

Research Article

Regions of Positive Vorticity in Steady Axisymmetric Flow Past a Viscous Spherical Drop

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The vorticity exterior and interior to a viscous liquid drop in steady motion in an unbounded fluid is investigated. The perturbation solution to first order in the Reynolds number derived by Taylor and Acrivos (1964) is used. New analytical results are derived for the attached region of positive vorticity behind the drop and for the region of positive vorticity inside the drop.

1. Introduction

In this paper we will consider the steady axisymmetric flow of a viscous fluid past a liquid drop with constant interfacial tension. From numerical investigations [1-4] it is known that a detached wake consisting of a standing eddy and a region of positive vorticity exist outside the viscous drop if the Reynolds number, Re, and the ratio of the viscosity of the drop to the viscosity of the surrounding fluid, κ , are sufficiently large and that a region of positive vorticity exists inside the drop if either Re is sufficiently large or κ is sufficiently small. In a recent paper [5] new analytical results for the detached wake and the streamlines inside and outside the liquid drop were derived using the singular perturbation solution for the stream function derived by Taylor and Acrivos [6]. In this paper we will derive corresponding analytical results for the equivorticity lines and for the regions of positive vorticity outside and inside the liquid drop.

The singular perturbation solution of Taylor and Acrivos [6] will again be used. This perturbation solution has two parameters, Re and κ . Although it was derived assuming that Re < 1, we will apply it to flows with Re > 1. There is evidence that the predictions of this solution are applicable for Re > 1. For example, Wellek et al. [7] found that the Taylor

and Acrivos perturbation solution predicted quite accurately the eccentricity of the deformed drop for Reynolds numbers up to Re = 20. Also as $\kappa \rightarrow \infty$, the solution of Taylor and Acrivos tends to the singular perturbation solution of Proudman and Pearson [8] for the stream function for slow viscous flow past a solid sphere. Van Dyke [9] found that the length of the attached wake behind a solid sphere calculated from the Proudman and Pearson perturbation solution to first order in the Reynolds number is in good agreement with experimental and numerical values for Reynolds number up to about Re = 60.

We will assume also that the interfacial tension is large so that the Weber number, We, is small, and therefore the deformation of the spherical drop is small.

An outline of the paper is as follows. In Section 2 the assumptions of the model are stated and the perturbation solution of Taylor and Acrivos for the stream functions outside and inside the liquid drop to first order in the Reynolds number Re is presented. In Section 3 the equivorticity lines and the attached region of positive vorticity exterior to the liquid drop are investigated. In Section 4 the equivorticity lines and the region of positive vorticity inside the liquid drop are considered. Finally the conclusions are summarised in Section 5.



FIGURE 1: Spherical polar coordinate system (r, θ, ϕ) for axisymmetric flow past a liquid drop. If $\hat{\rho} > \rho$, the gravity vector **g** points in the direction shown while if $\hat{\rho} < \rho$, **g** points in the opposite direction.

2. Stokes Stream Functions

In this section we will summarise the assumptions made in the derivation of the perturbation solution of Taylor and Acrivos [6] and state the Stokes stream functions inside and outside the liquid drop.

Consider the steady axisymmetric motion under gravity of a viscous liquid drop slightly deformed from the spherical shape in an unbounded quiescent fluid. The fluids inside and outside the liquid drop are incompressible and immiscible and the interfacial tension is assumed to be uniform. Fluid variables inside the liquid drop are denoted by a circumflex. The terminal velocity of the drop is *U*. The spherical polar coordinate system (r, θ, ϕ) shown in Figure 1 with origin at the centre of mass of the drop is used. The fluid variables are dimensionless, and since the flow is axisymmetric, they are independent of ϕ . The characteristic length is the radius, *a*, of the spherical drop with the same volume, and the characteristic velocity is the terminal velocity, *U*.

Since the fluids outside and inside the liquid drop are incompressible and the flow is axisymmetric with $v_{\phi} = 0$ and $\hat{v}_{\phi} = 0$, Stokes stream functions, $\psi(r, \theta)$ and $\hat{\psi}(r, \theta)$, can be introduced outside and inside the liquid drop. They are defined in terms of the velocity components parallel to the *r* and θ coordinate lines by

$$\begin{split} v_r(r,\theta) &= \frac{1}{r^2 \sin \theta} \frac{\partial \psi}{\partial \theta}, \qquad v_\theta(r,\theta) = -\frac{1}{r \sin \theta} \frac{\partial \psi}{\partial r}, \\ \widehat{v}_r(r,\theta) &= \frac{1}{r^2 \sin \theta} \frac{\partial \widehat{\psi}}{\partial \theta}, \qquad \widehat{v}_\theta(r,\theta) = -\frac{1}{r \sin \theta} \frac{\partial \psi}{\partial r}. \end{split}$$
(1)

The continuity equations outside and inside the liquid drop are automatically satisfied.

The perturbation parameter is the Reynolds number, Re, defined in terms of the parameters of the flow outside the drop by

$$\operatorname{Re} = \frac{Ua}{\nu},$$
(2)

where $\nu = \eta/\rho$ is the kinematic viscosity and η is the shear viscosity of the exterior fluid. Taylor and Acrivos [6] used the method of matched asymptotic expansions outside the

liquid drop to obtain an expansion uniformly valid in r for $a \leq r \leq \infty$. The inner expansion outside the drop is the straightforward expansion in powers of Re. This inner expansion is used to analyse the exterior flow close to the drop which includes the region of positive vorticity. The deformation of the drop at zero order in Re was found to be zero. Hence the boundary condition for the first order in Re solution was imposed at r = 1. The inner expansion for the stream function outside the drop to first order in Re found by Taylor and Acrivos [6] can be written as

$$\psi(r,\theta) = \frac{1}{4} (r-1) \sin^2 \theta$$

$$\times \left[\left(1 + \frac{1}{8} \left(\frac{2+3\kappa}{1+\kappa} \right) \operatorname{Re} \right) \right]$$

$$\times \left(2r - \frac{\kappa}{1+\kappa} - \frac{\kappa}{1+\kappa} \frac{1}{r} \right)$$

$$- \frac{\operatorname{Re}}{8} \left(\frac{2+3\kappa}{1+\kappa} \right)$$

$$\times \left(2r - \frac{\kappa}{1+\kappa} - \frac{\kappa}{5(1+\kappa)^2} \frac{1}{r} - \frac{\kappa(6+5\kappa)}{5(1+\kappa)^2} \frac{1}{r^2} \right) \cos \theta$$

$$+ O\left(\operatorname{Re}^2 \right),$$
(3)

as Re \rightarrow 0, where κ is the ratio of the shear viscosity of the drop to the shear viscosity of the exterior fluid:

$$\kappa = \frac{\widehat{\eta}}{\eta}.$$
 (4)

Since shear viscosity is nonnegative, the range of values of κ is $0 \le \kappa \le \infty$. For an inviscid gas bubble, $\kappa = 0$, while for a solid sphere, $\kappa = \infty$. The stream function inside the liquid drop to first order in Re can be written as

$$\widehat{\psi}(r,\theta) = -\frac{r^2 \left(1-r^2\right) \sin^2 \theta}{4 \left(1+\kappa\right)} \\ \times \left[1+\frac{\kappa \left(2+3\kappa\right)}{40 \left(1+\kappa\right)^2} \operatorname{Re}\right.$$
(5)
$$\left.+\operatorname{Re}\frac{\left(2+3\kappa\right) \left(5+4\kappa\right)}{40 \left(1+\kappa\right)^2} \left(1-r\cos\theta\right)\right] \\ \left.+O\left(\operatorname{Re}^2\right),$$

as Re $\rightarrow 0$.

The deformation of the drop to first order in Re is proportional to the Weber number We and depends on the density ratio γ (and on κ) where

We =
$$\frac{\rho a U^2}{\sigma}$$
, $\gamma = \frac{\widehat{\rho}}{\rho}$, (6)

and σ is the uniform interfacial tension. The boundary conditions for the order Re solution were imposed on the zero order surface of the drop, r = 1, which is not deformed. The results therefore apply only for small Weber number.

3. Attached Region of Positive Vorticity Exterior to the Liquid Drop

Consider first the fluid flow exterior to the liquid drop.

Since the flow is axisymmetric, the vorticity $\boldsymbol{\omega}$ expressed in terms of the stream function $\psi(r, \theta)$ is

$$\boldsymbol{\omega} = -\frac{1}{r\sin\theta} D^2 \boldsymbol{\psi} \boldsymbol{e}_{\phi} = \omega_{\phi} \boldsymbol{e}_{\phi}, \qquad (7)$$

where

$$D^{2} = \frac{\partial^{2}}{\partial r^{2}} + \frac{\sin\theta}{r^{2}} \frac{\partial}{\partial \theta} \left(\frac{1}{\sin\theta} \frac{\partial}{\partial \theta} \right), \tag{8}$$

and \mathbf{e}_{ϕ} is the unit base vector parallel to the ϕ -coordinate line in the direction of increase of ϕ . For the exterior flow close to the drop the stream function is given by (3). With the aid of the identities

$$D^{2}\left(f\left(r\right)\sin^{2}\theta\right) = \left(\frac{d^{2}f}{dr^{2}} - \frac{2}{r^{2}}f\right)\sin^{2}\theta,$$

$$D^{2}\left(f\left(r\right)\sin^{2}\theta\cos\theta\right) = \left(\frac{d^{2}f}{dr^{2}} - \frac{6}{r^{2}}f\right)\sin^{2}\theta\cos\theta,$$
(9)

it can be verified that

$$\omega_{\phi}(r,\theta) = -\frac{1}{2} \left(\frac{2+3\kappa}{1+\kappa} \right) \frac{\sin\theta}{r} \\ \times \left[\left(1 + \left(\frac{2+3\kappa}{1+\kappa} \right) \frac{\mathrm{Re}}{8} \right) \frac{1}{r} \right. \\ \left. + \frac{\mathrm{Re}}{8} \left\{ 4 - 3 \left(\frac{2+3\kappa}{1+\kappa} \right) \frac{1}{r} \right.$$
(10)
$$\left. + \frac{3\kappa \left(4 + 5\kappa \right)}{5\left(1 + \kappa \right)^2 r^2} \right] \right]$$

$$-\frac{2\kappa}{(1+\kappa)r^3}\bigg]\cos\theta\bigg].$$

The curves ω_{ϕ} = constant in an axial plane ϕ = constant are the equivorticity lines [10].

To zero order in Re

$$\omega_{\phi} = -\frac{1}{2} \left(\frac{2+3\kappa}{1+\kappa} \right) \frac{\sin\theta}{r^2},\tag{11}$$

and hence $\omega_{\phi} < 0$ except when $\theta = 0$ and $\theta = \pi$ in which case $\omega_{\phi} = 0$. When Re > 0, ω_{ϕ} may not always be negative everywhere. We will show that a region of positive vorticity exists behind the drop and that it is attached to the surface of the drop. We will then investigate the properties of this region of positive vorticity.

From (10), $\omega_{\phi}(r, \theta) > 0$ if $\cos \theta > H(r; \kappa, \text{Re})$, where

$$H(r;\kappa, \text{Re}) = \left(\frac{8}{\text{Re}} + \frac{2+3\kappa}{1+\kappa}\right) 5(1+\kappa)^2 r^2 \\ \times \left(\left[-20(1+\kappa)^2 r^3 + 15(1+\kappa)(2+3\kappa)r^2 - 3\kappa(4+5\kappa)r + 10\kappa(1+\kappa)\right]\right)^{-1}.$$
(12)

The dividing curve in an axial plane ϕ = constant between a region of positive vorticity and a region of negative vorticity outside the drop is

$$\cos\theta = H(r;\kappa,\text{Re}). \tag{13}$$

The curve will be attached to the surface of the drop, r = 1, if there is a solution, $\theta = \theta_P$, to the equation

$$\cos \theta_{P} = H (1; \kappa, \text{Re})$$

= $\frac{5 (1 + \kappa) [8 (1 + \kappa) + (2 + 3\kappa) \text{Re}]}{(5 + 4\kappa) (2 + 5\kappa) \text{Re}}.$ (14)

Since $\cos \theta_p \leq 1$, (14) has a solution for θ_p only if $\text{Re} \geq \text{Re}_p$, where

$$\operatorname{Re}_{P} = \frac{40(1+\kappa)^{2}}{\kappa (8+5\kappa)}.$$
(15)

We have

$$\operatorname{Re}_{P} = 8\left(1 + \frac{2}{5\kappa} + \frac{9}{25\kappa^{2}} + O\left(\frac{1}{\kappa^{3}}\right)\right) \quad \text{as } \kappa \longrightarrow \infty,$$

$$\operatorname{Re}_{P} = \frac{5}{\kappa}\left(1 + \frac{11}{8}\kappa + \frac{9}{64}\kappa^{2} + O\left(\kappa^{3}\right)\right) \quad \text{as } \kappa \longrightarrow 0.$$
(16)

If $\text{Re} < \text{Re}_P$, there is no region of positive vorticity attached to the surface of the drop. It can be shown that Re_P is a decreasing function of κ .

For an inviscid gas bubble, $\kappa = 0$ and $\text{Re}_P = \infty$. This indicates that there is not a region of positive vorticity attached to an inviscid gas bubble. For an inviscid gas bubble there is also no downstream wake with standing eddies because no vorticity is generated upstream on the surface of an inviscid bubble [5].

For a solid sphere, $\kappa = \infty$ and $\text{Re}_P = 8$. At Re = 8 the perturbation solution of Proudman and Pearson [5, 8, 9] predicts that an attached wake consisting of two standing eddies first appears downstream of the solid sphere. The standing eddies are due to the accumulation of vorticity generated upstream on the surface of the sphere. For a solid sphere, the attached region of positive vorticity and the attached wake first appear at the same value of the Reynolds number, Re = 8.

For $0 < \kappa < \infty$ the standing eddy is detached from the surface of the liquid drop. It first appears in the flow down-stream of the drop at Reynolds number Re_{*A*}. A perturbation solution with perturbation parameter $1/\kappa$ as $\kappa \to \infty$, and a

numerical solution have been derived for Re_A [5]. It can be shown that $\text{Re}_A > \text{Re}^*$, where

$$\operatorname{Re}^{*} = \frac{120(2+3\kappa)(1+\kappa)^{2}}{\kappa(2+3\kappa)(4+5\kappa)}.$$
(17)

It is readily verified that $\text{Re}_P < \text{Re}^*$, and hence the attached region of positive vorticity appears outside the drop before the appearance of the standing eddy.

The value of κ for given Re > 8 at which the region of positive vorticity first occurs as κ is increased from zero is obtained by solving (14) with $\theta_P = 0$ for κ . This gives the quadratic equation

$$5 (Re - 8) \kappa^{2} + 8 (Re - 10) \kappa - 40 = 0.$$
 (18)

For Re > 8, (18) has one real positive root

$$\kappa_P = \frac{-8 \left(\text{Re} - 10\right) + \left[32 \text{Re} \left(2 \text{Re} - 15\right)\right]^{1/2}}{10 \left(\text{Re} - 8\right)}.$$
 (19)

Consider now the range of θ_P on the outer surface of the drop for $0 < \kappa \le \infty$ and $\operatorname{Re}_P \le \operatorname{Re} \le \infty$. It can be shown from (14) that

$$\frac{\partial \theta_p}{\partial \operatorname{Re}} > 0, \qquad \frac{\partial \theta_p}{\partial \kappa} > 0,$$
 (20)

and hence θ_P is an increasing function of Re and κ . Also,

$$\lim_{\text{Re}\to\infty} \theta_P = \cos^{-1} \left[\frac{5(1+\kappa)(2+3\kappa)}{(5+4\kappa)(2+5\kappa)} \right],$$
 (21)

$$\lim_{\kappa \to \infty} \theta_P = \cos^{-1} \left[\frac{3}{4} + \frac{2}{\text{Re}} \right].$$
 (22)

Equation (21) gives the maximum value of θ_P for a given value of κ while (22) gives the maximum value of θ_P for a given value of Re. Further

$$\lim_{\text{Re}\to\infty}\lim_{\kappa\to\infty}\theta_P = \lim_{\kappa\to\infty}\lim_{\text{Re}\to\infty}\theta_P = \cos^{-1}\left(\frac{3}{4}\right) = 41.4^0.$$
 (23)

For $\operatorname{Re}_P \leq \operatorname{Re} \leq \infty$, θ_P lies in the range $0 \leq \theta_P \leq 41.4^0$. When $\operatorname{Re} = \operatorname{Re}_P$, $\theta_P = 0$ and when $\operatorname{Re} = \infty$ and $\kappa = \infty$, $\theta_P = 41.4^0$. In Figure 2, θ_P is plotted against Re for a range of values of κ . Each curve starts at $\theta_P = 0$, $\operatorname{Re} = \operatorname{Re}_P$, increases steadily for $\operatorname{Re} > \operatorname{Re}_P$, and tends to (21) for large values of Re. The distribution of vorticity over the outer surface of the drop, $w_{\phi}(1, \theta)$, is illustrated in Figures 3 and 4. The vorticity is positive on the outer surface of the drop for $0 \leq \theta < \theta_P$ provided either $\operatorname{Re} > \operatorname{Re}_P$ or $\kappa > \kappa_P$.

Consider now the maximum point of extension, $r = r_P$, of the region of positive vorticity downstream of the drop. By putting $\theta = 0$ in (13), we find that r_P satisfies the cubic equation

$$Q\left(r\right) = 0,\tag{24}$$

where

$$Q(r) = r^{3} - \left(\frac{2+3\kappa}{2(1+\kappa)} - \frac{2}{\text{Re}}\right)r^{2} + \frac{3\kappa(4+5\kappa)}{20(1+\kappa)^{2}}r - \frac{\kappa}{2(1+\kappa)}.$$
(25)



FIGURE 2: Graphs of θ_P plotted against Re for a range of values of κ .



FIGURE 3: Graphs of $\omega_{\phi}(1,\theta)$ plotted against θ for $\kappa = 2$ and a range of values of Re. When $\kappa = 2$, Re_p = 10.

When $\kappa = 0$, which describes an inviscid gas bubble, (24) reduces to

$$r^{2}\left[r-\left(1-\frac{2}{\operatorname{Re}}\right)\right]=0.$$
 (26)

The roots of (26) are r = 0 (twice) and r = 1 - 2/ Re which do not lie outside the inviscid bubble. These results indicate that there is not a region of positive vorticity in the flow outside an inviscid gas bubble. We therefore consider $\kappa > 0$.

Consider first $\text{Re} = \text{Re}_p$. Then (24) reduces to

$$(r-1)\left[20(1+\kappa)^2 r^2 - \kappa (2+5\kappa) r + 10\kappa (1+\kappa)\right] = 0, (27)$$

which has one real root, r = 1, and two complex conjugate roots. When Re = Re_{*p*}, $r_p = 1$ and $\theta_p = 0$. The region of positive vorticity first appears behind the drop.



FIGURE 4: Graphs of $\omega_{\phi}(1,\theta)$ plotted against θ for Re = 20 and a range of values of κ . When Re = 20, κ_P = 0.39.

Consider next Re > Re_P . We first show that (24) always has a positive real root greater than unity. Now

$$Q(1) = -\frac{2(\operatorname{Re} - \operatorname{Re}_{P})}{\operatorname{Re} \operatorname{Re}_{P}},$$
(28)

and hence Q(1) < 0 since $\text{Re} > \text{Re}_P$. Also since $Q(r) \to \infty$ as $r \to \infty$, it follows that Q(r) = 0 for some $r = r_P > 1$. This root is the end point on the axis of symmetry $\theta = 0$ of the region of positive vorticity.

Since the production of vorticity at the interface increases as κ and Re increase, we can expect that r_p attains its maximum value when $\kappa = \infty$ and Re = ∞ . We have seen that this is indeed the case for θ_p which attains its maximum value when $\kappa = \infty$ and Re = ∞ . When $\kappa = \infty$ and Re = ∞ , (24) becomes

$$r^{3} - \frac{3}{2}r^{2} + \frac{3}{4}r - \frac{1}{2} = 0.$$
 (29)

Now the standard form of a cubic equation is [11]

$$s^3 + 3Hs + G = 0. (30)$$

In order to transform (29) to the standard form, let

$$r = s + \frac{1}{2}.$$
 (31)

Then (29) becomes

$$s^3 - \frac{3}{8} = 0. ag{32}$$

Thus $G^2 + 4H^3 > 0$ and there is one real root and two complex conjugate roots [11]. The real root is s = 0.72, and hence

$$r_P(\max) = 1.22.$$
 (33)

The region of positive vorticity behind the drop is therefore a thin layer attached to the rear surface of the drop. Its



FIGURE 5: The numerical solution for r_p , the end point of the region of positive vorticity behind the drop, plotted against Re for a range of values of κ .



FIGURE 6: Graphs of $\hat{\theta}_P$ plotted against Re for a range of values of κ .

maximum extension is $0 \le \theta \le 41.4^{\circ}$ and $1 \le r \le 1.22$. The dividing curve (13) generates a surface of revolution about the line $\theta = 0$ which encloses the attached region of positive vorticity downstream of the drop.

A straightforward perturbation solution of (24) for r_p in terms of the perturbation parameter

$$\varepsilon = \frac{\operatorname{Re} - \operatorname{Re}_P}{\operatorname{Re}_P}, \quad \operatorname{Re} > \operatorname{Re}_P,$$
 (34)



FIGURE 7: Graphs of $\hat{\omega}_{\phi}(1,\theta)$ plotted against θ for $\kappa = 2$ and a range of values of Re. When $\kappa = 2$, $\widehat{\text{Re}}_{P} = 14$.



FIGURE 8: Graphs of $\hat{\omega}_{\phi}(1,\theta)$ plotted against θ for Re = 15 and a range of values of κ . When Re = 15, $\hat{\kappa}_{p}$ = 2.72.

is readily derived:

$$r_{P} = 1 + \frac{\kappa (8+5\kappa)}{\left(25\kappa^{2} + 48\kappa + 20\right)}\varepsilon + O\left(\varepsilon^{2}\right), \qquad (35)$$

as $\varepsilon \to 0$. For small κ ,

$$r_P - 1 = \frac{2\kappa}{5} (1 + O(\kappa)) \varepsilon, \quad \text{as } \kappa \longrightarrow 0,$$
 (36)

while for large κ ,

$$r_P - 1 = \frac{1}{5} \left(1 - \frac{8}{25\kappa} + O\left(\frac{1}{\kappa^2}\right) \right) \varepsilon, \quad \text{as } \kappa \longrightarrow \infty.$$
 (37)

Equations (36) and (37) give an approximation to the maximum thickness of the region of positive vorticity for small ε when κ is small and κ is large, respectively.

The numerical solution for the real root of (24) is plotted in Figure 5. For each value of κ the curve starts at r = 1, Re = Re_{*P*}. The graphs clearly show that r_P increases as both κ and Re increase and that (33) gives an upper bound for r_P .

We have seen that if Re or κ are sufficiently large, a thin region of positive vorticity exists behind the drop and is attached to the surface. It appears before the appearance of the standing eddies and occurs due to the accumulation of positive vorticity at the outer surface of the drop. The size of the region of positive vorticity increases as each of Re and κ increases because the generation of positive vorticity at the outer surface increases as Re and κ increase as shown in Figures 3 and 4.

4. Region of Positive Vorticity inside the Liquid Drop

Inside the drop the equivorticity lines have more structure than the streamlines [5]. In this section we investigate the region of positive vorticity inside the drop and compare its properties with the properties of the attached region of positive vorticity outside the drop.

The vorticity $\widehat{\boldsymbol{\omega}}$ inside the drop is given by

$$\widehat{\boldsymbol{\omega}} = -\frac{1}{r\sin\theta} D^2 \widehat{\psi} \mathbf{e}_{\phi} = \widehat{\omega}_{\phi} \mathbf{e}_{\phi}, \qquad (38)$$

where D^2 and $\hat{\psi}(r, \theta)$ are defined by (8) and (5). With the aid of the identities (9) it can be shown that

$$\widehat{\omega}_{\phi}(r,\theta) = -\frac{5r\sin\theta}{2(1+\kappa)} \times \left[1 + \frac{\operatorname{Re}}{8}\left(\frac{2+3\kappa}{1+\kappa}\right) -7\operatorname{Re}\frac{(2+3\kappa)(5+4\kappa)}{200(1+\kappa)^2}r\cos\theta\right].$$
(39)

To zero order in Re,

$$\widehat{\omega}_{\phi}\left(r,\theta\right) = -\frac{5r\sin\theta}{2\left(1+\kappa\right)}.\tag{40}$$

Thus when Re = 0, $\hat{\omega}_{\phi}(r, \theta) < 0$ if $\theta \neq 0$ and $\theta \neq \pi$. The equivorticity lines, ω_{ϕ} = constant, in the plane ϕ = constant are straight lines parallel to the axis of symmetry, θ = 0.

Consider now $\hat{\omega}_{\phi}(r,\theta)$ to first order in Re. From (39), $\hat{\omega}_{\phi}(r,\theta) > 0$ if

$$r\cos\theta > \frac{25(1+\kappa)\left[8(1+\kappa) + \operatorname{Re}(2+3\kappa)\right]}{7(2+3\kappa)(5+4\kappa)\operatorname{Re}}.$$
 (41)

The region of positive vorticity therefore consists of the part of the drop

$$\frac{25(1+\kappa)[8(1+\kappa) + \text{Re}(2+3\kappa)]}{7(2+3\kappa)(5+4\kappa)\text{Re}} < r\cos\theta < 1.$$
(42)

It exists provided $\operatorname{Re} > \widehat{\operatorname{Re}}_p$, where

$$\widehat{\operatorname{Re}}_{P} = \frac{200(1+\kappa)^{2}}{(2+3\kappa)(10+3\kappa)}.$$
(43)



FIGURE 9: Equivorticity lines inside the drop in an axial plane for $\kappa = 2$ and Re = 0, 5, 14, and 40. When $\kappa = 2$, $\widehat{\text{Re}}_p = 14$.

We have

$$\widehat{\operatorname{Re}}_{P} = \frac{200}{9} \left[1 - \frac{2}{\kappa} + \frac{61}{9\kappa^{2}} + O\left(\frac{1}{\kappa^{3}}\right) \right] \quad \text{as } \kappa \longrightarrow \infty,$$

$$\widehat{\operatorname{Re}}_{P} = 10 \left[1 + \frac{\kappa}{5} + \frac{19}{100}\kappa^{2} + O\left(\frac{1}{\kappa^{3}}\right) \right] \quad \text{as } \kappa \longrightarrow 0.$$
(44)

It can be shown that $\widehat{\text{Re}}_p$ is an increasing function of κ , which compares with Re_p which is a decreasing function of κ . The Reynolds number $\widehat{\text{Re}}_p$ increases steadily from 10 at $\kappa = 0$ for an inviscid gas bubble to 22.22 at $\kappa = \infty$ for a solid sphere. For Re < 10, the region of positive vorticity inside the drop does not exist for any value of κ while for Re > 22.22 it exists for all values of κ .

The value of κ for given Re at which the region of positive vorticity first occurs as κ decreases from $\kappa = \infty$ is obtained by solving (43) for κ . This yields the quadratic equation

$$(200 - 9 \text{ Re})\kappa^2 + 4(100 - 9 \text{ Re})\kappa + 20(10 - \text{Re}) = 0.$$
(45)

For 10 < Re < 22.22, (45) has one real positive root:

$$\widehat{\kappa}_{p} = \frac{-2(100 - 9 \operatorname{Re}) + 2[2 \operatorname{Re}(18 \operatorname{Re} - 175)]^{1/2}}{(200 - 9 \operatorname{Re})}.$$
 (46)

The region of positive vorticity exists for $0 \le \kappa < \hat{\kappa}_p$. It does not exist for $\kappa > \hat{\kappa}_p$.



FIGURE 10: Equivorticity lines inside the drop in an axial plane for Re = 15 and κ = 0, 0.5, 2.72, and 10. When Re = 15, $\hat{\kappa}_p$ = 2.72.

On the inner surface of the liquid drop the region of positive vorticity extends over the range $0 \le \theta \le \hat{\theta}_P$, where $\hat{\theta}_P$ is obtained from (41) with r = 1:

$$\widehat{\theta}_{P} = \cos^{-1} \left[\frac{25(1+\kappa) \left[8(1+\kappa) + (2+3\kappa) \operatorname{Re} \right]}{7(2+3\kappa) (5+4\kappa) \operatorname{Re}} \right]. \quad (47)$$

It can be verified that

$$\frac{\partial \hat{\theta}_P}{\partial \operatorname{Re}} > 0, \qquad \frac{\partial \hat{\theta}_P}{\partial \kappa} < 0, \tag{48}$$

and hence $\widehat{\theta}_P$ is an increasing function of Re and a decreasing function of $\kappa.$ Also

$$\lim_{\text{Re}\to\infty}\widehat{\theta}_P = \cos^{-1}\left[\frac{25(1+\kappa)}{7(5+4\kappa)}\right],\tag{49}$$

$$\lim_{\kappa \to 0} \widehat{\theta}_P = \cos^{-1} \left[\frac{5}{7} \left(1 + \frac{4}{\text{Re}} \right) \right].$$
 (50)

Equation (49) gives the maximum value of $\hat{\theta}_P$ for a given value of κ while (50) gives the maximum value of $\hat{\theta}_P$ for a given value of Re. Further,

$$\lim_{\mathrm{Re}\to\infty}\lim_{\kappa\to 0}\widehat{\theta}_P = \lim_{\kappa\to 0}\lim_{\mathrm{Re}\to\infty}\widehat{\theta}_P = \cos^{-1}\left(\frac{5}{7}\right) = 44.4^0.$$
 (51)



FIGURE 11: Equivorticity lines for flow past a drop with $\kappa = 5$ and Re = 40. The direction of flow is from left to right.

Equation (51) gives the maximum value of $\hat{\theta}_p$. It compares with 41.4⁰ for the maximum value of θ_p derived in (23). In Figure 6, $\hat{\theta}_p$ is plotted against Re for values of κ ranging from 0 to ∞ . The curves are confined to a narrow band emanating from 10 \leq Re \leq 22.22. The limiting cases, $\kappa = \infty$ and $\kappa = 0$, are reversed in Figures 2 and 6. The distribution of vorticity over the inner surface of the drop, $\hat{\omega}_{\phi}(1,\theta)$, is shown in Figures 7 and 8. The vorticity is positive on the inner surface for $0 < \theta < \hat{\theta}_p$ provided Re $> \hat{\text{Re}}_p$ or $\kappa < \hat{\kappa}_p$. The vorticity is discontinuous across the interface r = 1 and the angles θ_p and $\hat{\theta}_p$ are different for given values of κ and Re.

In Figure 9 the equivorticity lines inside the drop are plotted for $\kappa = 2$ and a range of values of Re. When $\kappa = 2$, the region of positive vorticity exists for Re > $\widehat{\text{Re}} = 14$. In Figure 10 the equivorticity lines inside the drop are plotted for Re = 15 and a range of values of κ . When Re = 15, the region of positive vorticity exists for $0 \le \kappa < \widehat{\kappa}_P = 2.72$.

If $0 \le \kappa < 1$, then $\widehat{\operatorname{Re}}_{P} < \operatorname{Re}_{P}$, and as Re increases from zero, the region of positive vorticity occurs inside the drop before it occurs outside and $\widehat{\theta}_{P} > \theta_{P}$. If $\kappa > 1$, then $\operatorname{Re}_{P} < \widehat{\operatorname{Re}}_{P}$ and the region of positive vorticity occurs outside the drop before it occurs inside and $\theta_{P} > \widehat{\theta}_{P}$. When $\kappa < 1$ the generation of vorticity at the interface due to the no-slip condition is more effective in the interior because the interior fluid is less viscous than the exterior fluid. When $\kappa > 1$, the opposite is the case.

In Figure 11, the equivorticity lines inside and outside the drop are plotted for $\kappa = 5$ and Re = 40. For these values of κ and Re, $\theta_P = 36^0$ and $\hat{\theta}_P = 23.4^0$. We see that there is also a region of positive vorticity upstream of the drop. In a diagram showing the streamlines there would be a standing eddy downstream of the drop since when $\kappa = 5$ and Re = 40, Re > Re_A [5].

5. Concluding Remarks

The significant fluid dynamical features in flow past a liquid drop are the detached wake behind the drop, the attached

region of positive vorticity outside the drop, and the region of positive vorticity at the rear inside the drop. Using the perturbation solution of Taylor and Acrivos [6] to first order in Re, we have derived in this paper analytical expressions for the main properties of the regions of positive vorticity outside and inside the drop. The results should be useful in numerical and experimental investigations when the Weber number, and therefore the deformation of the drop, is small. The analytical results are in qualitative agreement with the numerical results of Dandy and Leal [4] who present plots of the equivorticity lines and regions of positive vorticity in flow past a liquid drop. The expansions for large values of the viscosity ratio κ should be useful in flow past a very viscous drop because they tend to results for a solid sphere derived from the perturbation solution of Proudman and Pearson [8] which are in good agreement with numerical and experimental results. The expansions for small values of κ should be useful in flow past a gas bubble.

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