feeding system, wind system, ignition system, control system, a swirl burner, temperature and gas species concentrations measurements system, and flame capture system. The coal feeding system included storage facilities and feeding devices, and the feeding speed was adjusted by frequency of feeding devices. During each experiment condition, three times of 10 min feeding speed calibration were carried out, and the error was maintained within ±8%. A Roots fan and three blowers provide PA (primary air), ISA, OSA, and TA (tertiary air), respectively. Then, the valve was adjusted to control the flow rate displayed by the mass flowmeter. The fuel oil for the ignition system was ignited first, then the PC was fed to achieve stable combustion, and finally, the fuel oil stopped being supplied. The control system was responsible for the start and stop of the whole experiment system. The schematic diagram of the swirl burner is shown in Figure 2, which had 9 axial movable swirl vanes in ISA, an expanding cone-shaped prechamber, a combustion stabilizing device, and an isolated area of PA and OSA.

2.2. Experiment Methods and Conditions.

The temperature and gas species concentrations measurements system and the flame capture system in Figure 1 were introduced as measurement methods. The 1.5 m long stainless steel K-type thermocouple with its own signal converter was adopted to realize the online display of temperature. The measurement range of the thermocouple was 0–1300°C with an error of 0.5%. After the temperature was stable, the fluctuation range of ±10°C was recorded as the measurement value. Flue gas was sampled by using a water-cooled sucking probe, which consisted of a centrally-located sampling pipe surrounded by a double-deck stainless steel tube with high pressure water for probe cooling. After being quickly cooled by water, gas samples through the unit and were filtered and, then, analyzed online by using a MRU VARIO PLUS flue gas analyzer to obtain the gas species concentrations, with an accuracy consisting of ±2% for the measurement values of O2 and CO. Sixty groups’ data were measured at each measuring point for 120 s, and the mean value of 30 s stability data was selected as the flue gas species concentration value of this point. The flame capture system mainly meant the high-speed camera, which used its supporting application software (PCC3.1) to select camera parameters such as a resolution of 1080×504, exposure time of 200 μs, and
sampling rate of 1700 fps etc. The scale was arranged at the same section with the burner axis, the high-speed camera took 8337 pictures of the flame, and the picture of the best flame stability and length was selected as the follow-up picture.

In this combustion experiment, Shenfu long flame coal in China was used as the experimental coal, and its basic characteristics are shown in Table 1. As a kind of high volatile coal, it could ensure the smooth ignition and stable combustion for the process of experiment. To avoid the problem of high temperature corrosion and slagging and the flame biasing of the swirl burner horizontal arrangement, wall and swirl wind should be controlled. Considering the flow type difference of ISA and OSA, three experimental cases (ISA/OSA \(2:1, 1:1, 1:2\)) were chosen, and the main flow gradually changed from ISA to OSA. The ISA swirl number \((S)\) in Table 2 was calculated using following formula [10]:

\[
S = \frac{2}{3} \times \frac{1 - (d_i/d_o)^3}{1 - (d_i/d_o)^2} \times \tan(\theta),
\]

where \(d_i\) is the inner diameter of the ISA duct, \(d_o\) is the outer diameter of the ISA duct, and \(\theta\) is the special swirl vane angle in experimental conditions. The other specific experiment parameters such as air mass flow and speed are shown in Table 2.

The axial distance of the burner outlet section and the radial distance of the central axis were defined as \(X\) and \(R\), respectively. Four sections \(X = 268, 536, 670, \) and \(804\) mm from the measurement position of the burner outlet were selected. The measurement points of each section were, respectively, 10, 60, 110, 160, 210, and 260 mm from the wall surface of the prechamber, and the last point was the central axis. Finally, the temperature and flue gas species concentrations, respectively, were measured.

### Table 1: The basic characteristics of experimental coal.

<table>
<thead>
<tr>
<th>Proximate analysis (as received wt %, ad)</th>
<th>Volatiles</th>
<th>Ash</th>
<th>Moisture</th>
<th>Fixed carbon</th>
<th>Net heating value (kJ/kg)</th>
</tr>
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<tbody>
<tr>
<td></td>
<td>33.60</td>
<td>7.02</td>
<td>5.62</td>
<td>53.76</td>
<td>27200</td>
</tr>
</tbody>
</table>

<table>
<thead>
<tr>
<th>Ultimate analysis (as received wt %, ad)</th>
<th>Carbon</th>
<th>Hydrogen</th>
<th>Oxygen</th>
<th>Nitrogen</th>
<th>Sulfur</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>61.54</td>
<td>4.16</td>
<td>11.64</td>
<td>0.82</td>
<td>0.43</td>
</tr>
</tbody>
</table>

### Table 2: Experimental conditions and parameters.

<table>
<thead>
<tr>
<th>ISA/OSA</th>
<th>2:1</th>
<th>1:1</th>
<th>1:2</th>
</tr>
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<tbody>
<tr>
<td>Feeding speed (kg/h)</td>
<td>1140</td>
<td>1140</td>
<td>1140</td>
</tr>
<tr>
<td>Primary air (kg/h)</td>
<td>900</td>
<td>900</td>
<td>900</td>
</tr>
<tr>
<td>Primary air speed (m/s)</td>
<td>26.3</td>
<td>26.3</td>
<td>26.3</td>
</tr>
<tr>
<td>Inner secondary air (kg/h)</td>
<td>3889</td>
<td>2917</td>
<td>1945</td>
</tr>
<tr>
<td>Inner secondary air speed (m/s)</td>
<td>22.3</td>
<td>16.7</td>
<td>11.1</td>
</tr>
<tr>
<td>ISA swirl number ((S))</td>
<td>1.6</td>
<td>1.6</td>
<td>1.6</td>
</tr>
<tr>
<td>Outer secondary air (kg/h)</td>
<td>1945</td>
<td>2917</td>
<td>3889</td>
</tr>
<tr>
<td>Outer secondary air speed (m/s)</td>
<td>14.0</td>
<td>21.0</td>
<td>28.0</td>
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<tr>
<td>Tertiary air (kg/h)</td>
<td>1955</td>
<td>1955</td>
<td>1955</td>
</tr>
<tr>
<td>Tertiary air speed (m/s)</td>
<td>4.5</td>
<td>4.5</td>
<td>4.5</td>
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<tr>
<td>All air temperature (°C)</td>
<td>20</td>
<td>20</td>
<td>20</td>
</tr>
</tbody>
</table>

### 3. Results and Discussion

The experimental results were obtained and divided into three parts to discuss the influence of ISA/OSA, and then, the specific process is as follows.

#### 3.1. Effect of the ISA/OSA for Temperature in the Prechamber

Figure 3 shows different temperature profiles in the prechamber with different ISA/OSA. (a), (b), (c), and (d) in Figure 3 are \(X = 268, 536, 670,\) and \(804\) mm, respectively. For all the cross sections of ISA/OSA in the radial direction, the high temperature zone could be seen in different areas of each temperature profile. This finding demonstrated that sufficient combustion of PC depended on ISA in the prechamber. OSA was used to decrease wall temperature and rich fuel combustion appeared on the central axis. \(T_p\) (peak temperature) \(=933°C\) appeared at \(R = 191\) mm for ISA/OSA \(=2:1\) was lower and farther away from the central axis than other cases in the high-temperature zone, Figure 3(a). The divergence ability of strong swirl was the main reason. Another \(T_p\) found was \(1015°C\) at \(R = 41\) mm, indicating that PC ignited and burned near the central axis. The temperature for ISA/OSA \(=2:1\) was higher than others in the area near the wall \((R > 191\) mm), indicating that the function of ISA was to ensure complete combustion. Figures 3(b) and 3(c) are same as 3(a). In Figure 3(d), \(T_p\) appeared at the same position, and the difference of vales was slight. The temperature for ISA/OSA \(=1:1\) was higher than that of others at the
307–357 mm area, indicating that the ISA or OSA remaining mainstream position helped to reduce wall temperature of the prechamber downstream.

Figure 4 shows the temperature profiles of the central axis (Figure 4(a)) and the wall position in the prechamber (Figure 4(b)) with different ISA/OSA. Along axis distance, the low-temperature zone could be seen for all ISA/OSA in Figure 4(a). The reason was that the mixing of ISA decayed and the endothermic process of PC pyrolysis appeared. Comparing different ISA/OSA, the temperature for ISA/OSA = 2:1 was lower than that of others. It was indicated that \( T_p \) was lower and farther at the same PA and PC feeding speed. In Figure 4(b), the distance from the measurement point to the prechamber inner wall was 10 mm, and temperatures for all ISA/OSA were lower than 400°C. It was indicated that high temperature corrosion could be avoided, and the prechamber adopted general steel material. The results showed that OSA designed had a cooling effect in the prechamber. Besides the \( X = 804 \) mm point, temperature for ISA/OSA = 1:2 was lower than that of others, indicating that increasing OSA enhanced the cooling effect.

For the swirl burner with a prechamber, the function of PA, ISA, and OSA, respectively, was ignition, ensuring stable combustion and decreasing temperature in the prechamber. Also, the endothermic process of PC pyrolysis appeared, and high-temperature corrosion was avoided. The influence of ISA/OSA on different position temperature in the prechamber was significant.

3.2. Effect of the ISA/OSA for Flue Gas Species Concentrations in the Prechamber. The \( \text{O}_2 \) and \( \text{CO} \) concentration profiles with different ISA/OSA are shown in Figures 5 and 6, respectively. The \( \text{O}_2 \) concentration increased from near 0% to near 21%, and the \( \text{CO} \) concentration decreased from high concentration to near 0 ppm along radial direction for different ISA/OSA at all cross sections. The oxygen-free and high CO concentration zone (\( \text{O}_2 < 1\% \), \( \text{CO} > 5 \times 10^4 \) ppm) could be found in the prechamber. It could be attributed to PC incomplete combustion and species diffusion.

For the case of ISA/OSA = 2:1, the \( \text{O}_2 \) concentration (\( R > 120 \) mm) and oxygen-free zone, respectively, were higher and smaller than others, and the \( \text{CO} \) concentration was lower first and higher than others, as shown in Figures 5(a), 5(b), 6(a), and 6(b). The reason was that the divergence ability of strong swirl inhibited species diffusion. In Figures 5(c) and 6(c), the difference of \( \text{O}_2 \) concentration profiles for three ISA/OSA was not obvious besides \( R = 90–140 \) mm, and \( \text{CO} \) concentration for ISA/OSA = 1:2 was slightly higher than others besides the central axis point.
It was indicated that ISA and OSA gradually mixed. In Figures 5(d) and 6(d), the oxygen-free zone and O\textsubscript{2} concentration (\(R > 120\) mm), respectively, were bigger and lower than others, and the CO concentration was higher than others for ISA/OSA \(\approx 1:2\). The reason was that the mixing of PA and SA was weak, under the diversity of ISA and OSA was larger condition.

Figures 7 and 8 showed the O\textsubscript{2} and CO concentration profiles of the central axis (Figures 7(a) and 8(a)) and the wall position of the prechamber (Figures 7(b) and 8(b)) for three ISA/OSA. There were oxygen-free and high CO concentration on the central axis with different ISA/OSA. The CO concentration for ISA/OSA \(\approx 2:1\) was higher than that of others, indicating that pyrolysis processing was
strong to decrease temperature. At the side wall of the prechamber, the O$_2$ concentration and CO concentration were close to 21% and 0 ppm with different ISA/OSA, indicating that the cooling effect of ISA was evidenced. Also, the high temperature corrosion and slagging could be avoided.

In the prechamber of the swirl burner, the zone of oxygen-free and high CO concentration was found on the centre. The results showed that strong reducing atmosphere inhibited NO$_x$ generation and decreased NO$_x$ emission. ISA/OSA had impacted on no oxygen boundary and CO concentration of different regions. The high temperature corrosion and slagging phenomenon did not occur.

3.3. Effect of the ISA/OSA for a Flame Shape beyond the Prechamber Outlet. Figure 9 shows different flame shapes and profiles for different ISA/OSA. All images in Figure 9
showed that the flame surface had a typical turbulence structure, which was favorable for mass, heat diffusion, and flame propagation beyond the prechamber outlet. This indicated that the prechamber had the advantages in enhancing flame stability when it was adopted in the swirl burner. Also, the interaction with external air flow indicates

Figure 8: CO concentration profiles along axis distance for different ISA/OSA.

Figure 9: Flame shapes and profiles for different ISA/OSA.
ISA/OSA, and conclusions were obtained as follows:

...of the burner were researched and analyzed with variable prechamber and flames shapes beyond the prechamber outlet. The specific data are shown in Table 3.

The divergence angle decreased from 12.1° to 10.5° at first and, later, rose to 11.9° with decreasing ISA/OSA. The finding indicated that the flame divergence angle for ISA/OSA = 1:1 was lower than that for others. Also, the flame length was longer than that of others, and the diameter was narrower than that of others. The length value varied from 4194 mm to 5926 mm at first and, later, to 5504 mm with decreasing ISA/OSA, and the diameter varied from 762.8 mm to 386.1 mm and to 424.8 mm. The rough and short flame for ISA/OSA = 2:1 were caused due to its rotational divergent ability. The flame length was shortened, and the diameter was widened due to the low-speed flow region slight shortening beyond the prechamber outlet. The gradient of jet velocity along the radial direction was low for ISA/OSA =1:1 which stretched the low-speed flow region of flame stability.

The swirl burner with the prechamber had stable PC combustion flame with different ISA/OSA. An inflection point of flame shape was found, indicating that reasonable ISA/OSA needed to be considered.

Temperatures and species concentrations in the prechamber reflected PC burning out, low nitrogen combustion, corrosion, and slagging. Flame shape beyond the prechamber outlet exhibited a jet characteristic and high temperature zone in the future boiler. Also, the flame shape was affected by the combustion characteristic in the prechamber. Thus, the combustion efficiency and NOx emissions were predicted by temperatures, species concentrations, and flame shapes. Combining with the influence of ISA/OSA, reasonable ISA/OSA was selected to optimize operation condition of the swirl burner with the prechamber.

### 4. Conclusions

The temperatures and flue gas species concentrations in the prechamber and flame shapes beyond the prechamber outlet of the burner were researched and analyzed with variable ISA/OSA, and conclusions were obtained as follows:

1. The high temperature, the oxygen-free zone, and high CO concentrations were found in the prechamber, and a long stable flame shape was observed beyond the prechamber outlet. It was evidenced that the swirl burner with the prechamber had certain ability of increasing the combustion efficiency and low nitrogen combustion. The high-temperature corrosion and slagging phenomenon of the prechamber were avoided by designing OSA.

2. The influence of ISA/OSA was reflected on the temperature peak, near wall temperature, oxygen-free boundary, and CO concentrations in the prechamber. In the prechamber upstream, the temperature peak and oxygen-free zone decreased, with increasing ISA/OSA, near wall temperature, and CO concentrations. In the prechamber downstream, the oxygen-free zone increased, with decreasing ISA/OSA, and CO concentrations increased. The temperature peak had a slight difference.

3. The influence of ISA/OSA on the flame shape was analyzed by flame length, diameter, and divergence angle. Flame length had a maximum inflection point, with increasing ISA/OSA, and flame diameter and divergence angle had a minimum inflection point. The relation between flame length and others was a contradiction and needed to consider comprehensively.

4. According to temperature profiles, species concentrations profiles, and flame shapes size, the ISA/OSA = 1:2 case had higher temperature peak and CO concentrations, larger oxygen-free zone, and lower near wall temperature. Also, flame length was longer, and flame diameter and divergence angle were larger. Therefore, the ISA/OSA = 1:2 experimental condition was selected as a reasonable operating condition, under the experimental coal, 63% load, and ISA swirl number $S = 1.6$ of the swirl burner with a prechamber.

### Data Availability

No data were used to support this study. The burn of the experiment is available from the authors.

### Conflicts of Interest

The authors declare that there are no conflicts of interest regarding the publication of this paper.

### Acknowledgments

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<table>
<thead>
<tr>
<th>ISA/OSA</th>
<th>Upper flame surface</th>
<th>Downward flame surface</th>
<th>Flame diameter (mm)</th>
<th>Flame divergence angle (°)</th>
<th>Flame length (mm)</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>Intercept (mm)</td>
<td>Slope</td>
<td>Intercept (mm)</td>
<td>Slope</td>
<td></td>
</tr>
<tr>
<td>2:1</td>
<td>941.9</td>
<td>0.3813</td>
<td>179.1</td>
<td>0.1670</td>
<td>762.8</td>
</tr>
<tr>
<td>1:1</td>
<td>542.4</td>
<td>0.1752</td>
<td>156.3</td>
<td>−0.0102</td>
<td>386.1</td>
</tr>
<tr>
<td>1:2</td>
<td>947.3</td>
<td>0.1079</td>
<td>522.5</td>
<td>−0.1033</td>
<td>424.8</td>
</tr>
</tbody>
</table>

This table shows the flame shapes size for different ISA/OSA.
References


