Research Article

Flow Characteristics and Fluid Forces Reduction of Flow Past Two Tandem Cylinders in Presence of Attached Splitter Plate

Ali Ahmed,1 Abdul Wahid,2 Raheela Manzoor,3 Noreen Nadeem,3 Naqib Ullah,4 and Shazia Kalsoom3

1Department of Mathematics, COMSATS University Islamabad, Park Road, Tarlai Kalan 45550, Islamabad, Pakistan
2Balochistan University of Information Technology Engineering and Management Science, Quetta, Balochistan, Pakistan
3Department of Mathematics, Sardar Bahadur Khan Women University, Quetta, Balochistan, Pakistan
4University of Central Punjab Islamabad Campus, Islamabad, Pakistan

Correspondence should be addressed to Ali Ahmed; alihmd87@gmail.com

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1. Introduction

The study of fluid forces and vorticity dynamics through the bluff body has been greatly improved in the last few decades. Most of these studies have been taken for single cylinder. However, much less attention has been paid to multiple cylinders flow compared to single cylinder. The addition of another bluff body can change the different aspects of flow such as fluid forces and transition threshold. To study the flow interference different models such as side-by-side, tandem and staggered models have been used. Among these models, tandem is the simplest one. A number of experimental and numerical studies have been conducted for flow past tandem cylinders. Kondo and Matsukuma [1] numerically analyzed the salient flow features through two tandem circular cylinders at Re = 1000. They found that the forces exerted on the last cylinder are substantially higher than those exerted on the first cylinder. While in case of tandem square cylinders, the upstream cylinder forces are larger than those of the downstream cylinder [2]. Azuma et al. [3] experimentally measured forces acting on square structures both side-by-side and in tandem. They observed that the drag forces of two tandem cylinders changed significantly when the separation ratio was greater than g/D = 3 (where g is the spacing between cylinders and D is cylinder diameter) as compared to side-by-side arrangement. Abbasi et al. [4] numerically analyzed the flow regime transitions over the flow around three tandem cylinders for the g/D between 0.5 and 16 at Re = 200 and found five different types of flow regimes. In addition, they noted that the g/D is the important analysis parameter. Abbasi et al. [5] analyzed the flow regime transitions around two-, three- and four-tandem cylinders for Re ranging from 1 to 130 at g/D = 2 and 5. They observed two separate trends in terms of flow transitions for g/D = 2 and 5. The more reduction in terms of drag is observed at g/D = 2. Mittal et al. [6] numerically...
analyzed the flow characteristics through two cylinders for Re = 100 and 1000 and found that the shedding starts at Re = 100. Abbasi et al. [7] numerically found three various types of flow features for two tandem cylinders. Vikram et al. [8] also analyzed the salient flow features past tandem cylinders. They observed that compared to downstream cylinder the upstream cylinder experience higher lift force. Sharman et al. [9] numerically analyzed the flow through two inline cylinders under the influence of g/D varying from 2 to 10 for Re = 100. They identified g/D = 3.75–4 as critical spacing, where the flow characteristics changes abruptly. Liu and Jerry [10] experimentally analyzed flow on two cylinders in tandem with Re = 2000–16000 and g/D = 1.5–9. They reported hysteresis with two discontinuous jumps associated with different flow regimes. Sohankar and Etminan [11] analyzed flow and heat transfer across cylinders arranged inline for Re = 1–200. They found that vortex shedding formation begins in the range 35 ≤ Re ≤ 40.

The addition of an eddy promoter improved the heat transfer of the downstream cylinder and controls the CDP. Bearman [12, 13] used the splitter plates to increase the formation length and reduce the drag. One of the most important studies was carried out by Zdravkovich [14], which divided the vortex suppression into three different branches, namely: (i) surface protrusions, (ii) shrouds and (iii) near-wake stabilizers. In literature both active and passive methods exist. Active control procedures generally require continuous external energy to reduce the drag forces and improve the lift [15, 16]. While for the passive methods there is no need internal energy, these include tripping rods [17], control cylinder [18–20], splitter plate [21], T-shaped plate [22] etc.

Anderson and Szewczyk [23] experimentally analyzed the impacts of low length splitter plates for the flow through circular cylinder and noticed that less than D/8 splitter length appreciably affect the wake zone for Re = 2700 to 46,000. You et al. [24] observed that significant noise reduction can take place for flow around circular cylinder once the splitter plate length is identical to the cylinder diameter. Uffinger et al. [25] analyzed the effects of different shapes on flow control behind a cylinder and found that the wedge shape behind the square body significantly control the flow. Ali et al. [26] computationally analyzed the influence of splitter plate length on a cylinder at Re = 150.

To the best of ours’ knowledge, for the proposed problem there is no numerical and experimental study reported in the literature. Hopefully, this work will help engineer’s working on fluid forces reduction. The main motivation is to examine the splitter plate effect on flow regimes. The other main objective is to stabilize the critical gap spacing. Furthermore, we want to systematically examine the change over behavior of the mechanism of wake structure behind the downstream cylinder and amplitude variation of fluid forces.

This paper is ordered as follows: The proposed problem, numerical method, initial and boundary conditions are discussed in Section 2. The effect of computational domain and code validation is done in section 3. The computed results are presented in section 4. Finally, the conclusion is presented in section 5.

2. Problem Description and Numerical Details

2.1. Problem Description. A schematic representation of the flow through two fixed tandem SCs in presence of attached splitter plate is shown in Figure 1. D, l and g are the width of the cylinder, length of the splitter plate and spacing between the cylinders, respectively. C1 and C2 are the first and second cylinders, respectively. Ll, Ld, Ls, and Lp are the upstream location, downstream location, length, and height of the domain, respectively. Parabolic velocity profile is adopted at the entrance position of the domain, while the convective boundary condition is adopted at the exit of the domain [27]. No-slip boundary condition is applied to the surface of the cylinders and splitter plate [28]. Free-slip boundary condition is adopted at the top and bottom lateral boundaries of the channel [29]. The method of momentum exchange [30] is used for the calculation of forces.

2.2. Lattice Boltzmann Method. We have established the 2-D code for the flow through two tandem SCs with and without attached splitter at (g/D, l/D) = (0–10, 0.5–10) for Re = 100. The lattice Boltzmann method (LBM) is applied for the numerical results obtained in this paper. As compared to well known numerical techniques, the LBM is relatively new technique [28]. It was developed by Frisch et al. [31]. Here we will present a short overview of this method. In this study we applied Q2N5 (where Q is the space dimension and N is the number of particles) lattice model. In this model, each computational node consists of a rest particle (i = 0) along with eight moving particles (i = 1–8) (see Figure 2).

The density evolution equation is given by;

\[ g_i(x + e_i, t + 1) = g_i(x, t) - \frac{g_i(x, t) - g_i^{(0)}(x, t)}{\tau} \tag{1} \]

where, \( g_i \), \( g_i^{(0)} \), \( x, e_i \) and \( \tau \) are the particle distribution function, the corresponding equilibrium distribution function, dimensionless time, position of particles, velocity directions, and single relaxation time, respectively.

The corresponding equilibrium distribution function is:

\[ g_i^{(0)} = \rho \omega_i \left( 1 + 3(e_i u) + 4.5(e_i u)^2 - 1.5u^2 \right). \tag{2} \]

Here, \( \rho \), \( u \), and \( \omega_i \) are the fluid density, velocity and corresponding weighting functions (\( \omega_i = 0 \) for \( i = 0 \), \( \omega_i = 1/9 \) for \( i = 1–4 \), and \( \omega_i = 1/36 \) for \( i = 5–8 \)), respectively. Equation (1) can be solved by two steps: collision which use a Bhatnagar-Gross-Krook (BGK) operator [32, 33] and propagation. These steps can be defined as:

Collision:

\[ g_i^{(\text{new})}(x, t) = g_i(x, t) - \frac{g_i(x, t) - g_i^{(0)}(x, t)}{\tau} \tag{3} \]

Streaming:

\[ g_i(x + e_i, t + 1) = g_i^{(\text{new})}(x, t). \tag{4} \]

Equations (5) and (6) are used to calculate the density and velocity at each computational node.
3. Computational Domain Study and Code Validation

In this section we will present the grid independence and code validation.

3.1. Grid Independence Study. Table 1 presents the grid independence study. We have taken the error with respect to $D = 30$. From the results it is observed that as the size of $D$ is increased from 20 to 30, the maximum variation in mean drag coefficient ($C_{D, mean}$) and Strouhal number ($St = f_s D/U_\infty$, where $f_s$ is the vortex shedding frequency) are 0.336% and 0.9%, respectively. Therefore, for the rest of simulation we used $D = 20$.

3.2. Computational Domain. The computational domain size strongly affects characteristics of flow around bluff bodies. The small change in computational domain changes the vortex shedding procedure, which affects the physical parameters. We have calculated the $C_{D, mean}$ and $St$ for different values of $L_u$, $L_d$ and $L_y$, so that we can choose a suitable domain. The data in Table 2 shows that there is a slight difference in between the resulted values. So we can consider any case given in Table 2. We will simulate the given problem by using $L_u = 8D$, $L_d = 25D$ and $L_y = 10D$. The numbers 1 and 2 in subscripts represents the physical parameters of upstream and downstream cylinders.

3.3. Code Validation. The validation of code is done for the flow past single cylinder for Re = 100. For the validation of the code we have used only two parameters that is $C_{D, mean}$ and $St$. For comparison the numerical results of Dutta et al. [34] as well as experimental data of Norberg et al. [35] and Okajima [36] are given in Table 3. The results shows that the present calculations of $C_{D, mean}$ and $St$ are in good agreement with the experimental data of Norberg et al. [35] and Okajima [36] and numerical data of Dutta et al. [34].

4. Results and Discussion

A two-dimensional (2D) numerical study is carried out to study the effect of $g/D$ and $l/D$ at Re = 100. The splitter plate is attached in the middle of the two cylinders. In this study
Table 1: Cylinder size effect on integral parameters at Re = 100.

<table>
<thead>
<tr>
<th>$D$</th>
<th>10</th>
<th>20</th>
<th>30</th>
</tr>
</thead>
<tbody>
<tr>
<td>$C_D$,mean</td>
<td>1.1916 (2.79%)</td>
<td>1.1622 (0.34%)</td>
<td>1.1583</td>
</tr>
<tr>
<td>$St$</td>
<td>0.1271 (3.78%)</td>
<td>0.1235 (0.9%)</td>
<td>0.1223</td>
</tr>
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</table>

Table 2: Effect of computational domain at $g/D = 1$.

<table>
<thead>
<tr>
<th>$l/D$</th>
<th>$L_d$</th>
<th>$L_u$</th>
<th>$C_{D,mean1}$</th>
<th>$C_{D,mean2}$</th>
<th>$St_1$</th>
<th>$St_2$</th>
</tr>
</thead>
<tbody>
<tr>
<td>8D</td>
<td>25D</td>
<td>10D</td>
<td>1.0873</td>
<td>−0.0828</td>
<td>0.1018</td>
<td>0.1018</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>(3.08%)</td>
<td>(3.8%)</td>
<td>(3.41%)</td>
<td>(3.41%)</td>
</tr>
<tr>
<td>8D</td>
<td>40D</td>
<td>10D</td>
<td>1.1208</td>
<td>−0.0796</td>
<td>0.1054</td>
<td>0.1054</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>(2.43%)</td>
<td>(3.86%)</td>
<td>(3.05%)</td>
<td>(3.04%)</td>
</tr>
<tr>
<td>12D</td>
<td>25D</td>
<td>10D</td>
<td>1.1144</td>
<td>−0.0860</td>
<td>0.0987</td>
<td>0.0989</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>(2.3%)</td>
<td>(3.86%)</td>
<td>(3.05%)</td>
<td>(3.04%)</td>
</tr>
<tr>
<td>8D</td>
<td>25D</td>
<td>10D</td>
<td>1.0873</td>
<td>−0.0828</td>
<td>0.1018</td>
<td>0.1018</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>(3.53%)</td>
<td>(2.9%)</td>
<td>(3.59%)</td>
<td>(3.60%)</td>
</tr>
<tr>
<td>8D</td>
<td>25D</td>
<td>14D</td>
<td>1.0489</td>
<td>−0.0852</td>
<td>0.1056</td>
<td>0.1058</td>
</tr>
</tbody>
</table>

Table 3: Comparison of present and previous results.

<table>
<thead>
<tr>
<th></th>
<th>Present</th>
<th>Dutta et al. [34]</th>
<th>Norberg et al. [35]</th>
<th>Okajima [36]</th>
</tr>
</thead>
<tbody>
<tr>
<td>$C_D$,mean</td>
<td>1.162</td>
<td>1.15</td>
<td>1.44</td>
<td>1.6</td>
</tr>
<tr>
<td>$St$</td>
<td>0.124</td>
<td>0.13</td>
<td>0.145</td>
<td>0.14</td>
</tr>
</tbody>
</table>

we will discuss the vorticity contours visualization, time analysis of $C_D$ and $C_L$ and power spectra of $C_L$. During this study the $g/D$ will be varied from 0 to 10 and $l/D$ will be varied from 0.5 to 10.

4.1. The Flow Over Two Tandem Square Cylinders without Splitter Plate. Figures 3(a)–3(f) presents the instantaneous flow visualization of flow field through two SCs in tandem arrangement without splitter plate. The different $g/D$ values in Figures 3(a)–3(f) represented the flow filed characteristics is SBB ($g/D=0.5$ and 1), SF regime ($g/D=2$ and 3), FDF regime ($g/D=5$) and FDTRVS regime ($g/D=9$), respectively. The pattern of vortex was a single row in SBB flow regime (Figure 3(a)). The phenomenon was analogous to the flow past a single SC. When the value of $g/D$ is increased up to 1, the shear layers detached from the $C_1$ reattach on the upper surface of the $C_2$ (Figure 3(b)). When the $g/D$ is increased to 2 and 3, no vortex shedding occurs behind the second cylinder (Figures 3(c), and 3(d)). When $g/D=5$, the fully developed vortex shedding can be clearly seen behind the upstream square cylinder. Under these conditions, the flow behind the downstream SC was almost matching to that around single cylinder, and there was a little affect by the upstream SC (Figure 3(e)). On the other hand, the downstream SC was still affected by the upstream SC, appearing to be a two-rows vortex street at $g/D=9$ (Figure 3(f)).

In the FDF regime, the two inline cylinders separately shed vortices at the same frequency. Igarashi [37] also reported that the two inline circular cylinders shed vortices at the same frequency at reasonably large spacing ratio. It is observed that the FDF or co shedding flow regime occurs at $g/D=5$ where the vortices shed separately from the two cylinders but with same frequency. The negative vortex shedding from $C_1$ hits the front face of the $C_2$ and at the same time the negative and positive shed vortices develop from the cylinder $C_2$. These different shed vortices interact with each other and results in a FDTRVS regime with multi-frequency variation in the spectra of the lift coefficient of $C_2$ (ref. spectrum in Figure 4(j)).

Instantaneous streamline visualization shows the alternate generation of negative and positive shed vortices presented in Figures 5(a)–5(f). It is found that the wake width and vortex formation length are considerably dependent on spacing ratio. In SBB regime, the shear layers separated from the front edges of $C_1$ quickly reattached on the lateral surface of $C_2$, forming two small recirculation regions within the cylinders (Figure 5(b)). Due to strong suction a negative drag value is observed for $C_2$. At $g/D=5$, both the cylinders ($C_1$ and $C_2$) shed vortices and the flow characteristics is called a FDF regime.

Time variation $C_D$ and $C_L$ of both cylinders are shown in Figures 6(a)–6(b) for different spacing ratios. As spacing ratio increases, the amplitude of drag coefficient also increases for FDF regime and FDTRVS regime (Figures 6(i), and 6(k)). It is observed that the $C_D$ of $C_2$ is modulated. At $g/D=0.5$ and 1, the $C_L$ become sinusoidal, and the first cylinder and second cylinder shed vortices result in an inphase mode (Figures 6(b), and 6(d)). At $g/D=2$, the $C_L$ of both cylinders becomes constant (Figure 6(f)).

The spectra graph shows a single dominant peak corresponding to the primary frequency; no secondary frequency was observed in the spectra in case of single bluff body flow regime (Figures 4(a)–4(d)). The small peak in the power spectra (Figures 4(h) and 4(j)) suggests that the second cylinder flow is still affected by the first cylinder.

4.2. The Flow Around Two Tandem Square Cylinders with Attached Splitter Plate. Figures 7(a)–7(e) presents the vorticity contours visualization of flow field around through inline SCs. The different splitter plate length within the spacing between the two cylinders represented the flow filed characteristics in reattachment flow regime ($g/D=1/D=0.5$ and 1) and steady flow regime ($g/D=1/D=2.5$, 5 and 10). In shear layers reattachment flow (SLR) regime, the shear layers separated from the $C_1$ reattach on the upper surface of the $C_2$ (Figures 7(a) and 7(b)). When $g/D=1/D≥2.5$, the steady flow regime can be clearly seen behind both cylinders (Figures 7(c)–7(e)). Under these circumstances, the flow behind the upstream and downstream SCs was almost similar, and it was hardly affected by the downstream SC. Inspection of Figures 8(a)–8(e) further confirms that the flow through the downstream SC becomes steady only in existence of the splitter plate of $1/D≥2.5$.

The higher upward mean lift force is observed for the downstream SC when the two cylinders are closely spaced as the viscous effect is more towards the lower face of the downstream square cylinder. From Figures 9(a), 9(c), 9(e) and 9(g) it can be seen that at $l/D=0.5$, 1, 2.5 and 10 the $C_D1$ and $C_D2$ are both constants. Furthermore, the $C_D2$ having negative drag coefficient at $l/D=0.5$, 1 and 2.5. On the other hand, the lift force has periodic behaviour with decreasing amplitude as the value of $l/D$ increased. Furthermore, at $l/D$
Figure 3: (a–f). Instantaneous vorticity contours visualization at different spacing ratios.

Figure 4: Continued.
Figure 4: Continued.
$D=10$, the lift force is a straight line due to steady flow behaviour behind the cylinders.

The power spectra of $C_L$ of the two cylinders with different splitter plate length are shown in Figures 10(a)–10(f). At $L/D=0.5$, the lift force oscillation of the upstream cylinder was stable, which ensures that the interference is weak between the cylinders. When the splitter plate length is varied from 0.5 to 1, the power spectra not changed. With the further increase in splitter plate length, the interference among the two tandem cylinders slowly disappeared, and the oscillation became stable again. For the downstream cylinder, its lift force oscillation had almost the same behaviour as the upstream square cylinder. The difference was observed when the splitter plate length was varying from 5 to 10. Some
Figure 6: Continued.
Figure 6: (a–l). Time variation of $C_D$ and $C_L$ at different spacing ratios.
Figure 7: (a–e). Vorticity contours at different splitter plate lengths.

Figure 8: (a–e). Streamlines visualization at different values of splitter plate length.
Figure 9: Continued.
Figure 9: (a–h). Time variation of $C_D$ and $C_L$ at different $l/D$ values.

Figure 10: Continued.
minor peaks in the spectra of the upstream square cylinder were observed. This is due to the vortex generated by the $C_1$ directly acts on the $C_2$.

The graphical representation of the different observed flow regimes is given in Figure 11. It can be observed that at small value of $g/D$ and splitter plate length the single bluff body flow regime occurs. At intermediate values of $g/D$ and $l/D$ the shear layers reattachment flow regime occurs. The FDF regime and FDTRVS regime can be seen only for the two tandem square cylinders without splitter plate. It can also be observed from the flow diagram that the splitter plate considerably suppressed the vortex shedding behind the cylinders and completely convert it to steady flow regime.

4.3. Analysis of Force Statistics. In Figure 12(a), compared with the $C_{D_{\text{mean}}}$ of a single SC, the $C_{D_{\text{mean}}}$ of $C_1$ was slightly reduced up to $g/D = 4.5$ without splitter plate. As the $g/D$ increased, the $C_{D_{\text{mean}}}$ of the $C_1$ remained unchanged and was almost equal to an isolated cylinder. The $C_{D_{\text{mean}}}$ of the $C_2$ was considerably smaller than that of single cylinder due to the influence by the wake of the upstream SC. The value of $C_{D_{\text{mean}}}$ of the $C_2$ was negative when $g/D$ is varied from 0.5 to 4. When the value of $g/D$ increased to 4, the $C_{D_{\text{mean}}}$ of $C_2$ changed from negative to positive. As the $g/D$ continued to increase ($g/D > 4$), the $C_{D_{\text{mean}}}$ of the downstream cylinder first increased and then slowly starts to decrease. The transition from shear layers reattachment flow regime to two-row vortex street flow regime was actually a positive-negative conversion of the $C_{D_{T2}}$. It is found that in presence with the splitter plate, the value of $C_{D_{\text{mean}}}$ of the $C_2$ is considerably smaller than in the cases without splitter plate. The splitter plate length has marginal role on drag reduction for $g/D > 5$.

$C_{D_{\text{rms1}}}$ and $C_{D_{\text{rms2}}}$ are the root-mean-square drag values of the first cylinder and second cylinder, respectively (Figure 12(b)). The discontinuity is observed in $C_{D_{\text{rms2}}}$ without splitter plate in Figure 12(b) for the case of $g/D = 4.5$ due to transition of flow regime from shear layers reattachment flow regime ($g/D = 4$) to fully developed flow regime ($g/D = 4.5$). For a splitter plate length of $l/D$ 1 to 10, the $C_{D_{\text{rms}}}$ of both cylinders is nearly equal to that of the isolated cylinder. However, it is found without splitter plate that the $C_{D_{\text{rms2}}}$ is irregular.

From Figure 13(a), it is seen that the $C_{l}$ of the cylinder $C_2$ is more affected as compared to the cylinder $C_1$ due to the

\begin{figure}
\centering
\includegraphics[width=\textwidth]{figure10}
\caption{(a–f). The spectra analysis of lift coefficients at different $l/D$ values.}
\end{figure}

\begin{figure}
\centering
\includegraphics[width=\textwidth]{figure11}
\caption{Flow regimes observed at different splitter plate lengths and spacing ratio.}
\end{figure}
change in $g/D$. The dependency of $C_{\text{rms}2}$ is more pronounced at higher spacing ratios. On the increase of length of the splitter plate, the $C_{\text{rms}2}$ apparently lower than the value of an isolated SC. The shedding frequency is one of the fluidic parameters which can affect the $C_2$ and alter wake dynamics. Similar to the numerical results of Sharman et al. [30], the $St$ values of the $C_1$ and $C_2$ are the same with all $g/D$ values considered in this study.

Figure 14 presents the percentage reduction of $C_{\text{Dmean}}$ of flow past two tandem cylinders. Regarding the $C_{\text{Dmean}2}$, the control effectiveness increases with increasing the splitter plate length: i.e., 49, 53.4, 57.2, 56.1, 62, 63.1, 67.1, 60, 53.1,
59.4, 61, 65.2, 79.1, 76.1, and 74.2% for \( l/D = 0.5, 1, 1.5, 2, 2.5, 3, 3.5, 4, 4.5, 5, 6, 7, 8, 9, \) and 10, respectively. The larger splitter plate length will lead to a better control of fluid forces.

5. Conclusions

In this article, the numerical simulation for flow past two tandem cylinders in presence of attached splitter plate was carried out at \( \text{Re} = 100. \) This study investigates the drag reduction and the interference among the cylinders at various splitter plate length of \( l/D = 0.5 \) to 10. The observed flow regimes were divided into five different regimes: single-bluff body, shear layers reattachment, steady, fully developed two-row vortex shedding and fully developed flow regimes. The \( C_D \) was negative when \( g/D \) is varied from 0.5 to 4. We not found fully developed shed vortices between the cylinders in case of single-bluff body and shear layers reattachment flow regimes. The discontinuity is observed in \( C_{D_{rms2}} \) without splitter plate for the case of \( g/D = 4.5 \) due to transition of flow regime from shear layers reattachment flow regime \( (g/D = 4) \) to fully developed flow regime \( (g/D = 4.5) \). The dependency of root-mean-square value of lift coefficient of the downstream cylinder \( (C_{L_{rms2}}) \) is more pronounced at higher spacing ratios. Regarding the mean drag coefficient of the downstream square cylinder, the maximum reduction about 79.1% is observed for \( l/D = 8. \)

Data Availability

Data will be provided on demand.

Conflicts of Interest

The authors declare that they have no conflicts of interest.

References


