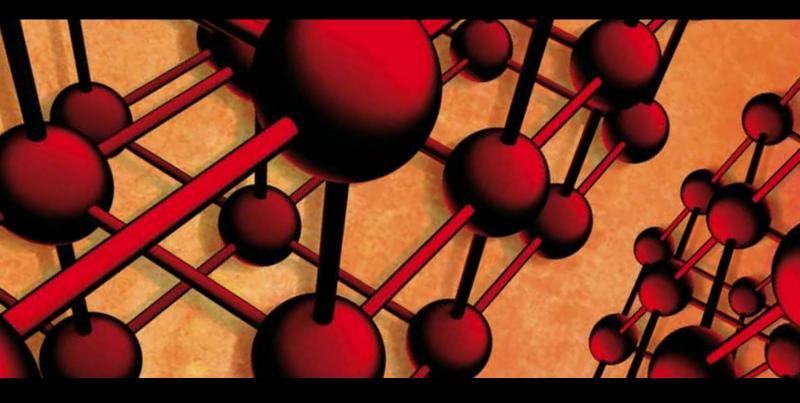
# Solar Energy: Materials, Devices, and Applications

Guest Editors: Ru-Yuan Yang, Yu-Pei Huang, Nowshad Amin, and Fengqiang Sun



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#### **Contents**

**Solar Energy: Materials, Devices, and Applications**, Ru-Yuan Yang, Yu-Pei Huang, Nowshad Amin, and Fengqiang Sun

Volume 2012, Article ID 956561, 1 page

**Segregation of Cu-In-S Elements in the Spray-Pyrolysis-Deposited Layer of CIS Solar Cells**, Seigo Ito and Toshihiro Ryo

Volume 2012, Article ID 136092, 6 pages

Series Resistance Analysis of Passivated Emitter Rear Contact Cells Patterned Using Inkjet Printing,

Martha A. T. Lenio, James Howard, Doris (Pei Hsuan) Lu, Fabian Jentschke, Yael Augarten, Alison Lennon, and Stuart R. Wenham

Volume 2012, Article ID 965418, 8 pages

Study of Ruthenium Complex Sensitizer and Gold Nanoparticles Doped Flexible Organic Solar Cells,

Cheng-Chiang Chen and Lung-Chien Chen

Volume 2012, Article ID 206380, 7 pages

Effects of Organic Compounds on Microstructure, Optical, and Electrical Properties of ITO Thin Films Prepared by Dip-Coating Method, Ru-Yuan Yang, Cheng-Jye Chu, Yu-Ming Peng, and Hui-Ju Chueng Volume 2012, Article ID 741561, 7 pages

**Performance Degradation of Dye-Sensitized Solar Cells Induced by Electrolytes**, Ru-Yuan Yang, Huang-Yu Chen, and Fu-Der Lai

Volume 2012, Article ID 902146, 4 pages

Modeling Approach for Determining Equivalent Optical Constants of Plastic Shading Nets under Solar Radiation Conditions, A. M. Abdel-Ghany and I. M. Al-Helal

Volume 2012, Article ID 158067, 8 pages

Experimental Study on Solar Cooling Tube Using Thermal/Vacuum Emptying Method, Huizhong Zhao,

Haibin Liang, Wenzhe Sun, Guoqing Yu, Dan Cao, and Jun Ji Volume 2012, Article ID 808210, 6 pages

Treatment of Color Filter Wastewater by Fresnel Lens Enhanced Solar Photo-Fenton Process,

Wen-shiuh Kuo and Chia-ling Wu

Volume 2012, Article ID 679206, 6 pages

Hindawi Publishing Corporation Advances in Materials Science and Engineering Volume 2012, Article ID 956561, 1 page doi:10.1155/2012/956561

#### **Editorial**

### Solar Energy: Materials, Devices, and Applications

#### Ru-Yuan Yang,<sup>1</sup> Yu-Pei Huang,<sup>2</sup> Nowshad Amin,<sup>3</sup> and Fengqiang Sun<sup>4</sup>

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As "a low-carbon society and CO<sub>2</sub>-free energy" have been the global issues, so have the opportunities and challenges for renewable energy technologies, like photovoltaic solar cells. Solar energy is an alternative of fossil fuels. Dyesensitized solar cells (DSSCs), organic thin-film solar cells, quantum dot solar cells, Schottky solar cells, inorganic-organic heterojunction solar cells, and many others have been developed with the promise of further improvements to both performance and affordability expected during the last years.

The aim of this special issue has been to present the latest and generalized coverage of the fundamental and constructive ideas, concepts, and important issues in the accepted original research articles stimulating the continuing efforts to solar energy. We received 12 research papers in the research fields. This special issue includes 8 high-quality peer-reviewed papers. We hope that this collection of papers will be a source of ideas and motivation for scientists across different fields in academia and industry to continue further research on solar energy including topics about materials, devices, and applications.

In the fascinating paper by A. M. Abdel-Ghany and I. M. Al-Helal, under solar radiation conditions, the modeling approach has been used to determine equivalent optical constants of plastic shading nets. W.-s. Kuo and C.-l. Wu provide a treatment of color filter wastewater using solar photo-Fenton process enhanced by high-concentrating Fresnel lens. Series resistance analysis is presented by M. Lenio et al. for passivated emitter rear contact cells patterned using inkjet printing. In the nonvacuum processes for solar cell materials, S. Ito and T. Ryo are working successfully

on finding segregation of Cu-In-S elements in the spraypyrolysis-deposited layer of solar cells. In the interesting paper by H. Zhao et al., the experimental study on solar cooling tube has been built using thermal/vacuum emptying method. These wonderful results in the studies of ruthenium complex sensitizer and gold nanoparticles doped flexible organic solar cells are given by L.-C. Chen and C.-C. Chen. Organic compounds effect on microstructure, optical, and electrical properties of ITO thin films prepared by dip coating method has been investigated by Y.-M. Peng et al. Finally, the other published paper has good studies on providing the phenomenon of performance degradation induced by electrolytes for dye-sensitized solar cells by H.-Y. Chen et al.

#### Acknowledgments

The Guest Editors are very thankful to the authors for their fascinating and interesting contributions to this issue with high-quality papers. We are particularly indebted to the staff of Advances in Materials Science and Engineering for their professional and timely support. Additionally, we would also like to show our greatest appreciation to the reviewers for their valuable suggestions/comments to make the special issue successful with highly qualified published papers.

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#### Research Article

## Segregation of Cu-In-S Elements in the Spray-Pyrolysis-Deposited Layer of CIS Solar Cells

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We report the fabrication of superstrate-structured solar cells by the deposition of Cu-In-S (CIS) films on  $\langle glass/FTO/TiO_2/In_2S_3 \rangle$  under air by spray pyrolysis. The cells had an open-circuit voltage of 0.551 V, a photocurrent density of 9.5 mA/cm², a fill factor of 0.45, and a conversion efficiency of 2.14%. However, transmission electron microscopy/energy dispersive X-ray (TEM-EDX) analysis revealed significant differences between the atomic ratio of the setting material in the spray-deposition solution and the elements in the layer. Moreover, TEM-EDX measurements suggested strong segregation of the Cu-In-S elements in the spray-pyrolysis-deposited layer. The degree of segregation depended on the substrate ( $\langle glass \rangle$ ,  $\langle glass/TiO_2 \rangle$ , or  $\langle glass/TiO_2/In_2S_3 \rangle$ ), although Cu<sub>3</sub>In<sub>5</sub>S<sub>9</sub> nanoparticles were segregated in the sulfur layer.

#### 1. Introduction

Compound solar cells with high-conversion efficiencies (20.3%) have been fabricated by vacuum methods [1], which are slow and require costly equipment. Nonvacuum processes for solar cell materials, such as  $Cu(In_{1-x}Ga_x)Se_2$ , CuInSe2, and CuInS2 (CIS), have been investigated with the aim of developing fast and inexpensive fabrication methods. Printing [2, 3], spray-pyrolysis-deposition (SPD) [4, 5], selenization of printed metal oxides with H<sub>2</sub>S or H<sub>2</sub>Se [6], and electrochemical deposition [7, 8] have been explored as alternative methods. Less toxic materials are required because nonvacuum methods are carried out in air; therefore CuInS<sub>2</sub> absorber materials are more suitable than CuInSe<sub>2</sub> or Cu(In,Ga)Se<sub>2</sub>. This is particularly important for SPD methods because aerosols are formed from the compounds. In this work, the structures of spray-pyrolysis-deposited Cu-In-S layers, which have 2.14% conversion efficiency in superstrate-structured solar cells, were studied by transmission electron microscopyenergy dispersive X-ray (TEM-EDX) analysis. It was confirmed that SPD formed a segregated structure in the Cu-In-S layers and the Cu-In-S structure differed between substrates.

#### 2. Experimental

Cu-In-S films were deposited on substrates at 300°C in air, by SPD. The substrates were glass, (glass/TiO<sub>2</sub>), and (glass/TiO<sub>2</sub>/In<sub>2</sub>S<sub>3</sub>). Figure 1 shows the fabrication processes for the Cu-In-S layer and the resulting Cu-In-S structures. The glass substrates were coated with a  $TiO_2$  layer (t =100 nm) by SPD at 400°C. The solution used for depositing the TiO<sub>2</sub> compact layer was a mixture of titanium acetylacetonate (TAA) and ethanol (9:1 v/v). TAA was prepared by slowly injecting acetylacetone (99.5%, Kanto Chemical Co. Inc., Tokyo, Japan) into titanium tetraisopropoxide (97%, Kanto Chemical Co. Inc.) at a mole ratio of 2:1. The  $In_2S_3$  layers (t = 100 nm) were used as the buffer layers and deposited using a precursor solution of InCl<sub>3</sub> (10 mM) and thiourea (20 mM) in water (10 mL) at 300°C. The Cu-In-S spray deposition was performed using an aqueous solution of CuCl<sub>2</sub>·2H<sub>2</sub>O (30 mM; 97.5%, Kanto Chemical Co.), InCl<sub>3</sub> (30 mM; 98%, Kishida Chemical Co., Ltd, Japan) and thiourea (150 mM; Tokyo Chemical Industry Co., Ltd, Tokyo, Japan) giving a Cu/In/S ratio of 1:1:5. The Cu-In-S absorber layer was deposited by spraying the Cu-In-S SPD solution (40 mL) on to each substrate at 300°C at a speed of 2 mL min<sup>-1</sup>. The Cu-In-S layers were scratched

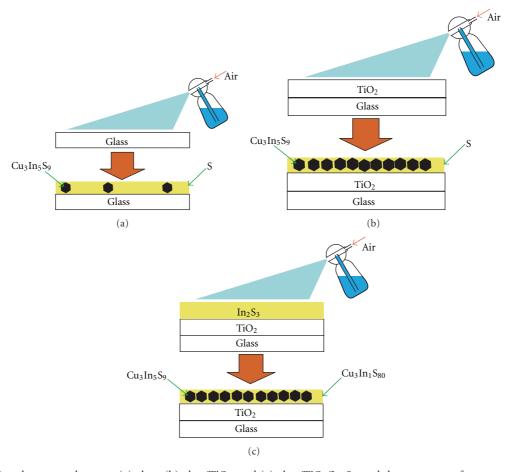


FIGURE 1: Relations between substrates, (a) glass, (b) glass/ $TiO_2$ , and (c) glass/ $TiO_2$ / $In_2S_3$ , and the structures of spray-pyrolysis-deposited Cu-In-S.

from the substrates and powdered, dispersed in ethanol, and attached to Mo grids for TEM observation. A TEM-EDX system (JEOL JEM2100) was used to characterize the Cu-In-S materials. XPS analysis conducted previously showed an oxidation state just on the Cu-In-S surface [5]. Thus, the powdered Cu-In-S samples for TEM observation show the inside of the SPD layer.

SEM cross-section images showed that the surface is relatively flat [5] with a roughness factor of only 1. However, there were several pinholes due to dust and aggregates. Moreover, observation by atomic scale view indicated a very rough surface because it is not a single crystal layer, hence the superstrate-type structure of the solar cells has been fabricated.

The back contact electrode formed from an Au layer deposited by vacuum evaporation produced superstrate-structured solar cells  $\langle \text{glass/F-doped SnO}_2 \text{ (FTO)/TiO}_2/\text{Cu-In-S/Au} \rangle$ . The samples used to obtain the photo I-V curve were 5 mm  $\times$  5 mm. The photovoltaic measurements employed an AM 1.5 solar simulator equipped with a xenon lamp (YSS-100A, Yamashita Denso, Japan). The power of the simulated light was calibrated to  $100 \, \text{mW cm}^{-2}$  by using a reference Si photodiode (Bunkou Keiki, Japan). The I-V curves were obtained by applying an external bias to the cell

and measuring the generated photocurrent with a DC voltage current source (6240, ADCMT, Japan). It is very important to obtain information regarding the electrical properties of samples on various substrates for the preparation of Cu-In-S solar cells. However, since the resistance of the Cu-In-S layer was very high, the electrical resistance and the Hall effects could not be measured.

#### 3. Results and Discussion

Figure 2 shows the photo and dark *I-V* curves for the superstrate-structured solar cell ⟨glass/FTO/TiO<sub>2</sub>/In<sub>2</sub>S<sub>3</sub>/Cu-In-S/Au⟩ fabricated by SPD. The crossing of the curves suggests double-diode effects in the CIS solar cells. The open-circuit photovoltage, the short-circuit photocurrent density, the fill factor, and the conversion efficiency were 0.521 V, 9.68 mA cm<sup>-2</sup>, 0.423, and 2.14%, respectively, and were improvements compared with our previous report [5], obtained by optimizing the SPD conditions. The conversion efficiency is far removed from the best Cu-based solar cells (20.1%) [1]; however, if the efficiency of SPD-processed solar cells can be enhanced by over 10% in the near future, this would be a very significant improvement due to the high-speed and nonvacuum processing methods used in

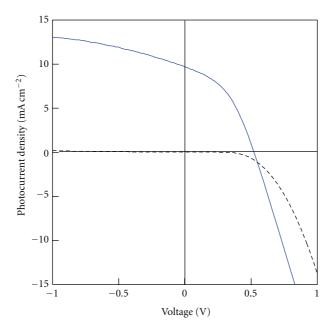


FIGURE 2: Photo (solid) and dark (dashed) *I-V* curves for the  $\langle glass/FTO/TiO_2/In_2S_3/Cu-In-S/Au \rangle$  solar cell. The cell size was 5 mm  $\times$  5 mm, and the cell was irradiated with AM 1.5 (100 mW cm<sup>-2</sup>) light.

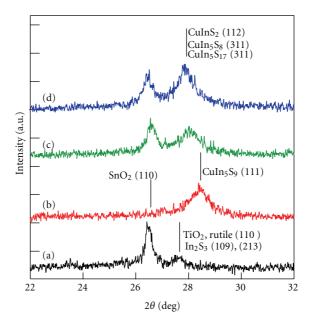
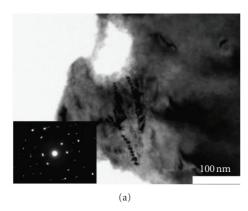


FIGURE 3: XRD patterns of  $\langle glass/FTO/TiO_2/In_2S_3 \rangle$  (a),  $\langle glass/Cu-In-S \rangle$  (b),  $\langle glass/FTO/TiO_2/Cu-In-S \rangle$  (c), and  $\langle glass/FTO/TiO_2/In_2S_3/Cu-In-S \rangle$  (d). Numbers in round brackets show the crystal plane of materials in reference to JCPDS card data.

the fabrication of cost-effective solar cells. Thus, further investigation is required to improve the conversion efficiency. Here, we report changes in the CIS layer as observed by XRD and TEM-EDX.

Figure 3 shows the XRD patterns for the Cu-In-S layers on the different substrates that produced the  $\langle glass/Cu-In-S \rangle$ ,  $\langle glass/FTO/TiO_2/Cu-In-S \rangle$ , and  $\langle glass/TO/TiO_2/Cu-In-S \rangle$ 

FTO/TiO<sub>2</sub>/In<sub>2</sub>S<sub>3</sub>/Cu-In-S $\rangle$  structures. The peak at 26.4° was attributed to SnO<sub>2</sub> (26.6° by JCPDS 88–0287) in FTO (Figure 3(a)); therefore, an SnO<sub>2</sub> peak was not observed in the XRD pattern of Cu-In-S on the glass substrate (Figure 3(b)). The peak at 27.6° in Figure 3(a) was assigned to In<sub>2</sub>S<sub>3</sub> (27.4° by JCPDS 73–1366) and TiO<sub>2</sub> (27.7° by JCPDS 88–1173) and was not observed



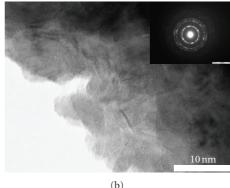
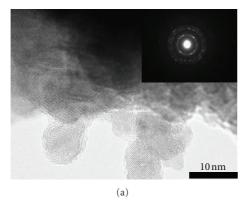


FIGURE 4: TEM image of spray-pyrolysis-deposited Cu-In-S with the electron diffusion patterns (inset) on a glass substrate: (a) the major part and (b) the minor part.



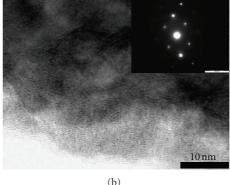


FIGURE 5: TEM image of spray-pyrolysis-deposited Cu-In-S with the electron diffusion patterns (inset) on a glass/TiO<sub>2</sub> substrate: (a) the major part and (b) the minor part.

TABLE 1: The atomic ratios of Cu-In-S analyzed by TEM-EDX. Each location is indicated by the relevant figure number.

Substrate	Major/Minor	Cu	In	S	Figures
(glass)	Major	0.06	0.00	99.94	Figure 4(a)
(grass)	Minor	16.00	28.41	55.58	Figure 4(b)
$\langle glass/TiO_2 \rangle$	Major	16.49	30.49	53.02	Figure 5(a)
	Minor	0.19	0.25	99.56	Figure 5(b)
\(\langle glass/\text{TiO}_2/\text{In}_2 \text{S}_3 \rangle	Major	17.85	29.51	52.65	Figure 6(a)
	Minor	3.78	1.17	95.05	Figure 6(b)

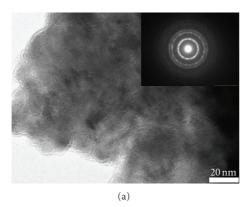
in the  $\langle glass/FTO/TiO_2/In_2S_3/Cu-In-S \rangle$  (Figure 3(c)) and  $\langle glass/FTO/TiO_2/In_2S_3/Cu-In-S \rangle$  (Figure 3(d)) XRD patterns. Hence, the  $In_2S_3$  layer had diffused into the Cu-In-S layer, confirmed by EPMA mapping analysis of the cross-sectional image [5]. The  $TiO_2$  peak was buried below the Cu-In-S layer (Figure 3(c)) because of the very thin  $TiO_2$  layer (t = 200 nm) and made evident by the small XRD signal.

Although the positions of the peaks were very close to the CuInS<sub>2</sub> peak (27.9° by JCPDS: 85–1575), the CuIn-S XRD peaks (27.8–28.4°) varied significantly among substrates (Figures 3(b)–3(d)) and the peak shifts suggested variations in the types of Cu-In-S crystals. Due to the large

ratio of sulfur in the Cu-In-S layer (Cu-poor), which will be addressed in the TEM-EDX discussion to follow, assignment of the peaks from 27.8° to 28.4° in Figures 3(b)–3(d) would be CuIn<sub>11</sub>S<sub>17</sub> (27.7° by JCPDS: 34–0797), CuIn<sub>5</sub>S<sub>8</sub> (27.7° by JCPDS: 72–0956), and CuIn<sub>5</sub>S<sub>9</sub> (28.4° by JCPDS: 49–1383). Therefore, it was thought that the peak shifts may be due to variations in the Cu-In-S crystals, which are projecting the compositions of the Cu-In-S.

The elemental analysis of Cu-In-S by TEM-EDX is shown in Table 1 and the locations analyzed are shown in Figures 4, 5, and 6. The Cu-In-S samples for TEM-EDX analysis were taken from the layers deposited on the different substrates: glass, glass/TiO<sub>2</sub>, and glass/TiO<sub>2</sub>/In<sub>2</sub>S<sub>3</sub>. It was confirmed that the Cu-In-S elements were segregated in the SPD layer. The components of the Cu-In-S materials were CuInS<sub>2</sub>, Cu<sub>3</sub>In<sub>5</sub>S<sub>9</sub>, Cu<sub>2</sub>In<sub>4</sub>S<sub>7</sub>, CuIn<sub>3</sub>S<sub>5</sub>, and CuIn<sub>5</sub>S<sub>8</sub> [9] with atomic ratios calculated as 25.00:25.00:50.00, 17.65:29.41:52.94, 15.38:30.77:53.85, 11.11:33.33:55.56, and 7.14:35.71:57.14, respectively. Therefore, the Cu-poor and In-rich portions of the segregated Cu-In-S layer were close to the composition ratio of Cu<sub>3</sub>In<sub>5</sub>S<sub>9</sub>.

Figure 4 shows the TEM images of Cu-In-S deposited on a glass substrate. It was confirmed that, although the spray-pyrolysis solution for the Cu-In-S layer contained a



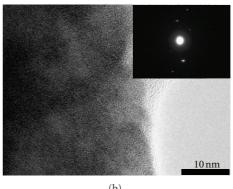


FIGURE 6: TEM image of spray-pyrolysis-deposited Cu-In-S with the electron diffusion patterns (inset) on a glass/ $TiO_2/In_2S_3$  substrate: (a) the major part and (b) the minor part.

significant amount of copper and indium, the layer on the glass substrate was mainly pure sulfur (Figure 4(a), Table 1). The sulfur particles were several hundred nanometers in size. The atomic lattice was not visible in the TEM images because sulfur is much lighter than the heavy metal elements. However, the electron scattering patterns showed a single crystal (inset, Figure 4(a)). A small number of nanoparticles around 10 nm in diameter were observed (Figure 4(b)) and revealed the atomic lattice because they contained metallic elements. The electron sputtering pattern (inset, Figure 4(b)) suggested the existence of a polycrystalline structure. EDX analysis indicated that the Cu-In-S elemental ratio was close to Cu<sub>3</sub>In<sub>5</sub>S<sub>9</sub>. Hence, a considerable amount of the copper metal source (CuCl<sub>2</sub>) did not end up in the Cu-In-S layer and was dispersed somewhere else during SPD. The structure of the Cu-In-S layer (Figure 1(a)) shows the segregated Cu<sub>3</sub>In<sub>5</sub>S<sub>9</sub> particles in the sulfur layer.

Figure 5 shows the TEM images of Cu-In-S deposited on a glass/TiO<sub>2</sub> substrate. In contrast to the glass substrate (Figure 4), most of the Cu-In-S layer consisted of Cu<sub>3</sub>In<sub>5</sub>S<sub>9</sub> nanocrystals, 10 nm in diameter (Figure 5(a)). The electron diffraction pattern also suggested it had a nanocrystalline structure. Again the heavy metal elements meant that the nanocrystal atomic lattice could be observed. Although the nanocrystals contained copper, the Cu/In ratio was only 0.54:1, which was half that of the setting ratio (1:1) in the spray-deposition solution. The CuCl<sub>2</sub> in the Cu-In-S solution was again dispersed and not deposited in the Cu-In-S layer. In the minor part of Cu-In-S layer, a small amount of copper was observed (Figure 5(b)). However, when the substrate was changed from glass to glass/TiO2, the amount of metal ([Cu + In]/[Cu + In + S]) in the sulfur rich part increased from 0.06% (Figure 4(a)) to 0.44% (Figure 5(b)). The electron scattering suggested a single crystal (inset, Figure 5(b)), although an atomic lattice was not observed, which may be because sulfur is a light element. Therefore, it was concluded that the substrate ( $\langle glass \rangle$  or  $\langle glass/TiO_2 \rangle$ ) significantly affected the composition and structure of the spray-pyrolysis-deposited CuInSe<sub>2</sub> layer. The structure of Cu-In-S layer deposited on the glass/TiO<sub>2</sub> substrate by spray pyrolysis is shown in Figure 1(b).

Figure 6 shows the TEM images of Cu-In-Se deposited on a glass/TiO<sub>2</sub>/In<sub>2</sub>S<sub>3</sub> substrate. The atomic ratio showed that, for Cu-In-Se, the layer mainly consisted of Cu<sub>3</sub>In<sub>5</sub>S<sub>9</sub> (Figure 6(a)), although a small amount of Cu<sub>3</sub>In<sub>1</sub>S<sub>80</sub> (Figure 6(b)) was present. Pure sulfur (Figures 4(a) and 5(b)) was not observed because of the In<sub>2</sub>S<sub>3</sub> buffer layer and interdiffusion to the upper Cu-In-S layer. Cu<sub>3</sub>In<sub>5</sub>S<sub>9</sub> was present as nanocrystals, around 10 nm in diameter (Figure 6(a)), and the electron diffraction pattern suggested a polycrystalline structure (inset, Figure 6(a)). The Cu<sub>3</sub>In<sub>1</sub>S<sub>80</sub> particles were around several hundred nanometers in size (Figure 6(b)) and the atomic lattice was not visible because of the light sulfur atoms, although the electron diffraction pattern suggests a single-crystalline structure (inset, Figure 6(b)). Therefore, Cu-In-S was segregated as Cu<sub>3</sub>In<sub>5</sub>S<sub>9</sub> and Cu<sub>3</sub>In<sub>1</sub>S<sub>80</sub>. The structure of the Cu-In-S layer deposited on the glass/TiO<sub>2</sub>/In<sub>2</sub>S<sub>3</sub> substrate by spray pyrolysis is shown in Figure 1(c).

The ratios of Cu-In-S, such as Cu<sub>3</sub>In<sub>5</sub>S<sub>9</sub> and Cu<sub>3</sub>In<sub>1</sub>S<sub>80</sub>, simply show integral multiplication of the TEM-XRD results of Table 1. From a scientific point of view, the crystal structures should be revealed by XRD analysis. However, the results from normal XRD were obscure and GIXRD may be a more suitable method. Nevertheless, although GIXRD may have provided better results, the Cu-In-S was a mixture of small crystals and amorphous phases of different Cu-In-S compositions, making crystal identification in this work very complicated. It would be desirable to improve the analytical methods in the future.

#### 4. Conclusions

Compound solar cells based on Cu-In-S (CIS) were prepared by SPD under air. Although the Cu-In-S layer had a segregated structure, the solar cells had a 9.68 mA cm<sup>-2</sup> short-circuit photocurrent density and 2.14% conversion efficiency. The segregated structures differed among substrates. The resulting Cu-In-S layers were copper poor due to the loss of CuCl<sub>2</sub> during SPD. Therefore, the next step in improving the conversion efficiency is to control the amount of copper in the Cu-In-S layer. Since the significance of the

contribution of a Cu-poor CuInS<sub>2</sub> and CuInSe<sub>2</sub> solar cells has been discussed in the publications [10, 11], we believe that a Cu-poor CuInS<sub>2</sub> layer, and hence the presence of Cu<sub>3</sub>In<sub>5</sub>S<sub>9</sub>, may contribute to the photovoltaic effects.

Samples prepared for this kind of work may be solid mixtures of CuInS<sub>2</sub>, CuIn<sub>3</sub>S<sub>5</sub>, and so on and should be clearly identified. Each major part of the sample was expressed in the TEM figures in this paper. It is very difficult to obtain the exact components of such segregated materials by other methods, such as XPS, Auger, SIMS, Raman, XRD, and EPMA, because the resolutions in these methods reach the submicron range and give mixed information about major and minor parts of the materials. Advancements in the analytical tools may reveal further details in the future.

#### Acknowledgment

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#### Research Article

## Series Resistance Analysis of Passivated Emitter Rear Contact Cells Patterned Using Inkjet Printing

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For higher-efficiency solar cell structures, such as the Passivated Emitter Rear Contact (PERC) cells, to be fabricated in a manufacturing environment, potentially low-cost techniques such as inkjet printing and metal plating are desirable. A common problem that is experienced when fabricating PERC cells is low fill factors due to high series resistance. This paper identifies and attempts to quantify sources of series resistance in inkjet-patterned PERC cells that employ electroless or light-induced nickel-plating techniques followed by copper light-induced plating. Photoluminescence imaging is used to determine locations of series resistance losses in these inkjet-patterned and plated PERC cells.

#### 1. Introduction

As the photovoltaics industry becomes more mature, manufacturers must find new ways of staying competitive. Developing cost-effective ways of fabricating higher-efficiency cell structures that have to date only been realized in a laboratory environment is an option that is being considered by many. An obvious cell structure to attempt to commercialise is the Passivated Emitter Rear Contact (PERC) cell [1, 2].

New patterning methods such as inkjet printing and laser doping [3–5] enable the patterning of dielectric layers for metal contacting and therefore eliminate the need to use techniques such as photolithography which enabled the earlier laboratory implementations of these cells. Metal plating, which has been successfully used for the manufacture of photovoltaic devices in industry [6], is compatible with these patterning methods and consequently presents as a commercially viable metallization method. In addition to enabling the use of less expensive metals like Ni and Cu, metal plating is a self-aligning process thus eliminating the need for the photolithographic lift-off steps which were used

in conjunction with evaporated Ti-Pd-Ag metal contacts. A further advance that is desirable to make PERC cells commercially viable is to reduce the number of high temperature steps [7, 8].

This paper contains an analysis of the series resistance losses of PERC cells that have been fabricated using inkjet printing (IJP) for the patterning steps and self-aligned Ni and Cu plating for the metallization. The fabricated PERC cells were analyzed using photoluminescence (PL) imaging, current-voltage (IV) measurements, and microscopy. Transmission line model (TLM) test structures were fabricated to characterize the metal-silicon interface and estimate the contact resistance associated with both the front and rear metal contacts. The findings of this work show that a decrease in fill factor due to high series resistive losses is a problem with electrolessly plated PERC cells. This is consistent with the findings of other researchers who have seen fill factor losses in their electrolessly plated PERC cells that were formed using laser-fired rear contacts [9]. It was found here that spurious Ni plating on the rear point contacts forms during electroless Ni plating, and this contributes

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significantly to the high series resistance and resulting low fill factors of final devices. Poorly adhered front contacts were also an issue with inkjet-printed and electrolessly plated PERC cells. It is shown that use of appropriate plating techniques, such as bias-assisted light induced plating, can help reduce these resistive effects.

#### 2. Experimental Procedure

2.1. Cell and Test Structure Fabrication. Cells and test structures were fabricated on planar,  $0.5\,\Omega\cdot\text{cm}$ , p-type,  $200\,\mu\text{m}$  thick, FZ Si wafers. The processing sequence used for the cells is outlined in Table 1. The emitter sheet resistance after processing was  $\sim 120\,\Omega/\square$ . Nickel contacts were formed using both electroless plating and bias-assisted LIP. In the latter process, a bias voltage of  $0.6\,\text{V}$  was applied to the rear Al surface of the devices (this setup can be seen in Figure 1(a)). All Cu plating was performed using noncontact LIP without an applied bias (see Figure 1(b)).

The dimensions of the completed cells are detailed in Table 2. The TLM test structures underwent the same thermal processing as the fabricated cells. The only difference in the fabrication sequence was the inkjet patterning. Instead of forming openings for front finger grids and rear point contacts, TLM contact pads were patterned using the indirect inkjet patterning method [5] for the (front) Ni and (rear) Al contact resistance test structures. For the rear measurements, TLM contact pads of Al were evaporated through a mask which was aligned to the inkjet-patterned openings in the rear SiO<sub>2</sub> dielectric layer.

2.2. Analysis. The series resistance of the final IJP PERC cells was estimated from comparing the light-IV measurements with the Suns- $V_{\rm oc}$  measurements [10]. Photoluminescence (PL) imaging was used to record a spatially resolved image of the voltage across the cells. Two types of PL imaging were used: open-circuit PL and  $R_s$ -PL [11, 12]. The contributing components of the series resistance were identified, and each component was calculated using actual dimensions and resistances measured from test structures. Scanning electron microscope (SEM), focused ion beam (FIB), and optical microscopy were used to inspect the quality of the metal contacts and to help determine the underlying causes of the high series resistance problems experienced by IJP PERC cells.

#### 3. Results and Discussion

3.1. Contact Resistance Results. The TLM measurements for the front Ni contacts depended on the plating technique used, with the average specific contact resistivity being  $0.07 \pm 0.04 \,\Omega \cdot \text{cm}^2$  and  $0.09 \pm 0.02 \,\Omega \cdot \text{cm}^2$  for electroless Ni and bias-assisted LIP Ni contacts, respectively. There were some variations between individual test structures using the same Ni-plating technique, particularly with the electroless Ni-plated cells. Specific contact resistivities as low as  $3.5 \times 10^{-5} \,\Omega \cdot \text{cm}^2$  have been reported previously for Ni/Cu-plated fingers [19]. The discrepancy between the resistivity values

could be due to the difficulty experienced in achieving good adhesion between the Ni and Si.

The specific contact resistivity for the Al-Si rear contact TLM test structures was measured to be  $0.004 \pm 0.003 \,\Omega \cdot \text{cm}^2$ and  $0.028 \pm 0.010 \,\Omega \cdot \text{cm}^2$ , before and after electroless Ni plating, respectively. The value before electroless Ni plating is higher but on the same order of magnitude as previously reported values of  $0.0015 \Omega \cdot \text{cm}^2$  for Al on  $0.5 \Omega \cdot \text{cm}$  p-type Si [18, 20, 21]. The increase in specific contact resistivity after electroless plating was due to spurious Ni plating at the Al-Si rear contacts [18]. Figure 2 shows an FIB image of Ni plated around a rear point contact on an IJP PERC cell that underwent electroless Ni plating. Nickel plates preferentially on the rear surface at regions where the Al is rough or contains a higher Si content than the surrounding Al [18]. In some areas, the Ni displaces the Al through galvanic displacement, coming into direct contact with the Si (see Figure 3). This plated Ni contributes to the metal Si contact and causes increased contact resistance due to the fact that Ni has a higher barrier height on p-type Si than Al [20].

The spurious rear-side Ni plating was only observed with cells and test structures which underwent electroless Ni plating. In bias-assisted LIP, the rear surface was protected from undesired plating by the bias voltage, and so rear-side plating was avoided. The absence of Ni on the rear contacts means that the Al-Si contact resistance measured from the test TLMs can be used as the contact resistance for rear contacts formed using BA-LIP.

3.2. Light IV Results. The cells were tested under standard conditions using an Adventest DC Voltage Current Source/Monitor, a temperature-controlled copper block, and a halogen lamp light source calibrated to one-sun using a calibrated reference cell. Suns- $V_{\rm oc}$  measurements were done using a flash tester, and the series resistance was estimated from comparing the light IV data to the Suns- $V_{\rm oc}$  data. The open-circuit voltage  $(V_{oc})$ , fill factor (FF), series resistance  $(R_s)$ , and shunt resistance  $(R_{sh})$  data for the cells plated using electroless Ni and BA-LIP Ni are listed in Table 3. The series resistance of the electroless Ni-plated cell was higher than that measured in the BA-LIP Ni-plated cell. The FFs of both cells are remarkably low. Shunting was an issue particularly for the BA-LIP sample, and the series resistance was high for both cells. The shunting in the BA-LIP batch of samples was due to inadequate resist coating on the front surface of the cell during the rear contact patterning step. Pinholes formed, creating holes through the dielectric and emitter which were subsequently plated with metal.

3.3. Photoluminescence Results. Photoluminescence imaging gives a spatially resolved image of locations of high and low voltages within a cell or wafer. When the cell is at open circuit, there is no lateral current flow, so areas of low voltage represent areas of high recombination. The PL intensity is directly proportional to the exponential of the voltage according to (1) [22]:

$$I_{\text{PL},i} = C_i \exp\left(\frac{eU_i}{kT}\right),\tag{1}$$

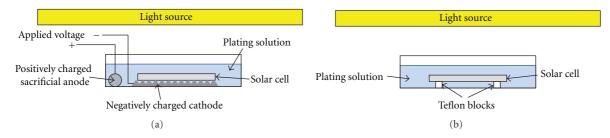


FIGURE 1: Experimental setup for (a) bias-assisted LIP; (b) noncontact LIP.

TABLE 1: Processing sequence for IJP PERC cells.

Step	Process	Conditions
(1)	Damage etch/texture	20 min etch in 30% NaOH at 80°C
(2)	Oxidation	Dry oxidation, $1030^{\circ}$ C for 4 hr with $1\%$ TCA in $O_2$
(3)	Strip front oxide	Mask rear; strip SiO <sub>2</sub> with buffered HF
(4)	Emitter diffusion + oxidation	Diffusion: P solid source, $850^{\circ}$ C, $15$ min Oxidation: $1100^{\circ}$ C, $5$ hr, $1\%$ TCA in $O_2$ , $15$ min anneal in $N_2$
(5)	IJP the front contacts	Indirect IJP method [5]
(6)	Groove diffusion + drive-in	Diffusion: P solid source, 940°C, 90 min Drive-in: 1000°C, 3 hr, N <sub>2</sub>
(7)	IJP the rear contacts	Indirect IJP method [5]
(8)	Evaporate rear Al + sinter	$1-2 \mu m$ Al, sinter at $400$ °C, $30 \min$ in forming gas
(9)	Ni plate + anneal	Various plating methods; anneal at 400°C, 10 min in forming gas
(10)	Cu light-induced plate	Cu electroplating solution, 5 min under high-intensity fluorescent light
(11)	Edge isolation	Cut with a 1064 nm Nd: YAG laser from the rear; cut 1/2 way thru wafer then snapped

Ni plating was done in one of two ways: (i) electroless Ni using Transene EN solution [9],  $80^{\circ}$ C for 3 min; or (ii) BA-LIP Ni,  $25-30^{\circ}$ C for 30 s under high-intensity fluorescent light. The BA-LIP Ni consisted of Watt's solution in the ratios  $10 \text{ g Ni}_2\text{SO}_4$ ,  $20 \text{ g Ni}_2\text{Cl}_2$ , 4 g boric acid in 100 mL deionized water [13]. The electroplating solution for the Cu plating used  $12 \text{ g CuSO}_4$ ,  $11 \text{ mL H}_2\text{SO}_4$ , and 50 mL deionized water.

TABLE 2: Dimensions for cell design and analysis.

Parameter	Value	Variability
Cell area	$8 \text{ cm}^2$	$\pm 0.15  \text{cm}^2$
Finger width	$90  \mu \mathrm{m}$	$\pm 10  \mu \mathrm{m}$
Finger height	$5  \mu \mathrm{m}$	$\pm 2 \mu\mathrm{m}$
Finger length	28 mm	$\pm 0.5  \mathrm{mm}$
Finger spacing	1.2 mm	$\pm 10  \mu \mathrm{m}$
Rear contact diameter	$100  \mu \mathrm{m}$	$\pm 10  \mu \mathrm{m}$
Rear contact spacing	1.5 mm	$\pm 10  \mu \mathrm{m}$

where  $I_{\mathrm{PL},i}$  is the PL intensity at a specific location i,  $U_i$  is the voltage at that location, and  $C_i$  is a local calibration constant. With an open circuit PL image, the calibration constant can be calculated using the  $V_{\mathrm{oc}}$  obtained from the light IV measurement along with the average PL signal from the PL image [22]. This then allows the voltage at any particular point in the image to be calculated from the PL signal.

Figure 4(a) shows an open-circuit PL image of an inkjetpatterned PERC cell that had its front metal contacts formed using electroless Ni plating followed by LIP Cu plating. The rear point contacts can be clearly seen in this image. At open circuit, with no current extraction occurring, locations of

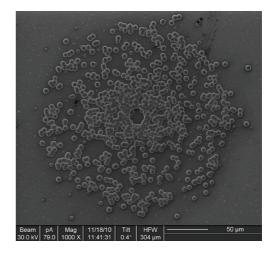


FIGURE 2: Focused ion beam (FIB) image of the rear of a test cell. Unwanted Ni plating can be seen around a rear point contact on an IJP PERC cell plated using electroless Ni [18].

low voltage must be due to either shunts or high recombination (low lifetime). Some shunts are apparent, as larger dark spots in a few locations on the wafer, but the regular

Ni-plating method	V <sub>oc</sub> (mV)	Fill factor	Series resistance $(\Omega \cdot cm^2)$	Shunt resistance (kΩ·cm²)
Electroless Ni	646	0.61	4.1	42.7
Bias-assisted LIP Ni	617	0.59	1.5	0.10

TABLE 3: Cell performance from light IV data.

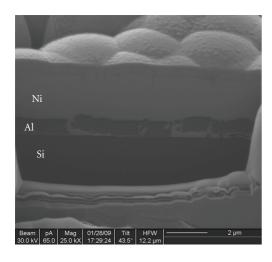


FIGURE 3: Focused ion beam (FIB) cross-section image of the rear contact of a test cell. Unwanted electroless Ni plating at the rear point contact has displaced some of the Al, contacting the Si surface and increasing the contact resistance [18].

rear contact design is also seen as a regular, shadowy pattern across the entire wafer. These contact locations are necessarily identified as locations of high recombination as a result.

Figure 4(b) shows the series resistance PL image of an electroless Ni-plated cell. In this image, bright areas indicate regions of high series resistance. Prominent features are the bright areas on the left and right edges of the cell, as well as the two darker regions spreading out from the busbar, again to the left and right sides of the cell. The bright regions on the very edges are regions of high series resistance caused by the edge cleave being too far away from the front contact grid. This can be easily corrected with more careful processing. The dark regions spreading out from the busbar indicate that the series resistance in these areas increases as you move away from the busbar—the resistance is limited by the line resistance of the fingers. In the centre, the whole area is orange (high resistance—about  $6 \Omega \cdot \text{cm}^2$ ) which is likely due to poor contact between the Ni and the Si, creating a high resistance everywhere. The average series resistance of this cell measured from the PL image data is  $5.25 \Omega \cdot \text{cm}^2$ .

Figure 5(a) shows the open-circuit PL image for a cell fabricated using BA-LIP Ni and LIP Cu. The rear point contacts are no longer visible, indicating that the recombination at the contacts is less than it was for the electrolessly Niplated cells.

Figure 5(b) shows the series resistance PL image of the same BA-LIP Ni-plated cell. Due to both the decreased resistive losses at both the front and rear contacts, it was expected that the total  $R_s$  of bias-assisted LIP Ni cells would be less than the electroless Ni-plated cells, and this is in fact

the case. There are fewer bright regions on this sample, with an average series resistance of  $2.9\,\Omega\cdot\text{cm}^2$  being measured using this method (IV measurements indicate  $1.48\,\Omega\cdot\text{cm}^2$ —the discrepancy between the measurements may be due to the low shunt resistance affecting the  $R_s$  calculation from the IV data). Some high resistance is again seen at the edge of the cell, due to the edge cleave again being too distant from the front contact grid. One finger peeled off the front, and this region of slightly higher series resistance is highlighted by the blue circle, but in general this image shows a much more uniform resistance across the surface of the cell. This means that the contact between the Ni and Si that is formed through BA-LIP Ni plating is more uniformly good across the surface of the wafer.

3.4. Breakdown Analysis of Series Resistance. Figure 6 depicts the sources of series resistance in a PERC cell. The lateral resistance through the emitter (1), line resistance through the fingers (3), resistance through the base (4), and spreading resistance at the rear contacts (5) are all functions of the material properties and geometry, and as such can be estimated from theory. The contact resistances, at (2) and (6), require measurements to be performed, as the actual resistance at contact locations is often very different to the theoretically expected resistance [23].

Table 4 summarizes the total estimated series resistance contribution based on the theoretical and experimental calculations, as well as the associated power loss from each type of series resistance. The percent power loss was calculated using (2). Effective resistances must be calculated in order to use this equation as, for example, not the full current generated flows through the full sheet resistance. Details on how to calculate the individual effective resistances are provided in the appendix:

$$\%P_{\text{loss}} = \frac{P_{\text{loss}}}{P_{\text{gen}}} = \frac{I_{\text{MP}}^2 R_{\text{eff}}}{I_{\text{MP}} V_{\text{MP}}} = \frac{I_{\text{MP}} R_{\text{eff}}}{V_{\text{MP}}}.$$
 (2)

As a percentage of total power loss, the rear point contacts are a major contributor to the overall series resistance on the electroless Ni-plated cells. For the cells Ni plated using BA-LIP, the calculated total resistance was within 1% of that estimated from the  $R_s$ -PL measurements. The value used for the rear contact resistance was that measured for an Al-Si contact after Ni plating; however, the FIB images show that there is also spurious Cu present at the rear contacts. As the calculated expected resistance is close to that measured, it is assumed that the spurious Cu did not have a significant impact on the series resistance of the finished devices.

For the cells where the Ni plating was achieved using electroless plating, the calculated total resistance is far greater than the resistance estimated from the IV measurements.

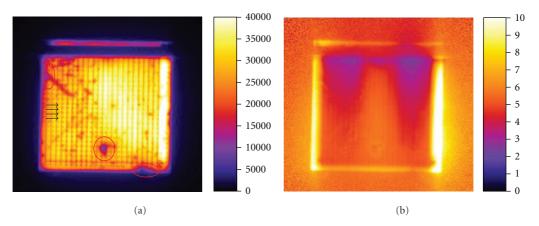


FIGURE 4: (a) Open-circuit PL image of a PERC cell made using EN and LIP Cu. The brighter the area, the higher the voltage in that location. The arrows highlight the locations of some of the rear point contacts, red circles are locations of shunts; (b) series resistance PL image of the same cell, bias voltage is -300 mV.

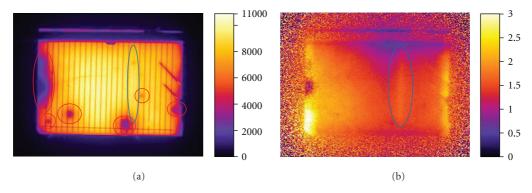


FIGURE 5: (a) Open-circuit PL image of a PERC cell fabricated using BA-LIP Ni and LIP Cu plating. The edges of the cell have been isolated with a laser. Red circles are shunt locations. Blue circle location of a peeled finger; (b) series resistance PL image of the same cell using a bias voltage of –300 mV.

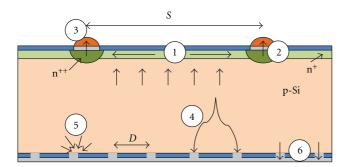


FIGURE 6: Locations of series resistance contributors in a PERC solar cell. S denotes the spacing between the front fingers, and D the spacing between the rear contact points. The length of the fingers is denoted by L (after [23]).

A worst-case scenario was used for the base contact resistance, as the variability in the contact resistance measurements can be great depending on how bad the spurious Ni on the rear is. Despite using the worst-case experimental values for  $\rho_c$ , the true value could be as low as  $0.049 \,\Omega \cdot \text{cm}^2$  contribution, resulting in a percent power loss of 2.5%.

The variation across the electroless plated Ni cells is thought to be due to the variation in the severity of the excess Ni plating that occurs from cell to cell.

Focused ion beam (FIB) was used to examine the test cell contacts in order to track down a cause of the high resistance in the cells plated using BA-LIP. The rear contacts exhibited some unwanted plating once again, but this time from the LIP Cu. Figure 7 shows a cross-section of a rear contact from a cell plated using bias-assisted LIP.

Light-induced plating is an equivalent technique to electroplating, with the plating voltage being supplied by the cell itself. As such, it was expected that Cu plating would only occur on the front surface. Cu plated to the rear, though, again in the locations around the rear point contacts. This is thought to be caused by local areas of relatively different voltage. At the rear surface, the Al is oxidizing due to electrons being drained to the front of the cell and driving the reduction of Cu at the front surface. However, the first Al to oxidize will be the Al that is in direct contact with the Si surface. The electrons will be taken from there first, and a voltage potential will form between the Al in contact with the Si and the Al that is floating on the dielectric. The reduction of hydrogen at cathodic sites on the rear surface

Resistance source	Electroless Ni Bias-Ass		Bias-Assiste	sisted LIP Ni	
Resistance source	$R_s (\Omega \cdot \text{cm}^2)$	$P_{ m loss}(\%)$	$R_s \left(\Omega \cdot \text{cm}^2\right)$	$P_{\mathrm{loss}}$ (%)	
Lateral resistance through the emitter	0.152	0.6	0.152	0.6	
Line resistance along the fingers*	0.112	0.4	0.112	0.4	
Resistance through the base*	0.072	0.3	0.072	0.3	
Spreading resistance**	0.560	2.2	0.560	2.2	
Front contact resistance	0.090	4.6	0.107	5.5	
Rear contact resistance***	0.028	28.7	0.004	4.1	
Total	4.9	36.7	2.7	13.0	
Total measured <i>R</i> from IV	4.1		1.48		
Total measured $R$ from $R_s$ -PL	5.3		2.9		

TABLE 4: Sources of series resistance.

<sup>\*\*\*</sup> From [18].

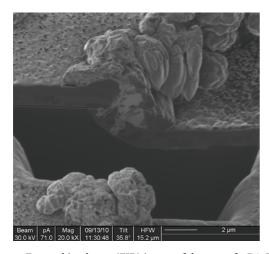


FIGURE 7: Focused ion beam (FIB) image of the rear of a BA-LIP Ni with LIP Cu test cell. Unwanted Cu plating can be seen at the edges of the rear point contacts.

can result in the formation of bubbles which can cause pitting and variations in surface potential [24]. Bias-assisted LIP of Cu where the rear surface is not in contact with the plating solution should address these issues. A number of commercial tool manufacturers are now developing BA-LIP tools which keep the Al rear surfaces of cells dry [25].

#### 4. Summary and Future Research

In order to achieve higher-efficiency solar cells at lower cost, new fabrication methods such as inkjet patterning and metal plating may need to be considered. This research has identified and quantified the major series resistance losses inherent in the IJP PERC cell. The rear contact resistance of the Al-Si contacts is higher than expected for cells that were Ni plated using both electroless plating and BA-LIP. This results in higher series resistance and lower fill factors being achieved than is desirable. The specific contact resistivity of the these rear contacts in the electroless Ni-plated cells was an order of magnitude greater than for the cell plated using

BA-LIP due to spurious plating of Ni in the regions of the rear contacts.

Future work should focus on methods of achieving low resistance contacts on the rear of the cell. Bias-assisted LIP tools which maintain the rear surface dry will be required to ensure that plated metals do not interfere the electrical properties of the rear contacts. In addition to the rear contact resistance, the rear spreading resistance also needs to be reduced. Ideally this would be achieved by spacing the contacts closer together; however, unless the contact regions are heavily doped to minimize the minority carrier concentration at the surface, the recombination in the device will be increased resulting in a lower device voltage. Future work can also focus on how to form doped rear contact regions, either through laser-fired contacts [2], laser doping [1, 3], or local Al BSFs formed by firing Al through openings in a rear passivation layer.

#### **Appendix**

The locations where series resistance occurs in the cell are shown in Figure 5. In this section, the calculations done for determining each portion of the series resistance are shown.

(A) Lateral Resistance through the Emitter. When calculating the series resistance as a result of the current flowing through the emitter, it is important to note that not all the current will see the full resistance; the current generated close to the contact fingers will have less distance to travel through the emitter and experience less resistance than current generated midway between two fingers. A proper summation of the current must be done in order to obtain the effective resistance contribution from the emitter. From [14, 15], the following equation can be used to determine the resistance contribution from the emitter:

$$R_{\text{eff}} = \frac{1}{3} \frac{S/2}{L} \frac{\rho}{t},\tag{A.1}$$

where *S* is the finger spacing, *L* is the length of the fingers, and  $\rho/t$  is the sheet resistance of the emitter. With an emitter sheet resistance of ~120  $\Omega$ /sq, the effective resistance

<sup>\*[14, 15].</sup> 

<sup>\*\*[16, 17].</sup> 

contribution of the emitter is calculated to be  $0.019 \Omega$ . As the dimensions on all the test cells are the same, this is the expected contribution on all the wafers.

(B) Line Resistance along the Fingers. As with the emitter, not all the current flows through the full length of the fingers; the current generated close to the busbar will have less distance to travel through the metal than the current generated on the far side of the cell. As such, the geometry of the problem is the same, and the same equation that was used to calculate the effective series resistance for the emitter can be used for the fingers. In this case,

$$R_{\text{eff}} = \frac{1}{3} \frac{L}{W} \frac{\rho}{t},\tag{A.2}$$

where L is again the length of the fingers, W is the width of the fingers,  $\rho$  is the specific resistivity of the Cu, and t is the thickness of the Cu. From the dimensions and the resistivity of Cu being  $16.78 \, \mathrm{n}\Omega \cdot \mathrm{m}$ , the effective resistance from the front fingers works out to be  $0.014 \, \Omega$ .

(*C*) *Resistance through the Base.* The resistance contribution from the base can be calculated from:

$$R_b = \rho_b D, \tag{A.3}$$

where  $\rho_b$  is the resistivity of the base and D is the spacing between the rear contacts [16]. From the geometry and a base resistivity of  $0.5 \Omega \cdot \text{cm}$ , the resistance through the base material is  $0.075 \Omega \cdot \text{cm}^2$ , and a total resistance contribution of  $9.4 \text{ m}\Omega$ .

(*D*) Spreading Resistance at the Rear Contacts. The spreading resistance at the base point contacts can be calculated from the geometry and the material properties of Si from:

$$R_{\rm sp} = D^2 \frac{\rho_b}{2d_c},\tag{A.4}$$

where  $\rho_b$  is the resistivity of the base, D is the spacing of the rear contacts, and  $d_c$  is the diameter of the rear contact [15, 16]. From the geometry and a base resistivity of  $0.5 \Omega \cdot \text{cm}$ , the spreading resistance at the rear contacts works out to be  $0.56 \Omega \cdot \text{cm}^2$ , and a total resistance of  $0.07 \Omega$ .

(*E*) Contact Resistance. Contact resistance between the metal contacts and the Si was determined from TLM test structures, the details of which were given in Sections 3.1 and 3.4.

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#### Research Article

## Study of Ruthenium Complex Sensitizer and Gold Nanoparticles Doped Flexible Organic Solar Cells

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This work presents a flexible organic solar cell with a structure for ITO/PEDOT:PSS/P3HT:PCBM + ruthenium complex sensitizer and Au nanoparticles on a flexible substrate. The process and thickness of the PEDOT:PSS hole transport layer and P3HT:PCBM active layer were optimized. A ruthenium complex sensitizer and Au nanoparticles were then introduced into the P3HT:PCBM active layer to improve the performance of solar cells. For the ITO/PEDOT:PSS/P3HT:PCBM + ruthenium complex sensitizer and Au nanoparticles structure on a flexible polyimide (PI) substrate under 0.1 and 1 sun conditions, the measured short-circuit current density ( $I_{sc}$ ), open-circuit voltage ( $V_{oc}$ ), fill factor (FF), and efficiency ( $\eta$ ) are 3.89 and 9.67 mA/cm<sup>2</sup>, 0.45 and 0.45 V, 0.266 and 0.232, and 4.65 and 1.01%, respectively.

#### 1. Introduction

Flexible organic solar cells (FOSCs) have received considerable attention recently owing to their ability to be fabricated at low temperatures, economic cost, large area production, high flexibility, roll-to-roll manufacturing, and easy fabrication, such as by spin coating, [1-5] printing, [6-9] slot-die coating, [9-12] or evaporation [13, 14]. The organic active layer in FOSCs typically consists of a p-conjugated polymer donor and acceptor. The power conversion efficiency of (PCE) of FOSCs has been improved to 2.5% ~3.7% using a bulk heterojunction (BHJ) structure comprising a blended film of poly(3-hexylthiophene) (P3HT) as the donor and [6,6]-phenyl-C<sub>61</sub>-butyric acid methyl ester (PCBM) as the acceptor. Their PCE is significantly lower much than that of organic-based PTB7/PC71BM structure solar cells on a glass substrate, that is, 7.4% [1, 11, 15-18]. However, polyimide (PI) substrates have become conventionally used in flexible electronic devices owing to their high transition temperatures, low surface roughness, low coefficients of thermal expansion, and high chemical resistance under typical fabrication conditions [1, 19, 20].

Owing to the inherent symmetry of the BHJ active layer, the nature of the electrodes largely determines the anode and cathode of the device [21]. Therefore, this work attempts to improve the PCE of solar cells by introducing a *cis*-bis(thiocyanato) bis(2,2'-bipyridyl-4,4'-dicarboxylate) ruthenium bis(tetrabutylammonium) (N719) sensitizer (Everlight Chemical Industrial Co., Taiwan) and Au nanoparticles (GNPs) (100 ppm, particle size: 2–5 nm, SD Technology Co., Taiwan) into the active layer of the FOSCs. The N719 and GNPs can achieve electron/hole collection efficiently. The characteristics of the ITO/PEDOT:PSS/P3HT:PCBM+N719+GNPs structure are also studied.

#### 2. Experiment Details

Figure 1(a) shows the structure of flexible solar cells using P3HT as the electron donor and PCBM as the electron acceptor fabricated on semitransparent ITO-coated polyethylene terephthalate (PET) substrate (sheet resistance = 15  $\Omega$ / $\square$  and thickness = 178  $\mu$ m) (CPFilms Inc., Taiwan) and PI substrate (sheet resistance = 15  $\Omega$ / $\square$  and thickness = 130  $\mu$ m) (CPFilms Inc., Taiwan), respectively. The transmittance of both PET

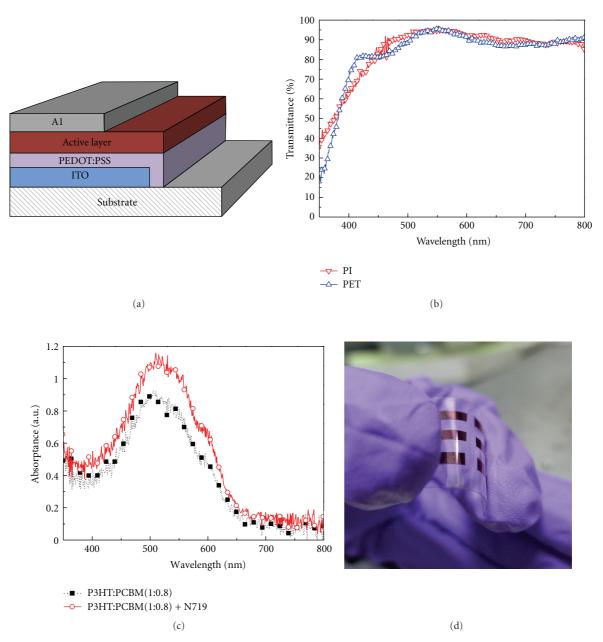


FIGURE 1: (a) Structure of a flexible organic solar cell. (b) Transmittance of PET and PI substrates with ITO layer. (c) Absorbance of P3HT:PCBM and P3HT:PCBM+N719. (d) Optical image of a flexible organic solar cell.

and PI substrates with ITO layer was about 95% at 550 nm, as shown in Figure 1(b). Therefore, PET and PI substrates are suitable for FOSCs. PEDOT:PSS hole transport layer was spun on the substrate with ITO layer and annealed at various temperatures for 10 min in a vacuum. An attempt was made to achieve the required viscosity in the range of 2 to 30 cps and reduce the tension of the PEDOT:PSS layer by adding a surfactant Triton X-100 to the PEDOT:PSS solution [22]. Next, the PEDOT:PSS solution was filtered through 0.45  $\mu$ m PP syringe filters before spin coating on the substrate. Additionally, P3HT and PCBM were blended with 1,2-dichlorobenzene(DCB) (1:0.8 at wt%) as an active layer. The solution was then filtered through 0.45  $\mu$ m PP

syringe filters before spin coating. P3HT:PCBM blended solution was spin coated on a dried PEDOT:PSS thin film and annealed at  $140^{\circ}$ C for  $10 \, \text{min}$  in a vacuum. Finally, Al layer was deposited under a base pressure of  $1 \times 10^{-6}$  Torr. Al cathode was deposited through a shadow mask to a thickness of 70 nm, given an active area of  $2 \, \text{mm} \times 5 \, \text{mm}$ . Therefore, the cell has an active area of  $2 \, \text{mm} \times 5 \, \text{mm}$ . Distance from the crucible to the substrate was fixed at 20 cm, and a substrate holder was rotated continuously to ensure uniform films. Next, film thickness and deposition rate, which was adjusted by SEM, were monitored using quartz crystal microbalance (QCM). Figure 1(c) shows the absorbance of P3HT:PCBM and P3HT:PCBM+N719. Therefore, in this study, the N719

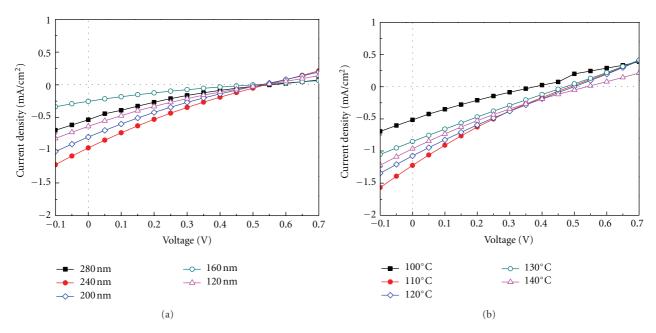


FIGURE 2: The *J-V* characteristics of the solar cells with PEDOT:PSS hole transport layer in (a) various thicknesses and (b) various annealing temperatures.

ruthenium complex sensitizer is employed to improve the absorption of light and the performance of cell. Figure 1(d) shows the flexibility of the as-prepared cell.

The current density-voltage (J-V) characteristics were then measured using a Keithley 2420 programmable sourcemeter under irradiation by a solar simulator with a 250 W xenon lamp. Finally, the irradiation power density in the surface of the sample was calibrated as 100 and  $1000 \text{ W/m}^2$  incident power densities.

#### 3. Results and Discussion

This work attempted first to optimize the hole transport layer PEDOT:PSS based on the structure of Figure 1(a) by using a 100 nm-thick P3HT:PCBM active layer annealed at 140°C. Figures 2(a) and 2(b) plot the I-V characteristics of the ITO/PEDOT:PSS/P3HT:PCBM/Al solar cells with various hole transport layer thicknesses and annealing temperatures under illumination, respectively. According to Figure 2(a), increasing the thickness of the PEDOT:PSS layer decreased both the transparency and sheet resistance, subsequently affecting the photocurrent and fill factor of the solar cells. However, decreasing the transparency of the PEDOT:PSS layer reduced the available photons to be absorbed by the active layer ultimately leading to a lower photocurrent density. However, this lowering of the photocurrent was offset by an increase in the fill factor due to the low sheet resistance [23]. The photocurrent of cells increased with an increasing annealing temperature, as shown in Figure 2(b). The photocurrent density increases from 0.516 mA/cm<sup>2</sup> (100°C annealing) to 1.24 mA/cm<sup>2</sup> (110°C annealing) and then decreases to 1.08 mA/cm<sup>2</sup> (120°C annealing), which subsequently increases to 0.97 mA/cm<sup>2</sup> (140°C annealing),

as shown in Figure 2(b). The photocurrent of cells increased with an increasing annealing temperature as the annealing temperature increases from 100 to 110°C. This indicates a variation in the conduction mechanism from the nearest neighbor hopping at the beginning of the heat treatment to the charging-energy limited tunneling between the conductive grains due to the shrinking of the PEDOT conductive grains [24]. The photocurrent of cells decreased with an increasing annealing temperature as the annealing temperature increases from 110 to 130°C. This may attributed to the oxidation or degradation of the PEDOT. Then, the photocurrent of cells increased with an increasing annealing temperature as the annealing temperature increases from 130 to 140°C owing to the PSS segregation effects [25]. The optimum thickness and annealing temperature of the PEDOT:PSS layer is 240 nm and 110°C, respectively.

Figure 3 plots the *J-V* characteristics of the ITO/PEDOT: PSS/P3HT:PCBM/Al solar cells with the optimized hole transport layer and various thicknesses of the active layer under illumination. Table 1 lists the characteristic parameters of solar cells on various substrates. The parameters of a solar cell with P3HT:PCBM active layer on the PI substrate exhibited  $J_{sc} = 3.18 \text{ mA/cm}^2$ ,  $V_{oc} = 0.4 \text{ V}$ , FF = 0.257, and a PCE of 3.27%, respectively. According to this table, the photocurrent of cells increases since the number of photogenerated electron-hole pairs increases with an increasing thickness of the active layer. However, the photocurrent decreases as the thickness of the active layer is higher than 200 nm. The thickness of the active layer increases, subsequently degrading the J-V characteristics and the fill factor. The solar cell can be modeled as an equivalent circuit consisting of a current generator of J<sub>sc</sub> and two resistances, series resistance  $(R_s)$  and shunt resistance  $(R_{sh})$ . If the  $R_{\rm sh}$  is sufficiently large to be neglected, the effect of the

Glass 0.			
Glass	45 3.61	0.253	4.1
PI 0	.4 3.18	0.257	3.27
PET 0	.4 2.14	0.261	2.24

TABLE 1: The parameters of solar cells with P3HT:PCBM active layer.

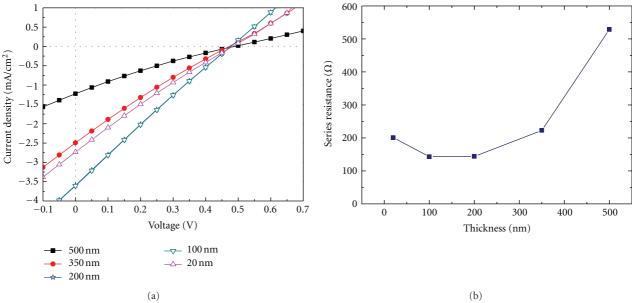


FIGURE 3: (a) The *J-V* characteristics of the solar cells with various thicknesses of P3HT:PCBM active layer on the PI substrates. (b) The series resistance of cells with various thickness active layers.

 $R_s$  on the I-V characteristics can be taken into account as shown below [26, 27]:

$$I = I_s \left[ \exp\left(\frac{q(V - IR_s)}{nkT}\right) - 1 \right] - I_{\text{ph}}, \tag{1}$$

where  $I_{ph}$  is the photocurrent,  $I_s$  is the saturation current, and n, k, and T are the ideality factor, Boltzmann constant, and temperature, respectively. Simple mathematical manipulation of (1) obtains [27]

$$\frac{dV}{dI} = R_s + \frac{nkT}{q} \left( I + I_{ph} \right)^{-1}. \tag{2}$$

As shown in Figure 3(b), the cell with 100 nm-thick active layer have a smaller series resistance ( $\sim$ 140  $\Omega$ ), and the cell with 500 nm-thick active layer have a larger series resistance ( $\sim$ 528  $\Omega$ ). A thicker P3HT:PCBM active layer implies a higher series resistance and poorer transparency, subsequently increasing of  $R_s$  and lowering of photocurrent, and degrading its performance [23, 28]. Therefore, the effective absorption of P3HT:PCBM active layer can be optimized by varying the active layer thickness.

Previous studies have applied a traditional ruthenium complex sensitizer *cis*-bis(thiocyanato) bis(2,2'-bipyridyl-4,4'-dicarboxylate) ruthenium bis(tetrabutylammonium) (N719) in dye-sensitized solar cells to extend the optical threshold wavelength since the N719 sensitizer should absorb

photons from the visible to near-infrared (NIR) region of the solar spectrum while maintaining sufficient thermodynamic driving force for the electron injection and dye regeneration process [29–32]. This work also attempted to increase the efficiency of flexible solar cells by introducing N719 into the P3HT:PCBM active layer. Figure 4 plots the *J-V* characteristics of the ITO/PEDOT:PSS/P3HT:PCBM+N719/Al (N719 = 0.3 mg) solar cells under illumination. Table 2 lists the characteristic parameters of solar cells with various structures. The parameters of solar cell with P3HT:PCBM+N719 active layer on the PI substrate exhibited  $J_{sc} = 3.89 \,\text{mA/cm}^2$ ,  $V_{\rm oc} = 0.4 \,\mathrm{V}$ , FF = 0.258, and a PCE of 3.68%, respectively. Notably, the PCE was improved by approximately 12.5% over that of the control sample. This improvement in PCE can be attributed to that the absorption of P3HT:PCBM active with N719 sensitizer have better than that of P3HT:PCBM active layer in visible, especially in the wavelength of 500–600 nm, as shown in Figure 1(c).

Figure 5 plots the J-V characteristics of the ITO/PEDOT: PSS/P3HT:PCBM+N719+GNPs/Al (P3HT:PCBM = 1:0.8 (20 mL:16 mL), N719 = 0.3 mg, GNPs = 0.3 mL) solar cells under illumination. Table 3 lists the characteristic parameters of solar cells with various substrates under 0.1 sun and 1 sun (AM 1.5) conditions, respectively. The parameters of solar cell with P3HT:PCBM+N719+GNP active layer on the PI substrate exhibited  $J_{\rm sc}=3.89\,{\rm mA/cm^2},\ V_{\rm oc}=0.45\,{\rm V},\ {\rm FF}=0.266,\ {\rm and}\ {\rm a}\ {\rm PCE}\ {\rm of}\ 4.65\%$  under 0.1 sun

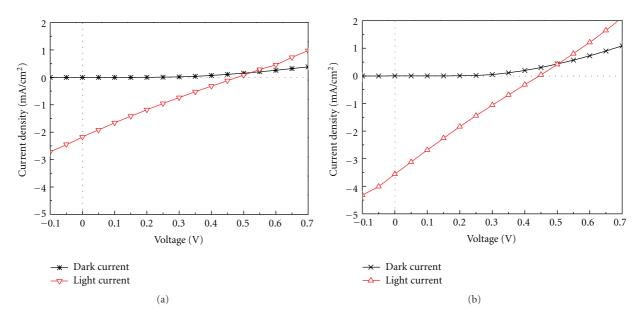


FIGURE 4: The J-V characteristics of the solar cells with P3HT:PCBM+N719 active layer on (a) the PET substrate and (b) the PI substrate.

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Substrate	$V_{\rm oc}$ (V)	J <sub>sc</sub> (mA/cm <sup>2</sup> )	FF	η (%)
Glass	0.45	3.96	0.245	4.36
PI	0.4	3.56	0.258	3.68
PET	0.45	2 18	0.243	2 38

TABLE 2: The parameters of solar cells with P3HT:PCBM+N719 active layer.

TABLE 3: The parameters of solar cells with P3HT:PCBM+N719+GNP active layer.

Condition	Substrate	$V_{\rm oc} ({ m V})$	$J_{\rm sc}~({\rm mA/cm^2})$	FF	η (%)
	Glass	0.45	4.06	0.261	4.76
0.1 sun	PI	0.45	3.89	0.266	4.65
	PET	0.45	2.87	0.248	3.21
	Glass	0.50	13.48	0.211	1.42
1 sun	PI	0.45	9.67	0.232	1.01
	PET	0.45	9.31	0.232	0.97

condition, respectively. The PCE was improved by approximately 42.2% over that of the control sample (without N719 and GNPs). Introducing N719 and GNPs may account for this improvement. When photo-generated electrons are injected into GNPs and the Fermi level  $(E_F)$  is raised as close to the lowest unoccupied molecular orbital (LUMO) of P3HT as possible, a quick shuttling of electrons occurs from Au to P3HT. Therefore, GNPs promote the generation of charge carriers and increase both the photocurrent and the efficiency of conversion of solar energy in solar cells [33, 34]. Meanwhile, the incorporation of N719 can assist transportation of the photo-generated electrons and holes. The energy level diagram and mechanism of photocurrent generation in the solar cells with P3HT:PCBM+N719+GNPs active layer is summarized in Figure 6. Finally, the efficiency improvement of solar cells with various active layers under

condition of 0.1 sun are listed in Table 4 for easy reading and understanding.

#### 4. Conclusions

This work demonstrated the feasibility of fabricating a flexible organic solar cell with a ITO/PEDOT:PSS/P3HT:PCBM + ruthenium complex sensitizer and Au nanoparticles structure on a flexible substrate. The process and thickness of PEDOT:PSS hole transport layer and P3HT:PCBM active layer were optimized. For the ITO/PEDOT:PSS/P3HT:PCBM + ruthenium complex sensitizer and Au nanoparticles structure on a flexible polyimide (PI) substrate under 0.1 and 1 sun conditions, the measured short-circuit current density ( $I_{\rm Sc}$ ), open-circuit voltage ( $V_{\rm oc}$ ), fill factor (FF), and efficiency ( $\eta$ ) are 3.89 and 9.67 mA/cm², 0.45 and

Substrate	P3HT:PCBM	P3HT:PCBM+N719		P3HT:	P3HT:PCBM+N719+GNP	
	η (%)	η (%)	Improvement (%)	η (%)	Improvement (%)	
Glass	4.1	4.36	6.34	4.76	16.1	
PI	3.27	3.68	12.54	4.65	42.2	
PET	2.24	2.38	6.25	3.21	43.3	

Table 4: The efficiency improvement of solar cells with various active layers under condition of 0.1 sun.

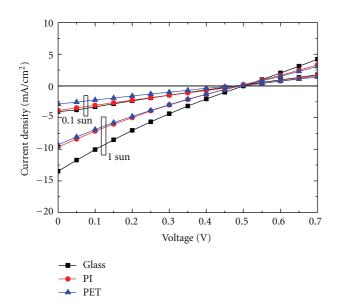


FIGURE 5: The *J-V* characteristics of the solar cells with P3HT:PCBM+N719+GNPs active layer on various substrates.

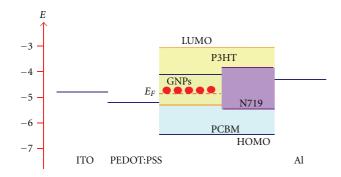


FIGURE 6: Energy level diagram and mechanism of photocurrent generation in the solar cells with P3HT:PCBM+N719+GNPs active layer.

0.45 V, 0.266 and 0.232, and 4.65 and 1.01%, respectively. Comprising the reported articles, the improved PCE of P3HT:PCBM-based FOSCs may be attributed to introduction of a ruthenium complex sensitizer and Au nanoparticles into the P3HT:PCBM active layer, subsequently increasing the photogenerated carrier injection.

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#### Research Article

# Effects of Organic Compounds on Microstructure, Optical, and Electrical Properties of ITO Thin Films Prepared by Dip-Coating Method

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Tin-doped Indium oxide (ITO) thin films were prepared by sol-gel dip-coating technique using low-cost metal salts and organic solvents. The coated films were treated without annealing or annealed at 400°C and 600°C in 3%  $H_2/97\%$   $N_2$  mixtures atmosphere. Microstructure, optical, and electrical properties of the prepared ITO films were investigated in detail. The maximum transmittance in the visible range (380–780 nm) is 85.6%, and the best resistivity is  $5 \times 10^{-2} \,\Omega$ -cm when annealed at 600°C in 3%  $H_2/97\%$   $N_2$  mixtures atmosphere. It is found that the optical and electrical properties of the prepared ITO films are strongly related to the microstructure variation. The organic compounds could not be removed completely, and the prepared ITO thin films were not dense when the prepared ITO film was annealed at 600°C in 3%  $H_2/97\%$   $N_2$  mixtures atmosphere, causing the poor conductivity.

#### 1. Introduction

Tin-doped Indium oxide (ITO) thin films have been widely applied in touch panel contacts, electrodes for LCD and electrochromic displays, gas sensors, heat-reflecting coatings to increase light bulb efficiency, antistatic window coatings, energy conserving architectural windows and so on [1–4]. A variety of fabricating methods have been employed to prepare the ITO thin films, such as sputtering [5], chemical vapor deposition [6], and sol-gel process [7]. Among the variously available kinds of techniques, the sol-gel technique seemed to attract much attention for its advantages such as simplicity, low cost, doping levels easily controlled and feasible preparation for large area films and without using expensive and complex equipments. Moreover, process conditions affect the densification and crystallization of the ITO films prepared by the sol-gel technique. However, the ITO films prepared by sol-gel technique exhibit a relatively low conductivity resulting from considerable porosity even after films with postannealed at a high temperature and the difficulty to obtain metal alkoxides as raw materials for their unavailability and high price [8–10].

In this paper, the ITO thin films were prepared by sol-gel dip-coating technique using low-cost metal salts and organic solvents. The effects of postannealing temperature in 3%  $\rm H_2/97\%$   $\rm N_2$  mixtures atmosphere on morphology, structure, and electrical properties of the ITO thin films are investigated to verify the relationship between the process condition and the properties of the prepared films. It is found that the optical and electrical properties of the prepared ITO films are strongly related to the microstructure variation, especially resulted from the organic compounds of the precursors.

#### 2. Experimental

Figure 1 shows a diagram of the synthesis and deposition process of the prepared ITO films coating on glass substrate in detail. First, anhydrous indium chloride (InCl<sub>3</sub>) was dissolved in isopropyl alcohol in the mix after adding

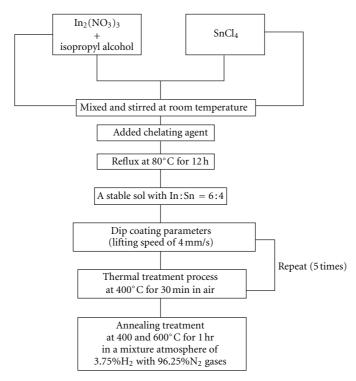


FIGURE 1: A diagram of the synthesis and deposition process of the prepared ITO films coating on glass substrate.

anhydrous tin chemical compound (SnCl<sub>4</sub>) and stirred at room temperature. Secondary, chelating agent added to the solution and maintained in reflux at 80°C for 12 h. Finally, a stable sol with the molar ratio of the In: Sn = 6:4 was obtained. Additionally, the cleaned glass plates (20 mm imes $20 \,\mathrm{mm} \times 3 \,\mathrm{mm}$ ) were used as the substrates for coating. The sol containing In and Sn sources was prepared on the glass substrate by dip-coating method at a withdrew speed of 4 mm/sec. Then, the film was fired at 400°C for 30 min in air and then cooled down to room temperature. A completely deposition involved 5 orders of the dipping and firing process to form the as-prepared ITO thin films. The total thickness of the as-prepared ITO films was controlled in the range of 250 to 300 nm. Finally, the as-prepared ITO films were annealed in 3%  $H_2/97\%\ N_2$  mixtures atmosphere in a tube furnace at 400 and 600°C for 1 hr.

Thermogravimetric-differential thermal analysis (TG-DTA 2000, MAC Science Co., Ltd., Japan) was used to obtain the weight loss and reaction behavior of the gel and performed under the atmospheric air condition with a heating rate of 5°C/min. X-ray diffraction system (XRD, BRUKER D8 ADVANCE) equipped with CuK $_{\alpha}$  radiation of average wavelength 1.5406 Å was used to specify the existent phases and the orientation of the ITO thin films. X-ray patterns were taken 2 $\theta$  between 20° and 80° and scan speed of 4.5°/min. Fourier Transform Infrared Spectroscopy (FTIR, Spectrum 100) and Energy Dispersive Spectrometer (EDS, JSM-6400F, JEOL, Japan) were used to detect the residue of the organic compounds in the ITO thin films, wherein the FTIR spectra were recorded at the range of 4000 cm $^{-1}$  to 400 cm $^{-1}$  [11]. Field emission-scanning

electron microscopy (FE-SEM, JSM-6400F. JEOL, Japan) and Atomic force microscopy (AFM, Veeco CP series) were used to observe the surface microstructure morphologies of the ITO thin films. Moreover, the standard four-point probe method was used to measure the room-temperature conductivity of the ITO thin films.

#### 3. Results and Discussion

Figure 2 shows the TG-DTA curves of the ITO gel. The weight mass of ITO gel displays continuous and significant decrease with the rising of heat treatment temperature before 361°C. There are four endothermic peaks at 65, 94, 213, and 279°C, respectively, and one distinct exothermic peak at 361°C. The endothermic peaks are attributed to heat release from charring and decomposition of organic groups and components, and the exothermic peak is proposed resulting from the transformation of In<sub>2</sub>O<sub>3</sub> to polycrystalline cubic bixbyite structure. In addition, the mass of ITO gel does not change at the temperature higher than 350°C. Therefore, the temperature above 400°C was selected as firing temperature to prepare the desired ITO thin films in this work.

Figure 3 shows the XRD patterns of the ITO thin films treated without annealing, and with annealing at 400°C and 600°C in 3%  $\rm H_2/97\%~N_2$  mixtures atmosphere. The major diffraction peaks angle of the  $\rm In_2O_3$  crystal located at 21.493°, 30.579°, 35.455°, and 51.013° are corresponding to the reflection planes of (222), (400), (440), and (622), respectively, described in JCPDS database (Card No. 44-1087), which indicates that  $\rm In_2O_3$  phase is in a cubic system with the space group,  $T_h^7$  Ia3, and lattice parameter,

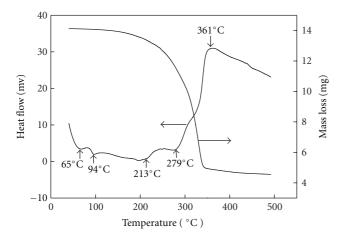


FIGURE 2: TG-DTA curves of the ITO gel.

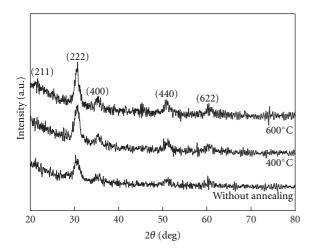


FIGURE 3: XRD patterns of the ITO thin films treated without annealing and with annealing at 400°C and 600°C in 3%  $H_2/97\%$   $N_2$  mixtures atmosphere.

 $a = 1.0117 \,\mathrm{nm}$  at 26°C [12]. The spectrums show that the diffraction peaks of the ITO thin films treated without annealing are not obvious on the planes of the (400), (440), and (622) of the In<sub>2</sub>O<sub>3</sub> crystal. When the ITO films treated with annealing temperature of 400°C, the ITO gel gradually began to lose the intermolecular water and revealed the characteristic diffraction peaks of the In<sub>2</sub>O<sub>3</sub> crystal [9, 10]. All the diffraction peaks were weak even when the annealing temperature further was increased to 600°C. In addition, no second phases corresponded to the other Sn compounds were found indicating that the Sn element was dissolved in the In<sub>2</sub>O<sub>3</sub> to form a good solid solution. In ITO material system, Tin ion is tetravalent and Indium ion is trivalent, each Sn<sup>4+</sup> replacing In<sup>3+</sup> substitutionally, thus, contributing a free carrier electron for the conductivity. Therefore, the ITO thin films retain the cubic In<sub>2</sub>O<sub>3</sub> structure up to the solid solubility limit of the Sn in the In<sub>2</sub>O<sub>3</sub> [13]. However, not all the Sn atoms can be substituted to In atom sites. Therefore, small amounts of Sn(IV) may be transformed to Sn(II) [14]. When the annealing temperature was increased,

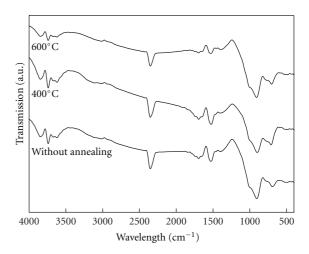


FIGURE 4: FTIR spectra of the ITO thin films treated without annealing and with annealing at 400°C and 600°C in 3%  $H_2/97\%$   $N_2$  mixtures atmosphere.

the width of the (222) diffraction peaks became more sharp due to the improved crystalline with increasing the postannealing temperature. The crystallinity of the ITO thin films can be improved by increasing the postannealing temperature [15]. Additionally, the crystallinity depends on the annealing temperatures rather than the atmosphere used in the postannealing process [5].

The average crystalline size (*D*) of the ITO thin films is determined by applying the Scherrer equation to the full width at half maximum (FWHM) of the (222) diffraction peaks, as given by [16]

$$D = \frac{0.9\lambda}{\omega\cos\theta},\tag{1}$$

where  $\omega$  is the calibrated FWHM of the selected diffraction line in radians,  $\theta$  is the Bragg angle, and  $\lambda$  is the X-ray wavelength (0.15406 nm). In Table 1, the FWHM of (222) diffraction peaks were decreased with an increase in annealing temperature. Thus, the crystalline size was increased from about 3.3 to 4.5 nm for that treated without annealing to that treated with annealing temperature of 600°C, indicating the crystalline of the ITO films can be improved with increasing annealing temperature [15].

Figure 4 shows the FTIR spectra of the ITO thin films treated without annealing and with annealing at 400°C and 600°C in 3% H<sub>2</sub>/97% N<sub>2</sub> mixtures atmosphere. The bands appearing at below 900 cm<sup>-1</sup> are corresponded to the stretching vibrations of In–O and Sn–O, as well as to the contributions of In–O and Sn–O bonds [9]. Moreover, there are a stretching vibration peak of C–C band in the range 1652–1579 cm<sup>-1</sup>, a stretching vibration peak of C–O band in the range 1727–1720 cm<sup>-1</sup>, and a stretching vibration peak of C–H band in the range 2800–2200 cm<sup>-1</sup> since the ITO thin films were treated without annealing. When the ITO thin films were treated without annealing and with annealing temperature at 400°C, the FTIR characteristics almost do not change. However, when the ITO thin films were treated with annealing at 600°C, the C–C band,

Annealing conditions	Carbon content <sup>a</sup> (weight%)	FWHM <sup>b</sup> (Degree)	Crystal size <sup>b</sup> (nm)	Conductivity <sup>c</sup> (S/cm)
Without annealing	8.15	2.5	3.3	$0.3 \times 10^1$
Annealed at 400°C	4.90	2.3	3.9	$0.8 \times 10^1$
Annealed at 600°C	0.00	1.9	4.5	$2 \times 10^1$

TABLE 1: Main characteristics of the prepared ITO thin films.

C=O band and C-H band, became broader. This result is due to the decreased organic compounds as increasing the annealing temperature [10, 11]. Furthermore, under annealing treatment at a certain temperature, thin films are formed after withdrawing and drying to lose their intermolecular water and organic components gradually, and translated into crystalline state [11]. In Table 1, the residues of carbon from the organic compounds detected by EDS were decreased with increased annealing temperature. As annealing temperature was reached to 600°C, carbon contents disappeared completely. Compare to the result from FTIR analysis, the organic compounds did not be decreased completely even as annealing temperature was reached to 600°C. These results may be attributed to the detection limit of the EDS analyzer. Although the burned out temperature of the organic compounds is around 350°C which is obtained from the DTA/TG curve, the organic compounds were not decomposed completely as the ITO films were fired at 400°C. The reason may be the holding time on the firing temperature is not enough to volatilize the organic compounds absolutely.

Figure 5 shows the SEM images of the ITO thin films treated without annealing, and with annealing at 400°C and 600°C in 3% H<sub>2</sub>/97% N<sub>2</sub> mixtures atmosphere. The prepared ITO thin films have a structure with full of cracks uniformly distributed such as [11]. All the SEM figures showed the presence of cracks, indicating the ITO thin films were not dense. The considerable porosity ( $P \sim 51\%$ ) of the ITO thin films by using sol-gel method would not be removed even after annealing at a high temperature as the crystalline nanoparticle suspensions consists of an agglomeration of such particles [17]. Figures 5(a) and 5(b) show the average surface grain size of about 30.1 and 32.0 nm for the ITO films without annealing and with annealing at 400°C in 3% H<sub>2</sub>/97% N<sub>2</sub> mixtures atmosphere, respectively. However, there are almost no significant changes in the morphology as the annealing temperature was further increased to 600°C, and the average surface grain size is about 32.3 nm.

Figure 6 shows the AFM surface views (Scanning range:  $10 \times 10 \, \mu \text{m}^2$ ) of the ITO thin films treated without annealing, and with annealing at 400°C and 600°C in 3% H<sub>2</sub>/97% N<sub>2</sub> mixtures atmosphere. The average surface grain size and root-mean-square (RMS) roughness were high with an increased annealing temperature. This result was associated with the tendency of the grain growth by fusing adjacent grains when sufficient energy for surface rearrangement is provided by annealing. Larger grains are associated with higher RMS roughness [18]. In our work, RMS roughness

and the average surface grain size were increased with the increased annealing temperature in the range from 2.0 to 4.8 nm, and 30.1 to 32.3 nm, for the ITO films without annealing and with annealing at 600°C in 3%  $\rm H_2/97\%~N_2$  mixtures atmosphere, respectively. The morphology of the prepared ITO thin films depended substantially on annealing temperature [19].

The average grain size from SEM data was significantly larger than the average crystallite size in the film bulk derived from the FWHM of the (222) diffraction peaks and the RMS roughness from the AFM results [20]. The significant difference between the average crystallite and grain size was determined from XRD and AFM measurement; the reason was due to the fact that the AFM measurement was more sensitive to the surface structure and that of the XRD measurement was sensitive to the structure of the film bulk. Thus, the columns grown during the deposition tend to have larger diameter at the surface, resulting in larger surface grains than average grain size in the film bulk [21].

Figure 7 displays the optical transmittance spectra of the ITO thin films treated without annealing and with annealing at 400°C and 600°C in 3% H<sub>2</sub>/97% N<sub>2</sub> mixtures atmosphere. The maximum transmittance in the visible range (380–780 nm) is 85.6% when the ITO films annealed at 600°C and approximately 74.6% and 81.4% for the films treated without annealing and annealed at 500°C, respectively. The results agreed with those reported by Alam and Cameron They pointed out that the transmission in the visible range wavelengths was enhanced with increasing the annealing temperature due to crystallization and organic quantity [5].

As shown in Table 1, the conductivity of the prepared ITO films was in the range of  $0.3 \times 10^1$  to  $2 \times 10^1$  S/cm for films without annealing, and with annealing at  $400^{\circ}$ C and  $600^{\circ}$ C in 3% H<sub>2</sub>/97% N<sub>2</sub> mixtures atmosphere. Since the resistivity is inverse to the conductivity, the resistivity of the prepared ITO films was in the range around  $3 \times 10^{-1}$  to  $5 \times 10^{-2}$   $\Omega$ -cm. Actually, the conductivity of the ITO thin films is mainly derived from the donor-doping effect generated though replacement of In ion sites by Sn ions in lattice and the oxygen vacancy caused by annealing process. When In<sub>2</sub>O<sub>3</sub> is doped by Sn ions, due to approximate radii between In<sup>3+</sup> and Sn<sup>4+</sup>, In<sup>3+</sup> ions site is easily replaced by Sn<sup>4+</sup> ions site. The doping reaction can be expressed as [22]

$$x \operatorname{In}_2 O_3 + x \operatorname{Sn}^{4+} \longrightarrow \operatorname{In}_{2-x}^{3+} (\operatorname{Sn}^{4+} \cdot e)_x O_3 + x \operatorname{In}^{3+}.$$
 (2)

The conductivity of the ITO thin films is affected by two major factors. One is the grain boundary scattering, and another is the ionized impurity centers scattering [19].

<sup>&</sup>lt;sup>a</sup> By EDS.

<sup>&</sup>lt;sup>b</sup>By XRD.

<sup>&</sup>lt;sup>c</sup>By 4-point probe.

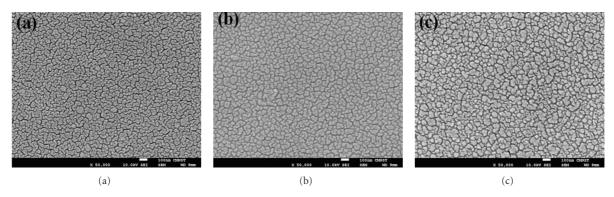


FIGURE 5: AFM surface views of the ITO thin films treated (a) without annealing and with annealing at (b)  $400^{\circ}$ C and (c)  $600^{\circ}$ C in 3%  $H_2/97\%$   $N_2$  mixtures atmosphere.

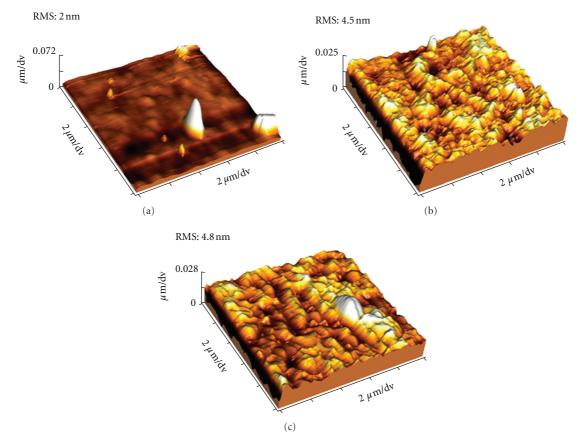
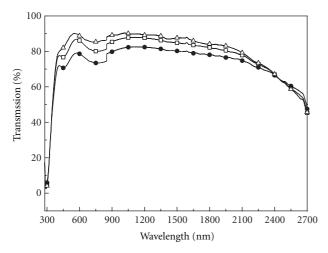


FIGURE 6: SEM images of the ITO thin films treated (a) without annealing and with annealing at (b)  $400^{\circ}$ C and (c)  $600^{\circ}$ C in 3% H<sub>2</sub>/97% N<sub>2</sub> mixtures atmosphere.

The grain size gradually increases the proportion of wellordered crystalline structures. Large grain size reduces the grain boundary scattering and enables the electron carriers to conduct smoothly. However, the ionized impurity centers served as the most important factor of the carrier concentration. The oxygen ion attracted by the doped ionized could be incorporated in lattice and segregated from the grain boundary, resulting in the distortion of the lattice and the generation of a neutral electron scattering center. As discussed in the Figures 4 and 6, the low conductivity of the prepared ITO films may be attributed to the undense film growth and the residual organic compounds, affecting the transportation of the carriers. The best resistivity is  $5 \times 10^{-2}~\Omega$ -cm obtained for the ITO film with an annealing temperature of 600°C owing to the mechanisms of the considerable porosity [8, 11, 23].



- -- Without annealing
- -□- 400°C
- -△- 600°C

FIGURE 7: Optical transmittance spectra of the ITO thin films treated without annealing and with annealing at  $400^{\circ}$ C and  $600^{\circ}$ C in 3% H<sub>2</sub>/97% N<sub>2</sub> mixtures atmosphere.

#### 4. Conclusion

In this paper, the ITO thin films were synthesized onto the glass substrates by a sol-gel process using a dip-coating method. A strong dependence of microstructure, crystal quality, electrical, and optical properties under annealing treatment conditions was found. The XRD results showed the prepared ITO thin films were cubic In<sub>2</sub>O<sub>3</sub> structure and the calculated crystal sizes were around 3.3 nm to 4.5 nm. The FTIR results showed the organic compounds could not be removed completely even when the postannealing temperature was operated at 600°C. The SEM images indicated the prepared ITO thin films were not dense. The AFM results showed the RMS roughness was increased with the increased annealing temperature due to crystal growth. Moreover, the maximum transmittance in the visible range (380–780 nm) of 85.6% and the best resistivity is  $5 \times 10^{-2} \Omega$ cm (namely, conductivity is  $2 \times 10^1$  S/cm) were obtained for the ITO film treated with the annealing temperature of 600°C. It is verified that the electrical properties of the prepared ITO films are strongly related to the microstructure variation, especially resulted from the un-dense film growth and un-removed organic compounds of the precursors.

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#### Research Article

# **Performance Degradation of Dye-Sensitized Solar Cells Induced by Electrolytes**

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We investigated the change of the electric characteristics in dye-sensitized solar cell (DSSC) when the electrolyte has been injected and measured initially and lately for a period of time. It was found that the short-circuit current density decreased from  $9.799 \, \text{mA/cm}^2$  to  $7.056 \, \text{mA/cm}^2$  and the fill factor increased from 0.406 to 0.559 when the cell had stood for an hour, while the open-circuit photovoltage did not change due to fixed difference between the Fermi level of  $\text{TiO}_2$  and the oxidation-reduction potential of electrolyte. The results can be explained by using the variation of the series resistance in the equivalent circuit of the DSSC.

#### 1. Introduction

Dye-sensitized solar cells (DSSC) have attracted much attention ever since Grätzel et al. demonstrated the possibility to convert solar energy to electricity with a photoelectrochemical dye-sensitized device [1]. The DSSC provides a technically and economically credible alternative concept to present day p-n junction photovoltaic devices. The development of these new types of solar cell is promoted by the increasing public awareness that the earth's oil reserves will run out during this century. Because the energy needs of the planet will at least double within the next 50 years, the stage is set for a major shortage of energy supply unless renewable sources can cover the substantial deficit that fossil fuels can no longer furnish.

This accomplishes the optical absorption and charge separation processes by the association of a sensitizer as a light-absorbing material with a wide-band-gap semiconductor of mesoporous or nanocrystalline morphology [1–3]. It also offers the prospect of very low cost fabrication without expensive and energy-intensive high-temperature and high-vacuum processes, compatibility with flexible substrates, and variety of presentations and appearances to facilitate market entry, both for domestic devices and in architectural or decorative applications. Generally, the semiconductor, which accepts the electron from the sensitizer and transfers

it to the electrode, is nanocrystalline anatase  $TiO_2$  which is mesoporous because of high surface area. High surface area of  $TiO_2$  thin film improves the adsorption of sensitizer and hence increases the light-harvesting capacity of the mesoporous film. However, the electrolyte may penetrate into the mesoporous film and contact the dye-free  $TiO_2$  and the electrode surface, resulting in the increase of the reverse saturation current. On the other hand, it also increases the contact area between the electrolyte and the sensitizer so that facilitates the reduction of  $I_3^-$  by the combination of the hole. It was found that the short-circuit photocurrent decreased and the fill factor of the dye-sensitized solar cell increased as time goes on.

In this study, the change of the electric characteristics in dye-sensitized solar cell (DSSC) when the electrolyte has been injected and measured initially and lately for a period of time was investigated. The short-circuit photocurrent density ( $J_{\rm sc}$ ) and the fill factor (E.F.) were varied and the results can be explained by using the variation of the series resistance in the equivalent circuit of the DSSC.

#### 2. Experimental Apparatus and Procedure

2.1. Preparing the Working Electrode. A TiO<sub>2</sub> thin-film electrode was designed and fabricated for use in a dye-sensitized solar cell. This TiO<sub>2</sub> thin-film was deposited on the top of

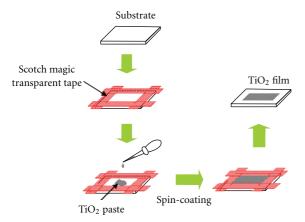


FIGURE 1: The procedure of preparing the working electrode.

an FTO-glass (Fluorine doped tin oxide,  $SnO_2$ :F) substrate, which has a size of  $20 \times 20 \times 3$  mm and a sheet resistance of  $8 \Omega$ /sq. The TiO<sub>2</sub> particles (P-25) are composed of 30% rutile and 70% anatase, with a particle size range (<100 nm).

Figure 1 shows the procedure of preparing the working electrode of DSSC with a layer of TiO<sub>2</sub> particles and the steps are described as follows. (1) Diluting 40 µL of acetylacetone in 1 mL of de-ionic (DI) water; (2) mixing 1 g of TiO<sub>2</sub> particles with the diluted acetylacetone, and stir well to make the colloid of TiO<sub>2</sub> particles; (3) adjusting the glutinosity of the colloid of TiO2 particles by adding 1.5 mL of DI water and 40 µL of surfactant (Triton-100, C<sub>8</sub>H<sub>17</sub>C<sub>6</sub>H<sub>4</sub>(OCH<sub>2</sub>CH<sub>2</sub>)nOH), and then homogenize the colloid of TiO<sub>2</sub> particles for 30 minute in a mortar; (4) dropping the quantitative colloid of TiO<sub>2</sub> particles on the top of the F:SnO<sub>2</sub> (FTO) glass substrate, and then spin coat the working electrode with rotational speed of 3000 rpm; (5) drying the working electrode with a layer of TiO<sub>2</sub> particles at room temperature for 10 minute, and then sinter this working electrode at 500°C for 30 minutes in a hightemperature furnace; (6) immersing the FTO-glass substrate with a layer of TiO<sub>2</sub> particles into the  $(3 \times 10^{-4} \text{ mol/L})$ solution of N-719 dye (Ruthenium, RuL<sub>2</sub>(NCS)<sub>2</sub>) and ethyl alcohol (CH<sub>3</sub>CH<sub>2</sub>OH, 95%) for 24 hours at room temperature. A conventional working electrode with a layer of nanocrystalline TiO2 on the FTO-glass substrate was fabricated using above procedures to demonstrate the feasibility and advantages of the working electrode with a layer of TiO<sub>2</sub> particles. An α-step (Dekeak 6 M) surface profiler was utilized to obtain the surface profile of the thin film and the average thickness of the thin film on the FTO-glass substrate of the working electrode. The thickness of the TiO<sub>2</sub> thin films was about 10  $\mu$ m. Figure 2 shows the practical working electrode.

2.2. Assembling the DSSC. Figure 3 shows the schematic of the DSSC. The thin film on the FTO-glass substrate of the working electrode was fringed using the Scotch magic transparent tape (3 M). Then, the working electrode and the counter electrode that a thin film of platinum was deposited on the FTO-glass substrate using a ion sputter (Hitachi E-1010) were fitted together, such that the space between the

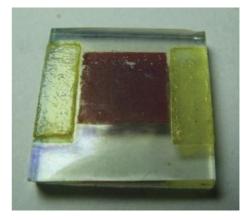


FIGURE 2: The photograph of the working electrode.

two electrodes was adjusted to approximately  $160\,\mu m$  for embarking the liquid electrolyte. After sealing, the liquid electrolyte, which was composed of  $0.5\,M$  lithium iodine (LiI) and  $0.05\,M$  iodine (I<sub>2</sub>) in 3-methoxypropionitrile, was injected into the cell through a hole on the cell that was prepared in advance.

2.3. Testing. A home-made I-V measurement system was adopted to measure the open-circuit photovoltage and short-circuit photocurrent of the DSSC. A solar simulator with a 500 W halogen lamp and a light intensity of 100 mW/cm², was employed to illuminate the DSSC. In addition, the power conversion efficiency  $\eta$  of the DSSC was determined by

$$\eta(\%) = \frac{V_{\text{oc}}J_{\text{sc}}FF}{P_{\text{in}}} \times 100. \tag{1}$$

In (1),  $V_{oc}$ ,  $J_{sc}$ , and  $P_{in}$  represent the open-circuit voltage, the short-circuit current density, and the incident light power (100 mw/cm<sup>2</sup>), respectively. Moreover, the fill factor FF is given by

$$FF = \frac{V_{\text{max}}J_{\text{max}}}{V_{\text{oc}}J_{\text{sc}}}.$$
 (2)

In (2),  $V_{\rm max}$  and  $I_{\rm max}$  represent the voltage and the current at the maximum output power point, respectively. The I-V characteristics of the prepared DSSC were measured at initial assembling stage and at one hour lately.

# 3. Results and Discussion

Figure 4 shows I-V characteristics of the DSSC when the electrolyte is just injected into the space between the working electrode and the counter electrode. The measured  $V_{\rm oc}$ ,  $J_{\rm sc}$ , and F.F. are 9.799 mA/cm², 0.658 V, and 0.406, respectively. Figure 5 shows I-V characteristics of the dye-sensitized solar cell after the electrolyte has been injected and stay for one hour. The measured  $V_{\rm oc}$ ,  $J_{\rm sc}$ , and F.F. are 7.056 mA/cm², 0.668 V, and 0.559, respectively. as Comparing Figure 4 to Figure 5, it is found that the  $J_{\rm sc}$  decreases from 9.799 mA/cm² to 7.056 mA/cm² and F.F increases from 0.406 to 0.559. The  $V_{\rm oc}$  does not change due to the fixed difference between

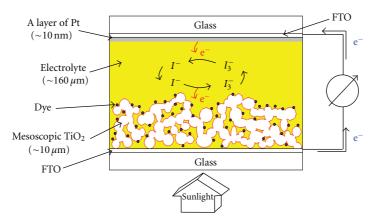


FIGURE 3: Schematic of the dye-sensitized solar cell.

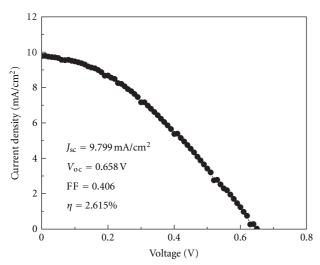


FIGURE 4: *I-V* curve of DSSC when the electrolyte is just injected.

the Fermi level of  $TiO_2$  and the oxidation-reduction potential of electrolyte. To understand the difference in their  $J_{\rm sc}$  for the measurement at initial assembling stage and at one, two, three and so forth hours lately. We conduct the standard I-V curve of the solar cell and discuss the change of the series resistance and the shunt resistance.

It has been known that the tangent slope of vertical part (near  $V_{oc}$ ) is proportional to the reciprocal of the series resistance (1/ $R_s$ ) and the tangent slope of transverse part (near  $J_{sc}$ ) is proportional to the reciprocal of the shunt resistance (1/ $R_{sh}$ ). When  $R_{sh}$  increase or/and  $R_s$  decrease, F.F. will become better. The tangent slope of  $V_{oc}$  part in Figure 5 is larger than that in Figure 4, which means  $R_s$  decreases as time goes on. However, the tangent slope of  $I_{sc}$  does not change obviously so that  $R_{sh}$  is almost the same. We thus discuss the factor that affects the series resistance  $R_s$  and ignores the shunt resistance  $R_{sh}$ .

The series-internal resistance of DSSCs was investigated by some researchers based on an equivalent circuit of DSSCs [4, 5]. It was found that series-internal resistance correlates with the charge-transfer at Pt counter electrode, TCO substrate resistance, and Nernstian diffusion in the

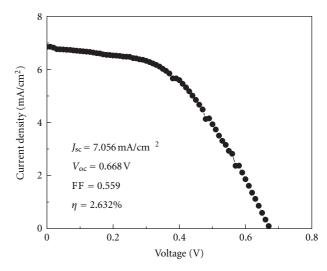


FIGURE 5: *I-V* curve of DSSC when the electrolyte has been injected and stay for one hour.

electrolyte. According to these, the equivalent circuit of DSSCs is constructed as shown in Figure 6. The series resistance is the sum of the charge transfer resistance at Pt/electrode interface ( $R_1$ ), the diffusion resistance of  $I_3$ ions in electrolyte ( $R_2$ ), and the sheet resistance of TCO ( $R_h$ ). Because  $R_1$  and  $R_h$  relate to the property of the material, they cannot change as time goes on. We think the major factor that influences  $R_s$  must be  $R_2$ . The probable explanation is that the electrolyte only contacts the top surface of TiO<sub>2</sub> thin film when the electrolyte is just injected. However, the electrolyte may permeate into the mesoporous film after an hour and the contact area with dye-adsorbed TiO2 will increase, so the charge-transfer from the electrolyte to the oxidized dye will be accelerated. The large contact area between the electrolyte and the dye-adsorbed TiO2 film improve the rate of  $I_3$ <sup>-</sup> reduction and hence decrease  $R_s$ .

According to the diode equation that correlates with Figure 6:

$$I = I_{\rm ph} - I_o \left\{ \exp \left[ \frac{q(V + IR_s)}{nkT} \right] - 1 \right\} - \frac{V + IR_s}{R_{\rm sh}}, \quad (3)$$

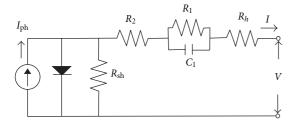


FIGURE 6: Equivalent circuit based on current-voltage characteristics of DSSCs. The sum of  $R_1$ ,  $R_2$ , and  $R_h$  corresponds closely to the series resistance of DSSCs.  $C_1$  is capacitance elements.

where  $I_{\rm ph}$  is the ideal photocurrent,  $I_0$  is the reverse saturation current, n is the ideality factor whose value is between 1 and 2 for the DSSC,  $R_s$  is the series resistance which is the sum of  $R_1$ ,  $R_2$ , and  $R_h$ , and  $R_{\rm sh}$  is the shunt resistance. The gain in open circuit voltage can be calculated from (3):

$$V_{\rm oc} = \frac{nkT}{q} \ln \left[ \frac{I}{I_o} - \frac{V_{\rm oc}}{I_o R_{\rm sh}} + 1 \right].$$
 (4)

As  $R_{\rm sh}$  increase,  $V_{\rm oc}$  will also increase as comparing Figure 4 to Figure 5, it is found that  $V_{\rm oc}$  does not change obviously. Since  $1/R_{\rm s}$  is unchanged, it confirms that the shunt resistance in DSSCs is almost the same as time goes on.

The short circuit current can be obtained from (3) when V = 0, and it can be found that  $I_{sc}$  will increase as  $R_s$  decreases. However,  $J_{sc}$  decreases from 9.799 mA/cm<sup>2</sup> in Figure 4 to 7.056 mA/cm<sup>2</sup> in Figure 5. It must be the influences of the dark current which correlates with the recombination of charge carriers by reduction of  $I_3$  at dyefree TiO<sub>2</sub> surface and bare FTO surface exposed to electrolyte through porous electrode [6]. As we discussed before, the electrolyte will permeate into the mesoporous film when DSSC has been staid for an hour. It may apply the electrolyte to contact the dye-free TiO<sub>2</sub> surface and even the FTO surface, so that accelerates the recombination of the charge carriers from the conduct band of TiO<sub>2</sub> to the electrolyte and produces the reverse saturation current. The increase of the dark current lowers  $I_{sc}$  seriously so that it is important to modify the working electrode surface to decrease the reverse charge flow.

Based on the above discussion, it is known how to improve the performance of DSSCs by modifying the interface between the working electrode and the electrolyte, as investigated by some research workers [7–9]. Su et al. fabricated layer-by-layer Au nanoparicles, which were prepared using chemical reduction method, onto the working electrode as a Schottky barrier in a water-based DSSC [10]. It was found that an interfacial blocking layer could suppress the interfacial recombination between TiO<sub>2</sub> and excited dye molecules or  $I^-/I_3^-$  couple, which led to an improvement on cell performance [7–9]. Moreover, in order to improve the performance of DSSCs, it is also necessary to suppress the dark current. The reverse charge flow, recapture of the electron by the electrolyte, could be impaired by judicious design of the sensitizer. It can also form a tightly packed insulating monolayer blocking the dark current.

Consequently, decreasing the recombination of charges in the dye or electrolyte is one of the important issues to increase the conversion efficiency of DSSC and is worthy of ongoing study.

#### 4. Conclusion

In this study, we discussed the change of the current-voltage characteristics in DSSCs as time goes on and found that fill factor (F.F) got better but short circuit current density  $J_{\rm sc}$  decreased. The results were explained by using the variation of the series resistance in the equivalent circuit of the DSSC. The increase of F.F. may result from the decrease of series resistance  $R_{\rm s}$  due to the electrolyte permeating into the mesoporous working electrode and hence increase the contact area with the dye-adsorbed TiO<sub>2</sub>. However, it also applies the electrolyte to contact the dye-free TiO<sub>2</sub> surface and even the FTO surface, so that accelerates the recombination of the charge carriers from the conduct band of TiO<sub>2</sub> to the electrolyte and produces the reverse saturation current.

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# Research Article

# Modeling Approach for Determining Equivalent Optical Constants of Plastic Shading Nets under Solar Radiation Conditions

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The radiative properties of several plastic shading nets were measured under natural solar radiation conditions. We found that the plastic nets behave as homogeneous translucent materials (e.g., plastic film, plastic sheets, and glass). Based on this behavior, we suggest that it is possible to treat plastic nets as translucent materials and to characterize them with equivalent optical constants (i.e., equivalent refractive indexes,  $n_{eq}$ , and equivalent extinction coefficients,  $\sigma_{eq}$ ). Here a physical model to determine  $n_{eq}$  and  $\sigma_{eq}$  of plastic nets was described in analogy to homogeneous translucent materials. We examined three groups of nets based on their color (black, black-green, and beige). Each group consisted of nets with four or five different porosities. Nets of each group had almost the same texture structure. For each group, we derived an equation for  $n_{eq}$  as a function of the net porosity and determined an average value for  $\sigma_{eq}$ . Once values of  $n_{eq}$  and  $\sigma_{eq}$  were determined, the solar radiative properties of a net could then be calculated from  $n_{eq}$  and  $\sigma_{eq}$  for any incident angle of solar beam radiation without the need of measurements. The present model was validated by comparing the calculated with the measured radiative properties of three nets at different incident angle of solar beam radiation. The calculated radiative properties reasonably agreed with measured values.

# 1. Introduction

During the last decade, the use of plastic nets for shading agricultural industrial and residential structures in hot and sunny regions has steadily expanded because plastic nets offer many economical and environmental benefits [1–4]. These include (i) reduction or elimination of energy consumption used for heating or cooling structures, (ii) reduction of crop transpiration as well as water consumption for irrigation in agriculture structures in arid regions, and (iii) improvement in environmental and human-health conditions by reducing the need for pesticides. The diffusive nature of the net threads causes the incident beam radiation to be scattered forward (specularly and diffusively) during transmission [5]. This provides a uniform radiation distribution inside structures covered with nets to add more advantages to plastic nets applications. Various types of plastic nets with different

colors and different shading powers are popular in the markets and are used for many purposes in many parts of the world. Commercial nets are usually defined by the following (i) the net porosity  $(\phi)$ , that is, the surface empty area (uncovered by the plastic threads) divided by the total surface area of the net. The value of  $\phi$  is usually determined by image processing or solar radiation transmission [6]. (ii) The shading factor (SF), defined as the percentage of global solar radiation that the net is able to block. SF strongly depends on the incident angle of the beam radiation ( $\theta$ ), and to estimate the value of SF for a net correctly, the directional solar radiative properties ( $\theta$  dependence) of the net should be determined. Accordingly, the directional solar radiative properties of nets are essentially needed to characterize different types of plastic nets according to their shading power. However, little information about how to determine these properties is available in the literature.

Some research groups have investigated the radiative properties of different types of plastic net or total net-covered structure models in laboratories under artificial lighting [2– 4, 7]. In order to replace expensive measuring techniques in laboratories, we developed a simple method for measuring the radiative properties of nets under natural conditions of global, diffuse, and direct beam solar radiation, and under natural conditions of the photosynthetically active radiation (PAR) [8, 9]. The method was used to test nets with different colors, porosities, and texture structures. Even though, nets are three-dimensional, nonhomogeneous, and porous materials, the behaviors of the plastic nets under solar radiation conditions were found to be similar to those of translucent homogeneous materials (e.g., plastic films, glass and rigid plastic sheets such as polycarbonate and acrylic) [8, 9]. In other words, the changes in the global, diffuse, and direct beam transmittances and reflectances of nets with the incident angle  $(\theta)$  were similar to those of different translucent materials that were measured under natural conditions of solar radiation [10-14]. This makes it possible to determine optical constants, in analogy to homogeneous transparent materials, to be used for calculating the radiative properties of nets. This is because calculation methods are preferable and easier than the measuring methods which are quite difficult and prohibitively expensive. Accordingly, the goal of the present study was to develop a theoretical model to investigate equivalent optical constants (i.e., equivalent refractive indexes and equivalent extinction coefficients) for plastic nets in analogy to homogeneous translucent materials. Three groups of nets (i.e., a black group, beige group, and black-green group) were selected to develop the model.

#### 2. Materials and Methods

2.1. The Plastic Net Materials. The nets selected for testing were classified into three groups. Nets in each group have the same color, same texture structure, and different porosities  $(\phi)$ . The nets were locally produced by Saudi companies. Samples of the nets  $(5 \text{ cm} \times 5 \text{ cm})$  were scanned at a resolution of 4800 dpi with a flatbed scanner (HP-5590). Photos of the scanned nets were magnified several times and converted into high-contrast black (thread projection area) and white (empty area) colors using Adobe Photoshop software. The resulting photos showed the net threads as black on a white background. The porosity (the empty area divided by the total surface area of the net,  $\phi$ ) of each net was estimated. The three groups were the black group having porosities  $\phi$  of 0.30, 0.36, 0.43, 0.54, and 0.64; the beige group having porosities  $\phi$  of 0.32, 0.34, 0.36, and 0.45; the black-green group having porosities  $\phi$  of 0.45, 0.46, 0.48, 0.50, and 0.51. In the latter group, the texture was interlaced threads made of black and green plastic robs knitted together. Photos of the tested nets (one from each group) are shown in Figure 1.

2.2. The Equivalent Optical Constants Model. In the case of homogeneous translucent materials (e.g., plastic films, plastic sheets, or glass), the measured radiative properties (reflectance, transmittance, and absorptance) are referred

to as effective properties. This is because the incident beam over the material surface suffers an infinite number of multiple internal reflections inside the material itself (Figure 2). With each internal reflection, there are transmitted and reflected portions below and above the material surfaces. The summation of the reflected components above the material surface is the effective reflectance and of those below the material surface is the effective transmittance; both can be measured using radiation sensors. According to [5], transmission of direct beam radiation through a plastic net was characterized as (i) the unscattered beam that is transmitted through the net pores, (ii) the beam that is reflected forward on the thread surfaces specularly, and (iii) the beam that is diffused during transmission. On the other hand, the reflected beam will be a combination of specularly reflected beam, and backward scattered beam. For several types of nets (having different colors, porosities, and texture structures) tested in [5], the forward diffused beam was less than 20% of the incident beam radiation. For the modeling approach, the unscattered beam, the specularly reflected (forward or backward) beam and the diffused beam were assumed to have the same characteristic manner and were considered as direct beams transmitted or reflected from the net. In analogy to homogeneous materials, the effective transmittance and reflectance of a plastic net to the direct beam solar radiation ( $\tau_r$  and  $\rho_r$ ) can be expressed as [15] by

$$\tau_r = \frac{\tau^* (1 - \rho^*)}{1 - (\tau^* \rho^*)^2}, \qquad \rho_r = \rho^* (1 + \tau^* \tau_r), \tag{1}$$

where  $\tau^*$  is the transmittance of the beam radiation due to absorption only in the net material with a porosity  $\phi$  and a solid matrix of  $(1-\phi)$ ;  $\rho^*$  is the interface reflectance between the net surface and air.

By eliminating  $\rho^*$  from (1) a second-order algebraic equation with the unknown  $\tau^*$  can be obtained. By solving the roots of this equation, the value of  $\tau^*$  is given by [15] as

$$\tau^* = \left\{ \frac{\tau_r^2 - (1 - \rho_r)^2}{2\tau_r} \right\} \pm \left\{ \left( \frac{\tau_r^2 - (1 - \rho_r)^2}{2\tau_r} \right)^2 + 1 \right\}^{1/2}.$$
(2)

Reasonable (i.e., positive) values for  $\tau^*$  are obtained by considering the plus sign of (2). The input parameters to (1) and (2) are the transmittance and reflectance of the net to direct beam radiation ( $\tau_r$  and  $\rho_r$ ) that can be measured using a pyranometer underneath the net and an albedometer above the net. The value of  $\rho^*$  is obtained from the direct substitution of  $\tau^*$  in (1). Once values of  $\tau^*$  and  $\rho^*$  were determined one time (e.g., at normal incidence), the equivalent optical constants ( $n_{\rm eq}$  and  $\sigma_{\rm eq}$ ) of the plastic net can be determined, in analogy to homogeneous translucent materials, as follows.

The interface reflectance  $\rho^*$  at normal incidence between the air (n = 1) and the net surface having the equivalent refractive index  $(n_{eq})$  is given by

$$\rho^* = \frac{\left(n_{\text{eq}} - 1\right)^2}{\left(n_{\text{eq}} + 1\right)^2}.$$
 (3)

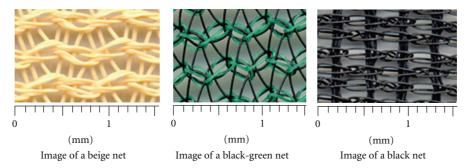


FIGURE 1: Scanner images of a net in each group tested in this study.

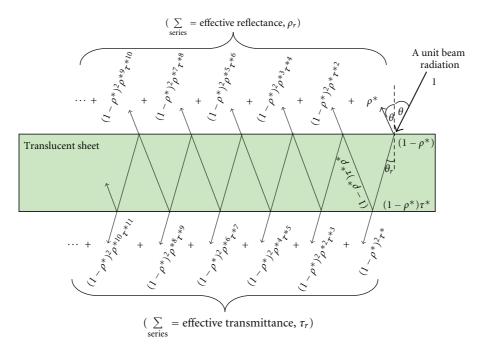


FIGURE 2: Tracing of a unit beam radiation through a translucent sheet to illustrate the concept of the effective reflectance and effective transmittance of the sheet.

Also at normal incidence, the transmittance due to absorption ( $\tau^*$ ) and the equivalent absorption coefficient ( $\sigma_{eq}$ ) of the net material can be expressed in similar manner of the homogeneous translucent films by replacing the film thickness with the net density or net solidity  $(1-\phi)$ ,  $\phi$  is the net porosity. Thus, the relation between  $\tau^*$  and  $\sigma_{eq}$  is given by

$$\tau^* = \operatorname{Exp} \left\{ -\sigma_{\text{eq}} (1 - \phi) \right\}. \tag{4}$$

In (4),  $\sigma_{eq}$  is dimensionless whereas the unit of the absorption coefficient of a homogeneous translucent sheet is mm<sup>-1</sup> if the sheet thickness is in mm.

Once the values of the equivalent optical constants ( $\sigma_{eq}$  and  $n_{eq}$ ) are determined for a net, the directional radiative properties of this net can be calculated at any incidence angle ( $\theta$ ) of the beam radiation. In this case, the directional

interface reflectance  $(\rho_{\theta}^*)$  between the net surface and air is given by [12, 13] as

$$\rho_{\theta}^{*} = \frac{1}{2} \left\{ \frac{\sin^{2}(\theta - \theta_{r})}{\sin^{2}(\theta + \theta_{r})} + \frac{\tan^{2}(\theta - \theta_{r})}{\tan^{2}(\theta + \theta_{r})} \right\},$$

$$\theta_{r} = \sin^{-1}\left(\frac{\sin \theta}{n_{\text{eq}}}\right),$$
(5)

where  $\theta_r$  is the equivalent angle of refraction for a beam radiation penetrates through the net. The directional transmittance due to absorption  $(\tau_{\theta}^*)$  is given by

$$\tau_{\theta}^* = \operatorname{Exp}\left\{\frac{-\sigma_{\operatorname{eq}}(1-\phi)}{\cos\theta_r}\right\}. \tag{6}$$

The directional radiative properties, with respect to the direct beam radiation, of a plastic net can be obtained by

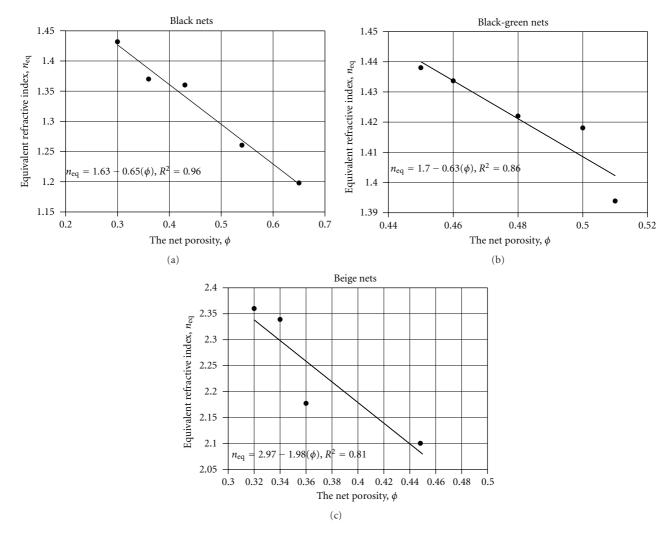


FIGURE 3: The equivalent refractive index ( $n_{eq}$ ) as affected by the porosity of the tested nets: (a) is for the black group, (b) for the black-green group, and (c) for the beige group.

resubstituting  $\tau_{\theta}^*$  and  $\rho_{\theta}^*$  into (1) to obtain  $\tau_r$  and  $\rho_r$  for the desired direction. The diffuse solar radiation incident over a surface can be treated as a direct beam radiation with an incidence angle ( $\theta$ ) of 60° [12]. Thus the directional transmittance and reflectance of a net with respect to the global solar radiation ( $\tau_g$  and  $\rho_g$ ) are defined by

$$\tau_g = \tau_{r,60^{\circ}} I_D + (1 - I_D) \tau_r, 
\rho_g = \rho_{r,60^{\circ}} I_D + (1 - I_D) \rho_r,$$
(7)

where  $I_D$  is the diffuse index estimated as  $(D_i/S_i)$  at the desired direction  $\theta$ .

2.3. Measuring the Required Parameters. For determining the transmittance and reflectance of the net to direct beam solar radiation ( $\tau_r$  and  $\rho_r$ ) to be used as input parameters to (1) and (2), the experiment was conducted on the roof of the building of the Agricultural Research and Experiment Station, Agriculture Engineering Department, King Saud University (Riyadh, Saudi Arabia, 46° 47′ E, longitude and

24° 39′ N, latitude). The measurements were conducted at around solar noon on clear, sunny days from September 10 to September 25, 2011. One pyranometer, CMP3 (Kipp & Zonen B.V. Inc., USA), and one albedometer, CMA-11 (Kipp & Zonen B.V. Inc., USA) were used. Each net sample was tacked onto a black painted wooden frame (50 cm ×  $60 \,\mathrm{cm} \times 30 \,\mathrm{cm}$ ). The frame was oriented toward the sun, so that incidence angle of the solar beam radiation  $(\theta)$ was nearly zero. The transmitted global solar radiation  $(S_t)$ was measured below the net surface using the pyranometer. The incident and reflected global solar radiation ( $S_i$  and  $S_r$ ) were measured above the net sample using the albedometer. This procedure was repeated while shading the frame with an opaque plate to measure the diffuse solar radiation components below  $(D_t)$  and above  $(D_i, D_r)$  the net sample. The measured parameters were recorded every 10 seconds, averaged over one-minute intervals and saved in a data logger (LI-1400, 9 channels, LI-COR, Inc.). For each parameter, five values were measured at normal incidence, and the average value was obtained. The sensors had been calibrated before

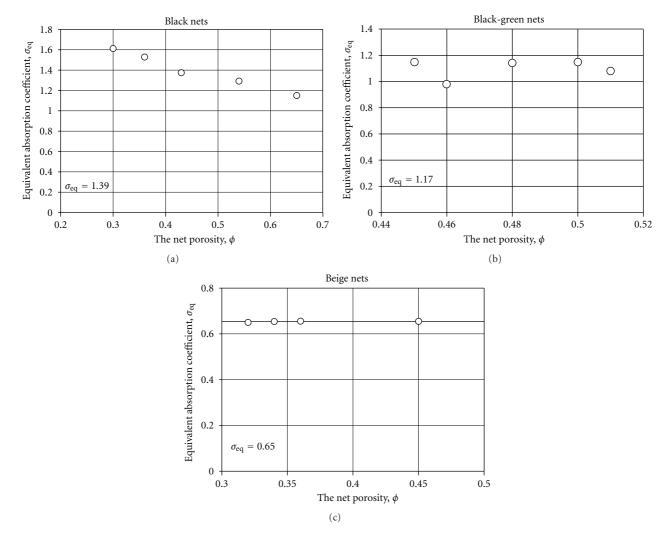


FIGURE 4: The equivalent absorption coefficient ( $\sigma_{eq}$ ) as affected by the porosity of the tested nets: (a) is for the black group, (b) for the black-green group, and (c) for the beige group.

use by the supplier. The components of the direct beam radiation  $(B_i, B_t, \text{ and } B_r)$  were determined as the difference between the global and diffuse radiation components. Thus at normal incidence, the net transmittance to direct beam radiation  $(\tau_r)$  was estimated as  $(B_t/B_i)$  and the net reflectance to direct beam radiation  $(\rho_r)$  was estimated as  $(B_r/B_i)$ .

# 3. Results and Discussion

For each net sample, the measured values of  $\tau_r$  and  $\rho_r$  at normal incidence were substituted consequently into (2) and (1) to obtain the values of  $\tau^*$  and  $\rho^*$ . Substituting the values of  $\tau^*$  and  $\rho^*$  into (3) and (4) gives the equivalent optical constants ( $n_{\rm eq}$  and  $\sigma_{\rm eq}$ ) of the selected net. The optical constants of a net did not depend on the direction of the incident beam radiation; therefore they are used to estimate the directional radiative properties of the net. The values of  $n_{\rm eq}$  as affected by the net porosities ( $\phi$ ) are illustrated in Figures 3(a), 3(b), and 3(c), for the black nets group, the black-green nets group and the beige nets group, respectively.

The data in Figures 3(a), 3(b), and 3(c) show that  $n_{\rm eq}$  decreases when  $\phi$  increases and correlations between  $n_{\rm eq}$  and  $\phi$  could be obtained with reasonable  $R^2$  values in the following form:

$$n_{\rm eq} = 1.63 - 0.65(\phi), \quad (R^2 = 0.96) \text{ for black nets,}$$
 (8)

$$n_{\rm eq} = 1.7 - 0.63(\phi), \quad (R^2 = 0.86) \text{ for black-green nets,}$$
 (9)

$$n_{\rm eq} = 2.97 - 1.98(\phi)$$
,  $(R^2 = 0.81)$  for beige nets. (10)

Ideally, if the value of  $\phi$  in (8), (9), and (10) increased to one (no net), then the values of  $n_{\rm eq}$  should equal to one (i.e., the refractive index of air). However, there are residuals of +0.02 in (8), -0.07 in (9), and +0.01 in (10) that should be added to  $n_{\rm eq}$  estimated form (8)–(10). These equations also show that value of  $n_{\rm eq}$  increases with increasing brightness of the net color, which means more reflection is expected. The nets with the brightest color in this study (the beige nets) showed

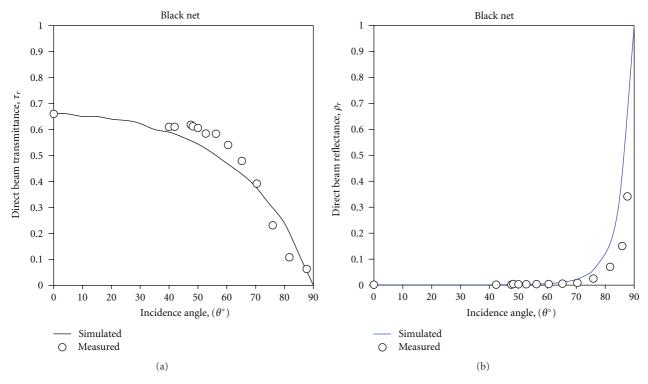


FIGURE 5: Comparison between the measured [8] and simulated values of (a) the direct beam transmittance ( $\tau_r$ ) and (b) the direct beam reflectance ( $\rho_r$ ) for the black net.

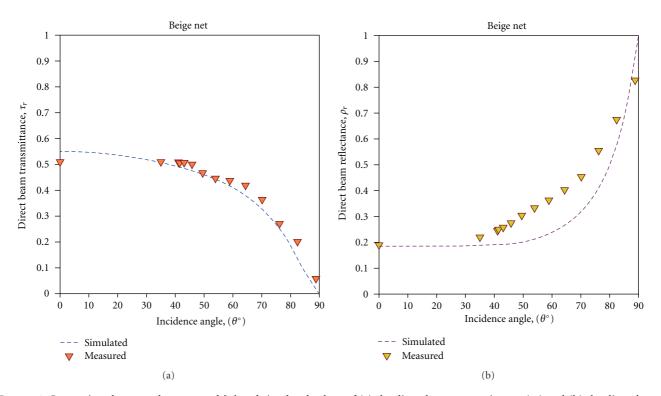


FIGURE 6: Comparison between the measured [8] and simulated values of (a) the direct beam transmittance ( $\tau_r$ ) and (b) the direct beam reflectance ( $\rho_r$ ) for the beige net.

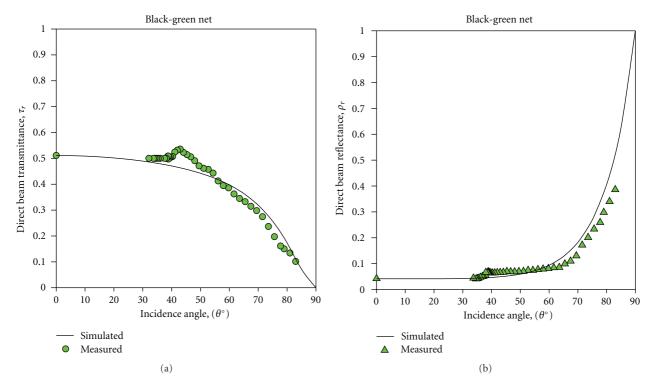


FIGURE 7: Comparison between the measured [8] and simulated values of (a) the direct beam transmittance ( $\tau_r$ ) and (b) direct beam reflectance ( $\rho_r$ ) for the black-green net.

the highest value of  $n_{eq}$  whereas nets with the darkest color (the black nets) showed the lowest  $n_{eq}$ .

The effects of the net porosity  $\phi$  on the value of  $\sigma_{eq}$  are illustrated in Figures 4(a), 4(b), and 4(c) for the black group, for the black-green group, and for the beige group, respectively. According to (4) and (6) and in analogy with homogeneous translucent materials, the value of  $\sigma_{eq}$  should be constant for each group of nets. And the value of  $\tau_{\theta}^*$  in (6) depends on the porosity,  $\phi$ , of the net and on the direction,  $\theta$ , of the incident beam radiation. The data in Figure 4(c) for the beige nets group satisfy the hypothesis that  $\sigma_{eq}$  is constant for each group of nets. However, the values of  $\sigma_{eq}$  for the black and black-green groups (Figures 4(a) and 4(b)) did not satisfy the hypothesis exactly. This was mainly due to the low number of data points as a result of the low availability of net groups in the local markets. Therefore, an average value for each net group was used.

#### 4. Validation of the Model

The main purpose of the validation is to check the capability of  $n_{\rm eq}$  and  $\sigma_{\rm eq}$ , estimated using the present model, to calculate the directional radiative properties of nets under natural solar radiation conditions. In a previous study [8] we measured the direct beam transmittance  $(\tau_r)$  and reflectance  $(\rho_r)$  for a black net  $(\phi = 0.65)$ , for a beige net  $(\phi = 0.12)$ , and for a black-green net  $(\phi = 0.47)$  at different incident angles  $(\theta)$  of the direct beam solar radiation. Values of  $\tau_r$  and  $\rho_r$  at normal incidence were measured for the three nets (see Section 2.2). The simulated values of  $\tau_r$  and  $\rho_r$  using the

present model at different  $\theta$  comparing with the measured values of  $\tau_r$  and  $\rho_r$  are illustrated, respectively, in Figures 5(a) and 5(b) for the black net, in Figures 6(a) and 6(b) for the beige net, and in Figures 7(a) and 7(b) for the black-green net. Reasonable agreement was shown between the simulated and the measured  $\tau_r$  and  $\rho_r$  for the black, beige, and black-green nets.

Figures 5(a), 5(b), 6(a), 6(b), 7(a), and 7(b) do not show measured values of  $\tau_r$  and  $\rho_r$  at low values of incidence angle  $(0^{\circ} < \theta < 33^{\circ})$  because of the latitude and the time of the year at which the experiments were carried out (the lowest value of  $\theta$  was estimated to be about 33° at solar noon). In addition, when  $\theta$  was near or equal to 90°, the beam radiation incident on the thread surfaces reflects downwards. This increased  $\tau_r$  to a value higher than zero and reduced  $\rho_r$  to a value much lower than one.

#### 5. Conclusions

A modeling approach for determining the equivalent optical constants ( $n_{\rm eq}$  and  $\sigma_{\rm eq}$ ) of plastic nets was described and validated. Three groups of nets (black, beige, and blackgreen) were tested. For each group, an equation for  $n_{\rm eq}$  as a function of the net porosity was derived, and an average value for  $\sigma_{\rm eq}$  was determined. Using values of  $n_{\rm eq}$  and  $\sigma_{\rm eq}$ , the directional solar radiative properties of the net can be calculated without the need of measurements which are expensive and time consumed. The resulting properties are equivalent for the whole net as a semitransparent material, not for the net material itself. The present model was

validated by comparing the measured radiative properties of three of the nets, at different incident angle of solar beam radiation, with those calculated using the present model. The calculated radiative properties agreed with the measured values. Further research is needed to investigate  $n_{\rm eq}$  and  $\sigma_{\rm eq}$  for other nets communities with different colors (e.g., a blue group, an orange group, a white group, a green group, etc.).

#### **Nomenclature**

- $B_i$ : Direct beam solar radiation flux incident on the net surface (W m<sup>-2</sup>)
- $B_r$ : Direct beam solar radiation flux reflected from the net (W m<sup>-2</sup>)
- $B_t$ : Direct beam solar radiation flux transmitted through the net (W m<sup>-2</sup>)
- $D_i$ : Diffuse radiation flux incident on the net surface (W m<sup>-2</sup>)
- $D_r$ : Diffuse radiation flux reflected from the net surface (W m<sup>-2</sup>)
- $D_t$ : Diffuse radiation flux transmitted through the net (W m<sup>-2</sup>)
- I<sub>D</sub>: The diffuse index (i.e., ratio of diffuse to global solar radiation flux)
- $n_{\text{eq}}$ : Equivalent refractive index of the net (dimensionless)
- $S_i$ : Global solar radiation flux incident on the net surface (W m<sup>-2</sup>)
- $S_r$ : Global solar radiation flux reflected from the net surface (W m<sup>-2</sup>)
- $S_t$ : Global solar radiation flux transmitted through the net (W m<sup>-2</sup>)
- Φ: The net porosity (i.e., the empty area per unit area)
- $\theta$ : Incident angle of solar beam radiation (degree)
- $\theta_r$ : Equivalent refracted angle of solar beam radiation (degree)
- $\rho_g$ : Reflectance of the net to global solar radiation (dimensionless)
- $\rho_r$ : Reflectance of the net to direct beam solar radiation (dimensionless)
- $\rho^*$ : Interface reflectance between the net surface and air (dimensionless)
- $\rho_{\theta}^*$ : Directional interface reflectance between the net surface and air (dimensionless)
- $\sigma_{\text{eq}}$ : Equivalent absorption coefficient of the net (dimensionless)
- $\tau_g$ : Transmittance of the net to global solar radiation (dimensionless)
- $\tau_r$ : Transmittance of the net to direct beam solar radiation (dimensionless)
- $\tau^*$ : Transmittance of the net due to absorption only in the net threads (dimensionless).

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# Research Article

# **Experimental Study on Solar Cooling Tube Using Thermal/Vacuum Emptying Method**

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A solar cooling tube using thermal/vacuum emptying method was experimentally studied in this paper. The coefficient of performance (COP) of the solar cooling tube was mostly affected by the vacuum degree of the system. In past research, the thermal vacuum method, using an electric oven and iodine-tungsten lamp to heat up the adsorbent bed and H<sub>2</sub>O vapor to expel the air from the solar cooling tube, was used to manufacture solar cooling tubes. This paper presents a novel thermal vacuum combined with vacuum pump method allowing an increased vacuum state for producing solar cooling tubes. The following conclusions are reached: the adsorbent bed temperature of solar cooling tube could reaches up to 233°C, and this temperature is sufficient to meet desorption demand; the refrigerator power of a single solar cooling tube varies from 1 W to 12 W; the total supply refrigerating capacity is about 287 kJ; and the COP of this solar cooling tube is about 0.215.

#### 1. Introduction

With the improvement of people's living standard, the demand for air conditioner is increasing. Use of CFCs for refrigeration compression has global warming potential (GWP) and ozone depletion potential (ODP), so their use should be minimized. The energy problem has become a major problem facing human development, and has led to efforts to reduce fossil fuel usage. Solar energy, one of the most abundant resources, has many advantages, most importantly that it is environmentally friendly. This has led to attention from the worldwide research community. Adsorption refrigeration uses nature working pairs as refrigerants and solar energy as a heat resource, so it consumes no fossil fuels during refrigeration process and is environment-friendly.

Ferreira Leite et al. [1] presented the characterization and the pre-dimensioning of an adsorption chiller as part of a 20 kW air conditioning central unit for cooling a set of rooms that comprises an area of 110 m<sup>2</sup>. The adsorption chiller's expected coefficient of performance (COP) was found to be around 0.6. Khattab [2] presented the description and

operation of a simple structure, low cost solar-powered adsorption refrigeration module. Test results showed that a module using bed technique Type 4 and reflector arrangement Type C provided the best performance. Wang et al. [3, 4] used a compound adsorbent of CaCl<sub>2</sub> and activated carbon as working pairs and to produce an ice-making test unit for fishing boats. At evaporating temperatures of -35°C and -25°C, the cooling powers are 0.89 and 1.18 kW respectively. Clausse [5] explored the possibility to perform heating and air-conditioning of a state-of-the-art building located near Paris in France. For air-conditioning, thermal comfort was achieved as indoor temperature was kept below 25°C during five consecutive hot days. Anyanwu et al. [6, 7] made a solid adsorption refrigerator, achieving a chilled water temperature around 1°C, suitable for drug, fruits, and vegetables preservation. Khattab [2, 8, 9] set up a solar-powered adsorption module, this module produced ice 6.9 kg/m<sup>2</sup> and the net solar COP is 0.136. Guilleminot et al. [10–12] presented experimental study on solar adsorptive ice maker and Heat transfer intensification in the adsorbent bed, and the results show the great improvement in the thermal transfer quality using new consolidated materials.

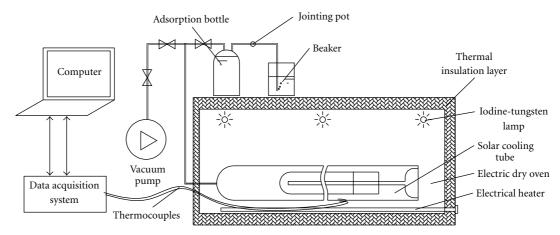


FIGURE 1: Sketch of manufacturing solar cooling tube by means of thermal/vacuum method.

Compared with the above refrigeration system, a solar cooling tube can accomplish the refrigeration cycle in one glass tube. The solar cooling tube [13] and freeze-proof solar cooling tube [14] which uses zeolite/water or active carbon/methanol as working pairs were designed and built. In the past research, the solar cooling tube was manufactured using the thermal vacuum method, which using electric oven and iodine-tungsten lamp to heat up the adsorbent bed, and using  $H_2O$  vapor to expel the air of the solar cooling tube and to reduce air partial pressure. This paper presents a novel thermal vacuum combined with vacuum pump method for producing solar cooling tube, resulting in a highly increased vacuum state.

# 2. Manufacture of the Solar Cooling Tube

The manufacturing process of solar cooling tube is mainly composed of three steps: (1) the preparation filling process; (2) preliminary drying of the solar cooling tube; (3) operating vacuum state by means of thermal/vacuum method. The steps are as follows.

First, the 13X zeolite is activated in the 325°C oven for 8 hours, and then an appropriate amount of highly pure sodium silicate and pure water is added to prepare the adsorption compound. The resulting adsorbent compound has better thermal conductivity and formability than 13X powder [15]. An electric mixer is used to stir the mixture until it becomes liquid state. A funnel is used to fill the confected the compound adsorbent into all-glass tubular solar collector and preliminary dries it by iodine-tungsten lamp.

Second, put the all-glass tubular solar collector filled with the compound adsorbent into a high borosilicate glass and welding pipe using glass welding lathe, then the semifinished solar cooling tube was made.

Third, 200 mL pure water is placed into the semi-finished solar cooling tube. The tube is then placed into an electric dry oven, and welding the solar cooling tube with adsorption bottle, jointing pot beaker and vacuum pump. Figure 1 shows a diagram of the system, and Figure 2 is a photograph of the production equipment. After several hours discharging



FIGURE 2: Photograph of manufacturing solar cooling tube.

the air in the solar cooling tube using the thermal emptying method, a vacuum pump is used to evacuate the solar cooling tube. Finally, welding the tail joint completes manufacture of the solar cooling tube.

# 3. Principle of Solar Cooling Tube

The structure of the solar cooling tube is shown in Figure 3. The solar cooling tube contains these major components: solar collector, adsorbent bed, condenser, inner tube, and evaporator. The solar collector, condenser, inner tube, and evaporator are made of hard borosilicate glass. Using 13X zeolite, the temperature difference between daytime and nighttime corresponds to the adsorption capability difference of refrigerant water; hence, the solar cooling tube achieves refrigeration cycle. The process goes as follows.

During the daytime, the adsorbent bed receives sunlight, and the adsorbent bed temperature rises up to the desorption temperature. When the water vapor flows from adsorbent and raises the water vapor pressure up to the condensing pressure, the desorbed water vapor, which desorbed from adsorbent bed, is condensed in the condenser and flows into the evaporator because of gravity. The water vapor is condensed in the inner wall of the whole outer tube and extracts heat from the environment. In the daytime, the inner

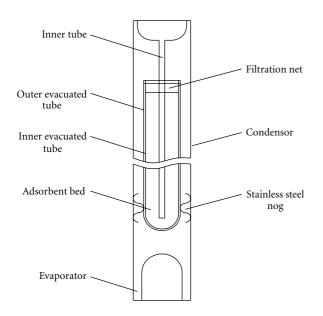


FIGURE 3: Sketch of the solar cooling tube.

tube is full of air and can reduce the thermal loss of adsorbent bed, so the adsorbent bed has higher temperature for desorption. In the whole day, the solar cooling tube receives solar radiation while the water steam continues desorbing from the adsorbent bed and is stored the evaporator. During the nighttime, the adsorbent bed temperature drops after sunset and the inner tube is full with water. This enhances heat transfer for cooling down the adsorbent bed and obtaining heating water. When the adsorbent bed temperature drops to adsorption temperature, the adsorption bed begins to adsorb water vapour and induces a decrease in water vapour pressure, causing the liquid water in the evaporator to vaporize. When the evaporating temperature has lowered enough, the system can provide cooling to the outside. In the adsorption process, the refrigerant water continues to vaporize to supply cooling capacity to the outside; the adsorption refrigeration will continue for the whole night until the next morning.

# 4. Experiment Setup

The sketch and photograph of the experiment in solar cooling tube was shown in Figures 4 and 5. The main apparatus used for this experiment are as followes: 2700 Multimeter/Data Acquisition system of Keithley Co., was used for collecting the data of temperature measurement, T-type thermocouples and K-type thermocouples are the temperature sensors for lower temperature and higher temperature testing, respectively, the model TRM-123 temperature and radiation instrument produced by Jinzhou was used for testing the solar radiation density, and the model RYQ-1 automatic surface meteorological station was used for measuring the environmental temperature and air relatives humidity.

Temperature and solar radiation were measured at fiveminute intervals and could be accessed instantaneously on the computer.

#### 5. Results and Discussion

- 5.1. The Variation of Solar Radiation and Ambient Temperature. During the experimental period, the weather was sunny and little cloudy. The solar radiation and ambient temperature variation was shown in Figure 6. The solar radiation value is about 20.1 MJ·m<sup>-2</sup>. The maximum solar radiation density is about 800 W·m<sup>-2</sup> at time 11:45 AM. The ambient temperatures were measured by T-type thermocouples in this experiment. The maximum and the minimum ambient temperature were about 33.8°C and 19.4°C respectively. The average ambient temperature was 25.9°C.
- 5.2. The Adsorbent Bed Temperature Variation. The adsorbent bed temperature variation of solar cooling tube was shown in Figure 7. In the daytime, the adsorbent bed received solar energy and the adsorbent temperature rose up rapidly to 233°C. This temperature met with desorption demand and the refrigerant water was desorbed from the 13X zeolite adsorbent bed. The steam released the latent heat during condensation and became liquid, before being stored in the evaporator due to gravity. Throughout the day, the solar cooling tube received solar radiation while the refrigerant water steam continued desorbing from the adsorbent bed until the solar radiation was too weak for desorption. At night, the adsorbent temperature dropped and began to adsorb the water steam. In the adsorption process, the adsorbent bed temperature cooled down to a minimum temperature of about 33°C. The temperature difference between adsorbent bed and ambient temperature was about 14°C.
- 5.3. Condensation Temperature Variation. The condensation temperatures of the solar cooling tube were tested at this experiment. Two temperature test points were set on the outside of the condenser. In the desorption process during daylight, the refrigerant water vapor, which desorbed from the adsorbent bed at high temperature, was condensed in the condenser. The variation of the condensation temperature of the solar cooling tube can be seen in Figure 8. The temperature of condenser varied from 31.6°C to about 40.5°C. The maximum and average temperature difference between condenser and ambient temperature was about 13.8°C and 9.7°C, respectively.
- 5.4. Evaporation Temperature Variation. Two temperature test points were set on the outside of the evaporator. In the adsorption process at nighttime, the adsorbent bed adsorbs the refrigerant gas and keeps the evaporator liquid water evaporating and supply cooling mass to the outside. The variation of the evaporator temperature of the solar cooling tube can be seen in Figure 9. The temperature of evaporator mainly varied from 15°C to about 10°C and the minimum evaporator temperature is about 9.2°C.

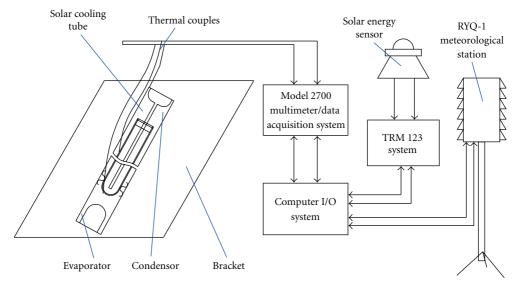


FIGURE 4: The experiment of solar cooling tube performance.



FIGURE 5: The photograph of the experiment.

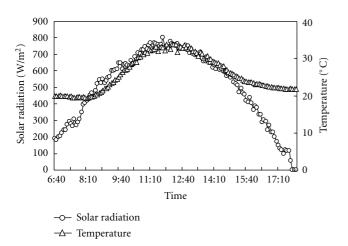


FIGURE 6: Solar radiation and ambient temperature variation.

5.5. Desorption Capacity Variation. The desorption capacity variation of the solar cooling tube can be seen in Figure 10. During the daytime, the adsorbent bed temperature rose as solar energy was received. The refrigerant water gas was

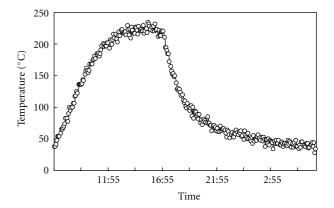


FIGURE 7: The adsorbent bed temperature variation of the solar cooling tube.

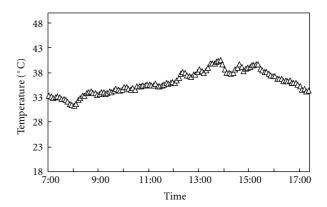


FIGURE 8: The condensation temperature variation.

desorbed from the adsorbent bed and stored in the evaporator. Desorption capacity was measured by the quantity of the refrigerant water. From 9:00 to 12:00, the speed of

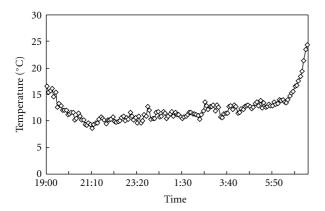


FIGURE 9: The evaporation temperature variation.

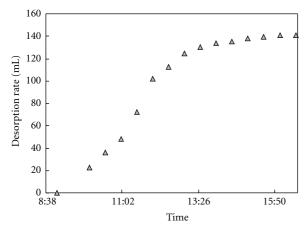


FIGURE 10: The desorption capacity variation of the solar cooling tube.

desorption was higher and was slow down after 13:00. The total desorption capacity was about 140 g.

5.6. Evaporative Refrigeration Capacity of a Single Solar Cooling Tube. The refrigerator power variation of a single solar cooling tube can be seen in Figure 11. In the adsorption process at nighttime, the adsorbent bed adsorbed the refrigerant gas and keeps the evaporator liquid water evaporating supply cooling mass to the outside. The refrigerator power of a single solar cooling tube varied from 12 W at about 20:00°C and weakened to less than 1 W by the following morning. The total supply refrigerating capacity was about 287 kJ and the COP of this solar cooling tube was about 0.215.

# 6. Conclusions

This paper focused on an experimental study of a solar cooling tube using a thermal/vacuum emptying method. The solar cooling tube uses solar energy as a heating resource to complete the adsorption cycle, reducing damage to the environment compared to common alternatives. The performance of solar cooling tube was experimentally

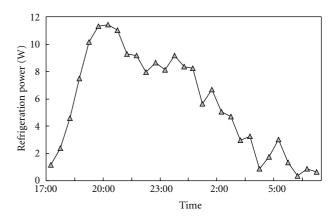


FIGURE 11: The refrigerator power of a single solar cooling tube.

studied in this research and the following conclusions can be drawn:

- (1) When ambient temperature is about 19.4° C−33.8° C, and the solar radiation is about 20.1 MJ·d<sup>-1</sup> m<sup>-2</sup>, the adsorbent bed temperature of solar cooling tube reaches up to 233° C. This temperature canmeet desorption demand.
- (2) At the nighttime, the adsorbent bed temperature of the solar cooling tube cooled down to the minimum temperature about 33°C and this temperature can meet adsorption demand. The temperature difference between adsorbent bed and ambient temperature is about 14°C.
- (3) The refrigerator power of a single solar cooling tube varied from 12 W to 1 W. The total supply refrigerating capacity is about 287 kJ and the COP of this solar cooling tube is about 0.215.

# Acknowledgments

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# Research Article

# Treatment of Color Filter Wastewater by Fresnel Lens Enhanced Solar Photo-Fenton Process

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Treatment of color filter wastewater using solar photo-Fenton process enhanced by high-concentrating Fresnel lens was investigated in this paper. Optimal reaction conditions based on response surface methodology (RSM) were established as under an initial pH of 5, a  $[H_2O_2]_0/COD_0$  ratio of  $1\sim1.35$  and a  $[H_2O_2]_0/[Fe^{2+}]_0$  ratio of 15 for a reaction time of 60 min, which could reach a readily biodegradable level, that is, the biodegradability (BOD $_5/COD$ ) of wastewater was more than 0.3. With the assistance of Fresnel lens, the solar photo-Fenton process increased the COD degradation rate and mineralization rate by a factor of 4.5 and 6.5, respectively. In addition, the microtoxicity ( $TU_{50}$ ) of wastewater was almost diminished after a 60 min of treatment, whereas the microtoxicity of treated wastewater without the assistance of Fresnel lens remained a  $TU_{50}$  value of 1.166. This could be mainly due to the concentrating effect of Fresnel lens for solar energy, resulting in an increase of  $2\sim3$  times of solar light intensity and a raising heat irradiation in terms of  $15\sim30$  °C of wastewater temperature. These results revealed that solar energy could be concentrated effectively by using Fresnel lens and showed a significant promoting effect on the photo-Fenton reaction for treating color filter wastewater.

# 1. Introduction

Organic wastewater from color filter industry generally contains so many residuals such as TMAH (C<sub>4</sub>H<sub>13</sub>NO), PGMEA (C<sub>6</sub>H<sub>12</sub>O<sub>3</sub>), acrylic resin, and pigments, and it is variable in composition and strength at different stages of process. The effluent is usually characterized by its high chemical oxygen demand (COD), low biodegradability (BOD5/COD), and with microtoxicity, implying the presence of refractory organic matter. Therefore, biological treatment processes are susceptible for treatment of color filter wastewater. Instead, activated carbon adsorption or coagulation is commonly used. However, new environmental laws may consider the spent adsorbents or sludge as hazardous waste and require further treatment. Consequently, intensive research for novel technologies with higher efficiency and less amount of waste generated has been stimulated. For that reason, advanced oxidation processes (AOPs) have been previously described as a promising option to remove persistent pollutants from contaminated water [1] when conventional water treatment

processes are not efficient enough. AOPs are able to produce a highly reactive, nonspecific oxidant, mainly hydroxyl radicals (\*OH). The hydroxyl radical possesses inherent properties that enable it to attack refractory organic pollutants in water to achieve a complete mineralization. However, the production of photons with artificial light sources requires significant electrical energy demand and UV lamp consumption, leading in a high operation cost in AOPs [2].

Alternatively, solar energy is essentially unlimited and its utilization is ecologically benign. In the wastewater treatment sector, solar technology has been extensively used as alternative to UV lamps to reduce the operation cost in AOPs [3]. In particular, photo-Fenton process using solar irradiation has been used as an economically viable process and has attracted great interest in recent years [4]. However, solar photo-Fenton process was usually carried out by using solar irradiation directly, resulting in a lower absorption and utilization of solar energy [5]. To improve the efficiency of solar photo-Fenton process, it is necessary to maximize the absorption of solar energy.

TABLE 1: Characteristics of color filter wastewater.

Item	Range
pН	10.4~10.7
$UV_{254}$	2.000~2.046
COD, mg/L	1674~1766
BOD <sub>5</sub> , mg/L	152~230
BOD <sub>5</sub> /COD	0.08~0.13
TOC, mg/L	405~430
SS, mg/L	2.4~3.0
TS, mg/L	$1145 \sim 1440$
Color (ADMI value)	1100~1400

In this study, the degradation and mineralization of color filter was tewater using solar photo-Fenton process enhanced by high-concentrating Fresnel lens was investigated. This lens is made of PMMA plastic materials. Response surface methodology (RSM) was employed to obtain the optimal reaction conditions of critical process parameters (initial pH of was tewater,  $[H_2O_2]_0/COD_0$  and  $[H_2O_2]_0/[Fe^{2+}]_0)$  to reach a readily biodegradable degree of color filter was tewater. Moreover, the effect of Fresnel lens on treatment performance in terms of COD degradation efficiency, mineralization efficiency, biodegradability, and microtoxicity of color filter was tewater was examined.

# 2. Materials and Methods

2.1. Materials. The color filter wastewater used in this study was obtained from an electrooptical industry plant located in Hsin-Chu, Taiwan. The characteristics of color filter waster are shown in Table 1. Basically, the color filter wastewater has the properties of high COD, low biodegradability, and with microtoxicity. Hydrogen peroxide ( $H_2O_2$ ) with a concentration of 35% was supplied by Panreac Co., EU. FeSO<sub>4</sub> · 7H<sub>2</sub>O (Panreac Co., EU) with a purity of 99% was used as a source of ferrous ion. All other chemicals used in this study were analytical grade and used as received.

2.2. Procedures. All experiments were carried out in a batch mode. A 1-L glass beaker containing 200 mL of color filter wastewater was used and maintained at a preset temperature in a water bath during the experiments. A 3-factor \*3-level RSM experimental design with three replicates at center point as shown in Table 2 was applied. The color filter wastewater was placed into the photoreactor and irradiated by artificial solar light with an intensity of 500 W/m<sup>2</sup> by using an ATLAS Suntest CPS+ solar simulator (ATLAS Co., USA). During the experiments, the pH of the solution was monitored using a pH meter (SP-701LI 120, Suntex Co., Taiwan) equipped with a glass electrode. Samples were withdrawn from the reactor at a reaction time of 60 min, tested for H<sub>2</sub>O<sub>2</sub> consumption according to the method reported by Seller [6] and iron as Fe<sup>2+</sup> ion determined by Fe(II)/1,10-phenanthroline complex at 510 nm [7] using a Hitachi (Japan) U-2001 spectrophotometer instantly, and then quenched with sodium hydrogen sulfite to avoid further

Table 2: Experimental range and levels of the process independent variables in this study.

Independent variable	Factor	Range and level		
		-1	0	+1
Initial pH	$X_1$	3	4	5
$g H_2O_2/g COD$	$X_2$	1.0	1.5	2.0
$[H_2O_2]_0/[Fe^{+2}]_0$	$X_3$	5	10	15

reactions. The remaining samples were then stored at 4°C for the following ADMI, COD, TOC, BOD<sub>5</sub>, and microtoxicity analysis.

As the optimal values of the process parameters were developed on the basis of RSM application and related equations, a Fresnel lens that was made of PMMA (thickness: 2 mm, pitch: 0.5 mm, facet depth: 0.2 mm, Fresnel circles: 395) was added into solar photo-Fenton system with a distance of 16 cm above the level of wastewater. To investigate the effect of Fresnel lens, a similar reactor without Fresnel lens was also performed under the same actual solar irradiation. A schematic diagram of the photoreactor using Fresnel lens is shown in Figure 1.

#### 2.3. Analytical Methods

2.3.1. Color Measurement of Color Filter Wastewater. A DR 4000 spectrophotometer (HACH Co., USA) was used for color measurement in terms of ADMI (American Dye Manufacturers Institute) values. The decolorization efficiency was calculated on the basis of ADMI reduction in color filter wastewater.

2.3.2. COD and TOC Measurement. COD (Chemical Oxygen Demand) of wastewater was carried out via a DR 4000 photometer (HACH Co., USA) by using a K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub> reagent. TOC (Total Organic Carbon) of wastewater was measured by a Shimadzu VCPH analyzer (Shimadzu Co., Japan).

 $2.3.3.~BOD_5$  Measurement. BOD<sub>5</sub> test was measured according to the procedures described in Standard methods [7] Section 5210D. The bacteria (2000~4000 mgMLSS/L) used in this test were obtained from local activation sludge system, operating at industrial wastewater treatment plant. The data showed that the BOD<sub>5</sub> value of untreated color filter wastewater in this study was  $0.08\sim0.13$ , indicating that the color filter wastewater was not readily biodegradable.

2.3.4. Microtoxicity Measurement. The microtoxicity of each sample was measured using an SDI M500 (SDI Co., USA) analyzer. Microtoxicity is expressed as  $EC_{50}$  (5 min, 15°C), which was defined as the effective concentration of solution for a 50% reduction of the luminescence of the bacterium *Photobacterium phosphoreum*. A lower  $EC_{50}$  value indicates a higher amount of toxic constituent presented in the pollutant solution. The  $EC_{50}$  values are expressed as percentage (% v/v) of the sample [8, 9]. In addition,  $EC_{50}$  values could be transformed to toxicity units ( $TU_{50}$ ), which was equal to

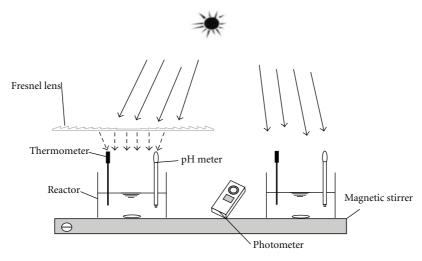


FIGURE 1: Schematic diagram of the solar photoreactor with and without Fresnel lens.

 $1/EC_{50}$ . The  $EC_{50}$  of color filter wastewater was measured, and it was  $76\sim78\%$ . Toxicity Unit ( $TU_{50}$ ) was, therefore, in the range of  $1.25\sim1.30$  for color filter wastewater. In this study, the  $TU_{50}$  value was used to trace the change in toxicity of color filter wastewater due to solar photo-Fenton treatment.

# 3. Results and Discussion

3.1. Optimization of Solar Photo-Fenton Treatment of Color Filter Wastewater. On the basis of RSM application, the empirical relationship between the biodegradability of color filter wastewater (*Y*) and independent variables studied are shown as follows:

$$\begin{split} Y_{\text{BOD}_5/\text{COD}} &= 0.4770 + 0.0066X_1 + 0.0968X_2 - 0.1251X_3 \\ &- 0.0374X_1^2 - 0.0291X_2^2 - 0.0084X_3^2 - 0.0795X_1X_2 \\ &- 0.0628X_2X_3 - 0.0565X_2X_3, \end{split}$$
 
$$r^2 = 0.904. \tag{1}$$

The regression model (1) had a high value of coefficient of determination ( $r^2 > 0.90$ ). This implies that the process efficiency could be predicted properly by the polynomial regression equations under the conditions studied. Based on the model equation, the optimal values of the process parameters were established as under a pH of 5, a  $[H_2O_2]_0/COD_0$  ratio of  $1\sim1.35$ , and a  $[H_2O_2]_0/[Fe^{2+}]_0$  ratio of 15 for a reaction time of 60 min, which could reach a readily biodegradable level, that is, the biodegradability (BOD<sub>5</sub>/COD) of wastewater was more than 0.3. In order to confirm the optimum conditions, five replicates and ttest analysis were performed. The results showed that the average of BOD<sub>5</sub>/COD was 0.306 and the 95% of confidence intervals for BOD<sub>5</sub>/COD was 0.290~0.322. Consequently, the credibility of the optimal conditions obtained in this study was acceptable.

3.2. Effect of Fresnel Lens on the Degradation Efficiency of Wastewater. Basically, it was found that the concentrating effect of Fresnel lens for solar energy could result in an increase 2~3 times of solar light irradiation and a raising heat irradiation in terms of 15~30°C of wastewater temperature in this study. Figure 1 showed the effect of Fresnel lens on COD and TOC degradation efficiency of color filter wastewater. As shown in Figure 2, an 85% of COD and a 70% of TOC degradation of color filter wastewater were achieved with the assistance of Fresnel lens, in contrast to a 48% of COD and a 32% of TOC degradation in solar photo-Fenton process with a solar irradiation of 1,000 W/m<sup>2</sup> was observed within 60 min. The decolorization efficiency of color filter wastewater also increased 17% as using Fresnel lens. Moreover, it was found that the degradation efficiency of color filter wastewater with the use of Fresnel lens at a reaction time of 30 min was higher than that without the assistance of Fresnel lens at a reaction time of 60 min. This could be due to a higher light irradiation and because water temperature increased the reaction rate between hydrogen peroxide and any form of ferrous/ferric ion, thus increased the rate of generation of oxidizing species such as \*OH radical [10]. A similar phenomenon was also found in the study of Will et al. [11]. Its result indicated that the TOC degradation efficiency of phenol wastewater was 45% and 55% for a solar irradiation of 450 W/m<sup>2</sup> and 750 W/m<sup>2</sup>, respectively. In addition, the study's results of Rodriguez et al. [12] showed that the degradation efficiency of textile wastewater increased while the temperature of water was improved obviously from 30°C to 60°C in photo-Fenton process.

To quantitatively analyze the effect of Fresnel lens on degradation of color filter wastewater, a pseudo-first-order model was applied to obtain the rate constants. It was found that both the COD and TOC degradation efficiencies of color filter wastewater with or without Fresnel lens followed the pseudo-first-order reaction kinetics as indicated by high correlation coefficient ( $r^2 > 0.90$ ) (Table 3). It was obvious that a significant enhancement for the degradation rate of color filter wastewater was achieved by using Fresnel lens. As

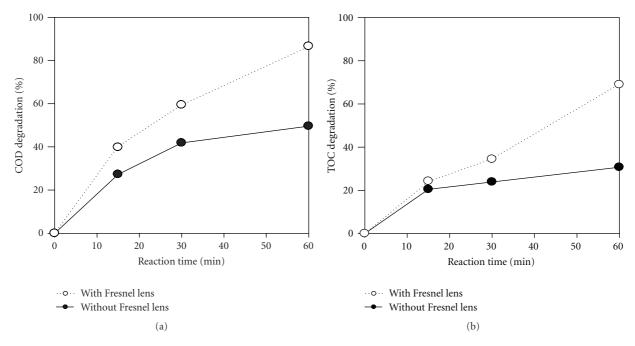


FIGURE 2: Effect of Fresnel lens on the degradation efficiency of (a) COD and (b) TOC of color filter wastewater in solar photo-Fenton process (initial pH: 5.0;  $H_2O_2/COD = 1.25 \, g/g$ ;  $[H_2O_2]_0/[Fe^{2+}]_0 = 15$ ).

TABLE 3: Effect of Fresnel lens on the degradation rate constant of color filter wastewater.

Solar Photo-Fenton Process	$^{ m a}k_{ m COD}$ , ${ m min^{-1}}$	$^{\mathrm{b}}k_{\mathrm{TOC}}$ , $\mathrm{min}^{-1}$	<sup>c</sup> UV <sub>a+b</sub> , W/m <sup>2</sup>
Without Fresnel lens	$0.0076 \pm 0.00079$	$0.0032 \pm 0.00050$	54.82
With Fresnel lens	$0.0342 \pm 0.00232$	$0.0208 \pm 0.00170$	138.09

<sup>\*</sup> Operation condition:  $pH_0$ : 5.0, 1.25  $gH_2O_2/gCOD$ ,  $[H_2O_2]_0/[Fe^{2+}]_0 = 15$ .

<sup>&</sup>lt;sup>c</sup>UV<sub>a+b</sub>: UV light (280–400 nm) intensity.

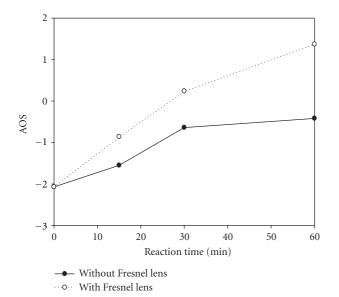


FIGURE 3: Effect of Fresnel lens on AOS of color filter wastewater in solar photo-Fenton process (initial pH: 5.0;  $H_2O_2/COD = 1.25 \text{ g/g}$ ;  $[H_2O_2]_0/[Fe^{2+}]_0 = 15$ ).

the rate constant shown in Table 3, the COD degradation rate and mineralization rate of color filter wastewater increased a factor of 4.5 and 6.5, respectively, mainly due to the  $UV_{a+b}$  light intensity increasing 2.5 times with assistance of Fresnel lens.

3.3. Effect of Fresnel Lens on the Biodegradability of Wastewater. The degree of oxidation and produced intermediates of color filter wastewater during solar photo-Fenton treatment could affect significantly the biodegradability of solution [13]. Average oxidation state (AOS) could be used to monitor the change in the degree of oxidation [14]. The average oxidation state of the organic carbon was calculated by

$$AOS = 4 - 1.5 \times \frac{COD}{TOC},$$
 (2)

in which the unit of COD and TOC is mol  $O_2/L$  and mol C/L, respectively. The AOS value indicates how chemical substances in the effluent become more oxidized. A higher AOS value implies a higher degree of oxidation. Theoretically, the AOS has a value of +4 for  $CO_2$ , the most oxidized state of C, and -4 for  $CH_4$ , the most reduced state of carbon. As shown in Figure 3, the untreated color

<sup>&</sup>lt;sup>a</sup>k<sub>COD</sub>: pseudo-first-order rate constant based on the degradation of COD in solution for 95% confidence coefficient.

 $<sup>^{</sup>b}k_{TOC}$ : pseudo-first-order rate constant based on the degradation of TOC in solution for 95% confidence coefficient.

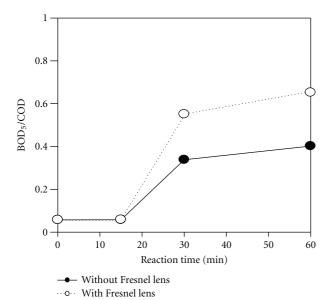


FIGURE 4: Effect of Fresnel lens on the biodegradability of color filter wastewater in solar photo-Fenton process (initial pH: 5.0;  $H_2O_2/COD = 1.25 \text{ g/g}$ ;  $[H_2O_2]_0/[Fe^{2+}]_0 = 15$ ).

filter wastewater has an AOS value of -2.07 and the AOS values increased to 1.37 and -0.42 at a reaction time of 60 min with and without using Fresnel lens, respectively. This result implied that a higher degree of oxidation happened in Fresnel-lens-assisted system. Figure 4 showed the effect of Fresnel lens on BOD<sub>5</sub>/COD of color filter wastewater. It was found that the Fresnel-lens-assisted solar photo-Fenton process could improve furthermore in the biodegradability of color filter wastewater. The required reaction time to reach the criteria of a ready biodegradability of wastewater, in which a BOD<sub>5</sub>/COD value of 0.3 was usually selected, was less as a result for the Fresnel-lens-assisted system.

3.4. Effect of Fresnel Lens on the Microtoxicity of Wastewater. The effect of Fresnel lens on the microtoxicity of color filter wastewater in solar photo-Fenton process was shown in Figure 5. It was found that the microtoxicity of color filter wastewater increased obviously at a reaction time of 15 min, which may be due to more toxic intermediates generated at initial reaction stage. A similar result was also found in the study of González et al. [8]. However, the  $TU_{50}$  value decreased almost to 0 in the Fresnel-lens-assisted system as reaction was proceeding to 60 min, while the solar photo-Fenton process without Fresnel lens remained a  $TU_{50}$  value of 1.116.

# 4. Conclusion

With the assistance of Fresnel lens, the efficacy of solar photo-Fenton process enhanced considerably in terms of the COD degradation rate, mineralization rate, and biodegradability of color filter wastewater. In addition, the  $TU_{50}$  value of wastewater was almost diminished after a 60 min of treatment, whereas the microtoxicity of treated wastewater

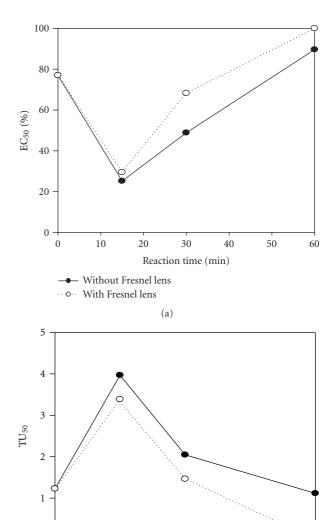


FIGURE 5: Effect of Fresnel lens on the microtoxicity of color filter wastewater in solar photo-Fenton process (initial pH: 5.0;  $H_2O_2/COD = 1.25 \text{ g/g}$ ;  $[H_2O_2]_0/[Fe^{2+}]_0 = 15$ ).

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Reaction time (min)

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60

without the assistance of Fresnel lens remained a  $TU_{50}$  value of 1.166. This could be mainly due to the concentrated effect of Fresnel lens for solar energy, resulting in an increase of  $2{\sim}3$  times of solar light intensity and a raising heat irradiation in terms of  $15{\sim}30^{\circ}\mathrm{C}$  of wastewater temperature. Accordingly, solar energy could be concentrated effectively by using Fresnel lens and showed a significant promoting effect on the performance of solar photo-Fenton process for treating color filter wastewater.

# Acknowledgment

0

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Without Fresnel lens
 With Fresnel lens

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