# Environmental Photocatalysis 2013

Guest Editors: Jiaguo Yu, Christos Trapalis, Pengyi Zhang, Guisheng Li, and Huogen Yu





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## **Editorial**

# **Environmental Photocatalysis 2013**

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Semiconductor photocatalysis has caused enormous attention in recent year and has been demonstrated to be one of the "green" and effective methods for water and air purification, water disinfection, hazardous waste remediation, antibacterial, and self-cleaning. However, owing to low photocatalytic efficiency, the environmental applications of various photocatalytic materials and technologies are still very limited. Thus, more improvement and investigations are highly required from the viewpoint of practical use.

This special issue contains 20 papers, which are mainly related to pollutant degradation and environmental purification. Among them, 10 papers are related to composite of two semiconductors including TiO<sub>2</sub> and other semiconductors, 4 papers deal with fabrication of new photocatalytic materials, 2 papers are about doping of TiO<sub>2</sub>, and 4 papers are devoted to immobilization of TiO<sub>2</sub>. Furthermore, there are 13 papers devoting degradation of pollutant in water, 4 papers on air purification including decomposition of formaldehyde, NO and benzene, 2 papers related to hydrogen production, and 1 paper dealing with bactericidal activity of TiO<sub>2</sub>. We would like to express our sincere thanks to all the authors for submitting their interesting works to this special issue. A brief summary of all 20 accepted papers is provided as follows.

In "A cost-effective solid-state approach to synthesize  $g-C_3N_4$  coated  $TiO_2$  nanocomposites with enhanced visible light photocatalytic activity," the authors describe the

fabrication and photocatalytic performance of g- $\rm C_3N_4/TiO_2$  nanocomposites by a facile solid-state method using urea and commercial  $\rm TiO_2$  as precursors. The prepared nanocomposites exhibited enhanced absorption and photocatalytic performance for degradation of aqueous MB in visible light region.

The paper "Synthesis and characterization of pyrochlore  ${\rm Bi_2Sn_2O_7}$  doping with praseodymium by hydrothermal method and its photocatalytic activity study" reports preparation of Pr-doped  ${\rm Bi_2Sn_2O_7}$  (BSO) by a hydrothermal method. The photocatalytic activity of the prepared samples was evaluated by the degradation of rhodamine Bextra (RhB) and 2,4-dichlorophenol (2,4-DCP) in aqueous solution under visible light. Pr-doped BSO samples exhibited enhanced visible-light photocatalytic activity and the optimal dopant amount of Pr was determined to be 1.0 mol%.

The paper "Single step formation of C-TiO<sub>2</sub> nanotubes: influence of applied voltage and their photocatalytic activity under solar illumination" presents fabrication of self-aligned and high-uniformity carbon (C)-titania (TiO<sub>2</sub>) nanotube arrays by single step anodization of titanium (Ti) foil at 30 V for 1h. The photocatalytic activity evaluation of C-TiO<sub>2</sub> samples was performed by degradation of methyl orange (MO) solution. The results revealed that controlled nanoarchitecture C-TiO<sub>2</sub> photocatalyst led to a significant enhancement in photocatalytic activity.

The paper "Removal of formaldehyde using highly active Pt/TiO $_2$  catalysts without irradiation" describes preparation of TiO $_2$  supported Pt catalysts by sol-gel method and their application for eliminating formaldehyde (HCHO) at room temperature without irradiation. More than 96% of the conversion of HCHO was obtained over 0.5 wt% Pt/TiO $_2$ -H $_2$  sample, on which highly dispersed metallic Pt nanoparticles with  $\sim\!2$  nm were identified.

The paper "CTAB-assisted hydrothermal synthesis of Bi<sub>2</sub>Sn<sub>2</sub>O<sub>7</sub> photocatalyst and its highly efficient degradation of organic dye under visible-light irradiation" reported preparation of Pyrochlore-type Bi<sub>2</sub>Sn<sub>2</sub>O<sub>7</sub> (BSO) nanoparticles by a hydrothermal method assisted with cetyltrimethylammonium bromide (CTAB). The photocatalytic activity of the BSO assisted with CTAB was two times that of the reference BSO.

The paper " $H_2$  fuels from photocatalytic splitting of seawater affected by nano-TiO $_2$  promoted with CuO and NiO" described preparation and photocatalytic performance of nanostructured TiO $_2$  loaded with NiO (2.5%) and CuO (2.5%). The accumulated  $H_2$  yielded from the photocatalytic splitting of seawater containing oxalic acid (50 mM) as the sacrificial reagents on CuO/nano-TiO $_2$  was 8.53  $\mu$ mol/ $g_{cat}$  after the 5 h radiation. On the NiO/nano-TiO $_2$  photocatalyst, the  $H_2$  yield was relatively low (i.e., 1.46  $\mu$ mol/ $g_{cat}$ ).

In "Dynamic hydrogen production from methanol/water photo-splitting using Core@Shell-structured CuS@TiO $_2$  catalyst wrapped by high concentrated TiO $_2$  particles," core@shell-structured CuS@TiO $_2$  catalysts were prepared and the prepared samples exhibited a wide absorption range above 700 nm comparing with pure TiO $_2$ . Hydrogen evolution rate from methanol/water photo-splitting over the core@shell-structured CuS@TiO $_2$  photocatalyst was about 10-fold higher than pure CuS.

In "Enhanced visible light photocatalytic activity for  ${\rm TiO_2}$  nanotube array films by codoping with tungsten and nitrogen," a series of W, N codoped  ${\rm TiO_2}$  nanotube arrays (TNAs) with different dopant contents, were fabricated by anodizing, followed with hydrothermal treatment. W and N codoping successfully extended the absorption of TNAs into the whole visible light region and resulted in remarkably enhanced photocatalytic activity under visible light irradiation.

The paper "Kinetics study of photocatalytic activity of flame-made unloaded and Fe-loaded CeO<sub>2</sub> nanoparticles" reported preparation and enhanced photocatalytic activity of Fe-doped and undoped CeO<sub>2</sub> by flame spray pyrolysis method. Photocatalytic studies showed that Fe-doped CeO<sub>2</sub> sample exhibited higher activity than un-doped CeO<sub>2</sub> sample, with optimal 2.00 mol% of iron loading concentration.

The paper "Solar photocatalytic degradation of bisphenol A on immobilized ZnO or TiO<sub>2</sub>" reported the removal of bisphenol A (BPA) under simulated solar irradiation in the presence of either TiO<sub>2</sub> or ZnO catalysts immobilized onto glass plates. BPA degradation followed first-order reaction kinetics.

In "Supported zinc oxide photocatalyst for decolorization and mineralization of orange G dye wastewater under UV365 irradiation," a photocatalytic system by utilizing both cold cathode fluorescent light (CCFL) UV irradiation and steel

mesh supported ZnO nanoparticles in a closed reactor for the degradation of azo dye C.I. Orange G (OG) was reported. The ZnO-coated steel mesh can be repeatedly used over 10 cycles without significant loss of catalyst mass.

In "The multiple effects of precursors on the properties of polymeric carbon nitride," polymeric graphitic carbon nitride (g- $C_3N_4$ ) materials were prepared by direct pyrolysis of thiourea, dicyandiamide, melamine, and urea under the same conditions, respectively. The photocatalytic activity of the samples was evaluated by the removal of NO in gas phase under visible light irradiation. Considering the cost, toxicity, and yield of the precursors and the properties of g- $C_3N_4$ , the best precursor for preparation of g- $C_3N_4$  was melamine.

In "One-step synthesis of  ${\rm TiO_2/perlite}$  composites by flame spray pyrolysis and their photocatalytic behavior,"  ${\rm TiO_2/perlite}$  composites were prepared by facile one-step flame spray pyrolysis (FSP) route using titanium alkoxide (TIPO) and expanded perlite as Ti source and substrate, respectively. The porosity and the light absorbance of the  ${\rm TiO_2/perlite}$  composites were examined and their photocatalytic activity in NO oxidation was evaluated. The best photocatalytic activity of the composites was connected to almost equal anatase-rutile ratio and possible synergetic effect of the two  ${\rm TiO_2}$  phases.

The paper "Au/TiO $_2$  reusable photocatalysts for dye degradation" reported preparation of Nanogold-doped TiO $_2$  catalysts and their application in the photodegradation of dye pollutants. Au-doped systems showed very good photoactivity in the degradation of dye pollutants under UV irradiation as well as in sunlight.

The paper "Fabrication, modification, and emerging applications of  ${\rm TiO_2}$  nanotube arrays (TNAs) by electrochemical synthesis: a review" reviewed the recent progress of the new research achievements of TNAs on the preparation processes, forming mechanism, and modification. In addition, the authors also reviewed potential and significant applications in the photocatalytic degradation of pollutants, solar cells, water splitting, and other aspects. Finally, the existing problems and further prospects of this renascent and rapidly developing field were also briefly addressed and discussed.

In "Photocatalytic degradation of organic dyes by  $H_4SiW_6Mo_6O_{40}/SiO_2$  sensitized by  $H_2O_2$ ,"  $H_4SiW_6Mo_6O_{40}/SiO_2$  was sensitized by  $H_2O_2$  solution that significantly improved its catalytic activity under simulated natural light. The photodegradation of malachite green, methyl orange, methylene blue, and Rhodamine B were also tested, and the degradation rate of dyes reached 90%–98%.

In "Enhancement of photocatalytic activity on  ${\rm TiO_2}$ -nitrogen-doped carbon nanotubes nanocomposites,"  ${\rm TiO_2}$ -nitrogen-doped carbon nanotubes ( ${\rm TiO_2}$ -CNx) nanocomposites were successfully synthesized by a facile hydrothermal method.  ${\rm TiO_2}$ -CNx nanocomposites exhibited much higher photocatalytic activity than neat  ${\rm TiO_2}$  and  ${\rm TiO_2}$ -CNTs mechanical nanocomposites. The improved photodegradation performances were attributed to the suppressed recombination of electrons and holes caused by the effective transfer of photogenerated electrons from  ${\rm TiO_2}$  to CNx.

In "Effect of different calcination temperatures on the structural and photocatalytic performance of Bi-TiO $_2$ /SBA-15," the Bi-TiO $_2$ /SBA-15 composite was synthesized by an easy wet impregnation method. It was found that SBA-15 retained the ordered hexagonal mesostructure after incorporation of TiO $_2$  and Bi. The Bi-TiO $_2$ /SBA-15 composite exhibited higher photocatalytic activities than pure TiO $_2$  and Bi $_2$ O $_3$ .

The paper "Photocatalytic oxidation of gaseous benzene under 185 nm UV irradiation" reported that benzene removal efficiency of Photocatalytic oxidation (PCO) with 254 nm UV irradiation (denoted as 254-PCO) was only 2.1%, while it was greatly increased to 51.5% in 185-PCO. 185-PCO exhibited superior capacity for benzene oxidation. In the 185-PCO process, much ozone was left in case of  ${\rm TiO_2}$  as photocatalysts while it could be nearly eliminated by 1% Co-TiO<sub>2</sub>.

The paper "Bactericidal activity of  ${\rm TiO_2}$  on cells of pseudomonas aeruginosa ATCC 27853" presented the antibacterial effects of  ${\rm TiO_2}$  and light exposure (at 365 nm) on Pseudomonas aeruginosa ATCC 27853. Following 90 minutes exposure to  ${\rm TiO_2}$  and UV light, logarithm of cell density was reduced from 6 to 3.

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## Research Article

# Au/TiO<sub>2</sub> Reusable Photocatalysts for Dye Degradation

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Nanogold doped  ${\rm TiO_2}$  catalysts are synthesized, and their application in the photodegradation of dye pollutants is studied. The materials are characterized using different analytical techniques such as X-ray diffraction, transmission electron microscopy, UV-visible diffuse reflectance spectroscopy, and X-ray photoelectron spectroscopy. The results revealed the strong interaction between the metallic gold nanoparticles and the anatase  ${\rm TiO_2}$  support. Au doped systems showed very good photoactivity in the degradation of dye pollutants under UV irradiation as well as in sunlight. A simple mechanism is proposed for explaining the excellent photoactivity of the systems. The reusability studies of the photocatalysts exhibited more than 98% degradation of the dye even after 10 repeated cycles.

#### 1. Introduction

Even though dyes are classified as pollutants, they are widely applied in the textile manufacturing industries. The discharge of dyes causes soil as well as water pollution depending on its mode of disposal. In addition, since the dye stuffs are intentionally designed to resist aerobic oxidation by microorganisms, only partial degradation of dye molecules are possible with aerobes, and it results in the formation of volatile carcinogenic compounds. So the treatment of these dye effluents is highly desired for the preservation of clean air, soil, and water.

 ${
m TiO_2}$ , in the anatase form, is one of the best photocatalysts for pollutant degradation [1]. However, because of the relatively high intrinsic band gap of anatase  ${
m TiO_2}$  (3.2 eV), ultraviolet (UV) irradiation is required for its photoactivity [2, 3], and thus only 4% of the sunlight (UV fraction of solar spectrum) can be utilized effectively [4]. Thus, pure  ${
m TiO_2}$  based systems have been found to be inactive under sunlight. Application of UV lamps has serious disadvantages including high energy consumption and handling problems.

Keeping this in mind, researchers focused to develop  ${\rm TiO_2}$  based systems having decreased band gap so as to show photocatalytic activity in the visible region. This will enable the use of sunlight for photocatalysis [5]. Several modification methods are available to shift the wavelength of absorption of  ${\rm TiO_2}$  from UV to visible region, among which anion doping succeed in this matter [6–11]. Nitrogen is the widely studied anion dopant where the photoactivity of the N doped  ${\rm TiO_2}$  even arises by the presence of molecularly adsorbed  ${\rm N_2}$  [12]. Thus, the activity may decrease by storing the catalyst for long time.

The second main drawback associated with the photocatalytic activity of  ${\rm TiO}_2$  is that most of the activated charge carriers will undergo recombination before reaching the surface, preventing interaction with adsorbed molecules. In fact, 90% of the charge carriers may be lost within a nanosecond of their generation leading to low photoactivity of  ${\rm TiO}_2$  [13]. The high recombination rate of photogenerated electronhole pairs, which controls the photocatalytic efficiency of semiconductors, can be reduced by trapping the electrons with noble metals [14]. The noble metals such as Pt, Ag, and

Au, when deposited over  ${\rm TiO}_2$ , can act as electron traps, since they have the high Schottky barriers among the metals [15–19].

Our aim is to develop highly competent catalysts, which can prevent the recombination of charge carriers effectively, so that the photocatalysts can act well even by utilizing the UV light from the sun. In the present work, the surface doping of sol gel TiO<sub>2</sub> has been done with gold nanoparticles (AuNPs), with an aim to trap the electrons to prevent recombination. The selection of AuNPs as dopant was also based on its property of UV light absorption, causing the transition of 5d electrons to the 6sp band (interband transition) [20, 21]. It is also reported that due to the high photon energy, UV light is able to drive chemical reactions on AuNPs [22]. AuNP supported over zeolite, ZrO<sub>2</sub>, and SiO<sub>2</sub>, were found to be effective for the degradation of dye pollutant sulforhodamine-B [22]. The incorporation of nanogold over supports other than TiO<sub>2</sub> required high percentage loading of gold for its effective photocatalytic activity [22]. Thus, a combination of AuNP and TiO2 can lead to the formation of a cost effective photocatalyst.

In the present study, nanogold particles were doped over  ${\rm TiO_2}$  catalysts, using chloroauric acid as the gold precursor, by deposition-precipitation method.  ${\rm TiO_2}$  was prepared by sol-gel method. Highly dispersed gold nanoparticles with diameter less than 5 nm were found to be deposited over  ${\rm TiO_2}$ . All the  ${\rm TiO_2}$  based catalysts of the present study were found to exist in the anatase phase. The reaction parameters were varied in the degradation of methylorange (MO) for attaining best conditions for photocatalysis.

#### 2. Experimental

- 2.1. Preparation of Titania Support. Titania photocatalysts using titanium (IV) isopropoxide (Sigma Aldrich) as titanium precursor were prepared by sol-gel method with slight modifications from the reported procedure [23]. 0.0628 mol titanium (IV) isopropoxide and 0.8563 mol ethyl alcohol (Hamberg Chemicals), were mixed first. Then a mixture of 0.8563 mol ethyl alcohol, 0.2186 mol glacial acetic acid (R &M Chemicals) and 6.25 mL distilled water was added to the above solution. The resultant solution was stirred to get transparent titania sol. It was then aged for 2 days and dried in an air oven at 80°C. Ground into fine powder and calcination was done at 400°C for 5 h to obtain TiO<sub>2</sub> powder.
- 2.2. Preparation of Nanogold Doped Titania. For the preparation of nanogold,  $2.1 \times 10^{-3}$  M chloroauric acid (Sigma Aldrich) solution was used as the gold precursor, and NaOH (R&M Chemicals) was added to it under stirring so as to adjust the pH of the solution to 8. For nanogold doping over  $\text{TiO}_2$ , required amount of  $\text{TiO}_2$  powder was added to the freshly prepared nanogold solution where the pH of 8 was kept constant at 70°C, and the solution was stirred well for 2 hours. The mixture was filtered, and the residue was washed with distilled water to remove chloride ions. The nanogold incorporated  $\text{TiO}_2$  was dried at 80°C and calcined at 200°C for 5 h. The doped systems were designated as  $n\%\text{Au/TiO}_2$ ,

where n indicates the weight percentage of gold taken for doping over  $TiO_2$ .

- 2.3. Catalyst Characterization. XRD patterns of the samples were recorded for  $2\theta$  between 3 and  $80^{\circ}$  on a Bruker AXS D8 Advance diffractometer employing a scanning rate of  $0.02^{\circ}$ /S with Cu K $\alpha$  radiation ( $\lambda = 1.5418 \,\text{Å}$ ). Transmission electron microscopic (TEM) analyses were conducted using ZEISS LIBRA 200 electron microscope. XPS of 1.5%Au/TiO<sub>2</sub> sample was recorded with a SPECS spectrometer using nonmonochromatic AlKα source (1486.6 eV) run at 150 W (12 kV and 12.5 mA). Survey scan was obtained with 70 eV pass energy and high resolution scan of Ti 2p, O 1s and Au 4f with 40 eV pass energy. The binding energies reported here were calculated with reference to C 1s peak at 284.6 eV. Au 4f core level was curve fitted into several components with Gaussian-Lorentzian peaks after subtracting Shirley background. Diffuse reflectance Ultraviolet-visible spectroscopy (UV-vis DRS) of powder catalyst samples was carried out at room temperature using a Varian, Cary 5000 spectrophotometer in the range of 200 to 800 nm. Elemental composition of the prepared samples was determined by using Thermo Electron IRIS INTREPID II XSP DUO Inductively Coupled Plasma Atomic Emission Spectrometer (ICP-AES).
- 2.4. Photoactivity Measurements. The efficiency of the nanogold doped TiO<sub>2</sub> photocatalysts was examined by the photodegradation of dye pollutants in a Rayonet type Photoreactor (Associate Technica, India) having 16 UV tubes of 8W (HITACHI F8T5 8 WATT Hittach, Ltd., Tokyo, Japan) capacity. In a typical experiment, 50 mL of 10 mg/L of MO was placed in a quartz tube containing 3 g/L of catalyst and was irradiated with UV light under continuous stirring by air flow for 1h. The above mentioned conditions were used in all experiments unless otherwise mentioned. The MO concentration was analyzed using a Varian, Cary spectrophotometer by absorbance measurements at the wavelength of maximum absorption of MO (464 nm) before and after degradation. The reaction conditions such as catalyst weight (1 to 5 g/L), dye concentration (5 to 20 mg/L), irradiation time (30 to 120 min under sunlight and 15 to 90 min under UV light irradiation), weight percentage of gold over TiO2, and so forth were varied to find out the best condition for maximum photodegradation. The degradation studies were also conducted under different pH. Performance of 2%Au/TiO<sub>2</sub> in degrading different dyes in the selected conditions was also evaluated. Activity studies under sunlight were investigated using 1.5%Au/TiO<sub>2</sub>.

#### 3. Results and Discussion

3.1. Catalyst Characterization. XRD patterns of the undoped and AuNP doped samples in Figure 1 showed anatase as the only phase (major peak at  $2\theta = 25.5^{\circ}$ ), which is reported as the most photocatalytically active crystalline state of TiO<sub>2</sub> [24]. No peaks for gold are found to be present, indicating efficient dispersion of the inserted metal with dimensions lower than 5 nm [25]. TEM images shown in Figure 2 supported the

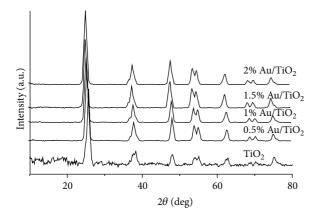


FIGURE 1: XRD patterns of the prepared photocatalysts.

above supposition. Well-dispersed gold nanoparticles, in the range of 2-3 nm diameters, appeared as black spots over the gray-coloured spherical particles of TiO<sub>2</sub>. Since AuNP over TiO<sub>2</sub> is having diameter less than 5 nm, it lies in the size range required for effective use of nanogold in catalysis [26]. The spherical shaped titania particles have diameters in the range of 15–25 nm. Anatase lattice fringes are visible, and the micrograms demonstrate that the particles are connected to each other to form a mesoporous crystalline framework [27].

The XPS spectrum of the representative sample, 1.5%Au/TiO<sub>2</sub>, was measured to elucidate the chemical state of Au and other species in the prepared samples. Figure 3 shows the wide scan spectra of the sample, and the spectra corresponding to Ti 2p, O 1s and Au 4f. From the high resolution spectra, it can be seen that the Ti 2p peaks appeared at binding energies (B.E.) of 458.7 (2p<sub>3/2</sub>) and 464.4  $(2p_{1/2})$ . The peak at 458.7 corresponds to titanium in pure anatase. Here, the energy splitting between Ti 2p<sub>1/2</sub> and Ti  $2p_{3/2}$  is 5.7 eV, which confirms the existence of titanium as  ${\rm Ti}^{4+}$  [28]. It is also reported that the position of the  ${\rm Ti}$   $2p_{3/2}$ component at 458.7 eV corresponds to the oxidation state of +4 of Ti in titanium dioxide [29, 30]. The O Is B.E. of the sample is located at 530.0 eV, which is assigned to bulk oxide (O<sup>2</sup>-) in the TiO<sub>2</sub> lattice. Therefore, it can be concluded that no obvious changes on the chemical state of Ti and O were caused by doped and deposited Au.

Au 4f XPS spectrum of 1.5%Au/TiO<sub>2</sub> sample exhibited peaks at the B.E. values of 83.6 and 87.1 eV for 4f<sub>7/2</sub> and 4f<sub>5/2</sub> electrons, corresponding to Au in the metallic state [31]. In addition, peaks arising from Au<sup>+1</sup> are observed at 84.8 eV (4f<sub>7/2</sub>) and 88.6 (4f<sub>5/2</sub>). It is depicted that 92% of Au exists in Au<sup>0</sup> state and 8% exists in its ionic state, Au<sup>+</sup>. This confirms the formation of nanogold, Au<sup>0</sup> on the TiO<sub>2</sub> surface. As per the reported data [32, 33], the doublet of Au<sup>0</sup> was centered at 84.0 and 87.7 eV. The decrease in the binding energies of Au 4f peaks in the present Au doped TiO<sub>2</sub> system may be due to the negative charge of the Au nanoparticles as a result of the charge transfer from the TiO<sub>2</sub> substrate as already reported [34]. The formation of negative charge of the Au nanoparticles may be due to the large difference in the work function of Au and TiO<sub>2</sub> which facilitates the

electron transfer from TiO<sub>2</sub> to Au [34]. The negative shift in comparison with bulk gold thus suggests the formation of a strong metal-support interaction [35] over the present catalyst. XPS analysis also confirmed the absence of any contamination from sodium and chlorine species (NaOH and HAuCl<sub>4</sub>), which were used during the doping process.

Two bands are observed in the UV-visible diffuse reflectance spectra of Au doped TiO<sub>2</sub> samples (Figure 4). The intense band with absorption maxima around 320 to 350 nm is associated to the O<sup>2-</sup>-Ti<sup>4+</sup> charge-transfer, corresponding to the electronic excitation from the valence band to the conduction band [36]. In the case of undoped TiO<sub>2</sub>, this band is found to be highly intense, which may be a result of the presence of greater number of Ti4+ ions and consequently a greater number of Ti<sup>4+</sup>-O<sup>2-</sup> bonds [37]. Gold doping decreases the intensity of this band, which can be due to the interaction between Au nanoparticles with the TiO<sub>2</sub> support [38]. The metal-support interaction is already suggested from the interpretation of XPS results. A slight red shift of the above band is observed upon gold doping. The shift may be due to the insertion of metal ions into the TiO<sub>2</sub> at substitutional sites [39]. XPS analysis revealed the presence of a minor percentage of Au<sup>+</sup> in the representative sample, 1.5%Au/TiO<sub>2</sub>, supporting this possibility. Nanogold doped samples show the presence of a comparatively less intense band with  $\lambda_{\rm max}$  in the region of 540-570 nm. This band can be attributed to the surface plasmon resonance of Au, which arises from the collective oscillations of the free conduction band electrons that are induced by the incident electromagnetic radiation [40, 41].

The elemental analysis results of representative samples, 1%Au/TiO<sub>2</sub>, 1.5%Au/TiO<sub>2</sub>, and 2%Au/TiO<sub>2</sub>, reveals the inserted Au contents as 0.074 wt%, 0.182 wt%, and 0.225 wt%, respectively. Increase in the amount of gold precursor in the preparation showed an increase in the amount of metal incorporated over TiO<sub>2</sub>. The incorporated amount was less than the amount of gold taken, which may be due to the loss of unbound nanogold while washing the catalysts with distilled water during the preparation.

3.2. Photocatalytic Activity. The activity of the different systems under visible light was investigated, and it was found that the photocatalysts were not active under visible light. But the experiments under UV irradiation were satisfactory in the degradation of MO. The reaction parameters were varied to get best results.

Figure 5 describes the effect of reaction conditions on the performance of the catalyst. Initial steep rise in photodegradation capacity is observed with increase in the amount of catalyst weight, which then attains saturation at a catalyst dosage of 3 g/L. Thus a catalyst weight of 3 g/L (0.15 g) was selected for further studies. The dye concentration is varied, and from the results, it is observed that the catalyst showed 100% degradation of the dye pollutant at low concentrations. The activity decreased from an increased dye concentration of 15 mg/L onwards as seen from the data shown in Figure 5(b). We also varied the pH of the solution, since the dye pollutant effluent from the industry may be of different pH. The

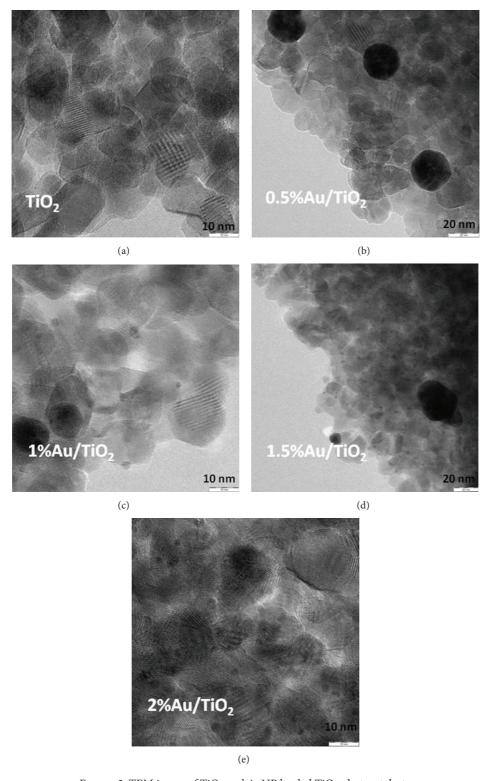
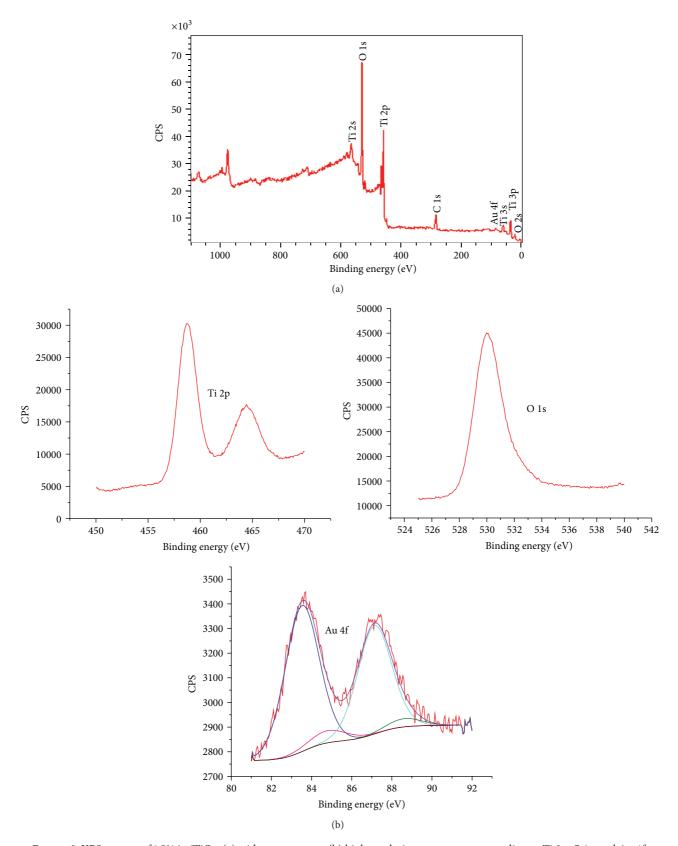


Figure 2: TEM image of  $\mathrm{TiO}_2$  and AuNP loaded  $\mathrm{TiO}_2$  photocatalysts.

catalysts worked well in lower pH values till the natural pH of the solution. Under basic pH, activity is reduced and the percentage dye degradation decreased to 84.9% at a high pH value of 11. Still, the activity is better since the percentage

dye degradation is more than 80% as observed in the results shown in Figure 5(c).

The percentage of gold doping over  ${\rm TiO_2}$  is varied to attain maximum photoactivity, and the dye degradation is



 $FIGURE \ 3: XPS \ spectra \ of \ 1.5\% Au/TiO_2: (a) \ wide \ scan \ spectra, (b) \ high \ resolution \ spectra \ corresponding \ to \ Ti \ 2p, O \ 1s, and \ Au \ 4f.$ 

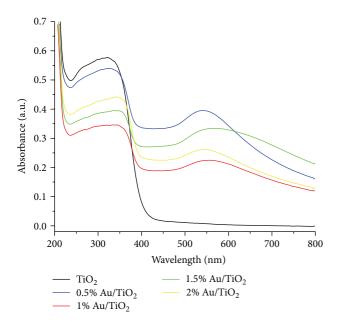


FIGURE 4: UV-visible diffuse reflectance spectra of Au doped  ${\rm TiO_2}$  samples.

monitored. Incorporation of gold increases the activity of  ${\rm TiO_2}$  drastically, which again moves up with increase in the amount of gold. Both 1.5% and 2 wt% AuNP doped systems gave 100% degradation of 50 mL, 10 mg/L MO dye over 3 g/L catalyst for 2 h exposure to UV light. In order to recognize the best Au doping, the time of UV irradiation was changed to 1 h, where  $2\%{\rm Au/TiO_2}$  provided the complete dye degradation. The results given in Figure 5(d) suggest  $2\%{\rm Au/TiO_2}$  as the best photocatalyst of the present investigation.

Reusability of the catalyst is one of the most projected attractions of any heterogeneous catalyzed reaction, but only limited experiments are there on the reusability studies of powder photocatalysts [42, 43]. This may be due to the difficulties in separation of the catalyst powder after pollutant degradation and may also be due to the low reusability of the catalysts. Present catalysts are easily separable from the solution and also well dispersible under stirring. It is simple to detach the catalyst from the cleaned solution either by filtration or by centrifugation. There was no permanent adsorption of dye over the catalyst, and the cleaning merely arises from photodegradation. Regeneration of the best catalyst, 2%Au/TiO<sub>2</sub>, was done after each reaction, by centrifugation, washing with water, and further treatment at the calcination temperature of the catalyst, that is, at 200°C, for 1h. The photocatalytic activity of the nanogold doped titania remains intact even up to ten consecutive experiments under the selected reaction conditions (Figure 6). The performance of the 2% Au/TiO<sub>2</sub> in the degradation of a number of dye pollutants was also tested where the activity is found to be admirable. The results are given in Table 1.

The excellent activity of the present nanogold loaded  ${\rm TiO_2}$  photocatalysts under UV light pinched us to test its ability to harvest the UV present in the sunlight. The photoactivity was also evaluated by the direct use of sunlight that may

Table 1: Photodegradation of aquatic dye pollutants over Au NP doped TiO<sub>2</sub>.

Dyes	% Degradation
Methylorange	100.00
Crystal violet	98.63
Methylene blue	95.30
Malachite green	100.00
Orange II	99.05
Acid blue	94.69

immediately turn the attention of industries for pollutant treatment. Akbarzadeh et al. had reported vanadium doped TiO<sub>2</sub> systems that are effective under sunlight where the catalyst used both UV and visible spectra of the sunlight for photoactivity [44]. The 0.5% vanadium doped TiO<sub>2</sub> showed 53.99% degradation of methyleneblue after 1h irradiation. Present AuNP doped TiO<sub>2</sub> displayed very good activity under sunlight where more than 80% of the methylorange dye is degraded within 1h and degradation reached around 93% by 2h exposure to sunlight over 1.5%Au/TiO<sub>2</sub>. The use of UV radiation of sunlight for the photocatalytic degradation is investigated in our experiments. When the reaction is conducted under sunlight using glass tubes instead of quartz tubes, the activity dropped drastically. Glass is opaque to UV light and that may be the reason for decreased activity which suggests the use of UV light for degradation. The degradation data of MO under sunlight over 1.5%Au/TiO<sub>2</sub> with time is presented in Figure 7(a). The degradation results under UV lamps are also offered for comparison in Figure 7(b).

3.3. Proposed Mechanism of Photodegradation. The plausible reaction mechanism for the photodegradation of dyes over nanogold doped TiO<sub>2</sub> under UV irradiation is suggested here. Upon UV irradiation, the electrons present in the valance band (VB) get promoted to the conduction band (CB) since the band gap of TiO<sub>2</sub> lies in the UV region [45–47]. In the CB, the electrons can be further transferred to the adsorbed O<sub>2</sub> on the surface of TiO<sub>2</sub> to form the superoxide radical anions, O<sub>2</sub> [48, 49]. In addition, in the case of metal nanoparticle doped TiO2, the metal nanoparticles can be considered as an electron sink, where the electrons in the conduction band can migrate to the noble metal surface, thereby preventing the recombination of electronhole (e<sup>-</sup>-h<sup>+</sup>) pairs [40, 45]. Thus the migration of electrons from the interior of the photocatalyst to the metal surface results in increased photoquantum efficiency, which can be the reason for the excellent photoactivity for the present nanogold doped systems even by using low intensity UV present in the sunlight. The transferred electrons in the metal surface facilitate the formation of oxygen superoxide radical anion. In the VB, the holes interact with water molecules, resulting in the formation of hydroxyl radical (OH) and proton. Protonation of the superoxide anion, O<sub>2</sub>•-, creates OOH radicals which leads to the formation of H2O2 and

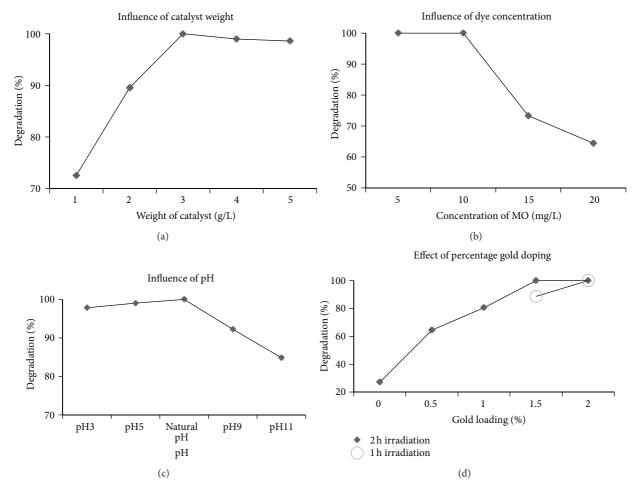


FIGURE 5: Influence of reaction conditions on photodegradation of methylorange over different photocatalysts.

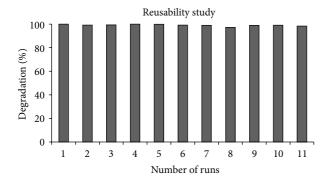


FIGURE 6: Reusability data over 2%Au/TiO<sub>2</sub> in the degradation of 50 mL of 10 mg/L MO, over 3 g/L catalyst, for 1 h irradiation under UV.

finally \*OH radical [50]. These \*OH radicals are responsible for the degradation of dye molecules. The presence of \*OH radicals for photoactivity is already confirmed in previous reports [50–53]. Thus it can be understood that insertion of AuNP as well as increase in the amount of inserted nanogold particles can increase the photoactivity of TiO<sub>2</sub> significantly. Increase in the number of AuNPs over the support can lead

to the enhanced migration of electrons from the CB of  ${\rm TiO_2}$  to the Au surfaces which promotes the electron transfer to the adsorbed  ${\rm O_2}$  molecules [54, 55]. This will facilitate the formation of more number of  ${\rm O_2}^{\bullet-}$  and finally can lead to the formation of more number of  ${}^{\bullet}{\rm OH}$  which is responsible for dye degradation. This explains the observed increase in the dye degradation over the present photocatalysts with an increase in the percentage gold doping. The mechanism of photodegradation is schematically represented in Figure 8.

#### 4. Conclusions

Highly efficient photocatalysts were prepared by nanogold doping over sol-gel  ${\rm TiO_2}$ . XRD patterns show the exclusive existence of anatase crystalline phase of  ${\rm TiO_2}$ . Majority of the incorporated gold exists in its metallic state, where the particles have diameters less than 5 nm. The strong interaction between the Au and the support, as evident from the characterization of the materials, leads to enhanced photocatalytic activity. The gold nanoparticles act as effective trapping centres to prevent recombination of electron-hole pairs, making the catalysts even active under sunlight for the efficient degradation of pollutants. Another attractiveness of

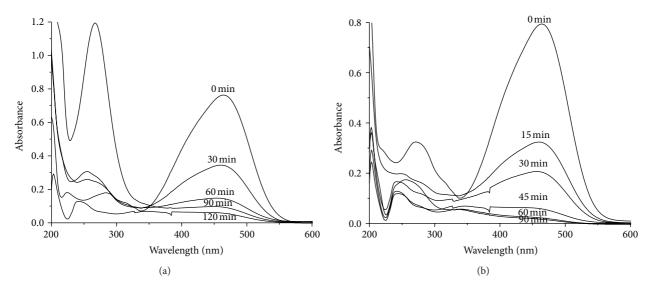


FIGURE 7: (a) Degradation of 10 mg/L MO under sunlight over 3 g/L of 1.5%Au/TiO<sub>2</sub>. (b) Degradation of 10 mg/L MO under UV irradiation over 3 g/L of 2%Au/TiO<sub>2</sub>.

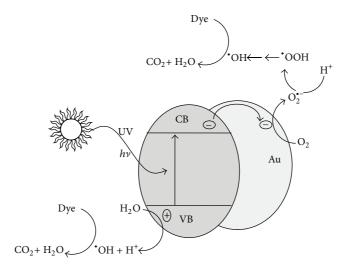


FIGURE 8: Plausible mechanism of photodegradation of dyes over AuNP doped TiO<sub>2</sub>.

the present photocatalysts lies in their easy separation from the cleaned solution and reusability.

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## Research Article

# One-Step Synthesis of TiO<sub>2</sub>/Perlite Composites by Flame Spray Pyrolysis and Their Photocatalytic Behavior

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 ${\rm TiO_2/perlite}$  composites were prepared via facile one-step flame spray pyrolysis (FSP) route. Titanium alkoxide (TIPO) and expanded perlite were used as Ti source and substrate, respectively. Precursor TIPO-ethanol solutions containing homogeneously dispersed perlite particles were processed through FSP setup at different experimental conditions regarding the gas flow and precursor supply rates. The structure, morphology, and the composition of the obtained powders were investigated. The porosity and the light absorbance of the  ${\rm TiO_2/perlite}$  composites were examined and their photocatalytic activity in NO oxidation was evaluated. Commercial titania powder P25 was also FSP processed and investigated for comparison. The XRD analysis revealed that biphased titania with different anatase-rutile ratio and particles size 20–40 nm was synthesized onto the perlite which according to microscopy results was covered by neck-connected  ${\rm TiO_2}$  nanoparticles. The anatase-rutile interplay was also demonstrated by the Raman spectra where presence of Si-O-Ti vibrational modes was observed for some samples. The UV-Vis diffuse reflectance spectra of the  ${\rm TiO_2/perlite}$  composites revealed up to 70% reflection that was connected to the presence of the gray perlite and superficial carbon. The best photocatalytic activity of the composites was connected to almost equal anatase-rutile ratio and possible synergetic effect of the two  ${\rm TiO_2}$  phases.

#### 1. Introduction

The  ${\rm TiO_2}$  semiconductor is one of the most investigated materials during the last years.  ${\rm TiO_2}$  nanoparticles are used nowadays in an enormous spectrum of applications such as solar cells [1], gas sensors [2], photochromic devices [3], superhydrophilic surfaces [4] and photocatalysts [5]. The above applications are related to the three different crystalline phases of  ${\rm TiO_2}$ , anatase, rutile, and brookite [6]. Both anatase and rutile crystal structures are commonly used as photocatalysts with anatase showing a greater activity for most photocatalytic processes. This is attributed to anatase's slightly higher Fermi level, its lower capacity to adsorb oxygen, and its higher degree of hydroxylation [7, 8]. There are also studies which claim that a synergetic effect occurs and a mixture of anatase and rutile is more active than pure anatase [9]. The

enhanced activity arises from the increased efficiency of the electron-hole separation due to the multiphase nature of the photocatalyst [10].

Various procedures are established for producing photocatalyst particles such as chemical vapour deposition [11], precipitation [12, 13], sol-gel methods [14], and hydrothermal synthesis [15–18].

The last one is a fast, profitable, and flexible process for the production of a wide variety of different nanoparticles [19]. In this process, flame is being used to drive chemical reactions of precursor compounds [20–26], resulting in the formation of clusters, which grow to nanometer-sized products by coagulation and sintering. In particular,  $\text{TiO}_2$  or  $\text{TiO}_2$ -containing composite systems were studied by flame spray pyrolysis such as  $(\text{TiO}_2)_x(\text{Al}_2\text{O}_3)_{1-x}$  [20],  $\text{Au}/\text{TiO}_2$  [21],

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 $\label{eq:continuous} \begin{array}{lll} Pt/TiO_2, & Fe/TiO_2 & [22], & V_2O_5/TiO_2 & [23], & Cr/TiO_2 & [24], \\ Ag/TiO_2 & [25], & and & SiO_2/V_2O_5/WO_3/TiO_2 & systems & [26]. \\ \end{array}$ 

There are several works investigating deposition of TiO<sub>2</sub> nanoparticles on various surfaces such as polymeric matrices [27], graphene oxide [28], carbon fibers [29], clays [30], and layered double hydroxide LDH [31-33]. Systems of nanosized TiO2 with highly adsorptive supports enhance the performance of the photocatalysts due to larger specific area, porosity, and higher adsorption capacity in comparison to the bare TiO<sub>2</sub>. Support limits the aggregation of TiO<sub>2</sub> nanoparticles, induces the microporosity into the materials [31], and contributes to the efficient spatial separation between the photogenerated electrons and holes. Glassy substrates were also used for deposition of TiO2 photocatalysts [34-37]. Such a glassy substrate is the perlite which is a natural amorphous material widely used in construction and industry. The use of natural perlite in blended cement production was investigated and the results revealed that perlite possesses sufficient pozzolanic characteristics [38]. Its average chemical composition is approximately 75% SiO<sub>2</sub> with oxides of Al (14.8%), K (4.8%), Na (2.9%), Ca (0.9%), Mg(0.1%),  $Fe_2O_3(1.5\%)$ , and water (4.0%) [39]. Crude perlite particles expand after heating to 870°C due to the presence of water and form innumerable sealed glassy cells in a manner similar to popcorn. These account for the excellent insulating properties and light weight of the expanded perlite. Being highly porous and chemically inert media, perlite granules can act as a good adsorbent. Therefore, expanded perlite can be selected as substrate for TiO<sub>2</sub> particles.

TiO<sub>2</sub>/perlite composites prepared by various experimental methods were investigated aiming at enhanced photocatalytic activity in water and air decontamination. Thus, the TiO<sub>2</sub>-coated perlite granules were prepared using sol-gel method and tested for photocatalytic purification of furfural polluted waste water [40]. Also, TiO<sub>2</sub> (Evonik-Degussa P25) immobilized on different supports (perlite granules, glass plates, and steel fiber) by sol-gel and investigated their photocatalytic oxidation of phenol [41]. The preceding works on TiO<sub>2</sub>/perlite composite materials used mainly wet chemistry to immobilize the photocatalyst onto the substrate. To the best of our knowledge, there is only one report on preparation of Ag-coated perlite by the spray pyrolysis method in order to obtain a catalyst for ozone decomposition using a cheap natural glass as substrate [42].

In this paper we present for the first time the onestep synthesis of the  ${\rm TiO_2/perlite}$  composites by flame spray pyrolysis (FSP) processing. The structural and the morphological properties of the prepared materials as well as their photocatalytic performance in air pollutants oxidation are examined.

#### 2. Experimental

2.1. Precursor Materials. The expanded perlite was provided by S&B Industrial Minerals S.A. to be used as a support for deposition of TiO<sub>2</sub> nanoparticles. Perlite was ground in a planetary mill for 2 h in order for fine granules to be obtained.

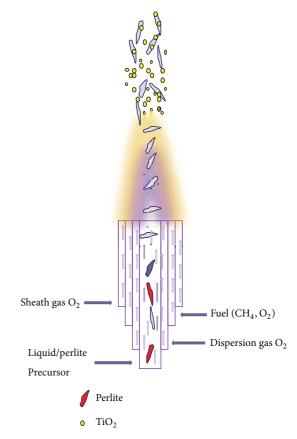


Figure 1: Schematic of the flame spray pyrolysis device. During spray procedure and after evaporation and combustion of precursor,  ${
m TiO_2}$  nanoparticles are formed on perlite substrate.

The  ${\rm TiO_2/perlite}$  composite materials were prepared as follows. Initially, 5 mL titanium isopropoxide (TIPO), Aldrich 97%, was dissolved in 40 mL ethanol, Carlo Erba, and stirred for 30 min. Then, 5 g perlite was added and the dispersion was stirred for 60 min. The mixture was further homogenized using an ultrasound tip sonicator (Hielscher UIP 1000 hd). Total energy input of 1 Wh was applied for sonication time for 2 min. Finally, the slurry was diluted with ethanol to receive 100 mL suspension and the liquid obtained was nominated as precursor solution (PS). The prepared PS was ready to be processed through the flame spray pyrolysis system. It should be noted that water was not used in order to avoid hydrolysis.

2.2. Flame Spray Pyrolysis Device. A homemade FSP setup was used to synthesize  ${\rm TiO_2/perlite}$  composites. In Figure 1 the schematic of the experimental set-up is shown. The FSP reactor consisted of four stainless steel concentric tubes. The PS was fed by a syringe pump (Inotec, IER-560) through the innest capillary tube (i.d. 0.8 mm). Oxygen was used as dispersion gas fed through the surrounding annulus (i.d. 2.5 mm, o.d. 3.0 mm) with a pressure drop of 1.5 bar and a rate in the range of  $10-20\,{\rm L\,min}^{-1}$ .

The resulting spray was ignited by a circular premixed flame (i.d. 17.0 mm, o.d. 19.7 mm) of  $CH_4$  (1.5 L min<sup>-1</sup>) and  $O_2$  (3.2 L min<sup>-1</sup>). An additional  $O_2$  sheath flow (20–40 L min<sup>-1</sup>)

Samples	Dispersion flow rates L min <sup>-1</sup>	Sheath flow rates L min <sup>-1</sup>	Syringe pump rates mL min <sup>-1</sup>	$d_A \atop  ext{nm}$	$d_R$ nm	$W_{A}$ (%)	W <sub>R</sub> (%)
P25				20	27	85	15
FSPA	14.0	20.0	12.0	24	30	48	52
FSPB	19.0	28.9	10.0	29	42	72	28
FSPC	17.3	38.8	12.0	27	31	70	30
FSPD	10.9	55.0	10.0	30	28	55	45

Table 1: Anatase ( $W_A$ %) and rutile ( $W_R$ %) compositions, crystallite sizes ( $d_A$  and  $d_R$ ) under different sheath, dispersion oxygen fractions, and syringe pump flow rates.

for complete combustion of the precursor was supplied through a sinter metal ring (i.d. 30 mm, o.d. 38 mm). In this paper, the total  $\rm O_2$  flow rate represents the sum of dispersion and sheath  $\rm O_2$  supply. The gas flow rates were regulated by calibrated mass flow controllers (Bronkhorst EL-Flow). The PS was processed through the FSP and the resulting powders were collected on glass microfiber filters (Whatman GF/D, 257 mm diameter) with the aid of a vacuum pump. Different  $\rm TiO_2/perlite$  samples were prepared by variation of the experimental conditions, namely, the gas flow rates (dispersion and sheath) and the syringe pump rate for the PS supply. Table 1 summarizes the above parameters used during the FSP process as well as the fraction of anatase and rutile phases of the flame made samples.

2.3. Characterization of  $TiO_2/Perlite$  Composites. The XRD patterns of the samples were obtained by X-ray diffractometer (SIEMENS D500) with secondary graphite monochromator and CuKa radiation operating in Bragg-Brentano geometry. The measured  $2\theta$  range between  $10^\circ$  and  $90^\circ$  was scanned in steps of  $0.03^\circ/2$  s. The accelerating voltage and applied current were  $40\,\mathrm{kV}$  and  $35\,\mathrm{mA}$ , correspondingly. The crystalline phases were identified with reference to the PDF cards of the International Centre for Diffraction Data. The average crystallite sizes of the anatase and rutile phases were determined from the intensities of the primary peaks of anatase (101) reflection at  $2\theta_B = 25.3^\circ$  and rutile (110) reflection  $2\theta_B = 27.5^\circ$  using the Scherrer relation [43] as follows:

$$d(\text{nm}) = \frac{0.89 \times \lambda}{B(\text{rad})\cos\theta_{\text{B}}},$$
 (1)

where  $\lambda = 0.15418$  nm is the X-ray wavelength, B (rad) is the full width at the half maximum of the diffraction peak, and  $\theta_{\rm R}$  is the Bragg angle.

Since only the anatase and rutile phases are present in the examined  ${\rm TiO_2/perlite}$  composites, the weight content of these phases was derived from the area of the corresponding peak after the background substraction using (2) [44] as follows:

$$W_R(\%) = \frac{S_R}{0.886 \times S_A + S_R},$$

$$W_A(\%) = 100 - W_R(\%),$$
(2)

where  $S_R$  and  $S_A$  are the surfaces of the primary rutile (110) and anatase (101) peaks, correspondingly.

TABLE 2: Measured BET SSA of the TiO<sub>2</sub>/perlite composites and calculated SSA of their TiO<sub>2</sub> component with respect to the total oxygen flow rate.

Samples	SSA <sub>COMP</sub> m <sup>2</sup> /gr	SSA <sub>TiO2</sub> m²/gr	O <sub>2</sub> flow rate L min <sup>-1</sup>
FSPA	20.0	55.6	34.0
FSPB	20.2	48.4	47.9
FSPC	19.4	53.4	56.1
FSPD	12.8	51.1	66.0

The specific surface areas (SSA) of the powders were determined via Brunauer-Emmett-Teller (BET) method. Standard device Sorptomatic 1990 FISONS was used for the nitrogen adsorption/desorption measurements at 77° K. All the samples were degassed at 453° K for 12 h. Assuming spherical and unagglomerated particles, the SSA of the TiO<sub>2</sub> nanoparticles (SSA<sub>TiO<sub>2</sub></sub>) was calculated from the average particle diameter estimated by XRD spectra,  $d^{\text{XRD}}_{A(R)}$ , and the weighted density of the particles  $\rho_{A(R)}$  (anatase:  $\rho_A = 3.84 \, \text{gr/cm}^3$ , rutile:  $\rho_R = 4.26 \, \text{gr/cm}^3$ ) by (3) as follows:

$$SSA_{A(R)} = \frac{6}{\left(\rho_{A(R)} \times d^{XRD}_{A(R)}\right)}.$$
 (3)

The  $SSA_{TiO_2}$  was calculated taking into account the mass fraction of anatase and rutile phases. The BET measured SSA of  $TiO_2$ /perlite composites ( $SSA_{COMP}$ ) and the calculated  $SSA_{TiO_2}$  are presented in Table 2.

The structural properties of the prepared composite materials were examined by Raman spectroscopy. The Raman spectra were measured with an inVia Raman microscope (Renishaw) using the 514.5 nm line of Ar+ laser emission with a resolution of 1.1 cm<sup>-1</sup>. The laser power was 50 mW as an output and Raman emission signal at each measurement point was accumulated for 20 s for all samples.

UV-Vis diffuse reflectance of the powders in the wavelength range  $350-800\,\mathrm{nm}$  as obtained using UV-2100 Shimadzu instrument. The measurements were performed using BaSO<sub>4</sub> etalon as a baseline.

The morphology of the powders was observed using scanning electron microscopy (SEM). An FEI Inspect microscope with tungsten filament operating at 25 kV was employed. In order to improve the surface conductivity of the samples standard gold deposition was applied through vacuum evaporation.

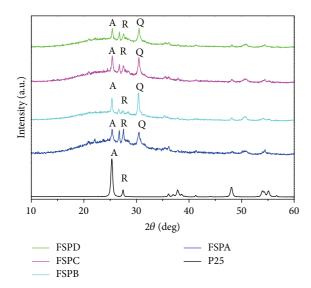


FIGURE 2: XRD patterns of  ${\rm TiO_2/perlite}$  correspond to the (101) reflection of the anatase and to the (110) of the rutile. For comparison, the XRD pattern of Degussa P25 is presented.

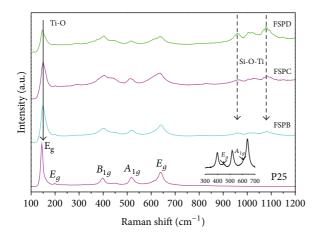


FIGURE 3: Raman spectra of samples P25, FSPB, FSPC, and FSPD.

The samples were also investigated using transmission electron microscopy (TEM). An FEI CM20 microscope operated at 200 kV was used. The samples for TEM observation were prepared as follows. Small amounts of the studied photocatalysts were dispersed in ethanol and the suspensions were treated in ultrasonic bath for 10 min. Then, a drop of the dilute suspension was placed on a carbon-coated grid and was allowed to dry by evaporation at ambient temperature.

Nitric oxide (NO) was chosen as representative airborne pollutant due to its potential health risks and ability to generate photochemical smog. The photocatalytic oxidation of NO by the prepared TiO<sub>2</sub>/perlite composite materials was investigated employing standard procedure based on ISO/DIS 22197-1 [45]. The experimental set-up, the procedures of specimens' preparation, and photocatalytic activity measurement are described elsewhere [46–49]. Briefly, the samples were placed in a flow-type photoreactor where model air containing 1 ppm NO was issued. Flow rate of 3 L/min

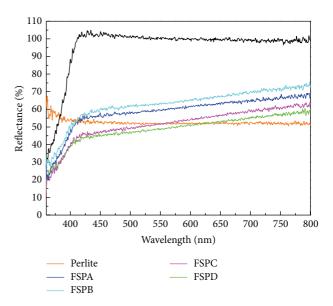


FIGURE 4: Diffuse reflectance spectra of TiO<sub>2</sub>/perlite samples.

and relative humidity of 50% were retained during the experiment. UV-A light illumination with intensity  $10 \, \text{W/m}^2$  for 90 min was applied. The concentrations of the NO, NO<sub>2</sub>, and NO<sub>x</sub> (NO<sub>x</sub> = NO – NO<sub>2</sub>) were monitored in dark and under illumination. The photocatalytic activity of the samples was expressed by the calculated photonic efficiency  $\zeta$  (mole/einstein) in NO and NO<sub>2</sub> oxidation as well as in NO<sub>x</sub> removal for the entire illumination period.

#### 3. Results and Discussion

The measured XRD patterns of the prepared materials are shown in Figure 2. It can be observed that the samples were crystallized in the form of anatase and rutile. The position and the relative intensities of the peaks are consistent with the anatase TiO2 JCPDS card number 21-1272 and rutile TiO<sub>2</sub> JCPDS card number 21-1276. The average crystallite size obtained from the most intensive diffraction peaks (101) and (110) at  $2\theta = 25.28^{\circ}$  and  $2\theta = 27.45^{\circ}$  ranged between 20 and 30 nm for anatase phase and 27 and 42 nm for rutile phase, respectively (Table 1). Also, a broadened bump in the  $2\theta$  range from 20° to 35° was observed originating from the amorphous nature of perlite. In the same time, the diffraction peaks (100), (101) and (110) were attributed to evident partial crystallization of the perlite during the flame processing procedure. The broadened part and quartz peaks are absent in the sample FSPA, which consist of P25 Degussa only. Finally, the interplay between the anatase and rutile phases in the composites (Table 1) is influenced by the PS and total O<sub>2</sub> flow rates [50], but the clear tendency in its behavior cannot be determined from our experiments.

In previous papers, it was demonstrated that the SSA of the particles decreased with the increase of the precursor flow rate [51, 52] as well as with the increase of the oxygen flow rate [23]. Higher precursor flow rate provokes higher frequency of the particle collision and sintering due to higher

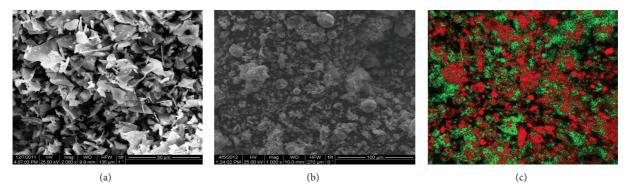


FIGURE 5: Scanning electron microscopy (SEM) micrographs of pure perlite (a), composite TiO<sub>2</sub>/perlite (b), and elemental mapping for the FSPD sample using energy dispersive spectroscopy (c). Red colour corresponds to Si and green to Ti.

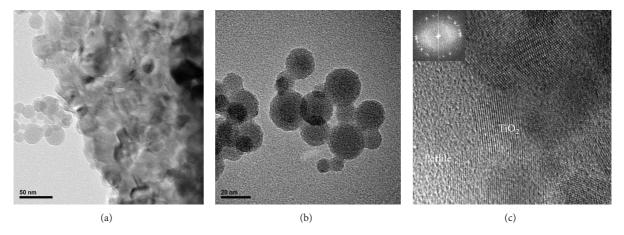


FIGURE 6: TEM micrographs of the composite TiO<sub>2</sub>/Perlite (a), TiO<sub>2</sub> nanoparticles (b), and HRTEM image of TiO<sub>2</sub>/Perlite (c).

concentration of the forming powder in the flame. Also, higher oxygen flow rate leads to higher flame temperature encountered by the particles. As a result, the enlargement of particle size and reduction of their SSA were observed in both cases.

The BET measured SSA of the composites (SSA $_{\rm COMP}$ ) and the calculated SSA of TiO $_2$  particles (SSA $_{\rm TiO}$ ) as well as total oxygen flow rate used in our experiments are given in Table 2. It can be perceived that the SSA $_{\rm COMP}$  is lower than SSA $_{\rm TiO}$ . This can be explained by mixing of photocatalytically active TiO $_2$  component with porous but lower SSA perlite substrate. In addition, given that the precursor flow rate does not vary considerably, it seems that both SSA values decrease with the increase of the oxygen flow rate. This correlates with the literature results mentioned above.

The Raman spectra of the investigated composites as well as of the reference P25 sample are given in Figure 3.

The presence of the two anatase and rutile phases demonstrated by the XRD results above and their alteration can be observed also for the prepared composites. Thus, the Raman lines of the anatase phase [53] at  $144\,\mathrm{cm}^{-1}$  ( $E_g$  mode),  $197\,\mathrm{cm}^{-1}$  ( $E_g$  mode),  $399\,\mathrm{cm}^{-1}$  ( $B_{1g}$  mode),  $515\,\mathrm{cm}^{-1}$  ( $A_{1g}$  mode), and  $639\,\mathrm{cm}^{-1}$  ( $E_g$  mode) can be observed in all the samples. Additionally, a weak peak at

 $450~{\rm cm}^{-1}$  and a small shoulder around at  $610~{\rm cm}^{-1}$  were also found in the reference sample (Figure 3-inset). Both peaks correspond to the  $E_g$  and  $A_{1g}$  modes of the rutile phase, respectively [54]. These rutile peaks were changed in the spectra of the  ${\rm TiO_2/perlite}$  composites (samples FSPA, FSPB, and FSPD). More specifically, the shoulder at  $610~{\rm cm}^{-1}$  disappeared and the weak peak at  $450~{\rm cm}^{-1}$  caused a broadening of the anatase peak around  $399~{\rm cm}^{-1}$ .

It can be also observed that the lowest  $E_g$  anatase mode near  $144\,\mathrm{cm}^{-1}$  is shifted to higher wavenumbers in the binary  $\mathrm{TiO_2/perlite}$  systems (samples FSPB, FSPC, and FSPD) in comparison to the bare  $\mathrm{TiO_2}$  nanoparticles (reference P25). The blue shift can be attributed to compressive stresses appeared in the samples during the flame processing procedure [55]. This procedure is very abrupt and can evoke stresses in the flame-made nanoparticles produced using alkoxide precursor in comparison to the sample P25.

In addition, the peaks at 950 cm<sup>-1</sup> and 1080 cm<sup>-1</sup> related to the vibrational modes of Si-O-Ti [56] were observed for the samples FSPB, FSPC, and FSPD. This is an indication of the bond formation between TiO<sub>2</sub> photocatalysts and perlite substrate during the FSP processing.

The UV-Vis diffuse reflectance spectra for the prepared photocatalysts are given in Figure 4. It can be observed that

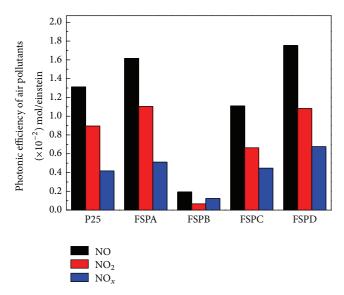


FIGURE 7: Photonic efficiencies in NO oxidation,  $NO_2$  formation, and overall  $NO_x$  removal of the TiO<sub>2</sub>/perlite composites.

the reflectance was high only for the reference sample P25. The bare perlite and all the  ${\rm TiO_2/perlite}$  composites had a reflectance not higher than 70%. It was attributed to the presence of gray colored perlite in the prepared composites and probably to a large amount of residual carbon from the precursor and gas combustion.

The SEM images of the pure perlite and the perlite with immobilized titania nanoparticles are shown in Figures 5(a) and 5(b), respectively. It can be seen that bare perlite has a flake-like form. In the FSP composites, the flakes become rounded and are covered with  ${\rm TiO_2}$  agglomerates. This change in the perlite morphology is attributed to the high temperature FSP processing. The elemental mapping analysis presented in Figures 5(b) and 5(c) reveals that titania (Ti green colour) is homogenously dispersed on the surface of perlite (Si red colour).

Further morphological and structural characterization of the samples was carried out using TEM. As can be seen in Figure 6(a) the perlite flakes are almost entirely covered by  ${\rm TiO_2}$  nanoparticles that appear as an aggregation of small spherical neck-connected particles. It is suggested that these particle aggregations were created from large precursor solution droplets originated from  $800\,\mu{\rm m}$  nozzle diameter. The precursor rapid hydrolysis accompanied with droplets' abrupt shrinkage, during their passage through the flame zone, results in the formation of neck-connected spherical  ${\rm TiO_2}$  nanoparticles, as shown in Figure 6(b). Their mean size is about 20 nm in agreement with XRD results.

A typical HRTEM image of the  $TiO_2$  nanocrystals on the perlite substrate is presented in Figure 6(c). It is evident that each nanoparticle is single crystalline. The lattice fringes shown in the HRTEM image correspond to the rutile and anatase crystal structure with d-spacing d=0.325 nm and d=0.352 nm, respectively. This result is further confirmed by the fast Fourier transform of the HRTEM image shown as inset in Figure 6(c).

The calculated photonic efficiencies of the investigated samples are presented in Figure 7. The calculated values for the commercial Evonik-Degussa P25 are also given for comparison. It can be seen that the FSPA and FSPD  ${\rm TiO_2/perlite}$  composite samples exhibited improved photocatalytic activity in comparison to P25. In these samples, the anatase and rutile phase as well as  ${\rm TiO_2}$  are almost equal according to the XRD results.

Although the anatase is considered a more superior photocatalyst than rutile, the better photocatalytic performance of these composites can be related to possible synergistic effect between the two titania phases. Below is given a simple interpretation of this effect. Because of the higher position of the anatase's conduction band edge relative to that of rutile, transfer of the photogenerated electrons from the anatase to rutile takes place. This leads to reduction of the electronhole recombination rate and as a result to enhancement of the photocatalytic activity of the composite material. Furthermore, the observed enhanced photoactivity of the  ${\rm TiO_2/perlite}$  system can be also attributed to the presence of semitransparent porous perlite substrate that facilitates the dispersion of the  ${\rm TiO_2}$  particles as well as the penetration of UV-irradiation into the depth of the material [52, 57].

#### 4. Conclusions

TiO<sub>2</sub>/perlite composites were synthesized with the help of a homemade FSP reactor and using milled perlite flakes dispersed in TIPO and ethanol as precursor solution. The obtained TiO<sub>2</sub> consisted of interconnected spherical nanoparticles homogenously distributed on perlite flakes. The XRD analysis showed that titania crystallized in the form of anatase and rutile with nanoparticles' size ranging from 20 to 40 nm. Raman microscopy revealed attachment of titania nanoparticles onto perlite substrate via formation of the Si-O-Ti bond. The SSA of the TiO<sub>2</sub>/perlite composites decrease with the increase of the oxygen flow rate. Although the SSA of the TiO<sub>2</sub>/perlite composites was lower than that of P25 sample, their photocatalytic activity in NO oxidation was comparable and even higher for some of them. This result was attributed to the presence of perlite glassy substrate that facilitates photocatalyst dispersion as well as to the synergistic effect between two crystalline phases.

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# Research Article

# Single Step Formation of C-TiO<sub>2</sub> Nanotubes: Influence of Applied Voltage and Their Photocatalytic Activity under Solar Illumination

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Self-aligned and high-uniformity carbon (C)- titania (TiO<sub>2</sub>) nanotube arrays were successfully formed via single step anodization of titanium (Ti) foil at 30 V for 1 h in a bath composed of ethylene glycol (EG), ammonium fluoride (NH<sub>4</sub>F), and hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>). It was well established that applied voltage played an important role in controlling field-assisted oxidation and field-assisted dissolution during electrochemical anodization process. Therefore, the influences of applied voltage on the formation of C-TiO<sub>2</sub> nanotube arrays were discussed. It was found that a minimal applied voltage of 30 V was required to form the self-aligned and high-uniformity C-TiO<sub>2</sub> nanotube arrays with diameter of ~75 nm and length of ~2  $\mu$ m. The samples synthesized using different applied voltages were then subjected to heat treatment for the conversion of amorphous phase to crystalline phase. The photocatalytic activity evaluation of C-TiO<sub>2</sub> samples was made under degradation of organic dye (methyl orange (MO) solution). The results revealed that controlled nanoarchitecture C-TiO<sub>2</sub> photocatalyst led to a significant enhancement in photocatalytic activity due to the creation of more specific active surface areas for incident photons absorption from the solar illumination.

#### 1. Introduction

Nowadays, various kinds of environmental contaminants are around all of us, especially organic and inorganic pollutants from industrial wastewaters [1–3]. Thus, the treatments of such wastewater have become a major concern and it is urgent to develop a sustainable and cost-effective treatment technology to solve global environmental problems [3, 4]. In recent years, the photocatalyst system has attracted much attention from science community as one of the most promising ways to solve the environmental problems [4–6]. This system is considered to be an ideal and green environmental solution for our green economy future.

In this case, TiO<sub>2</sub> based nanomaterials have been broadly studied as the most promising photocatalyst for environmental remediation such as air purification, water purification,

heavy metals degradation, and hazardous waste remediation [6-10]. The reasons are mainly attributed to the nontoxicity, cost-effectiveness, long-term stability, widespread availability, and high stability against photocorrosion with great capacity for oxidation and high photocatalytic property. To date, development of nanoarchitecture of TiO<sub>2</sub> assemblies with precisely controllable nanoscale features has gained significant scientific interest [11, 12]. Among different nanoarchitectures of TiO<sub>2</sub>, one-dimensional (1D) TiO<sub>2</sub> is considered as a promising candidate in environmental and industrial pollutants degradation due to the well controllable dimensional features such as pore diameter, length, and wall thickness [6–9, 11–15]. However, its practical application was limited by poor absorption of photons from the solar illumination and high recombination losses of photoinduced electron-hole pairs [1, 4, 10, 16-18].

Recently, numerous research studies have been paid for the rational design of high efficiency heterostructure C-TiO<sub>2</sub> based nanomaterial for remarkable solar absorption and higher separation efficiency of photo-induced charge carriers [4, 19–22]. In particular, C-TiO<sub>2</sub> based nanomaterials can exert a substantial influence on modifying electronic structure and the construction of heterotomic surface structure that allow higher efficiency photocatalysis reaction under solar irradiation [19, 21, 23]. Several literatures have reported that incorporation of anion C-dopants into TiO2 crystalline could shift its photoresponse into visible region, which accounts for 40-45% irradiation from the solar light. The main reason was attributed to the narrowing of the band gap energy, which resulted from an increase in the width of the valence band. The reduction of band gap energy was believed to be from the mixing of the p-state of C dopants with O 2p and Ti 3*d* orbital constituting valence band [21, 23, 24].

In the present study, a detailed study on the C-doped  ${\rm TiO_2}$  nanotubes via single step of electrochemical anodization technique was performed. An organic electrolyte of ethylene glycol was selected as C source to dope into  ${\rm TiO_2}$  nanotubes during electrochemical anodization. This study aims to determine the minimal applied voltage to grow the self-aligned and high-uniformity C- ${\rm TiO_2}$  nanotubes for better photocatalytic performance. The novelty of this work is to synthesize a potential photocatalyzer, which shows strong absorption range in UV-visible region, strong oxidation ability, cost-effective and time saving process.

#### 2. Experimental Procedure

2.1. Preparation of Anodic C-TiO<sub>2</sub> Nanotubes. 99.6% purity of Ti foils (Strem Chemical, USA) with dimension of 50 mm  $\times$  10 mm  $\times$  0.127 mm was used in this experimental study. The electrochemical anodization process was performed in an organic electrolyte of EG (C<sub>2</sub>H<sub>6</sub>O<sub>2</sub>, >99.5%, Merck, USA), 5 wt% of NH<sub>4</sub>F (98%, Merck, USA), and 5 wt% of H<sub>2</sub>O<sub>2</sub> (30% H<sub>2</sub>O<sub>2</sub>:70% H<sub>2</sub>O, J.T. Baker, USA). This composition was selected because it favors the formation of well-aligned and highly ordered nanotubular structure based on our previous studies [25]. Electrochemical anodization process was conducted for 1h with three different applied voltages (e.g., 10 V, 20 V, and 30 V). Anodization was performed in a two-electrode configuration bath with Ti foil as the anode and a platinum rod as the cathode. Subsequently, these samples were annealed at 400°C for 4 h in an argon atmosphere.

2.2. Characterization of Anodic C-TiO<sub>2</sub> Nanotubes. The Field Emission Scanning Electron Microscopy (FESEM) and Energy Dispersive X-Ray (EDX) were conducted (FEI Quanta 200 FESEM model, USA). The cross-sectional measurements were carried out on mechanically bent samples, where a partial lift-off of the anodic layer occurred to obtain the thickness of the anodic oxide formed on Ti foil. The crystalline phase of the synthesized samples was identified by power X-ray Diffraction (XRD), using a Bruker X-ray Diffraction Model D-8, USA, equipped with a Cu K $\alpha$  monochromatized radiation source ( $\lambda$  = 1.5406 Å). The

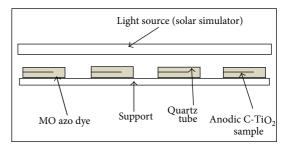


FIGURE 1: Schematic diagram of the experimental setup for quartz glass tube custom-made photoreactor used in photocatalytic degradation MO dye studies.

sample with dimension ( $10 \, \text{mm} \times 10 \, \text{mm}$ ) was placed onto a specimen holder and then placed in the rotating unit stage of diffractometer system. The data was collected within  $2\theta$  of  $10^{\circ}$  to  $70^{\circ}$  with a step size of  $0.034^{\circ}$  at scan time 71.6 sec. Photoluminescence (PL) spectra were obtained at room temperature using an LS 55 luminescence spectrometer (Jobin-Yvon HR 800UV). The photoelectron spectra were obtained through X-ray photoelectron spectroscopy (XPS; JEOL JPS-1000SX) with a dual X-ray source, in which an Al-K $\alpha$  (30 kV) anode and a hemispherical energy analyzer were used. The background pressure during data acquisition was maintained at  $7.0 \times 10^{-9}$  Torr. All binding energies were calibrated using contaminant carbon (C1s = 284.8 eV) as a charge reference.

2.3. Photocatalytic Degradation of MO Dye Study. Photocatalytic degradation MO dye was conducted by dipping 4 cm<sup>2</sup> of anodic C-TiO<sub>2</sub> nanotubes samples into a 100 mL of quartz glass tube containing 30 ppm of MO dye. The quartz glass tube was then placed in a custom-made photorecator for photocatalytic degradation studies. A schematic diagram of quartz glass tube custom-made photo-reactor used in photocatalytic degradation MO dye is exhibited in Figure 1. In this study, a blank sample (without anodic sample) was prepared in order to eliminate the effect of light towards the degradation of MO dye solution. All anodic samples were left in a custom-made photo-reactor for 30 min in dark environment to achieve adsorption and desorption equilibrium. Then, samples were photoirradiated using a 150 W Xenon solar simulator (Zolix LSP-X150, China) with intensity of 800 W/m<sup>2</sup>. Three mL of MO dye solution was withdrawn from the quartz glass tube every 1 h to investigate the degradation of MO dye solution under solar irradiation. The concentration of the degraded MO dye solution assisted by the anodic sample was determined using UV-Vis spectrometer (PerkinElmer Lambda 35, USA).

#### 3. Results and Discussion

3.1. Surface Morphology of Anodic C-TiO $_2$  Nanotubes. The effect of applied voltage in an organic electrolyte of EG solution containing 5 wt% of NH $_4$ F and 5 wt% of H $_2$ O $_2$  on the morphology of the self-organized TiO $_2$  nanotubes

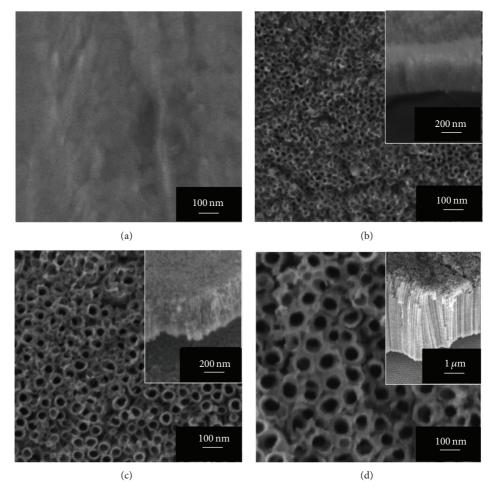


FIGURE 2: FEESEM images of (a) pure Ti foil and C-TiO<sub>2</sub> nanotube arrays fabricated at different applied voltage in an EG electrolyte containing 5 wt% of NH<sub>4</sub>F and 5 wt% of H<sub>2</sub>O<sub>2</sub> for 1 h at (b) 10 V, (c) 20 V, and (d) 30 V (inset: cross-sectional view).

is discussed. Based on our preliminary study, an optimum content of 5 wt% H<sub>2</sub>O<sub>2</sub> played an important role in increasing the oxidation rate of Ti to form TiO2, while 5 wt% of NH<sub>4</sub>F was sufficient to trigger the chemical dissolution reaction to form nanotubular structure during electrochemical anodization [25-27]. The morphology of the Ti foil before conducting electrochemical anodization was characterized by FESEM (Figure 2(a)). It is clearly shown that Ti foil was flat without any pits or pores on its surface. The oxide layer has not yet been formed. The FESEM micrographs of the synthesized nanostructures of anodic C-TiO<sub>2</sub> samples after electrochemical anodization varied from 10 V to 30 V are shown in Figure 2(b) to Figure 2(d). The inset micrographs show the cross-sectional morphology of oxide layer on the anodized Ti foil. These FESEM micrographs clearly show that the applied voltage affects the geometric features are the appearance of the nanotubular structure on the Ti foils. It could be observed that anodized samples exhibited uniform growth of nanotube arrays throughout the surface of Ti foil. The surface and inset of cross-sectional morphology of the Ti foil anodized at a lower applied voltage of 10 V are shown in Figure 2(b). It was found that an average of 25 nm diameters and an average thickness of 550 nm of nanotube

arrays were produced. Upon increasing the applied voltage to 20 V, the average diameter for the nanotubular structure was increased to 45 nm with thickness of 750 nm (Figure 2(c)). It is noteworthy to mention that uniform circular nanotube arrays were successfully formed when minimum voltage of 30 V was applied during electrochemical anodization. The average diameter of 80 nm and thickness of 2  $\mu$ m nanotubes were produced (Figure 2(d)). Therefore, uniform growth of anodic nanotube arrays at lower 30 V of applied voltage was selected and duplicated for the investigation studies.

3.2. Chemical Compositions of Anodic C-TiO $_2$  Nanotubes. EDX analysis was employed to investigate the chemical stoichiometry of the anodic C-TiO $_2$  nanotubes after heating treatment at 400°C in argon atmosphere. As determined through EDX analysis, the anodic C-TiO $_2$  nanotubes synthesized at 30 V consisted of 60.14 at% of Ti element, 33.68 at% of O element and 6.18 at% of C element (Figure 3). An additional spectrum of C was observed at about 0.2 keV from the EDX spectra. This result showed the presence of C species in anodic TiO $_2$  nanotubes. The main reason is favorable to the oxidation of organic EG electrolyte to carbonate type

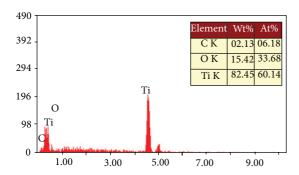


FIGURE 3: EDX spectra of self-aligned and high-uniformity C-TiO<sub>2</sub> nanotube arrays formed in an EG electrolyte containing 5 wt% of NH<sub>4</sub>F and 5 wt% of H<sub>2</sub>O<sub>2</sub> for 1 h at 30 V.

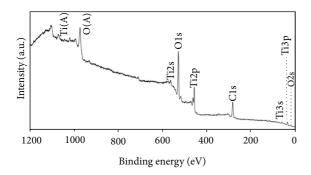


FIGURE 4: XPS survey spectra of self-aligned and high-uniformity C-TiO<sub>2</sub> nanotube arrays formed in an EG electrolyte containing 5 wt% of NH $_4$ F and 5 wt% of H $_2$ O $_2$  for 1 h at 30 V.

species which gets absorbed on the wall of nanotubes during the electrochemical anodization [19, 24, 28]. These resultant carbonate type species were reduced to C species during heat treatment process and diffused into the  ${\rm TiO_2}$  lattice [29]. In this manner, the single step incorporation of C species to  ${\rm TiO_2}$  nanotubes could be achieved.

Next, XPS measurements were carried out to further investigate the chemical composition and oxidation state of C-TiO<sub>2</sub> nanotubes. XPS survey spectra for the sample synthesized at 30 V are presented in Figure 4. The elements of Ti, O, and C were detected from the XPS survey spectra, which indicated that the carbon species were successfully loaded into the lattice of TiO<sub>2</sub>. It was found that the peak of Ti2p (binding energy of about 460 eV) is attributed to Ti<sup>4+</sup>. Besides, it could be observed that the peak of O1s (binding energy of about 530 eV) showed the presence of oxygen atoms in the TiO<sub>2</sub> structure. Meanwhile, the detection of the peak C1s at about 285 eV can be ascribed to the Ti–C–O bonds of the carbonate species originating from the residual carbon of the organic ethylene glycol electrolyte.

3.3. Crystalline Structure of Anodic C-TiO<sub>2</sub> Nanotubes. In the present study, XRD measurements were conducted to reveal the crystal phase transition of the as-anodized and annealed samples. The results are presented in Figure 5. Based on preliminary study,  $400^{\circ}$ C was sufficient to convert  $TiO_2$  amorphous structure to high crystallinity of anatase

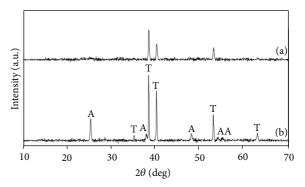


FIGURE 5: XRD pattern of self-aligned and high-uniformity C-TiO $_2$  nanotube arrays formed in an EG electrolyte containing 5 wt% of NH $_4$ F and 5 wt% of H $_2$ O $_2$  for 1h at 30 V, (a) as-anodized and (b) annealed at 400°C under argon atmosphere for 4 h (Ti: titanium; A: anatase).

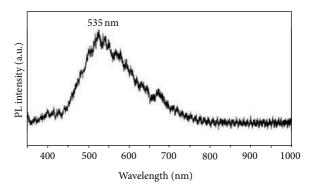


FIGURE 6: The PL emission spectra of self-aligned and high-uniformity C-TiO $_2$  nanotube arrays formed in an EG electrolyte containing 5 wt% of NH $_4$ F and 5 wt% of H $_2$ O $_2$  for 1 h at 30 V.

phase, which exhibited thermodynamically stable and higher surface stability [30–33]. It was found that the presence of Ti phase only was detected from the XRD pattern for the as-anodized sample, which represents the amorphous phase of  $\text{TiO}_2$  (Figure 5(a)). However, high crystallinity of anatase phase was detected for the sample subjected to annealing at  $400^{\circ}\text{C}$  in argon atmosphere (Figure 5(b)). It can be seen that the diffraction peaks of the entire samples are ascribed to the  $\text{TiO}_2$  with anatase phase (JCPDS no. 21–1272). The diffraction peaks allocated at  $25.37^{\circ}$ ,  $38.67^{\circ}$ ,  $48.21^{\circ}$ ,  $54.10^{\circ}$ , and  $55.26^{\circ}$  are corresponding to (101), (112), (200), (105), and (211) crystal planes for the anatase phase, respectively.

 $3.4.\ Optical\ Property\ of\ Anodic\ C-TiO_2\ Nanotubes.$  PL emission spectra were broadly used to investigate the competency of charge carrier trapping, migration, and transfer behaviors of anodic C-TiO\_2 nanotubes. The information from PL emission spectra is important to understand the state of electron-hole pairs in C-TiO\_2 nanotubes photocatalyst since the emission mainly resulted from recombination dynamics of these free carriers. The PL measurement was conducted at room temperatures in the wavelength range of 350 nm to 1000 nm as presented in Figure 6. The dominant PL emission

spectrum of the samples prepared at 30 V is clearly observed at 535 nm, implying the visible-light characteristics of the sample. The dominant PL spectrum of anatase phase TiO<sub>2</sub> was closely related to the recombination of self-trapped excitons localized on the TiO<sub>6</sub> octahedral, which results from the interaction of the negative electrons located in the Ti 3d states with the positive holes in the O 2p state [7, 16, 19]. In this case, the peak position at 535 nm might be attributed to the radioactive recombination of self-trapped excitons localized on TiO<sub>6</sub> octahedron. On the other hand, the PL emissions above 535 nm might be attributed to the presence of surface state and intrinsic defects such as oxygen vacancies, which give rise to donor states located below conduction band. Several literatures have reported that the resultant PL emission spectra were attributed to the oxygen-related defects within the sample lattice [34, 35]. Zhao and coworkers have been reported that the carbon species doping into the lattice of TiO<sub>2</sub> nanotubes favored the formation of oxygen vacancies [36]. They proposed that the electrons were easily trapped by those oxygen vacancies, while the holes were trapped by carbon species. This condition could decrease the PL intensity significantly. Hence, the presence of carbon species could improve the separation extent and restrain the recombination losses of the photo-induced charge carriers. Besides, PL technique has been widely used to investigate the energy levels of samples [23, 37]. The energy level ( $E_b$ ) of the samples was calculated using the equation  $E_b = hc/\lambda$ , where  $E_h$  is the band gap energy, h is Planck's constant (4.135667 ×  $10^{-15}$  eV s), c is the velocity of light (2.997924 × 108 m/s), and  $\lambda$  is the wavelength (nm) of PL emission. The  $E_h$  was found at around 2.3 eV, which is relatively low as compared to the  $E_h$  of pure TiO<sub>2</sub> (3.2 eV for anatase phase) [7, 10]. The result clearly demonstrates that visible emission is likely facilitated by the interstitial C species within the lattice of TiO<sub>2</sub>.

3.5. Formation Mechanism of Anodic C-TiO<sub>2</sub> Nanotubes. In the present study, applied voltage played an important role in controlling the field-assisted oxidation of Ti metal to form TiO2 and field-assisted dissolution of Ti metal ions into electrolyte [38, 39]. A simple schematic illustration about the formation mechanism of anodic C-TiO<sub>2</sub> nanotube arrays was presented in Figure 7. The compact oxide layer was formed through the hydrolysis of Ti foil (stage A) which was oxidized to TiO<sub>2</sub> forming a barrier type layer under applied voltage. This layer grew predominantly by the inward migration of oxygen ions (O2-) through this layer toward Ti/TiO2 interface with further growth of barrier layer (stage B). The high electric field across the oxide layer subsequently induced the polarization of Ti-O bonding. In this manner, Ti<sup>4+</sup> ions from the barrier layer of TiO<sub>2</sub> will dissolve into the electrolyte and form pits randomly on the surface of oxide layer. The pits will act as nucleation sites for the porosification (stage C). The titanium-fluoro complexes  $(TiF_6)^{2-}$  will induce the chemical dissolution and continuous dissolve the pits, which will further enlarge and deepenly the pits into nanotubular structure. The rate of migration of the Ti<sup>4+</sup>, O<sub>2-</sub>, and F<sup>-</sup> ions was higher during the higher voltage electrochemical anodization. The higher electron flow promoted increased

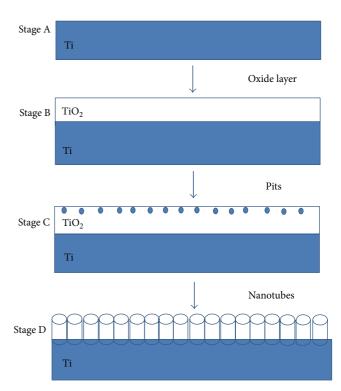


FIGURE 7: Schematic illustration for the formation mechanism of a nodic C-TiO  $_2$  nanotube arrays via electrochemical ano dization technique.

field-assisted oxidation and field-assisted dissolution, which leads to an increase in nanotube length and pore size (stage D). The porosity will reach a steady-state, resulting in the formation of uniform of  $\text{TiO}_2$  nanotubes [9, 11, 26].

In this manner, organic EG electrolyte was oxidized to carbonate-species under applied voltage, which get absorbed on the wall of nanotubes. Then, these carbonate-species were reduced to C species during annealing treatment process, which might diffuse into the lattice of TiO<sub>2</sub> [29]. Thus, the presence of the C species was found within TiO<sub>2</sub> nanotubes. Valentin and coworkers have proposed that the possible causes for the presence of C atoms in the anatase TiO<sub>2</sub> are due to the substitution of the oxygen lattice with a C atom, the replacement of Ti atoms with a C atom; and stabilization of a C atom at interstitial position of TiO<sub>2</sub> lattice [21]. As a matter of fact, the interstitial C atom arises from the pyrogeneration of EG electrolyte, which reduces the band gap marginally or to introduce mid-gap level to increase the light absorption into visible region. In this case, the band gap level reduction was believed to result from an increase in the width of the valence band due to the mixing of the delocalized p-state of carbon dopants with O 2p. The mixing p-state of the C dopants with 2p of O will shift the valence band edge upwards (~0.8 eV above the valence band) to narrow down the band gap of TiO<sub>2</sub> to ~2.3 eV [11, 19]. A comparison between the pure TiO<sub>2</sub> and C-TiO<sub>2</sub> under solar irradiation for the photo-induced electrons transfer pathways was exhibited in Figure 8. Thus, electronic coupling of these states with electronic

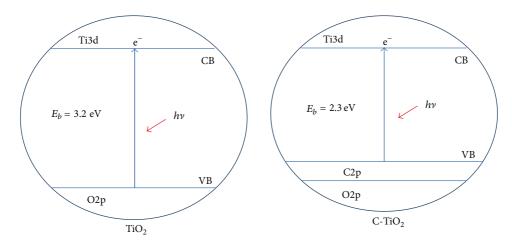


FIGURE 8: The comparison of the photo-induced electrons transfers pathways for pure TiO<sub>2</sub> and C-TiO<sub>2</sub> under solar irradiation.

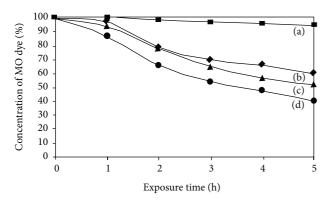


FIGURE 9: Photodegradation of MO dye solution under solar illumination. (a) Blank sample (without anodic sample); samples of C-TiO<sub>2</sub> nanotube arrays produced at (b) 10 V, (c) 20 V, and (d) 30 V.

continuum of TiO<sub>2</sub> valence band state yields a band of surface state at where the electrons could be generated in conduction band by low energy of visible light irradiation [23].

3.6. Photocatalytic Decolorization of MO Dye Evaluation. The significance of C-TiO<sub>2</sub> nanotubes from different applied voltages (10 V-30 V) was applied as the photocatalytic performance evaluation by decolorization of MO dye under visible light irradiation. Figure 9 clearly shows the continuous decrease in the concentration of MO dyes with increasing exposure time. It was found that the decolorization of MO dye follows an apparent first-order kinetic reaction. The decolorization rate order was C-TiO<sub>2</sub>-30 V > C-TiO<sub>2</sub>-20 V > C-TiO<sub>2</sub>-10 V. It could be observed that the C-TiO<sub>2</sub>-30 V exhibited the highest photocatalytic performance of ~60% after exposure to solar irradiation for 5 h. The dominating factor in decolorization of MO dye is attributed to the active surface area of the catalyst to absorb more photons from the solar irradiation [40, 41]. In addition, higher active surface area will allow more organic MO molecules to absorb onto the C-TiO<sub>2</sub> surface. Furthermore, higher uniformity of nanotube arrays will result in more rapid diffusion of

the organic MO molecules into the inner of nanotubes for photocatalytic reaction [41, 42]. In this case, C content within the nanotubes could play an important role in reducing the band gap energy of TiO<sub>2</sub> nanotubes (from 3.2 eV to 2.3 eV based on the anatase phase). The visible emission is likely facilitated by the interstitial C species within the lattice of TiO<sub>2</sub>. Thus, the photo-induced charge carriers could be generated effectively under solar illumination. Besides, the photo-induced electrons were easily trapped by this C content and led to higher transportation of charge carriers from bulk to surface of TiO<sub>2</sub>, which retards the recombination losses. It is a well-known fact that MO molecule has one -SO<sub>3</sub> group and two alkyl groups (-CH<sub>3</sub>), which can improve the adsorption of the H<sub>2</sub>O or OH<sup>-</sup>ions on C-TiO<sub>2</sub> surface [43]. In this manner, C-TiO<sub>2</sub> nanotubes play an essential role in promoting the adsorption of OH species on the inner and outer wall surface of nanotubes and consequently promoting the photocatalytic reaction.

In the present study, photocatalytic reaction in decolorization of MO dye strongly depends on the ability of catalyst to create photo-induced charge carriers, which generate free radicals (hydroxyl radicals of 'OH) able to undergo secondary reactions [6, 8, 9]. Theoretically, the exposure of a photocatalyst to irradiation (hv) higher than its  $E_h$  will result in the transition of photo-induced electrons (e<sup>-</sup>) from the O 2p state to the Ti 3d state and leave behind photo-induced holes  $(h^+)$ . Nevertheless, photo-induced  $e^-$  and  $h^+$  recombine quickly in ordinary substances. This recombination process can occur either in bulk or on the surface of catalyst by releasing energy in the form of unproductive heat or photons [44]. The photo-induced  $h^+$  escaping from the pair recombination preferentially moves to the photocatalyst/electrolyte interface. The photo-induced  $h^+$  plays an important role in generation of 'OH radicals by the trapping of adsorbed H<sub>2</sub>O or OH<sup>-</sup> ions from the MO dye, which has strong oxidative decomposing power in decolorization of MO dye. Meanwhile, photo-induced  $e^-$  escaping from recombination will be trapped on the surface of photocatalyst by reaction with adsorbed oxygen species to generate superoxide anion radicals (O2°), which then will contribute to the formation of \*OH radicals by reactions with H<sub>2</sub>O [45]. In this case, more \*OH radicals will react with organic MO dye to decompose them into harmless substance.

#### 4. Conclusion

The formation of C-TiO<sub>2</sub> nanotubes via single step electrochemical anodization technique successfully formed selfaligned and high-uniformity C-TiO2 nanotube arrays with diameter of  $\sim$ 75 nm and length of  $\sim$ 2  $\mu$ m with a minimal applied voltage of 30 V. The applied voltage played an important role in enhancing the field-assisted oxidation rate and field-assisted dissolution rate. The reduction of band gap energy level of C-TiO<sub>2</sub> nanotube arrays (3.2 eV to 2.3 eV) was due to the mixing states of the delocalized C 2p and O 2p. In photocatalytic evaluation, it was found that C-TiO<sub>2</sub> synthesized at 30 V exhibited the highest decolorization rate under solar irradiation among samples. The reason was mainly attributed to higher active surface area and higher uniformity of nanotube arrays has better photons absorption from solar illumination to trigger more photoinduced charge carriers for decolorization of MO dye.

#### Acknowledgment

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# Research Article

# Kinetics Study of Photocatalytic Activity of Flame-Made Unloaded and Fe-Loaded CeO<sub>2</sub> Nanoparticles

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Unloaded  $CeO_2$  and nominal 0.50, 1.00, 1.50, 2.00, 5.00, and 10.00 mol% Fe-loaded  $CeO_2$  nanoparticles were synthesized by flame spray pyrolysis (FSP). The samples were characterized to obtain structure-activity relation by X-ray diffraction (XRD), high-resolution transmission electron microscopy (HRTEM), Brunauer, Emmett, and Teller (BET) nitrogen adsorption, X-ray photoelectron spectroscopy (XPS), and UV-visible diffuse reflectance spectrophotometry (UV-vis DRS). XRD results indicated that phase structures of Fe-loaded  $CeO_2$  nanoparticles were the mixture of  $CeO_2$  and  $Fe_2O_3$  phases at high iron loading concentrations. HRTEM images showed the significant change in morphology from cubic to almost-spherical shape observed at high iron loading concentration. Increased specific surface area with increasing iron content was also observed. The results from UV-visible reflectance spectra clearly showed the shift of absorption edge towards longer visible region upon loading  $CeO_2$  with iron. Photocatalytic studies showed that Fe-loaded  $CeO_2$  sample exhibited higher activity than unloaded  $CeO_2$ , with optimal 2.00 mol% of iron loading concentration being the most active catalyst. Results from XPS analysis suggested that iron in the Fe<sup>3+</sup> state might be an active species responsible for enhanced photocatalytic activities observed in this study.

#### 1. Introduction

Organic compounds from industries are one of the major causes of water pollution [1]. Various strategies have been employed to remove these toxic compounds [2, 3]. One of the most interesting approaches is heterogeneous photocatalysis because the process is based on the use of solar energy, which is clean and abundant in nature [4, 5]. In the recent years, cerium dioxide (CeO2 or ceria) has received considerable attention because this material shows promising applications in solid oxide fuel cells [6], environmental catalysis [7, 8], redox catalysis [9], and wet catalytic oxidation of organic pollutants [10]. However, the band gap of CeO<sub>2</sub> (3.22 eV) has limited the activation of solar energy; only UV light can be applied to generate electron-hole pairs at the beginning of photocatalytic processes. Thus, it is necessary to extend the absorbance of CeO2 into visible region and reduce the electron-hole pairs recombination [11, 12]. There are many

methods to modify light absorption properties of CeO<sub>2</sub>, such as metal doping [13, 14], surface sensitization [15], and coupling with semiconductor that has smaller band gap [16]. Recently, transition metal doping/loading has been widely used to enhance the light absorption of CeO<sub>2</sub> [17, 18]. It has been reported in many works of literature that the metal ions of Pt [19], Ag [20], Fe [21], Mn [22], Co [23], Ni [24], and Zn [25] in CeO<sub>2</sub> could improve CeO<sub>2</sub> photocatalytic activity towards the visible-light region. Among these metals, Fe has been considered as a candidate owing to its special Fenton reaction of iron. The Fenton process can improve the photocatalytic activity by producing the hydroxyl radicals (OH\*) which are very powerful oxidizer in photocatalytic process [26]. There are many methods to prepare unloaded CeO<sub>2</sub> and Fe-doped/-loaded CeO<sub>2</sub> nanoparticles such as sol-gel [27], sonochemical [28], homogeneous precipitation [29], hydrothermal [30], microemulsions [31], surfactant-assisted precipitation [32], and flame spray pyrolysis (FSP) methods [33].

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Among them, the latter one is a promising approach because FSP can produce the nanoparticle products with particle size in the range of 1–200 nm at high production rates up to 250 g/h in one step [34]. Other advantages are the ability to dissolve the precursor directly in the fuel and the simplicity of introduction of the precursor into the hot flame zone. In addition, the process of loading/doping metal oxide with metals can easily be done by adding dopant in the precursor solution [35, 36]. In the present work, unloaded  ${\rm CeO_2}$  and Fe-loaded  ${\rm CeO_2}$  nanoparticles were directly synthesized by FSP method. The formic acid and oxalic acid were chosen as model organic pollutants for photocatalytic study under visible-light irradiation.

#### 2. Experimental

2.1. Preparation of Powders. The precursor solutions for FSP consisted of cerium nitrate hexahydrate (Sigma-Aldrich, 99.99 wt%) and iron acetyl acetonate (Sigma-Aldrich, 97 wt%). The cerium precursor was dissolved in absolute ethanol (Scharlau, 98%) to obtain a 0.50 M concentration. Amounts of Fe loading concentration were varied as 0.50, 1.00, 1.50, 2.00, 5.00, and 10.00 mol% in order to prepare Feloaded CeO<sub>2</sub> samples. The precursor mixtures were fed into the center of flame by syringe pump with a rate of 5 mL/min and dispersed by 5 L/min oxygen according to the previous report [37]. Then, the liquid precursor was dispersed quickly in an upward direction by gas stream and ignited by premixed oxygen/methane flame. The gas flow rates of oxygen and methane-supporting flame were set as constant rates of 1.19 and 2.46 L/min, respectively. After evaporation and combustion of liquid precursor droplet, nanoparticle products were collected on a glass microfiber filter papers (Whatmann GF/A, 25.7 cm in diameter) with a vacuum pump controller.

2.2. Characterization of Nanoparticles. The phase and crystallinity of the synthesized samples were analyzed by X-ray powder diffraction (XRD; Philips X'Pert MPD; CuK $\alpha$  radiation). The most intense peak corresponding to (111) plane was chosen to calculate the crystallite sizes (D) using Scherrer equation as follow:

$$D = \frac{k\lambda}{\beta\cos\theta},\tag{1}$$

where k is a constant equal to 0.89,  $\lambda$  is the X-ray wavelength equal to 0.154 nm,  $\beta$  is the full width at half-maximum (FWHM), and  $\theta$  is the half-diffraction angle [38]. The chemical composition and oxidation state of material were studied by X-ray photoelectron spectroscopy (XPS) using Mg X-ray source (MgK $\alpha$ , Kratos Axis Ultra DLD). The binding energy of the adventitious carbon (C 1s) line at 285 eV was used for calibration, and the position of other peaks was corrected according to the position of the C 1s signal. High-resolution transmission electron microscopy (HRTEM, JEOL JEM-2010) was employed to determine the morphology of prepared samples. The mean particle size and specific surface area (SSA) were investigated using the Brunauer, Emmett,

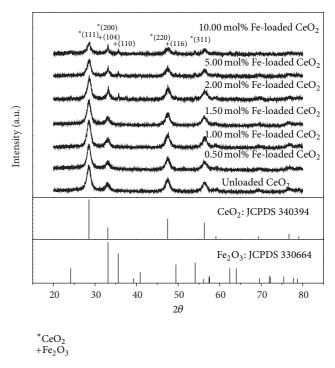


Figure 1: X-ray diffraction patterns of  ${\rm CeO_2}$  with different iron content.

and Teller (BET) nitrogen adsorption method (QuantachromeAutosorp 1MP). The reflectance spectra of the nanoparticle powders were obtained by using UV-visible diffuse reflectance spectrophotometry (UV-vis DRS) equipped with integrating sphere detector (Shimadzu, UV-3101PC).

2.3. Photocatalytic Activity. 1.00 g/L of photocatalyst suspensions was prepared in deionized water and circulated in closed system spiral photoreactor. In a typical run, carbon burn-off step was firstly carried out by illuminating the photocatalyst suspension with a UV-A lamp (Sylvania Blacklight Blue, 18 W) in order to remove any organic impurities from the photocatalyst. The photocatalytic activities were evaluated through formic acid (Sigma-Aldrich, 98 wt%) and oxalic acid (Sigma-Aldrich, 99.99 wt%) degradations under the visible irradiation for 120 min. Finally, the generated carbon dioxide (CO<sub>2</sub>) was measured using the conductivity meter (Eutech Instruments Cyberscan PC5500, μS/cm<sup>2</sup> precision). At the end of each photocatalytic experiment, the recorded data presented the increase in conductivity value. In order to calculate amounts of generated CO2, the values were converted from conductivity at that time to the amount of carbon by the interpolated from calibration curve.

#### 3. Results and Discussion

3.1. X-Ray Powder Diffraction (XRD). In Figure 1, the X-ray diffraction pattern has been used in order to study the structure and phase composition of the prepared samples. It can be seen that all samples had similar diffraction patterns of cubic fluorite structure of ceria (JCPDS 340394) [39]. However,

Iron loading	111 plane						
concentration (mol%)	$2\theta$ (degree)	<i>d</i> -spacing (nm)	Lattice parameter (nm)	Unit cell volume (nm³)	Crystalline size (nm)		
0.00	28.4601	0.3132	0.5426	0.1597	8.3586		
0.50	28.5479	0.3123	0.5409	0.1583	7.8555		
1.00	28.5699	0.3121	0.5405	0.1579	7.4111		
1.50	28.5772	0.3120	0.5404	0.1578	7.4081		
2.00	28.6284	0.3114	0.5394	0.1570	6.9682		
5.00	28.6490	0.3112	0.5390	0.1566	6.2226		
10.00	28.7098	0.3106	0.5380	0.1557	5.7476		

Table 1: The calculated d-spacing, lattice parameters, unit cell volume, and crystalline size.

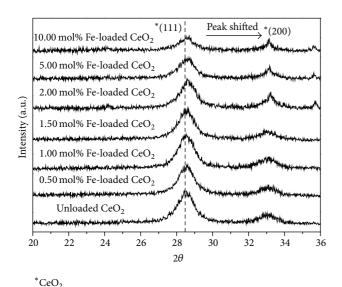


Figure 2: The shift of  $2\theta$  of samples.

the sample with high amount of iron loading (2.00, 5.00, and 10.00 mol%) exhibited the mixed phase of  $CeO_2$  and  $Fe_2O_3$  (JCPDS 330664) [40]. The XRD peaks of all samples were magnified as shown in Figure 2. It was found that  $CeO_2$  peaks shifted towards higher  $2\theta$  upon increasing iron content. The calculated d-spacing, lattice parameter, unit cell volume, and average crystallite size were also decreased as shown in Table 1. These observations could be ascribed to partial substitution of  $Ce^{4+}$  ions (0.101 nm) by  $Fe^{3+}$  ions (0.064 nm) [41]. A decrease of unit cell parameters due to the substitution of larger ion by the smaller one was also found in previous reports [42, 43].

3.2. High-Resolution Transmission Electron Microscopy (HRTEM). As seen from Figure 3(a), the unloaded  $CeO_2$  clearly showed the cubic morphology of cubic fluorite  $CeO_2$  structure. In Figure 3(b), the particles became more spherical upon loading  $CeO_2$  with iron. This change in  $CeO_2$  morphology might be due to the incorporation of iron ions in  $CeO_2$  lattice, thus affecting the particle growth and causing lattice deformation [44]. This assumption was supported by the shift of XRD peak and the changes of lattice

TABLE 2: Summary of analytical data.

Iron loading concentration (mol%)	SSA (m <sup>2</sup> /g)	$E_g$ (eV)	BET diameter (nm)	
0	130.00	3.21	6.39	
0.50	134.00	2.95	6.20	
1.00	137.97	2.70	6.02	
1.50	137.99	2.65	6.02	
2.00	139.00	2.55	5.98	
5.00	140.82	2.45	5.57	
10.00	148.76	2.35	5.27	

parameters as reported in Table 1. The average particle sizes as seen from HRTEM image were about 6–8 nm. This was in good agreement with the calculated sizes obtained by using the Scherrer equation. Figure 3(c) shows the lattice fringes of 2.00 mol% Fe-loaded CeO $_2$ . The lattice planes with d-spacing of 0.16 and 0.20 nm were attributed to the (311) and (220) planes of cubic fluorite CeO $_2$ , respectively, whereas the plane with d-spacing of 0.24 was assigned to the (110) plane of Fe $_2$ O $_3$ . These results confirmed the presence of mixed phase between CeO $_2$  and Fe $_2$ O $_3$  in the nominal 2.00 mol% Fe-loaded CeO $_2$  as found previously in the XRD patterns (Figure 1).

3.3. Nitrogen Adsorption-Desorption Isotherms. The specific surface areas (SSA) of different samples were analyzed by Brunauer-Emmett-Teller (BET) method based on the nitrogen adsorption/desorption isotherm. The mean BET diameter (D) was also calculated by using the following equation [45]:

$$D = \frac{6000}{(S_{\text{BET}} \times \rho)},\tag{2}$$

where  $S_{\rm BET}$  is the BET-specific surface area and  $\rho$  is the density of the CeO<sub>2</sub> (7.32 g/mL). As shown in Table 2, an increase of surface area accompanied with a decrease of BET diameter was clearly observed upon increasing iron content. This increased surface area would be beneficial to the efficient photocatalytic performance due to high surface adsorption of organic pollutants. The calculated BET diameter was in

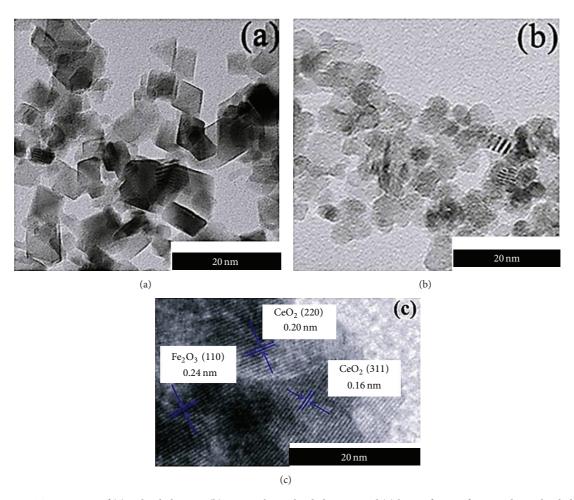


FIGURE 3: HRTEM images of (a) unloaded CeO<sub>2</sub>, (b) 2.00 mol% Fe-loaded CeO<sub>2</sub>, and (c) lattice fringe of 2.00 mol% Fe-loaded CeO<sub>2</sub>.

the range of 5–7 nm which was very well in agreement with those obtained by using the Scherrer equation (Table 1).

3.4. UV-Visible Spectroscopy. UV-vis reflectance analysis was performed by converting the obtained reflectance spectra (Figure 4(a)) to the Kubelka-Munk absorbance spectra using the Kubelka-Munk equation as follows [46]:

$$F\left(R_{\infty}\right) = \frac{\left(1 - R_{\infty}\right)^2}{2R_{\infty}},\tag{3}$$

where  $F(R_{\infty})$  and  $R_{\infty}$  are the Schuster-Kubelka-Munk absorbance and the absolute reflectance of the sample, respectively. The plot of absorbance against wavelength for the  $CeO_2$  nanoparticle powders is shown in Figure 4(b).

The spectra showed that the absorption edge shifted to longer wavelength upon increasing the iron loading concentration. Band gap energies of the obtained samples can then be determined by using the intercept of the tangent to the graph plotting between the Kubelka-Munk absorption function and photon energy (hv) as shown in Figure 4(c) [47, 48]. The obtained band gap energies  $(E_g)$  as reported in Table 2 decreased with increasing iron loading concentration.

3.5. Photocatalytic Activity. The photocatalytic activity of unloaded and Fe-loaded CeO<sub>2</sub> was evaluated by degradation of formic and oxalic acids. The effects of different iron loading concentrations on the photocatalytic efficiency of CeO<sub>2</sub> nanoparticles were evaluated under visible-light irradiation for 120 min, and the results are presented in Figure 5. According to the results, the photocatalytic activities of Fe-loaded CeO<sub>2</sub> nanoparticles were significantly higher than those of unloaded CeO<sub>2</sub> nanoparticles. This improved photoactivity could be partially ascribed to the enhanced light absorption in visible-light region as observed from the UV-vis study in Figure 4. However, the activity was clearly dependent on the amount of iron loading. The results demonstrated that the nominal 2.00 mol% was an optimal iron concentration for photocatalytic activity of CeO<sub>2</sub> nanoparticles in this research. On the other hand, 5.00% and 10.00 mol% iron concentrations showed poor photocatalytic activity, probably because high iron concentration tended to cover CeO2 surface, thus preventing light from contacting the CeO<sub>2</sub> surface [49].

Another possible reason was that too high iron loading can act as the electron-hole recombination centers instead of the trapping level, resulting in a decreased photocatalytic activity [47, 50]. The kinetic data for formic and oxalic acids degradations under visible-light illumination were found to

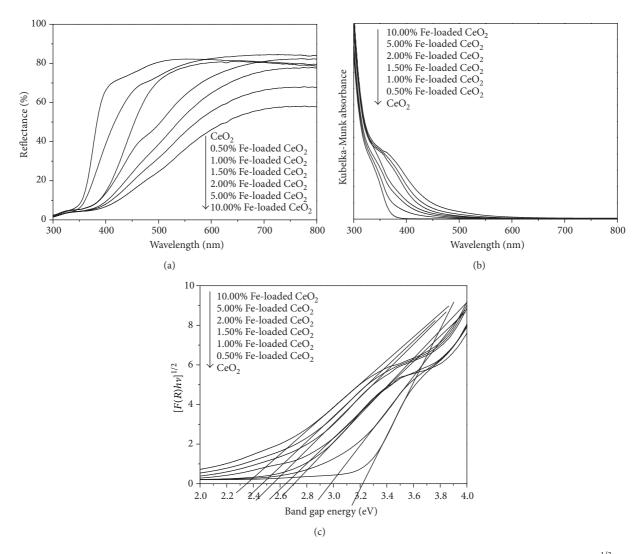


FIGURE 4: UV-vis (a) reflection spectra, (b) Kubelka-Munk absorbance, and (c) relation between band gap energy and  $[F(R)hv]^{1/2}$  of  $CeO_2$  with different iron content.

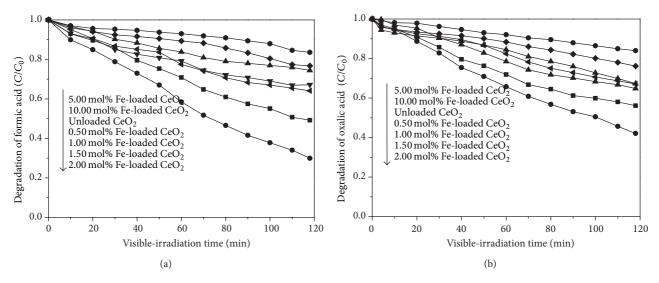


FIGURE 5: Photocatalytic degradation of (a) formic acid and (b) oxalic acid by CeO<sub>2</sub> with different iron content as a function of visible-light irradiation time.

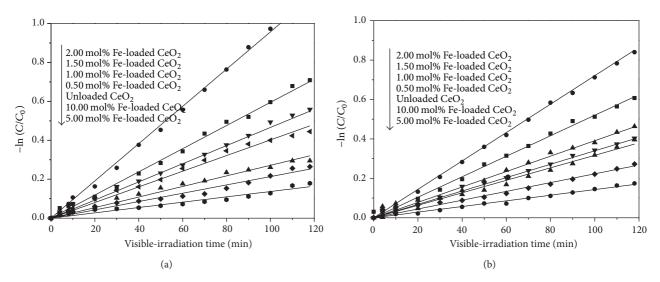


FIGURE 6: Kinetics plots for linear fitting of data obtained from pseudo first-order reaction for (a) formic acid and (b) oxalic acid degradation under visible-light irradiation.

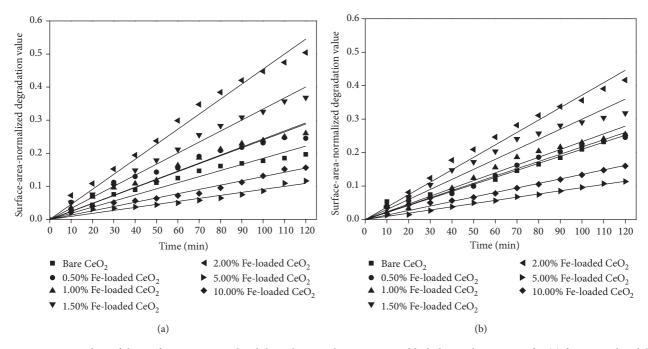


FIGURE 7: Kinetics plots of the surface-area-normalized degradation values against visible-light irradiation time for (a) formic acid and (b) oxalic acid.

follow pseudo first-order reaction [51] as shown in Figure 6. The pseudo first-order model is explained by

$$-\ln\left(\frac{C}{C_0}\right) = kt,\tag{4}$$

where k is the apparent rate constant (min<sup>-1</sup>),  $C_0$  means the initial concentration of acid, and C refers to the concentration of acid at various reaction times (t). The determined pseudo first-order rate constants (k, min<sup>-1</sup>) are presented in Table 3. It can be seen that the loading of 2.00 mol% iron in  $CeO_2$  nanoparticles could remarkably improve the apparent rate

constant up to 5 times for formic acid and 3 times for oxalic acid compared with the unloaded one.

In order to investigate the effect of surface area on the degradation activity, the surface-area-normalized degradation values against visible-light irradiation time were plotted as shown in Figure 7, and the calculated surface-area-normalized rate constants are presented in Table 3. The results clearly suggested that surface-area of the catalyst has a crucial impact on the activity of acid degradation in this study because the surface area-normalized rate constants are significantly decreased from the original values. However, other factors such as band gap energy, amount of Fe loading,

Samples	Rate consta	$\operatorname{nt}(k, \min^{-1})$	Surface-area-normalized rate constants (min <sup>-1</sup> m <sup>-2</sup> g)	
Samples	Formic acid	Oxalic acid	Formic acid	Oxalic acid
$5.00  \mathrm{mol}\%$ Fe-loaded $\mathrm{CeO}_2$	0.0014	0.0014	0.0009	0.0010
10.00 mol% Fe-loaded ${\rm CeO_2}$	0.0017	0.0020	0.0013	0.0014
Unloaded CeO <sub>2</sub>	0.0021	0.0022	0.0019	0.0021
$0.50\mathrm{mol}\%$ Fe-loaded $\mathrm{CeO}_2$	0.0040	0.0034	0.0024	0.0022
1.00 mol% Fe-loaded CeO <sub>2</sub>	0.0054	0.0039	0.0024	0.0023
1.50 mol% Fe-loaded $CeO_2$	0.0060	0.0052	0.0033	0.0030
2.00 mol% Fe-loaded ${\rm CeO_2}$	0.0096	0.0072	0.0045	0.0037

TABLE 3: Apparent rate constants and surface-area-normalized rate constants.

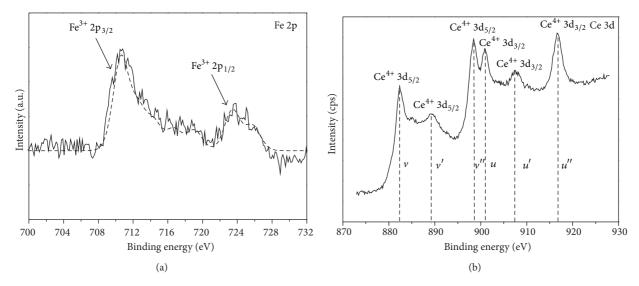


FIGURE 8: The XPS spectra of Fe-loaded CeO<sub>2</sub> nanoparticles: (a) Fe 2p and (b) Ce 3d.

sample crystallinity, and phase composition [52] could not be neglected as these could also contribute to the difference in photocatalytic activity of the catalysts being studied.

3.6. X-Ray Photoelectron Spectroscopy (XPS). In order to characterize the valence state of cerium and iron in 2.00 mol% Fe-loaded CeO<sub>2</sub>, X-ray photoelectron spectroscopy (XPS) was carried out as shown in Figure 8.

According to Figure 8(a), the peaks at 710.6 and 723.4 eV assignable to the core level of  $2p_{3/2}$  and  $2p_{1/2}$ , respectively, corresponded to  $Fe^{3+}$  species in  $Fe_2O_3$  [53, 54]. No other peaks due to  $Fe^0$  and  $Fe^{2+}$  were found in the XPS results. From the Ce 3d XPS spectrum, the binding energies of all peaks are shown in Figure 8(b). These peaks corresponded to the three pairs of spin-orbit doublets assignable to  $Fe^{4+}$  valence state which were very well in agreement with the previous reports [55, 56].

#### 4. Conclusions

Fe-loaded CeO<sub>2</sub> nanoparticles with different iron loading concentrations have successfully been synthesized by flame spray pyrolysis (FSP). Loading CeO<sub>2</sub> with Fe<sup>3+</sup> resulted in a decrease of *d*-spacing, lattice parameter, unit cell volume, and

crystallite size but an increase of BET surface area. The UV-vis absorption spectra displayed a red shift in the band edge transition upon increasing of iron loading concentration. XPS analysis showed the presence of  ${\rm Fe^{3+}}$  species on the surface of  ${\rm CeO_2}$ . This could be attributed to the presence of  ${\rm Fe_2O_3}$  as observed from the XRD and HRTEM analyses. Increased photocatalytic activity compared with unloaded  ${\rm CeO_2}$  was clearly obtained from the Fe-loading sample. It was found from this study that the nominal 2.00 mol% was an optimum iron loading concentration, giving the highest photocatalytic activity. Band gap energy and surface of the catalyst were found to be important factors affecting the photocatalytic activity observed in this study. However, other factors such as amount of Fe loading, sample crystallinity, and phase composition could not be neglected.

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# Research Article

# Supported Zinc Oxide Photocatalyst for Decolorization and Mineralization of Orange G Dye Wastewater under UV365 Irradiation

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To solve the environmental challenge of textile wastewater, a UV/ZnO photocatalytic system was proposed. The objective of this study was to prepare a photocatalytic system by utilizing both cold cathode fluorescent light (CCFL) UV irradiation and steel mesh supported ZnO nanoparticles in a closed reactor for the degradation of azo dye C.I. Orange G (OG). Various operating parameters such as reaction time, preparation temperature, mixing speed, ZnO dosage, UV intensity, pH, initial dye concentration, and service duration were studied. Results presented efficient color and total organic carbon (TOC) removal of the OG azo dye by the designed photocatalytic system. The optimal ZnO dosage for color removal was  $60 \, \mathrm{g} \, \mathrm{m}^{-2}$ . An alkaline pH of 11.0 was sufficient for photocatalytic decolorization and mineralization. The rate of color removal decreased with the increase in the initial dye concentration. However, the rate of color removal increased with the increase in the UV intensity. The steel mesh supported ZnO can be used repeatedly over 10 times without losing the color removal efficiency for 120 min reaction time. Results of Fourier transform infrared (FTIR) and ion chromatography (IC) indicated the breakage of N=N bonds and formation of sulfate, nitrate, and nitrite as the major and minor products. The observation indicated degradation of dye molecules.

#### 1. Introduction

In the last few decades, the textile industry is one of the most important industries, which make contribution toward Taiwan's economic development. Wastewater effluents from textile and dye manufacturing industries receive much attention from public and governmental enforcements, because this type of wastewater can hardly meet the national discharge standards. In Taiwan, the national effluent standard (NES) has enforced the criteria of textile dyeing industries that chemical oxygen demand (COD) meets <100 to 160 mg/L and American Dye Manufacturers Institute (ADMI) color index meets <550 unit by the year 2003. On the other hand, most dyestuffs from the effluent of textile dyeing and finishing industry are complicated organic compounds with high color intensity, are recalcitrant to conventional biological wastewater treatment, and cause major environmental concerns [1–4]. To resolve the wastewater treatment problem, textile industrial treatment plants usually employ chemical

coagulation integrated with activated sludge process. Unfortunately, these traditional treatment processes cannot meet the increasingly stringent criteria of color in dye wastewater treatment in Taiwan [5]. Under this situation, textile dyeing industries should pursue a more efficient technique to be the pretreatment or polishing processes to decolorize the highly colored wastewater. In this category of wastewater, azo dyes with nitrogen double bond (-N=N-) are the largest class of commercial dyestuffs used in the textile industries. Thus, many studies focused on decolorizing azo dye compounds by various techniques [6-8].

Advanced oxidation processes (AOPs), such as ozonation, UV/ $\rm H_2O_2$ , UV/ $\rm O_3$ ,  $\rm Fe^{2+}/\rm H_2O_2$ , and UV/ $\rm O_3/\rm H_2O_2$ , are widely used to decompose organic products in industrial wastewater and groundwater. The extensive literatures of these technologies have been reviewed by Venkatadri and Peters [9]. These processes have the potential ability to mineralize most of the organic contaminants into carbon dioxide and water. There were reports of successful color removal with final

mineralization from azo dye wastewater using advanced oxidation processes (AOPs) such as UV/H<sub>2</sub>O<sub>2</sub> [10-12], UV/O<sub>3</sub> [13, 14], or the Fenton reaction [15, 16]. Additionally, it has been reported that photocatalytic processes such as UV/ZnO system can also be effective in treating dye wastewaters [17-19]. The preparation of ZnO catalyst can be demonstrated by hydrothermal synthesis [20] and the doping of carbon on ZnO can improve its visible light application [21]. Much research focused on slurry type reactor. However, the limitation on the need of further separation of ZnO particles made the process more complicate and expensive. Therefore, fixing the ZnO particles onto supported materials such as glass plate, silica plate can avoid the particle separation step and can enable the easy operation of heterogeneous ZnO photocatalysis [22-24]. The aim of this work was to study the degradation of azo dye C.I. Orange G (OG) using a batch photocatalytic reactor in which the photocatalytic ZnO particles were supported on steel mesh and six cold cathode fluorescent lamps (CCFL) were used (wavelength of 365 nm) to provide UV irradiation. Operating parameters such as preparation temperature, mixing speed, ZnO dosage, UV intensity, pH, initial dye concentration, and reaction time that may affect the degree of the dye degradation were studied. Changes in color intensity, total organic carbon (TOC), pH, oxidation reduction potential (ORP) were monitored in addition to the analysis of reaction products by Fourier transform infrared (FTIR) and ion chromatography (IC).

#### 2. Materials and Methods

2.1. Materials and Apparatus. A mono-azo dye, C.I. Orange G (OG), was selected as target compound for this photocatalytic decolorization study. OG (C<sub>16</sub>H<sub>10</sub>N<sub>2</sub>Na<sub>2</sub>O<sub>7</sub>S<sub>2</sub>, 60% purity) with a characteristic wavelength ( $\lambda_{max}$ ) of 479 nm and a molecular weight of 452.38 g mole<sup>-1</sup> was purchased from Sigma-Aldrich, Inc. and used as received without further purification. The chemical structure of OG can be obtained from our previous study [25]. The commercial available nanosized zinc oxide (ZnO), with a specific surface area of 25.68 m<sup>2</sup> g<sup>-1</sup> from Aldrich, was used as the photocatalyst. The steel mesh (mesh size no.140, 0.106 mm) was purchased from a local hardware store and trimmed into pieces with a gross area of  $252 \,\mathrm{cm}^2$  (36 × 7 cm). A dip coating technique was used to prepare ZnO-coated steel meshes. The trimmed steel mesh was washed, dried, and weighted first, then dipped into a designed concentration of ZnO mixed liquid for 30 minutes, and then dried in a 105°C oven for 30 minutes. The coating process was repeated three times. After all, the ZnOcoated steel mesh was weighted to measure the amount of ZnO on steel mesh. The detailed preparation procedure was reported in our previous work with the replacement of TiO<sub>2</sub> with ZnO nanoparticles [25]. Table 1 shows the steel mesh with specific surface. ZnO concentration of 8-67 g m<sup>-2</sup> can be obtained by dip coating 0.20-1.67 g of ZnO nanoparticles on the given steel mesh with gross area of 252 cm<sup>2</sup>. Based on images obtained with the field emission scanning electron microscope (FESEM), model JEOL 6330CF, the bare steel

TABLE 1: The ZnO-coated weight on the steel meshes.

ZnO	ZnO solution concentration	ZnO weight on the coated steel	ZnO weight per unit area
weight (g) $(W_1)$	$(g L^{-1})$ $(W_1/V)$	meshes (g) $(W_2)$	$(g m^{-2})$ $(W_2/A)$
15	30	0.20	8
25	50	0.37	15
37.5	75	0.75	30
50	100	1.51	60
62.5	125	1.67	67

V: the ZnO solution of 500 mL, A: the steel net area of 252 cm<sup>2</sup>.

mesh showed smooth surface with no particles attached as shown in Figures 1(a) and 1(b). As for ZnO-coated steel mesh, it is seen that ZnO particles were uniformly coated on the steel mesh surface and the particles were of cylindrical shape as shown in Figures 1(c) and 1(d). The crystallinity of ZnO particles was provided by Aldrich as wurtzite structure. The photocatalytic reactor setup was also presented in our previous work [25]. The reactor was a 36 cm  $(L) \times 7$  cm  $(W) \times 7$ 7.8 cm (H) black acrylics container fixed on a horizontal shaker with 75 rpm mixing speed. At the upper cover of the reactor, six cold cathode fluorescent lamps (CCFL), each of which has a diameter of 0.25 cm, length of 30 cm, light intensity of 4 W, and irradiation wavelength of 365 nm, were equipped which yielded a total light energy of 2.1 mW cm<sup>-2</sup> measured at the surface of the solution. In each experimental run, 200 mL dye solution was introduced to the photocatalytic reactor. At the bottom of the reactor, there was ZnOcoated steel mesh with total gross surface area 252 cm<sup>2</sup> placed.

2.2. Experimental Procedure and Analysis. OG azo dye solution at various concentrations was prepared with deionized water. The experimental variables studied included reaction time, preparation temperature, mixing speed, ZnO dosage, UV intensity, pH, initial dye concentration, and application duration of ZnO. At a predetermined reaction time, an aliquot of the solution was withdrawn and analyzed for residual dye concentration, TOC, and color.

Dye concentration was determined by measuring the absorbance at a wavelength of 479 nm using Hitachi U-2000 spectrophotometer. Color intensity was determined based on the American Dye Manufacturers Institute (ADMI) standard color measurement by applying the Adams-Nickerson color difference formula following method 2120E of the standard methods. The pH and redox potential (ORP) were monitored by a Eutech PH5500 dual channel pH/ion meter with specific probes. TOC was obtained with a total organic carbon analyzer from O.I. Analytical Aurora, model 1030. Besides, the degradation products were identified using Perkin Elmer FTIR spectrophotometer model, Spectrum One. Ions such as sulfate, nitrate, and nitrite were identified with ion chromatography (IC), Dionex ICS-1000.

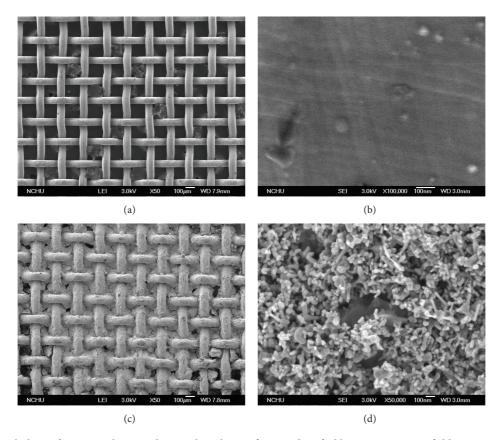


FIGURE 1: The morphology of ZnO powder coated on steel mesh at 150°C was identified by a JEOL 6330CF field emission scanning electron microscope (FESEM). (a) Bare steel mesh, 50 times enlargement. (b) Bare steel mesh, 100,000 times enlargement. (c) ZnO-coated steel mesh, 50 times enlargement. (d) ZnO-coated steel mesh, 50,000 times enlargement.

#### 3. Results and Discussion

3.1. Synergic Effect of Combining CCFL UV 365 Irradiation and ZnO Catalyst. The color removal was first compared for various systems, that is, UV/ZnO, UV alone, and ZnO alone, at the initial OG concentration of 50 mg L<sup>-1</sup>, ZnO dosage of 60 g m<sup>-2</sup>, and 6 CCFL lamps with total light intensity of 24 W and at wavelength of 365 nm in 120 min of reaction in the closed reactor. Figure 2(a) shows results of color removal by various systems. Results indicated that the system of UV alone and ZnO alone could not remove color at any significant level. The UV/ZnO system removed color effectively with 100% removal, in 120 min. It was also observed that the pH remained relatively constant from 5.5 to 5.0 with time. This was expected as ZnO is a known photocatalyst that, upon radiation with light whose wavelength is shorter than that of its bandgap, can generate electron-hole pair and hydroxyl radicals, strong oxidation agents that can oxidize a wide group of organic compounds nonspecifically. Figure 2(b) shows the UV spectra of OG at different reaction time periods. There were three major absorption peaks for OG dye, that is, 248, 330, and 479 nm. During the photocatalytic reaction, all three major absorption peaks were diminished. For example, at the wavelengths of 479, 330, and 248 nm, the original absorbance was 1.8514, 1.1891, and 2.4417, respectively. After 120 min of reaction, the absorbance of 479, 330, and

248 nm changed to 0, 0, and 0.0145, respectively. The figure illustrates the total removal of color by UV/ZnO system.

3.2. Effect of Preparation Temperature and Mixing Speed. The effect of steel mesh supported ZnO preparation temperature on color removal was studied at the initial OG concentration of 50 mg L<sup>-1</sup>, ZnO load dosage of 60 g m<sup>-2</sup>, and 6 CCFL lamps in 120 min in the closed reactor. Figure 3(a) shows insignificant color removal differences in the range of 100–300°C. It was noted that pH remained unchanged at around 5 to 6. The reaction kinetics of UV/ZnO photocatalytic system was suggested to follow the Langmuir-Hinshelwood (L-H) reaction kinetics. And, in most of the designed reaction conditions, the L-H kinetic model of the UV/ZnO system can be further simplified into pseudo-first-order reaction kinetics. Therefore, the color removal of this study was treated using pseudo-first-order reaction as follows:

$$C_{\rm dye} = C_{\rm dye,0} \times e^{-kt},\tag{1}$$

where k denotes the pseudo-first-order reaction rate constant (min<sup>-1</sup>), t is the reaction time (min),  $C_{\rm dye,0}$  designates the initial concentration (mg L<sup>-1</sup>) of OG, and  $C_{\rm dye,t}$  is the concentration (mg L<sup>-1</sup>) of OG at time t. The curve fitting of experimental results by (1) was shown in the figures as solid lines to demonstrate the consistence of kinetic model and

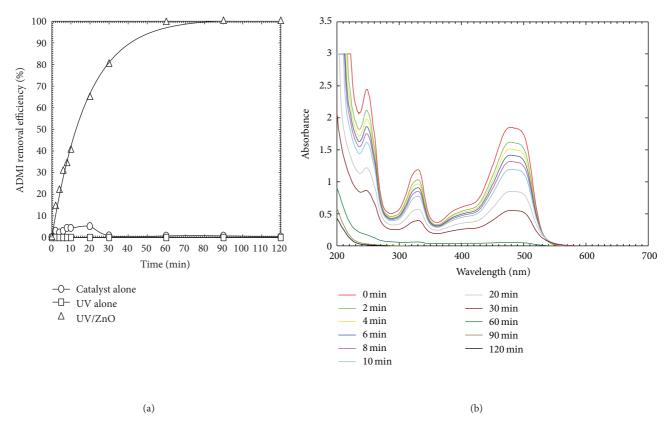


FIGURE 2: (a) Synergic effect of UV and ZnO on UV/ZnO photocatalytic system. (b) UV spectra of OG under UV/ZnO decolorization. The conditions were initial dye concentration of  $50 \text{ mg L}^{-1}$ , ZnO loading of  $60 \text{ g m}^{-2}$ , light intensity of  $2.1 \text{ mW cm}^{-2}$ , and reaction time during 120 min.

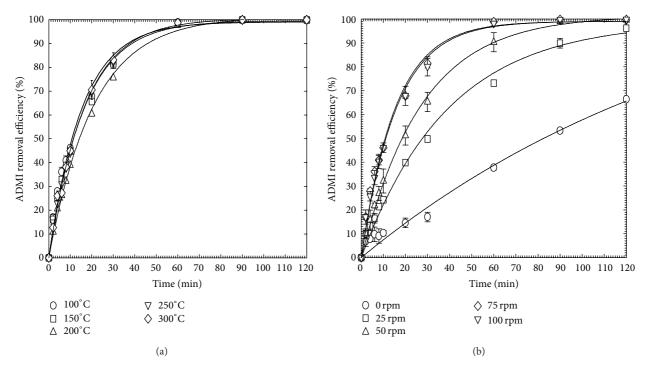


Figure 3: Effect of (a) preparation temperature and (b) mixing speed. The conditions were initial dye concentration of 50 mg  $L^{-1}$ , ZnO loading of 60 g m $^{-2}$ , light intensity of 2.1 mW cm $^{-2}$ , and reaction time during 120 min.

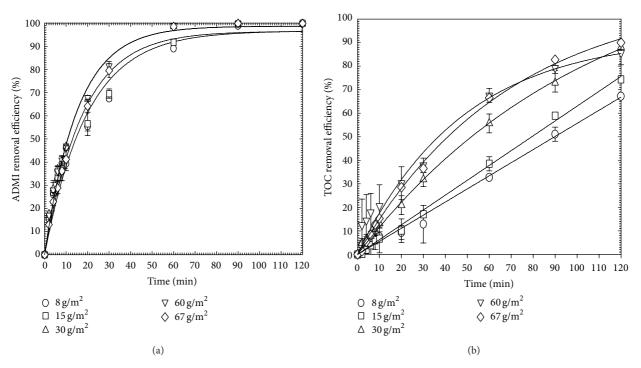


FIGURE 4: Effect of surface loading of ZnO. The conditions were initial dye concentration of  $50 \, \mathrm{mg} \, \mathrm{L}^{-1}$ , light intensity of  $1.05 \, \mathrm{mW} \, \mathrm{cm}^{-2}$ , and reaction time during  $120 \, \mathrm{min}$ .

experimental data. The calculated rate constants (from curve fitting) were 4.44, 4.37, 3.68, 4.32, and 4.57  $(10^{-2})$  (min<sup>-1</sup>) at 100, 150, 200, 250, and 300°C, respectively. The preparation temperature shows neglected effect on OG color removal. Preparation temperature of 150°C was chosen as the working condition for its low energy consumption and fast dyeing speed. Figure 3(b) shows the effect of mixing speed on color removal under UV/ZnO photocatalytic system. Mixing speed is definitely an important factor that affects the color removal efficiency. From the results, the higher the mixing speed is, the faster the decolorizing reaction can be obtained. The calculated rate constants (from curve fitting) were 0.60, 2.78, 4.44, and 4.32  $(10^{-2})$  (min<sup>-1</sup>) at 0, 50, 75, and 100 rpm, respectively. Therefore, the mixing speed was fixed at 75 rpm for further experimental runs. Since the photocatalytic degradation of OG happened on the surface of ZnO catalyst, the mass transfer of OG molecules from aqueous solution to the surface of ZnO catalyst was rather important to affect the reaction rate. The higher mixing speed caused better contact of OG molecules and ZnO catalyst and presented higher degradation rate of OG. However, when the mixing speed increased to higher than 75 rpm, the limited surface of ZnO cannot provide enough active sites for OG molecules. Therefore, the degradation rate of OG under UV/ZnO system hardly increased while the mixing speed was adjusted to higher than 75 rpm.

3.3. Effect of ZnO Load Dosage. Figure 4(a) shows the removal of color as a function of load dosage of ZnO under 1.05 mW cm<sup>-2</sup> of UV irradiation. Results indicated that the

color removal increased from 89 to 98.5% in 60 min when the surface loading of ZnO particles increased from 8 to 60 g m<sup>-2</sup>. The color removal then decreased from 98.9 to 98.5% when the surface loading of ZnO increased from 60 to 67 g m<sup>-2</sup>. An optimal ZnO loading for color removal occurred at 60 gm<sup>-2</sup>. However, the differences of color removal rate between various ZnO loads were not significant. The rate constants followed similar trend to percent color removal; the observed rate constants were 0.66, 0.67, 1.25, 2.94, and 2.98  $(10^{-2} \text{ min}^{-1})$ at surface ZnO loading dosages of 8, 15, 30, 60, and 67 g m<sup>-2</sup>, respectively. From Figure 4(b), the TOC removal was 67.2% for ZnO loading of 8 g m<sup>-2</sup> and increased up to 88.3% for ZnO loading of 60 g m<sup>-2</sup>. Results indicated that the TOC removal was highly affected by various ZnO loading dosages. On the other hand, ZnO dosage presented insignificant effect on color removal. To decolorize and mineralize simultaneously, one should choose higher ZnO loading to both color and TOC removal requirements.

3.4. Effect of UV Light Intensity. Theoretically, the higher the UV light intensity applied to a photocatalytic system, the faster the electron-hole pairs and OH• free radical form to obtain the higher dye decolorization and mineralization rate. Thus, the rate constant increases by UV intensity increase, while the same ZnO catalyst surface is loading. Since the photolysis of ZnO catalyst is enhanced to produce abundant electron-hole pairs and OH• in the dye solution to be used for decolorization, it is obvious that the more UV intensity employed to the system is, the faster the dye is decolorized.

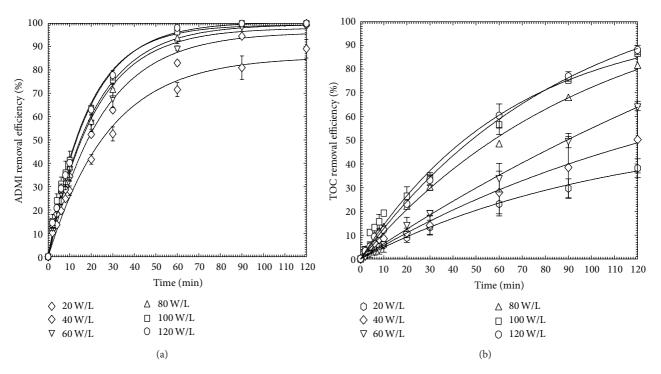


FIGURE 5: Effect of UV light intensity on OG (a) decolorization and (b) mineralization by UV/ZnO photocatalytic system. The conditions were initial dye concentration of  $50 \text{ mg L}^{-1}$ , ZnO-coated amounts of  $60 \text{ g m}^{-2}$ , and UV light intensity of 20 to  $120 \text{ W L}^{-1}$  ( $120 \text{ W L}^{-1}$  measured as  $2.1 \text{ mW cm}^{-2}$ ).

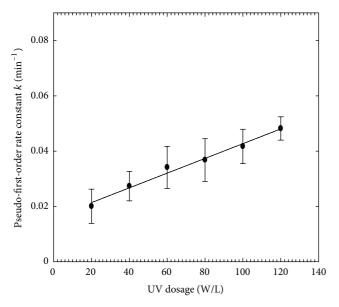


FIGURE 6: Effect of UV light intensity on pseudo-first-order rate constant of OG decolorization by UV/ZnO photocatalytic system. The conditions were the same as in Figure 5.

Figure 5(a) shows the removal of color as a function of UV intensity. Results indicated that the color removal increased from 71.6 to 98.8% in 60 min when the UV intensity increased from 20 to 120 W  $\rm L^{-1}$ . The rate constants followed similar trend to percent color removal; the observed rate constants were 2.01, 3.42, and 4.82 ( $10^{-2}$  min<sup>-1</sup>) at UV intensity

Table 2: The first-order reaction rate constant k ( $10^2 \,\mathrm{min}^{-1}$ ) for operating parameter of UV intensity and initial concentration.

Effect of UV inten	sity	Effect of initial concentration		
UV intensity, W $L^{-1}$ $k$		Concentration, $mg L^{-1}$		
20	2.00	12.5	20.14	
40	2.74	18.8	16.26	
60	3.42	25	17.55	
80	3.68	50	5.95	
100	4.17	75	5.88	
120	4.82			

which increased from 20, 60, and  $120\,\mathrm{W\,L^{-1}}$ , respectively, as shown in Table 2. Figure 5(b) presents the mineralization of OG in solution as a function of UV intensity. Results denote that the TOC removal increased from 38.2 to 88.3% in 120 min when the UV intensity increased from 20 to  $120\,\mathrm{W\,L^{-1}}$ . Therefore, applying sufficient UV intensity with ZnO photocatalyst can fairly mineralize portion of TOC to reach almost total mineralization.

Figure 6 shows the relationship between pseudo-first-order rate constants and UV light intensity that a linear relationship can be obtained. This presents that the UV light intensity is an important operating parameter which linearly affects the decolorization of OG under UV/ZnO photocatalytic system. In this work, the maximum UV light intensity was  $120~\mathrm{W}~\mathrm{L}^{-1}$ , which can be transferred into photo

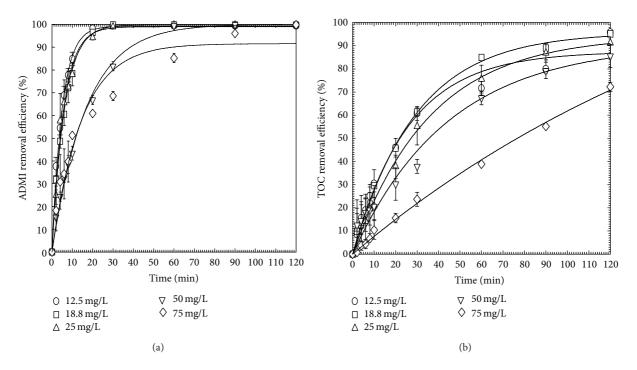


FIGURE 7: Effect of initial concentration on (a) ADMI color and (b) TOC removal. The conditions were ZnO-coated amounts of  $60 \, \mathrm{gm}^{-2}$ , light intensity of  $2.1 \, \mathrm{mW \, cm}^{-2}$ , and reaction time during 0– $120 \, \mathrm{min}$ .

flux density as  $2.1\,\mathrm{mW\,cm^{-2}}$ . From previous studies, photocatalytic reaction rate constant is linearly increased with UV intensity while operating in low region of UV intensity, that is, between 0 and  $20\,\mathrm{mW\,cm^{-2}}$  [17, 20]. The degradation of OG under UV/ZnO system was major caused by formation of OH• free radicals. From a previous study by Xiang et al., ZnO had the third highest formation rate of OH• free radicals following P25 and anatase  $\mathrm{TiO_2}$  [26]. Under higher UV irradiation intensity, the formation rate of OH• free radicals was higher. This caused faster degradation reaction of OG under UV/ZnO system.

3.5. Effect of Dye Initial Concentration. To present the validity of L-H model on our CCFL/ZnO system, the effect of initial dye concentrations on the photodegradation of azo OG dye was studied at initial concentrations of  $12.5-75 \,\mathrm{mg}\,\mathrm{L}^{-1}$ , ZnO dosage of 60 gm<sup>-2</sup>, and 6 CCFL lamps for a period of 120 min in the closed reactor. Figure 7 shows results of dye photodegradation as a function of reaction time at various initial dye concentrations. Results indicated that the rate of dye removal decreased from 20.1 to 5.95 ( $10^{-2} \,\mathrm{min}^{-1}$ ) when the initial dye concentration was increased from 12.5 to  $50\,\mathrm{mg}\,\mathrm{L}^{-1}$ , as shown in Table 2. The rate constant then remained constant and independent of the dve concentration as the initial dye concentration increased to greater than 50 mg L<sup>-1</sup>. This is typical Langmuir-Hinshelwood (L-H) reaction kinetics which is generally capable of modeling UV/ZnO photocatalytic oxidation process [27-30]. According to the

L-H reaction kinetics, the rate of dye degradation can be described by the following equation:

$$r = \frac{dC}{dt} = \frac{kK_AC}{1 + K_AC},\tag{2}$$

where r is the degradation rate of dye (mg L<sup>-1</sup> min<sup>-1</sup>) and k,  $K_A$ , and C are the rate constant (mg L<sup>-1</sup> min<sup>-1</sup>), equilibrium adsorption constant (L mg<sup>-1</sup>), and residual dye concentration (mg L<sup>-1</sup>), respectively. According to the above equation, at high dye concentration, that is,  $1 \ll KC$ , the rate equation is

$$r = k. (3)$$

Likewise, at low dye concentration, that is,  $1 \gg KC$ , the above equation (2) becomes

$$r = kK_AC. (4)$$

That is, as the initial concentration increases, the reaction no longer follows the first-order expression; it rather becomes independent of the dye concentration as shown in (3). By rearranging (2), one has

$$\frac{1}{r_0} = \frac{1}{kK_A} \times \frac{1}{C_0} + \frac{1}{k},\tag{5}$$

where  $r_0$  and  $C_0$  are the initial rate (mg L<sup>-1</sup> min<sup>-1</sup>) and initial dye concentration (mg L<sup>-1</sup>), respectively. A plot of the reciprocals of initial rate and initial concentration yields the rate

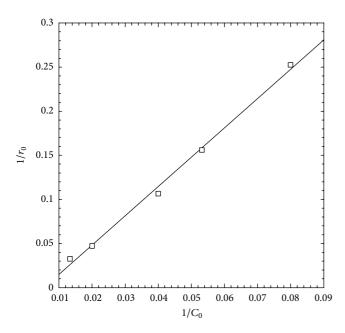


FIGURE 8: Langmuir-Hinshelwood kinetic model (ZnO loading dosage of  $60\,\mathrm{g\,m^{-2}}$  with light intensity of  $2.1\,\mathrm{mW\,cm^{-2}}$ ).

constant, k, and the adsorption constant, K (Figure 8). The initial rate  $r_0$  was calculated by the first 2 min of Figure 7 with ZnO loading dosage of 60 g m $^{-2}$ . From the slope  $(1/kK_A)$  and the intercept (1/k) of Figure 8, the calculated kand  $K_A$  were 54.35 mg L<sup>-1</sup> min<sup>-1</sup> and 0.0055 mg<sup>-1</sup> for ZnO loading dosage of  $60 \,\mathrm{g \, m^{-2}}$ . The rate constants (k) obtained in this work of  $54.35 \,\mathrm{mg \, L^{-1} \, min^{-1}}$  were higher than that of previous works [27-30] such as 1.66, 1.67, 0.95, and 0.17 mg L<sup>-1</sup> min<sup>-1</sup> for various dyes such as direct red 16, Remazol Black 5, Procion Red MX-5B, and indigo carmine, respectively. Similarly, the equilibrium adsorption constants ( $K_A$ ) of 0.0055 L mg<sup>-1</sup> from this work were in the range of previous studies, such as 0.0093, 0.072, 0.071, and  $0.78 \,\mathrm{Lmg}^{-1}$ , for various dyes as above. The results indicate that the photocatalytic degradation of Orange G by CCFL/ZnO process followed the Langmuir-Hinshelwood kinetic model with fairly good prediction of  $r^2 = 0.996$ .

3.6. Effect of pH. The effect of pH on the degradation of azo dye was conducted by adjusting the initial pH value of 5.0 to the range of 2 to 11 using HCl and/or NaOH with initial OG dye concentration of 50 mg L<sup>-1</sup> and 60 g m<sup>-2</sup> of ZnO dosage. Figure 9(a) shows OG dye removal as a function of time at various pH values. Results indicated that, at original pH, the color removal reached 78.5% in 30 min of photocatalytic reaction. At acidic pH of 2 and 3, the color removal rates of 76.7 and 76.1% were obtained, respectively. This implies that acidic pH provides no benefit for OG decolorization under UV/ZnO system. On the other hand, at alkaline pH of 11, the color removal rate sharply increased up to 95.6%. Figure 9(b) shows the TOC removal as a function of time at various pH values. Results indicated that, at original pH, the TOC removal reached 88.3% in 120 min of photocatalytic

Table 3: The first-order reaction rate constant  $k (10^2 \text{ min}^{-1})$  for operating parameter of pH and duration.

Effect of initial pH		Duration test		
pН	k	Cycle	k	
2	3.74	1	4.41	
3	3.74	2	3.95	
5	4.18	3	3.44	
9	3.69	4	3.33	
11	9.15	5	3.24	
		6	3.11	
		7	2.84	
		8	2.35	
		9	2.31	
		10	2.31	

reaction. At acidic pH of 2 and 3, the color removal rates of 70.1 and 82.8% were obtained, respectively. At alkaline pH of 11, TOC removal rate was 87.8%. This implies that the TOC removal rate is rather stable in the range of 82.8–88.3 for pH range 3–11. And for pH 2, an extremely acidic condition, the TOC removal dropped from 12–18% to 70.1%. Extremely acidic pH has disadvantage for TOC removal under UV/ZnO system for OG solution, since 0.1 N HCl solution was used to adjust solution pH value to 2-3. At this operating condition, there were abundant amounts of high concentration chloride ions in the solution to play the role of free radical scavenger. Chloride ions competed with OG molecules to consume free radicals. Therefore, the decolorization and mineralization rate of OG by UV/ZnO system decreased. The observed rate constants for various pH values were summarized in Table 3.

3.7. The Product Analysis by FTIR and IC. The change of functional groups of azo dye after photocatalytic treatment was surveyed. The initial dye concentration was  $50 \,\mathrm{mg} \,\mathrm{L}^{-1}$ and was treated with a ZnO dosage of 60 g m<sup>-2</sup> and reaction time of 120 min. The scan spectra (Figure 10(a)) for the functional groups are SO<sub>3</sub>Na of 1150~1250 cm<sup>-1</sup>, N=N of 1426, 1462 and 1495 cm<sup>-1</sup>, C=O of 1690~1760 cm<sup>-1</sup>, and C-H and N-H of 3300~3500 cm<sup>-1</sup>. After the photocatalytic oxidation (Figure 10(b)), a new double bond C=O at 1637 cm<sup>-1</sup> was produced. Meanwhile, the N=N from dye at 1426, 1463, and 1496 cm<sup>-1</sup> disappeared due to attack by the hydroxyl radicals that cleaved the double bond N=N. Accordingly, the dye molecule was degraded and decolorized. The ions such as sulfate, chloride, nitrite, and nitrate were determined. Figure 11(a) shows that the major ion concentration of sulfate significantly increased to 16 mg L<sup>-1</sup> over time. The chloride ion produced due to the impurity of OG dye was as low as 1.5 mg L<sup>-1</sup>. The nitrate ion concentration was about from 1.0 to 4.5 mg L<sup>-1</sup>, and nitrite concentration was less than  $0.5 \text{ mg L}^{-1}$  as shown in Figure 11(b).

3.8. Application Duration. The steel mesh supported ZnO catalyst was used repeatedly to treat the OG solution.

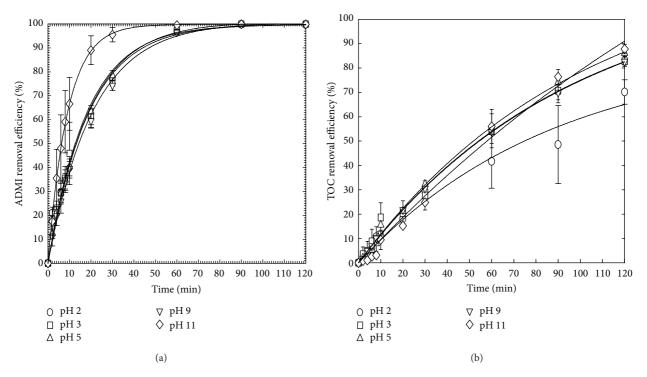


Figure 9: Effect of initial pH on (a) decolorization and (b) mineralization of OG under UV/ZnO system. The conditions were initial dye concentration of  $50 \text{ mg L}^{-1}$ , ZnO-coated amounts of  $60 \text{ g m}^{-2}$ , light intensity of  $2.1 \text{ mW cm}^{-2}$ , and reaction time during 120 min.

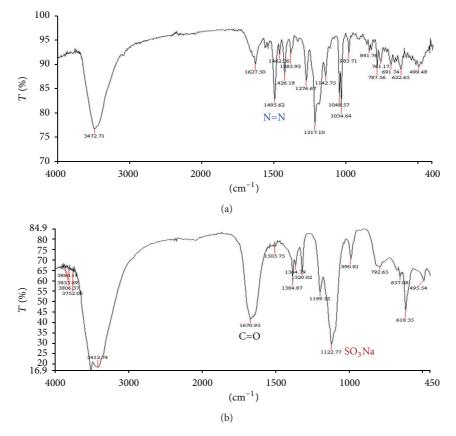


FIGURE 10: FTIR spectra for OG decolorization and demineralization (a) before and (b) after UV/ZnO photocatalytic degradation. The operating conditions were the same as in Figure 2.

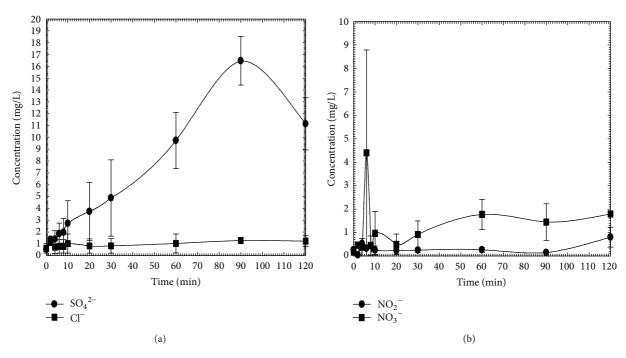


FIGURE 11: The product analysis by IC, (a)  $SO_4^{2-}$  and  $Cl^-$ , and (b)  $NO_3^-$  and  $NO_2^-$ . The conditions were initial dye concentration of 50 mg  $L^{-1}$ , ZnO-coated amounts of 60 g m<sup>-2</sup>, and light intensity of 2.1 mW cm<sup>-2</sup> at 120 min.

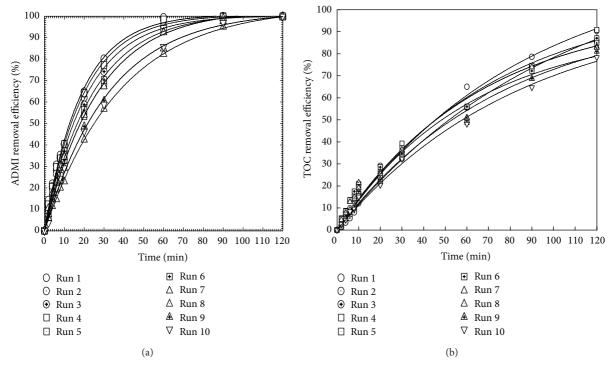


FIGURE 12: Duration test on (a) color and (b) TOC removal. The conditions were initial dye concentration of 50 mg  $L^{-1}$ , ZnO-coated amounts of 60 gm $^{-2}$ , light intensity of 2.1 mW cm $^{-2}$ , and reaction time during 120 min.

Figure 12 shows the system performance over 10 cycles. Results indicated that, although the rate of OG degradation decreased as the reuse cycle of catalyst increased, the total amount of dye removal remained relatively unchanged at 100% in the treatment time range of 100–120 min, however.

Instead of ADMI color, the TOC removal decreased from 90 to 78% after ten experimental runs. In the meantime, there was nearly neglected loss (0.04%) of ZnO in each operation even after 10 cycles according to the solution Zn concentration analysis by atomic absorption. The observed

rate constants declined with more reuse cycles as shown in Table 3 from 0.0441 to 0.0231 min<sup>-1</sup>, however. This can be attributed to potential surface poisoning of the photocatalyst, ZnO, due to adsorption of reaction products.

#### 4. Conclusions

Steel mesh supported ZnO catalyst illuminated with cold cathode fluorescent light (CCFL) UV was effective in the removal of ADMI color and TOC from the OG azo dye solution. Preparation temperature showed insignificant effect on color and TOC removal. An optimal ZnO surface loading or dosage of 60 g m<sup>-2</sup> exhibited the highest color removal as well as the fastest rate; further increase in surface ZnO loading had no benefit in increasing the color removal, however. An alkaline pH of 11 had the best photocatalytic oxidation rate; the rate of color removal was stable in the range from pH 3 to 9. At pH 2, the TOC removal rate was the lowest among all pH range. The rate of color removal decreased with initial dye concentration as was expected by the Langmuir-Hinshelwood kinetics. The rate of color removal increased with UV intensity linearly. The ZnO-coated steel mesh can be repeatedly used over 10 cycles without significant loss of catalyst mass; the percent dye removal remained close to 100% in 10 cycles except for about 50% decrease in reaction rate constants apparently due to possible surface poisoning. Based on FTIR analysis, there was decrease of N=N bonding which indicated chemical transformation of the dye OG compound. Results of analyzing the inorganic byproducts revealed that sulfate production was predominant; nitrite and nitrate were produced at minor quantities.

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## Review Article

# Fabrication, Modification, and Emerging Applications of TiO<sub>2</sub> Nanotube Arrays by Electrochemical Synthesis: A Review

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Titania nanotube arrays (TNAs) as a hot nanomaterial have a unique highly ordered array structure and good mechanical and chemical stability, as well as excellent anticorrosion, biocompatible, and photocatalytic performance. It has been fabricated by a facile electrochemical anodization in electrolytes containing small amounts of fluoric ions. In combination with our research work, we review the recent progress of the new research achievements of TNAs on the preparation processes, forming mechanism, and modification. In addition, we will review the potential and significant applications in the photocatalytic degradation of pollutants, solar cells, water splitting, and other aspects. Finally, the existing problems and further prospects of this renascent and rapidly developing field are also briefly addressed and discussed.

#### 1. Introduction

Nanostructured materials with peculiar properties are not expected in bulk phase and have already led to a breakthrough in various fields of science and technology. Moreover, much of the current interest in one-dimensional nanostructures, such as nanotube, nanowire, nanorod, and nanobelts, was initiated by the discovery of carbon nanotubes by Iijima et al. in 1991 [1]. Within these nanostructure materials, TiO2-based nanotubes attracted engrossing interest and intensive researches due to their merits of high specific surface area, ion-changeable ability, and photocatalytic ability. Over the past decades, nanostructured materials derived from TiO2 have extensively been investigated for many promising applications, including solar cells/batteries, selfcleaning coatings, electroluminescent hybrid devices, and photocatalysis, owing to their peculiar chemical and physical behaviors. Currently, developed methods of fabricating TiO<sub>2</sub>based nanotubes comprise the assisted-template method [2, 3], hydrothermal treatment [4-6], and electrochemical anodic oxidation [7–10]. Each fabrication method has unique

advantages and functional features and comparisons among these approaches. Regarding the template-assisted method, anodic aluminum oxide (AAO) nanoporous membrane, which consists of an array of parallel straight nanopores with controllable diameter and length, is usually used as template. However, the template-assisted method often encounters difficulties of prefabrication and postremoval of the previous templates and usually results in impurities. Concerning hydrothermal treatment, the self-assembled  ${\rm TiO_2}$  nanotubes are based on the treatment of Ti foils or TiO<sub>2</sub> powders in a tightly closed vessel containing highly concentrated NaOH solution (5-10 M) to obtain TiO<sub>2</sub> nanotube layer or TiO<sub>2</sub>based powder [6, 11]. These methods, other than the electrochemical anodic oxidation, are either not suitable for rapid production or notable to yield uniform TiO2 nanotubes with vertical alignment. The demonstrated architecture of TiO<sub>2</sub> nanotube arrays (TNAs) by a facile electrochemical anodizing process is capable of an ordered alignment with high aspect ratio and establishment of pure-phase TiO<sub>2</sub> structure in one step under ambient environment. More importantly, the electrochemical anodization technique allows the growth

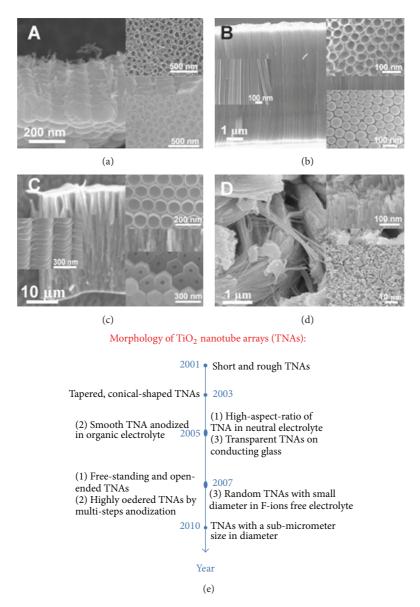


FIGURE 1: SEM images of TNA layers grown with different electrolytes. (a) Typical morphology obtained in acidic fluoride or HF electrolytes, (b) glycerol/fluoride electrolytes, and (c) ethylene glycol/fluoride electrolytes containing small amount of water. The insets show top views, bottom views, and side walls in detail. (d) Fluoride ions free electrolyte; these tubes grow in disordered bundles within seconds at comparably high anodic potentials. (e) Morphology of new type TNAs with time.

of other oxides with self-ordering nanostructures for several transitional and valve metals, such as Al, Zr, Hf, Nb, Ta, W, and Fe and their alloys TiAl, TiZr, TiNb, Ti<sub>6</sub>Al<sub>4</sub>V, and so on [8, 10].

In 1999, Zwilling et al. firstly reported the self-ordered TiO<sub>2</sub> nanostructures by a simple electrochemical anodizing process in a fluoride electrolyte [12]. Since then, several anodizing approaches, mainly focused on finding the optimal electrolyte and experimental parameters, have been explored to efficiently achieve high quality self-organized TNAs (Figure 1) [13–18], such as short and rough TNAs [13], tapered and conical-shaped TNAs [18], smooth and high-aspect-ratio TNAs [16, 17], transparent TNAs [19, 20], free-standing and

open-ended TNAs [21, 22], highly ordered TNAs by multistep anodization [23, 24], and TNAs with a submicrometer size in diameter [25, 26]. These results demonstrated that structure and morphology of TNAs, including tube diameter, length, wall thickness, and crystallinity, can be controlled by adjusting key parameters such as composition/shape of Ti substrate, electrolyte, pH, temperature, anodization voltage, current, and anodization time. It is, therefore, essential to understand the various factors influencing the characterizations of asprepared amorphous TNAs. Also, it should be noted that either the annealing posttreatment or the modification of  $\text{TiO}_2$ -based nanotubes would dominate the corresponding features and the performance of  $\text{TiO}_2$ -based devices. The aim

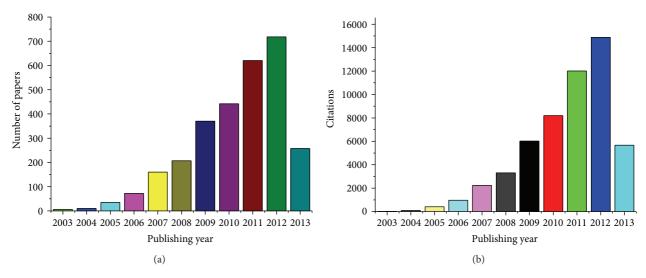


FIGURE 2: The number of articles (a) published on TNAs formed by electrochemical anodization and corresponding aggregated citations (b). (Statistics analysis was obtained from web of science database on May 30, 2013). Topic:  $TiO_2$  nanotube, with the exclusion of nanotube formed by hydrothermal, sol-gel, and template or carbon nanotube.

is to make the material more suitable for various applications that rely on specific electrical, optical, or chemical properties. In view of electronic properties, annealing to a crystalline structure mainly changes the conductivity and lifetime of charge carriers, while modification with active doping or band gap engineering by introducing other elements targets for the decreasing of the optical band gap, thus enabling a visible-light photoresponse [27].

Based on extensive literatures with regard to self-ordered TNAs, the authors have categorized three broad groups, preparation and formation mechanism, modifications, and applications, which are further subdivided according to their pertinent studies. First, the formation mechanisms and phenomenon of the electrochemical formation of nanopores and nanotubes by a self-ordering process are explained. Among the aforementioned experimental parameters, both electrolyte and anodizing voltage will be focused on and discussed. Then properties and modification of the TNA materials are addressed briefly, including technique examples of doping, noble metal decoration, and semiconductor composite which are to be discussed. Finally, the current stage of knowledge and recent studies on their potential applications, such as photocatalysis, solar cell, water splitting, and other aspects are introduced. Analysis of the physicochemical properties and recent advances in their modification and applications allow the identification of gaps in our knowledge and highlight the need for critical studies in the area of TNAs.

#### 2. Electrochemical Anodization of TNAs

This section presents recent developments on preparation of self-ordered  ${\rm TiO_2}$  nanoporous and nanotubular, focused primarily on TNAs by electrochemical synthesis. First, the related statistics of the paper about TNAs and phenomenon of the electrochemical formation of nanoporous  ${\rm TiO_2}$  materials

by a self-organization process is introduced. Then some experimental parameters of synthesis, which are responsible for regulation of the morphology of  ${\rm TiO_2}$  nanostructures, are considered. Finally, the formation mechanisms of TNA materials fabricated by electrochemical anodization are presented.

The progressively increasing research interest in the TNA layers formed by electrochemical oxidation can be easily seen from publication statistics (see Figure 2). Publication number and corresponding aggregated citations increased several times from the first work by Zwilling et al. [12], where only a tube length of a few hundred nanometers with a rough and high degree of disorder morphology could be obtained, to nowadays, where smooth and almost ideally hexagonally ordered arrays can be produced with individual nanotube lengths of hundreds of micrometers [22]. In other words, by controlling the electrochemical anodization parameters of Ti (temperature, potential ramping speed, applied potential, electrolyte species, electrolyte pH, viscosity, aqueous or organic electrolyte, etc.), one can obtain different titanium oxide structures such as a flat compact oxide, a disordered porous layer, a highly self-organized porous layer, or finally a highly self-organized nanotube layer (schematically shown in Figure 3(a)).

#### 2.1. Effects of Fabrication Factors on TNAs

2.1.1. Electrolyte. Hydrofluoric acid (HF) is the firstly and most widely studied electrolyte in titanium anodization to produce TiO<sub>2</sub> nanostructures. Since then, several optimized electrolytes of diverse acid/HF mixed electrolytes are put forward to successful fabrication of TiO<sub>2</sub> nanostructures [14]. A brief summary of various synthesis generations of TNAs is given in Table 1. However, the nanotube length in this first synthesis generation is limited to a few hundred nanometers. This second generation of TNAs was obtained with a remarkably high aspect ratio, in a neutral

Generation	Electrolyte type	Potential	Anodized time	Morphology	Main Factor	Reference
First generation: inorganic aqueous electrolytes (HF-based electrolyte)	0.5 wt% HF	10-23 V	≥20 min	Short nanotubes Length: 200–500 nm Diameter: 10–100 nm Wall thickness: 13–27 nm	Potential,	[13]
	0.3–0.5 wt% HF + 1 M H <sub>3</sub> PO <sub>4</sub>	1–25 V	2 h	Length: 20–1000 nm Diameter: 15–120 nm Wall thickness: 20 nm	electrolyte	[32]
Second generation: buffered electrolytes (F <sup>-</sup> -based electrolytes)	1 M Na <sub>2</sub> SO <sub>4</sub> + 0.1–1.0 wt% NaF	20 V	10 min–6 h	Roughwall with rings Length: $0.5-2.4 \mu m$ Diameter: $100 nm$ Wall thickness: $12 \pm 2 nm$	Potential, pH,	[28]
	$1 \mathrm{M} (\mathrm{NH_4})_2 \mathrm{SO_4} + 0.5 \mathrm{wt\%} \mathrm{NH_4F}$	20 V	15-30 min	Length: $0.5-1.0 \mu m$ Diameter: $90-110 nm$	time	[33]
Third generation: organic electrolyte containing F <sup>-</sup> ions	$0.5 \text{ wt\% NH}_4\text{F} + 0-5 \text{ wt\% H}_2\text{O} \text{ in glycerol}$	20 V	13 h	Smooth tube Length: $7.0  \mu m$ Diameter: $\approx 40  nm$ Wall thickness: $12 \pm 2  nm$	Potential, water content, time	[17]
Ü	0.1– $0.7$ wt% NH <sub>4</sub> F + $2$ – $3.5$ wt% H <sub>2</sub> O in ethylene glycol	60 V	216 h	Ultra-long tube Length: $1000 \mu m$ Diameter: $120 \pm 10 nm$		[22]
Fourth generation: fluoride-free electrolytes	$0.013\mathrm{MHClO_4}$	1 min	15-60 V	Disordered tubes Length: 30 μm Diameter: 20–40 nm	Electrolyte, time	[30]

TABLE 1: Brief summary of various synthesis generations of TNAs.

type of electrolyte containing fluoride ions, for example,  $Na_2SO_4/NaF$ ,  $(NH_4)_2SO_4/NH_4F$  [28, 29]. The reason for the tube-length increase is the limited dissolution on the top of nanotubes in the neutral electrolyte. The nanotubes by the above inorganic electrolyte were always accompanied with a rough external structure, that is, "rings" or "ripples", due to current oscillations along the anodization process. The thirdgeneration electrolyte, organic electrolytes with additions of fluoride salts, allows the construction of smooth and much taller TNAs to the regime of hundreds of micrometers. To date, the highest tube lengths can be up to  $1000 \,\mu m$  in organic viscous electrolytes [22]. The pH of the electrolyte and the amount of water greatly influence the morphology, structure, and growth rate of the as-formed TiO<sub>2</sub> nanotube. Recent synthesis development of TNAs by using fluoride-free electrolytes is commonly considered as the fourth generation. The results of this rapid breakdown anodization (RBA) are also bundles of disordered nanotubes that grow within very short times (several minutes) [30, 31]. Depending on electrolyte nature, each electrolyte provides a unique geometrical feature of the nanotubes and consequently varying surface properties; thereby, a selection of electrolyte medium for the TNA fabrication is a primary concern.

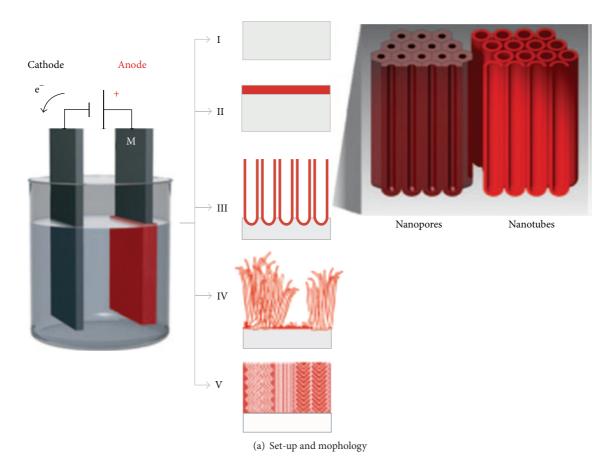
fluoride-free electrolytes

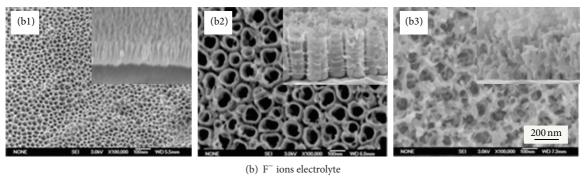
2.1.2. Voltage. The anodization voltage influences the morphology of formed nanostructures [34]: pores instead of tubes grow at low voltages of 5 V (Figure 3(b1)), while, at voltages higher than 8 V, the diameter of the TiO2 nanotubes is also influenced linearly by the applied voltage (Figure 3(b2)).

However, at high anodization voltages (>50 V), breakdown events can be observed inside the nanotube resulting in formation of sponge-like structures (Figure 3(b3)). At even higher anodization voltages (>80 V), electropolishing of the samples would take place at a high current density (>100 mA cm<sup>-2</sup>) in this electrolyte. Therefore, the retardation of breakdown events taking place is vital for the creation of a larger tube diameter. Yin et al. reported that TNAs with larger diameter about 600 nm can be obtained in ethylene glycol electrolytes containing 0.09 M ammonium fluoride and 10 vol% water [35]. Albu and Schmuki further increase the tube diameter to reach 800 nm. However, these tubes are not highly organized and seem loosely assembled in a mesoporous matrix rather than in a neatly defined nanotube array [36]. Recently, Ni et al. successfully demonstrated welldefined, large diameter (680-750 nm) TNAs, with the most uniform and clean morphology by using a higher voltage regime of up to 225 V [25].

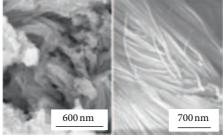
Diameter: 20-40 nm Wall thickness: 10 nm

2.1.3. Other Factors. In addition to the vital factor of the electrolyte and voltage to the high aspect ratio of the as-prepared nanotube, anodizing time and step, fluoride concentration, and pH and temperature also have a great synergistic effect on the morphology, structure, growth rate, crystallization, and even photoelectrochemical properties of the as-prepared TNAs [8, 37-42]. For example, the transition from porous TiO<sub>2</sub> to a nanotubular structure is not only dependent on water content [43, 44] but also depends on the anodization voltage. The applied voltage directly determines the tube





.



(c) F ions free electrolyte

FIGURE 3: The electrochemical anodization process and typical morphologies: (a) (I) metal electropolishing, (II) formation of compact anodic oxides, (III) self-ordered oxides (nanotubes or nanopores), (IV) ordered nanoporous layers, and (V) rapid (disorganized) oxide nanotube formation. Examples of morphologies of obtained structures: (b) classical ordered  ${\rm TiO_2}$  nanopores (b1), nanotubes (b2), sponge-like nanoporous structures (b3) anodized in  ${\rm F^-}$  ions containing electrolyte, and (c) disordered  ${\rm TiO_2}$  nanotubes growing in bundles anodized in  ${\rm F^-}$  ions free electrolyte.

diameters but also strongly influences the rate of TNAs growth, length, and crystallization.

2.2. Growth Mechanism of Anodized TNAs. Self-organized oxide tube arrays or pore arrays can be obtained by an anodization process of a suitable metal, such as transitionmetal and valve metal. When metals are exposed to a sufficiently anodic voltage in an electrochemical configuration, an oxidation process will be initiated. Depending mainly on the electrolyte and the particular anodization parameters, essentially three possibilities for reactions exist (see illustration of Figure 3(a)): (I) the metal is continuously dissolved (metal corrosion, or electropolishing), (II) the metal titanium ions (M<sup>n+</sup>) formed react with O<sup>2-</sup> (provided by H<sub>2</sub>O in the electrolyte) and forma compact oxide layer, and (III) under some electrochemical conditions, competition between dissolution and oxide formation is established leading to porous structures. Under even more specific experimental conditions, a situation is established where self-organized growth of TNAs, formation of thick self-organized mesoporous layers ((IV) in Figure 3(a)), or disordered rapid-breakdown anodization (RBA) of nanotube bundles ((V) in Figures 3(a) and 3(c)) can be observed [10].

In general, it can be concluded that all investigated organized oxide structures grown by anodization in fluoridecontaining electrolytes on different metals or alloys seem to follow the same growth mechanism and influence by key factors [7, 8, 10]. Ti was firstly oxidized to form a thin barrier oxide layer of TiO<sub>2</sub> due to interaction of the metal with O<sup>2-</sup> or OH<sup>-</sup> ions. Then, the presence of electric field and fluoride ion led to the creation of random pits and small pores. Finally, self-ordered TNAs formed resulted from the allowance of optimal pores to grow continuously and thicker wall to split by chemical dissolution. The tube diameter is determined by the anodization voltage, etching of the tubes (and thus the achievable length of the tubes) depends on the chemical resistance of the oxide against fluoride etching (in a particular electrolyte), and water plays the key role for providing the oxygen source for tube growth, splits pores into tubes, and is responsible for sidewall rings formation. Obviously, anodization techniques in fluoride-containing electrolytes allow the fabrication of nanostructured oxide layers on an extremely wide range of valve metals and alloys that enable the controllable fabrication of mixed nanostructured oxides with virtually endless possibilities to create enhanced properties and therefore have also a very high and widely unexplored technological potential.

#### 3. Modification of TNA

TiO<sub>2</sub> semiconductor material plays the most important role owing to its excellent chemical and physical properties. However, the higher band gap of the annealed TiO<sub>2</sub> between the valence band (VB) and conduction band (CB) makes them inactive under visible irradiation (Figure 4(a)). In this regard, great efforts have been made to extend the absorption of the wavelength range into the visible light range via the modification of its electronic and optical properties.

Over the past decade, considerable effort has gone into the modification of TiO<sub>2</sub> to exploit the solar spectrum much better. For example, dye sensitization and doping TiO<sub>2</sub> using either nonmetal anions or metal cations is one of the typical approaches that have been largely applied (Figure 4(b)). Coupling TiO<sub>2</sub> with a narrow band gap semiconductor represents another approach (Figure 4(c)). Decoration of noble metal particles with surface plasmon effects allows for more efficient charge transfer (Figure 4(d)). In all of these cases, essentially three beneficial effects are expected: (1) to promote the photogenerated separation between the electron hole (e<sup>-</sup>/h<sup>+</sup>) and to prevent their recombination, (2) surface plasmon effects, leading to field enhancement in the vicinity of noble metal particles and thus allowing more efficient charge transfer and effective visible light absorption, and (3) heterojunction formation that either changes the band bending (metal clusters on semiconductor) or provides suitable energy levels for synergic absorption and charge separation for enhanced utilization of solar energy.

3.1. Doping. Doping or sensitizing pure  $TiO_2$  by introducing a secondary electronically active species into the lattice for sensitizing TiO2 to visible light, which promotes the harness of the main range of the solar spectrum and also can ensure the charge trapping for effective photogenerated carries separation (Figure 4(b)). Asahi et al. firstly reported that the nitrogen doping on TiO<sub>2</sub> by sputtering in nitrogen containing gas mixture improves the photoelectrochemical reactivity under visible light irradiation [45]. In the following years, other doping species, such as a number of nonmetals like carbon [46], fluorine [47], sulphur [48], and boron [49], have been introduced into TiO<sub>2</sub> by using various techniques. The results indicated that the visible light absorption and photoelectrochemical activities of these doped crystallized TNAs were not only influenced by the energy gaps and the distributions of impurity states but were also affected by the locations of Femi levels and the energies of band gap edges [50, 51]. Among all these anions, the doping of TNAs with nitrogen or carbon has been found to receive significant attention [52-59]. Highly promising N-doping approach for TNAs includes one-step direct electrochemical anodization of a TiN alloy or growing TNAs in a solution containing doping species [59]. High-energy ion implantation or sputtering in an atmosphere of doping species following an annealing process has been verified to be an effective doping method [60, 61]. However, these methods require special high energy accelerators be operated in a high vacuum environment and the doping depth be limited to several micrometers. Thermal treatment of TNAs in gas atmospheres of the doping species is regarded as a facile one-step doping technique [62, 63]. Moreover, such surface-modified nanotubes shows a significant photoresponse in the visible range compared to nonmodified nanotubes.

At the same time,  ${\rm TiO_2}$  doped with transition metal cations (e.g., Fe, V, Cr, and Mn) [64–66] have also been reported to widen visible light absorption range, increase the redox potential of the photogenerated radicals, and enhance the conversion efficiency by extending the life of photogenerated electrons and holes. Although the metal cation doping of

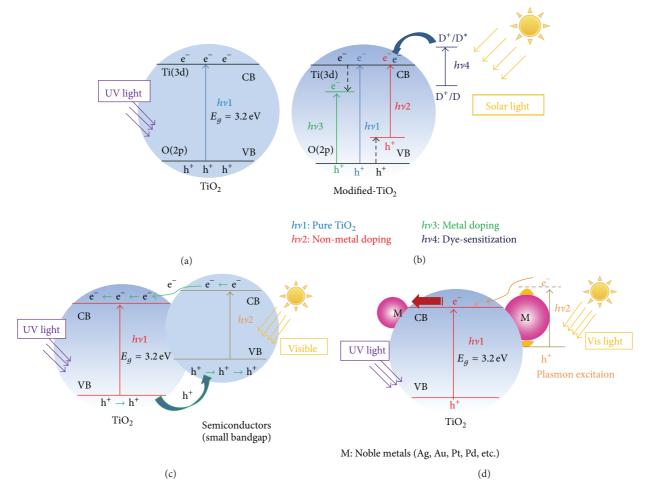


FIGURE 4: Schematic of energy level of pure  $TiO_2$  (a) and corresponding modification ((b)–(d)). (b) Doping or dye-sensitization, semiconductors (c), and noble metals (d) coupling.

 ${
m TiO_2}$  improves the visible light absorption of the host material to increase photocatalytic activity, a large amount of research also concluded that, when the doping content is excessively high, extra defects can also act as recombination centers to decrease the photocatalytic activity. This adverse effect could be avoided by a suitable doping amount or annealing the doped  ${
m TiO_2}$ .

3.2. Semiconductor Composites. In the past decade, many efforts have been devoted to extend the light absorption range of TNAs and to alleviate the charge carrier recombination, such as formation of semiconductor heterostructures with visible light excited narrow band gap semiconductors (Figure 4(c)), for example, CdS, CdSe, and so forth [67–69]. However, it must be expected that the stability of many applied narrow band gap semiconductors fails quickly, not only due to corrosion or photocorrosion, but also due to instability of some of the materials under applied voltage [70].

TNAs essentially provide a very versatile tool to fill or decorate other semiconductors to form composite electrode [71–73]. One of the most followed-up schemes to establishing p-n heterojunctions for high efficient photoelectrocatalytic devices is the direct deposition of p-type semiconductor onto TNAs [74, 75]. For example, Wang et al. prepared Cu<sub>2</sub>O/TiO<sub>2</sub> p-n heterojunction photoelectrodes by depositing p-type Cu<sub>2</sub>O nanoparticles on n-type TiO<sub>2</sub> nanotube arrays via an ultrasonication-assisted sequential chemical bath deposition (Figures 5(A)–5(D)) [76]. The largely improved separation of photogenerated electrons and holes was revealed by photocurrent measurements. Consequently, p-n Cu<sub>2</sub>O/TiO<sub>2</sub> heterojunction photoelectrodes exhibited a more effective photoconversion capability than single TiO<sub>2</sub> nanotubes (Figure 5(E)). Furthermore, Cu<sub>2</sub>O/TiO<sub>2</sub> composite photoelectrodes also possessed superior photoelectrocatalytic activity and stability in rhodamine B degradation with a synergistic effect between electricity and visible light irradiation (Figures 5(F)–5(H)).

 ${\rm TiO_2}$  nanoparticle decoration on TNAs can be obtained by slow hydrolysis of  ${\rm TiCl_4}$  precursors [20]. In DSSCs, the TNAs decorated with  ${\rm TiO_2}$  nanoparticles show higher solar cell efficiency in comparison to pure TNAs. The  ${\rm TiO_2}$  nanoparticles can be deposited inside as well as outside of the tube wall by hydrolysis of a  ${\rm TiCl_4}$  solution, which significantly increases the surface area and thereby improves the solar-cell efficiency [77].

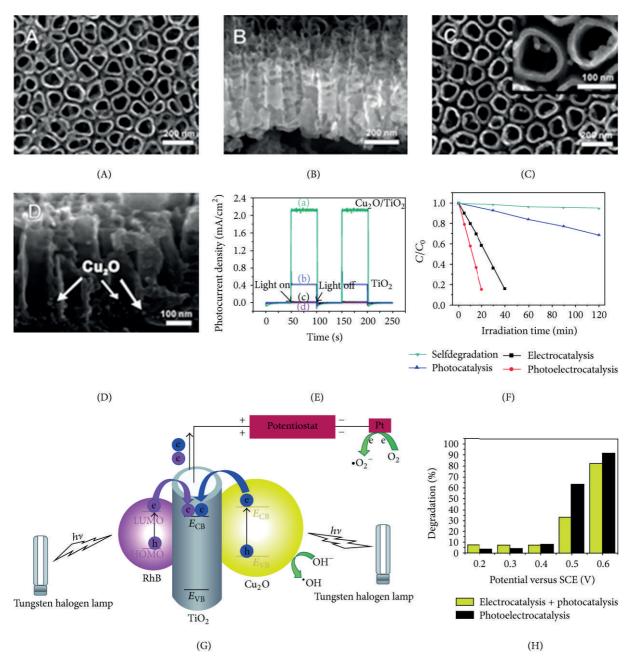


FIGURE 5: SEM image of TNAs (A, B) and  $Cu_2O/TiO_2$  NTAs (C). TEM image of  $Cu_2O/TiO_2$  NTAs (D). (E) Photoresponse of  $Cu_2O/TiO_2$  NTAs (a, c) and TNAs (b, d) with (a, b) or without (c, d) a bias potential of 0.5 V (versus SCE) under one sun visible light irradiation. (F) Comparison of photocatalytic, electrocatalytic, and photoelectrocatalytic degradation of RhB under visible light irradiation for  $Cu_2O/TiO_2$  NTAs. (G) Schematic illustration of photoelectrocatalytic degradation of RhB under visible light irradiation. (H) Comparison of RhB degradation efficiency using  $Cu_2O/TiO_2$  NTAs in the process of photoelectrocatalysis (right) with the sum of photocatalysis and electrolysis (left).

3.3. Noble Metal Nanoparticles Decoration. Another approach related to  ${\rm TiO}_2$  modification is the decoration of  ${\rm TiO}_2$  surfaces with noble metal nanoparticles (such as, Ag, Au, Pt, Pd, or alloys). Noble metal loading is proved to be an effective way to restrain the recombination of photogenerated electron/hole pairs resulting in photoelectrocatalytic activity enhancement (Figure 4(d)) [78–83]. Moreover, recent study reveals that noble metal nanoparticles can improve the photoresponse ability of  ${\rm TiO}_2$  in the visible region based on

the surface plasmon resonance (SPR) [84, 85]. It is known that the free electrons of metal can collectively oscillate induced by light irradiation; when the oscillation frequency of light electromagnetic field is in accordance with the free electrons, the SPR effect is generated and light energy is coupled to the metal nanoparticles in the meantime. For example, Ag nanoparticles can be deposited on the tube wall by a photocatalytically reducing process on a TiO<sub>2</sub> surface with UV illumination [86]. Other metal nanoparticles

are preferably deposited by UHV evaporation, sputtering, or chemical/electrochemical deposition techniques [78, 87]. Pt/TiO<sub>2</sub> or Pd/TiO<sub>2</sub> nanotubes also shows a significantly higher photocatalytic activity and water splitting performance compared with plain nanotubes [79, 80].

3.4. Other Aspects. More recent work deals with decoration with grapheme [88, 89], Ag/AgCl [85], or AgBr [90] onto  ${\rm TiO_2}$  to enhance their photocatalytic activity. Amorphous nanotubes synthesized by room-temperature electrochemical anodization are also reported to be annealed in oxygenrich (O<sub>2</sub>), oxygen-deficient (Ar, N), and reducing (H<sub>2</sub>) environments, to modify  ${\rm TiO_2}$  crystal structure, morphology, and electronic properties.

#### 4. Applications of TNA Materials

Porous and tubular titanium dioxide nanostructures have attracted great interest because of their applications in photocatalysis, photovoltaic cells (solar cell), water splitting, biomedical scaffold, wetting template, and other aspects. This porous  ${\rm TiO_2}$  material is desirable for these applications because of its multifunctional semiconductor properties that are based on its excellent physical and chemical behavior, along with its specific nanostructured architecture that owns it high surface area, high surface activity and fast carries transfer path.

4.1. Photocatalyst. One of the most practical applications of  ${\rm TiO_2}$  today is in photocatalytic toxic pollutant decomposing. After Fujishima and Honda reported for the first time on light-induced water electrochemical photolysis on  ${\rm TiO_2}$  surfaces, this functional semiconductor material has been intensively investigated for applications in heterogeneous catalysis [91]. Since then,  ${\rm TiO_2}$  has shown to be an excellent photocatalyst due to the fact that the material has a set of good properties of long-term stability, low-cost preparation, and a strong enough oxidizing power to be useful for the decomposition of unwanted organic compounds [92–96].

The basic principles involved in the photocatalytic mechanism are shown in Figure 6. UV light promotes electrons excited from the valence band to the conduction band, and then separated holes and electrons will be transported to the semiconductor-environment interface and react with adsorbed molecules. In aqueous solution, highly reactive \*OH radicals are generated by charge exchange at the valence band ( $\rm H_2O + h^+ \rightarrow {}^*OH$ ), whereas excited electrons at the conduction band mainly reduce dissolved molecular oxygen to super-oxide anions ( $\rm O_2 + e^- \rightarrow \rm O_2^-$ ). These \*OH radicals and  $\rm O_2^-$  ions are able to virtually oxidize all organic materials to  $\rm CO_2$  and  $\rm H_2O$ .

Among many  ${\rm TiO_2}$  nanotubes preparation strategies, the electrochemical anodization process as a simple, cheap, and rapid growth method has been widely utilized to large-scaled preparation of  ${\rm TiO_2}$  nanotubes with controllable size and morphology [13, 15, 28]. However, smooth surface, relative low surface area, and the amorphous structure of the obtained anodic  ${\rm TiO_2}$  nanotubes result in low light utilization efficiency and photogenerated charges separation efficiency,

thus leading to the poor photocatalytic activity [92]. Many efforts have been made to enhance the photocatalytic activity of the anodic TiO<sub>2</sub> nanotubes. For example, annealing of anodic TiO<sub>2</sub> nanotubes in conventional air environment contributes to converting the amorphous TiO<sub>2</sub> into anatase, which can efficiently enhance the photocatalytic performance [93]. In order to achieve maximal decomposition efficiency, in addition to crystallized TNAs with adequate band edge positions, rapid charge separation, and high quantum yield, a large area of the catalyst is desired. Crystallized TNAs with suitable posttreatment processes fit these requirements comparably well [92-94, 97]. In previous work, we used anatase TNAs as the photoanode and verified that such novel TNAs showed higher efficiencies than common TiO<sub>2</sub> nanoparticle photocatalysts (Figures 6(b)-6(d)) [93]. Moreover, the annealing temperature has also greatly influenced the crystal structure and photocatalytic activity of TNAs [96, 98, 99].

Up to today, many posttreatment methods for the construction of high efficient TNAs photocatalyst, such as annealing in specific gas atmosphere [100, 101], hydrothermal treatment [102, 103], and vapor-thermal treatment [104], have been generally used to synthesize special crystallized TNAs with high devices performance. Annealing the anodic TNAs through a derivative annealing method in a sealed container with specific environments, such as oxygen-rich (O<sub>2</sub>), oxygen-deficient (Ar, N), and other reducing (H<sub>2</sub>) gas, can modify the TNAs crystal structure, morphology, and electronic properties and influence the photocatalytic performance [105–107]. However, this method is expensive and has high energy consumption. Recently, considerable efforts have been shifted to the construction of hierarchical architectures based on the 1D TNA nanostructure templates. For example, a simple hydrothermal treatment was adopted to reduce the heat treatment temperature for the construction of anatase TiO2 nanostructure due to a dissolutionrecrystallization transformation of amorphous anodic TNAs, and the resultant hierarchical TiO<sub>2</sub> structures decorated with TiO<sub>2</sub> nanoparticles possess a higher surface area than that of smooth TNAs, which showed enhanced photocatalytic performance [103]. Compared to the heteroelement doping (e.g., N, F, and C) of TNAs, very recently, in situ self-doping with homospecies (e.g., Ti<sup>3+</sup>, and H<sup>+</sup>) by an electrochemical reduction treatment has been emerging as a rational solution to enhance TiO2 photoactivity within both UV and visible light regions [105]. Despite the great efforts contributed by many groups, well-designed posttreatment strategies for constructing desired crystalline structures with high surface area and anatase phase for highly efficient pollutant degradation have still been an attractive ongoing task.

In addition to many posttreatment methods of the anodic TNAs, the direct decoration of noble metal or semiconductor nanoparticles on crystallized TNAs is also verified to be beneficial for photocatalytic activity enhancement [78, 86, 97, 108, 109]. For example, we reported that a pulse current deposition of Ag nanoparticles modified TNAs was used as the photoanode for photoelectrocatalytic decomposition of methyl orange (MO) pollutant [108]. In this case, we found

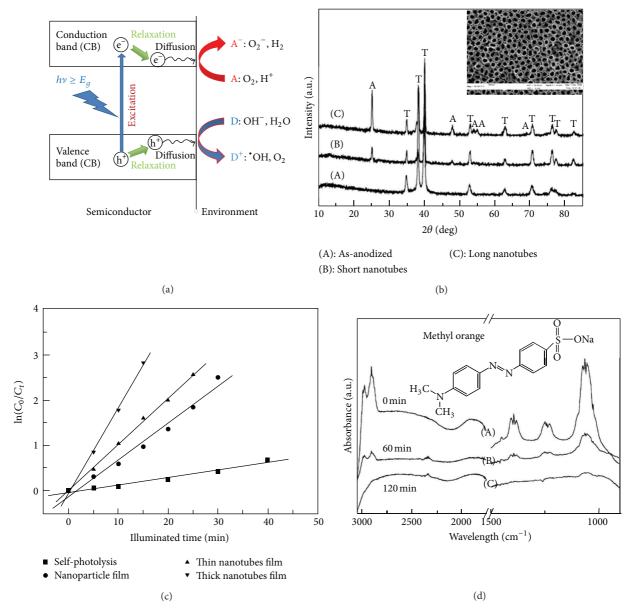


FIGURE 6: (a) Scheme of photo-induced processes at a  $TiO_2$  semiconductor/electrolyte interface. Light ( $h\nu$ ) excites valence band electron to conduction band. Electrons and holes react with environment acceptor (A) and/or donor (D). (b) XRD patterns of TNAs film. (c) Comparison of photocatalytic degradation rates of MO for nanoparticle film and two different thicknesses of nanotubes films (A) under the high-pressure mercury lamp illumination. (d) ATR–IR spectra of MO before and after photocatalytic degradation.

that photocatalytic activity of titania nanotube layers can be significantly increased by applying an external bias [108]. Xie et al. performed photocatalytic decomposition of a model organic pollutant (methylene blue) in self-organized TNAs decorated with Ag and CdS nanoparticles. The CdS-Ag-TiO $_2$  three-component nanotube arrays system exhibited superior synergy effect on both photoelectrochemical and photocatalytic activities compared to those of the pure  ${\rm TiO}_2$  and Ag or CdS modified  ${\rm TiO}_2$  systems [109].

4.2. Solar Cells. One of the most promising applications of  ${\rm TiO_2}$  today is in dye-sensitized solar cells (DSSCs), a concept

introduced by O'Regan and Grötzel in 1991 [110]. The classical DSSCs operate with sintered or compressed nanoparticulate  ${\rm TiO_2}$  layers as electron harvesting material. Compared to agglomerate  ${\rm TiO_2}$  nanoparticle layer containing a high number of grain boundaries that can act as recombination sites, the new architecture of TNAs by electrochemical anodization has been verified to be an ideal photoanode in photoelectrocatalytic devices due to its improved charge-collection efficiency and short pathway for the photogenerated excitons along the vertically aligned tubes to the conducting substrate. As such, it may be expected that optimized TNAs can significantly increase the solar energy conversion efficiency.

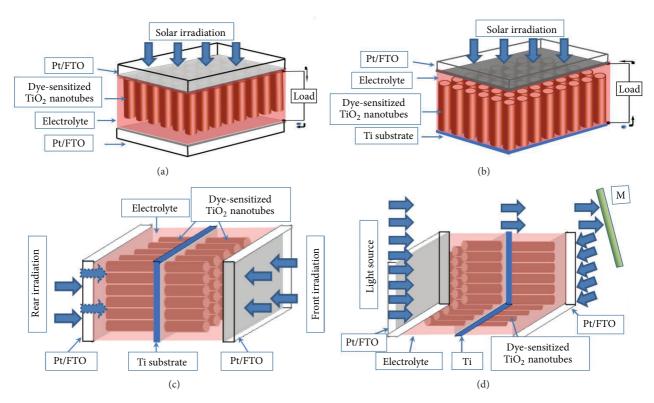


FIGURE 7: Schematic illustration of front-side illuminated DSSC based on transparent TNAs on FTO substrate (a), backside illuminated DSSC based on TNAs on Ti substrate (b), two light sources illuminated DSSC based on both sides of TNAs on Ti substrate (c), and parallel configuration DSSC with one light source irradiation on double-sided TNAs by using a dielectric mirror (d).

4.2.1. Dye-Sensitized Solar Cells (DSSCs). Owing to welldefined structural parameters and enhanced electronic properties, highly ordered TNAs have been employed to substitute TiO<sub>2</sub> nanoparticles for use in DSSCs [111]. Mor et al. reported the integration of TiO<sub>2</sub> nanoparticles modified transparent nanotube array (360 nm in length) architecture in fluorinedoped tin oxide (FTO) glass for front-side illuminated dye solar cell and displayed a photoconversion efficiency (PCE) of 2.9% (Figure 7(a)) [20]. They also observed that solar cells constructed by longer nanotubes formed from titanium foils (backside illumination) have superior charge transfer efficiency and more dyes absorption in comparison with solar cells fabricated with transparent short nanotubes formed on FTO glass. However, the overall power conversion efficiency of dye-sensitized TNA solar cells remained relatively low as a result of incomplete coverage of dye molecules on the TNAs and insufficient infiltration of electrolyte into nanotubes. For example, backside illuminated N719 DSSC based on 6 µm long TNAs film on titanium substrate shows a PCE of 4.24% under AM 1.5 sunlight source (Figure 7(b)) [112]. To further improve the performance of dye-sensitized TNA solar cells, efforts have been directed toward the improvement of dye loading, charge transport, light absorption, and optimization of TiO<sub>2</sub> nanostructures [77, 111, 113-115]. Recently, Liu and Misra applied double-sided TNAs for bifacial dye-sensitized solar cells and reported that a photocurrent density of such bifacial DSSCs was almost twice that of one-sided illumination (Figure 7(c)) [115]. Sun et al. demonstrated a new

parallel configuration of DSSCs using double-sided TNAs as the photoanode and a dielectric mirror for sunlight to be irradiated on both sides of TNA photoanode (Figure 7(d)) [116]. An average 70% increment in photocurrent and 30% enhancement in PCE were obtained relative to those of the single cells. Zheng et al. constructed a layer-by-layer hierarchical photoanode consisting of  ${\rm TiO_2}$  particles and free-standing TNAs for DSSCs with a PCE of 8.80%, which exhibited increased light-harvesting efficiency, longer electron lifetimes, and more efficient electron extraction than those in single particle film or nanotube array based devices [117].

4.2.2. Quantum Dots Sensitized Solar Cells (QDSSCs). Typically, CdX (X = S, Se, and Te) QDs with size-dependent band gaps provide new opportunities for harvesting light energy yin the visible and infrared regions of solar light [118]. In addition, through the impact ionization effect, it is possible to generate multiple excitons from single-photon absorption in QDs [119]. In the case of the QDSSCs, excited electrons of CdX nanocrystals are injected into a large band gap semiconductor (e.g., TiO<sub>2</sub> and ZnO), and holes reacted with a redox couple. Recently, Sudhagar et al. prepared the CdS/CdSe coupled TiO<sub>2</sub> nanofibrous electrode with a maximum PCE of 2.69% [120], while Shen et al. fabricated a CdSe QDs-sensitized TNAs photoelectrode with an optimal photovoltaic conversion efficiency of 1.80% [121]. Recently, we report that a PCE of 2.74% is achieved on novel QDSSCs

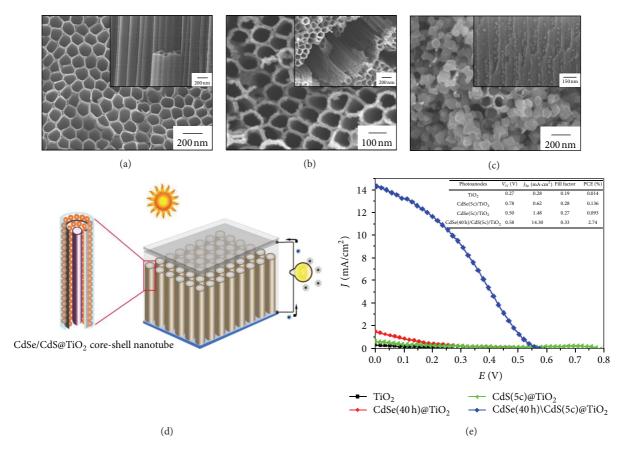


FIGURE 8: Top view and cross-sectional SEM images of TNAs (a), CdS@TNAs (b), and CdSe/CdS@TNAs (c). (d) Schematic of CdSe/CdS@TNAs for QDSSC. (e) J-V characteristics of corresponding QDSSCs.

based on the CdS/CdSe QDs cosensitized TiO<sub>2</sub> nanocrystal arrays by a sealed annealing process (Figure 8) [67]. We found that such coupled CdS/CdSe QDSSC exhibited a greatly enhanced short-circuit current density (Figure 8(e)) as compared to pure TNAs and single CdS or CdSe QDSSC because the combination of CdS and CdSe QDs has a complementary effect in light harvest and surface area increment, and a stepwise band edge level structure of CdSe/CdS@TNAs beneficiated for electron injection into TNAs. Sun et al. reported a novel CdS QDs sensitized TNA photoelectrodes by a sequential chemical bath deposition technique and found that the CdS QDs among the TNAs significantly increased the QDSSC efficiency up to 4.15% [122]. These results clearly demonstrate that the unique nanotube structure can facilitate the propagation and kinetic separation of photogenerated charges, suggesting potentially important applications of the inorganic TNA QDSSCs in solar cell applications. However, compared to DSSCs with PCE up to 12%, QDSSCs have not been demonstrated as an efficient inorganic dye than expected. Therefore, great efforts are still needed to inhibit charge recombination at the semiconductor surface for the efficiency improvement of QDSSCs [123].

4.3. Water Splitting. Considering that the principle of photoelectrolysis for water splitting is the same with photocatalysis,

TNAs are considered as good candidates for high efficient water splitting (see Table 2). The photoelectrolysis process using TiO<sub>2</sub> nanotube cells as a photoanode is as follows: when the photoanode is immersed in water and exposed to light irradiation, it absorbs photonic energy over its band gap energy; then, electron-hole pairs are generated in it. The generated holes oxidize O<sup>2-</sup> ions from absorbed water and produce oxygen gas and an electric current that moves through the external circuit to the conducting cathode in which it reduces H<sup>+</sup> ions to produce hydrogen gas. Recently, TNAs prepared by anodization of titanium have attracted extensive interest in photocatalytic water splitting. Mor et al. find a hydrogen generation rate of 96 µmol/h/cm<sup>2</sup> for the utilization of nanotube array (224 nm in length) for water splitting under a constant voltage bias of -0.4 V (versus Ag/AgCl) [124]. Recently, we reported an enhanced hydrogen generation rate of 150 µmol/h/cm<sup>2</sup> by a three-step electrochemical anodized TNAs with a regular porous top layer (Figures 9(a) and 9(b)) [125]. Moreover, we found that palladium quantum dots sensitized TNAs exhibited highly efficient photocatalytic hydrogen production rate of 592 µmol/h/cm<sup>2</sup> under 320 mW/cm<sup>2</sup> irradiation (Figures 9(c)-9(h)) [79]. In general, the hydrogen production rate is greatly depending on the electrolyte, external bias, light intensity, and TiO<sub>2</sub> morphology and structure. Therefore, it is important to

Photoanode	Light intensity (mW/cm <sup>2</sup> )	Electrolyte	Photocurrent (mA/cm <sup>2</sup> )	Water splitting $(\mu \text{mol/h/cm}^2)$	Reference
C-TNAs	N/A; 500 W Xe lamp	0.1 M Na <sub>2</sub> S + 0.02 M Na <sub>2</sub> SO <sub>3</sub>	N/A	1.6 (0.040 mL/h/cm <sup>2</sup> )	[126]
TNAs	70; 300 W Xe lamp	1 M KOH	0.58@0.6 V versus NHE	7.1 (0.178 mL/h/cm <sup>2</sup> )	[127]
C-TNAs (C-containing TiO <sub>2</sub> based nanotube arrays)	12.7, 300 W Xe Lamp	1 M KOH	1.96@0 V versus Ag/AgCl	$11.28$ $(0.282 \mathrm{mL/h/cm}^2)$	[128]
TNAs with etching pretreatment	87, 300 W AM 1.5	1 M KOH	1.78@1.23 V RHE	34.8 (0.87 mL/h/cm <sup>2</sup> )	[129]
Ru/TNAs@0.05 at% Ru	100	1 M KOH	1.78@0.4 V versus Ag/AgCl	45 (1.08 mL/h/cm <sup>2</sup> )	[130]
TNAs (224 nm length, 34 nm wall thickness)	100	1 M KOH	13.0@0 V versus Ag/AgCl	96 (2.30 mL/h/cm <sup>2</sup> )	[124]
TNAs	110	$1 \mathrm{M}\mathrm{KOH} + 0.5 \mathrm{M}\mathrm{H}_2\mathrm{SO}_4$	4.95	97 (2.32 mL/h/cm <sup>2</sup> )	[131]
TNAs	74	1 M KOH	N/A	140 (3.28 mL/h/cm <sup>2</sup> )	[132]
Leaf-like TiO <sub>2</sub> /TNAs	320	$2 \mathrm{M}\mathrm{Na_2CO_3} + 0.5 \mathrm{M}\mathrm{EG}$	16.3@0.9 V versus SCE	150	[125]
Pyrococcus furiosus/TNAs	74	1 M KOH	N/A	234.88	[133]
TNAs	74	1 M KOH	32.8@1.5 V versus Ag/AgCl	250	[134]
TNAs (three-step anodization)	320	2 M Na <sub>2</sub> CO <sub>3</sub> + 0.5 M EG	24@-0.3 V versus SCE	420	[135]
Pt@TNAs	320	2 M Na <sub>2</sub> CO <sub>3</sub> + 0.5 M EG	24.2@-0.3 V versus SCE	495	[80]
Pd@TNAs	320	$2 \text{ M Na}_2 \text{CO}_3 +$	26.8@0.9 V versus	592	[79]

0.5 M EG

TABLE 2: Summary of TNAs based materials in water splitting.

optimize these parameters and fundamentally understand their possible correlations to clarify the approaches toward to construct high efficient cell for hydrogen generation.

4.4. Other Applications. As mentioned above, another special electrochemical feature of TNAs or some other TiO2 nanotube based materials is its ability to serve as a host for small ions insertion, typically hydrogen ion or lithium ion, into the lattice, leading to the drastic change of electronic and optical properties for potential applications in lithium-battery [4, 136, 137], electrochromic devices [138, 139], and supercapacitor [140, 141]. The kinetics, magnitude, and reversibility of the ion insertion and electrochromic reaction strongly depend on the ion diffusion length and therefore on geometry of the electrode surface. Due to the specific vertical alignment of the TNAs, a very high contrast can be obtained using vertically oriented nanotubes. By deposition of Ag nanoparticles on the TNAs, a material can be created that shows considerable photochromic contrast [142]. Furthermore, the TNA has also been proved to be good support for Pt or Pt/Ru catalysts for enhanced methanol electrooxidation [143, 144].

Other applications of the TNAs for biomedical implant are wetting template, target hydrogen sensing, electrochemical detection, and photogenerated cathode anticorrosion

[145-147]. For instance, the combination of organic modification with a controllable photocatalytic reaction of TiO<sub>2</sub> was used to create microscale patterning surfaces with any desired wettability value. Wetting micropatterns with different physical or chemical properties have frequently acted as templates for fabricating various functional materials in a large scale [148]. Moreover, wetting patterns with tailored and reversible adhesion for microfluidic devices and microdroplet manipulation have also been reported [149]. For example, Ag@TNA micropatterns show not only the highthroughput molecular sensing feature with high sensitive, reproducible performance but also show promising targeted antibacterials properties [148]. For gas sensing, Varghese et al. have shown instant resistance response in order of several magnitudes for the TNA layer upon exposure to 1000 ppm H<sub>2</sub> containing nitrogen atmospheres at room temperature [145].

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The applications of TNAs can significantly be expanded if secondary material can successfully be deposited into the tubes. The TNAs can also be converted to other titanates  $MTiO_3$  (M = Sr, Pd, Zr) with specific bioactive, piezoelectric or ferroelectric properties and keep with its original tube structure by a simple hydrothermal process in the corresponding precursor solution or a direct anodizing process in appropriate alloy substrates [150–153].

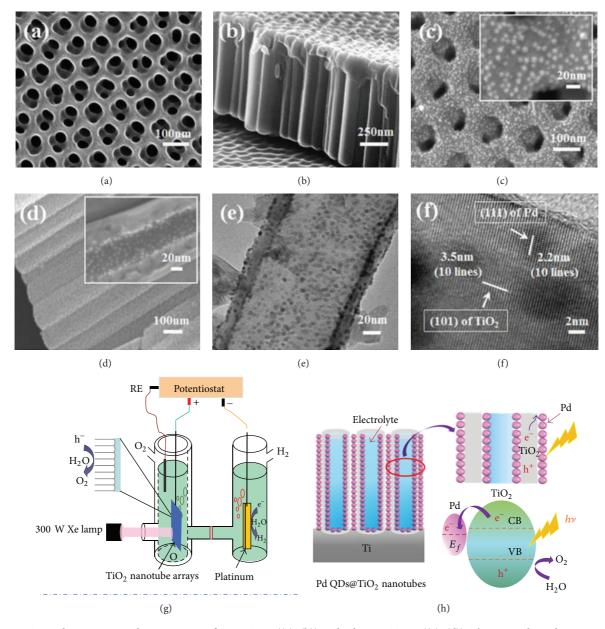


FIGURE 9: Top and cross-sectional SEM images of pure TNAs ((a), (b)) and Pd QDs@TNAs ((c), (d)). The insets show the corresponding magnified images. TEM images of TNAs coated with Pd QDs. (g) Schematic of TNAs on photoelectrolytic water splitting for hydrogen production. (h) Schematic illustration of TNAs deposited with Pd QDs and the charge transfer process from TiO<sub>2</sub> to Pd (lower right panel).

#### 5. Conclusion

Till now, a large number of fundamental studies and application-oriented researches and developments are extensively carried out by many researchers for this low-dimensional nanomaterial due to the expected various properties of  ${\rm TiO_2}$  (high surface area and controllable nanotube dimensions, geometries, and surface chemistry). This work has presented the recent progress of preparation and modification on the electrochemically anodized TNA materials. These unique low dimensional nanostructure materials have been shown to have many favourable properties for potential applications, including pollutant photocatalytic decomposition,

photovoltaic cells, biomedical scaffold, and wetting template. On the other hand, extensive challenges to fabricate high quality TNAs and develop various oxide nanotubes have been continued. For instance, rapid and high-efficient synthesis of anatase TNAs and other multicomponent nanotubes under ambient low-temperature conditions have recently been reported [154]. Some other aspects aim to encompass the new progress of  ${\rm TiO}_2$  for an efficient utilization in photocatalytic or photovoltaic applications under visible light, emphasize the future trends of  ${\rm TiO}_2$  in the environment and/or energy related fields, and suggest new research directions, including preparation aspects for the development of this promising material [155].

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#### Research Article

# Photocatalytic Oxidation of Gaseous Benzene under 185 nm UV Irradiation

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Benzene is a toxic air pollutant and causes great harm to human being. Photocatalytic oxidation (PCO) has been frequently studied for benzene removal, however, its PCO efficiency is still very low and the photocatalysts are easy to be deactivated. To improve the efficiency and stability of PCO, UV lamps with partial 185 nm UV irradiation were used to activate photocatalysts (denoted as 185-PCO). Cobalt modified TiO<sub>2</sub> (Co-TiO<sub>2</sub>) was developed to improve the PCO activity and eliminate ozone generated from 185 nm UV irradiation. Results show that benzene removal efficiency of PCO with 254 nm UV irradiation (denoted as 254-PCO) is only 2.1% while it was greatly increased to 51.5% in 185-PCO. 185-PCO exhibited superior capacity for benzene oxidation. In the 185-PCO process, much ozone was left in case of TiO<sub>2</sub> as photocatalysts while it can be nearly eliminated by 1% Co-TiO<sub>2</sub>.

#### 1. Introduction

With the rapid development of economy and the increase in population, massive volatile organic compounds (VOCs) are discharged from both industry (such as chemical, petrochemical, painting, and coating factories) and human activities [1, 2]. VOCs not only do great harm to the health of human being but also cause serious damage to the atmospheric environment. They can lead to atmospheric compound pollution and haze. The haze weather, which lasted for a long time in many cities of China in early 2013, had caused much trouble to local people. It is of great significance to control VOCs pollution.

Benzene is a representative VOC. It is very toxic and carcinogenic. Benzene is hard to be destructed by conventional technology due to its benzene ring. The methods of benzene removal include conventional ways such as adsorption [3, 4], catalytic combustion [5], and biological degradation [6] and emerging ways such as nonthermal plasma [7] and photocatalysis [8–10]. However, the application of these methods is greatly limited due to their inherent drawbacks such as high cost, deactivation, and byproducts [11–14].

PCO is one of the fastest developed technologies for VOCs control. The most widely used UV sources in PCO are 254 nm and 365 nm UV lamp. However, the conventional PCO process has disadvantages such as photocatalyst deactivation, recombination of electron-hole pair, and low efficiency [15]. In order to improve the efficiency and stability of PCO, UV lamps with partial 185 nm UV irradiation (denoted as 185-PCO) were used to activate photocatalysts [16–18]. 185 nm UV lamps cannot only irradiate photocatalyst but also generate active oxidants such as •O, •OH, and ozone. They are also facile, cheap, and energy efficient. Previous study showed that the toluene removal of 185-PCO is 7 times higher than that of PCO under 254 nm UV irradiation (denoted as 254-PCO), and no obvious deactivation was observed in the former [19]. However, massive ozone was residual at the outlet of photocatalytic reactor since TiO<sub>2</sub> had poor activity towards ozone decomposition. Ozone is a byproduct and it is harmful to the environment and the health of human being; meanwhile it is a strong oxidant and can be used to enhance the oxidation of pollutants.

Cobalt is a commonly used metal not only for TiO<sub>2</sub> doping but also as an active component of ozone decomposition

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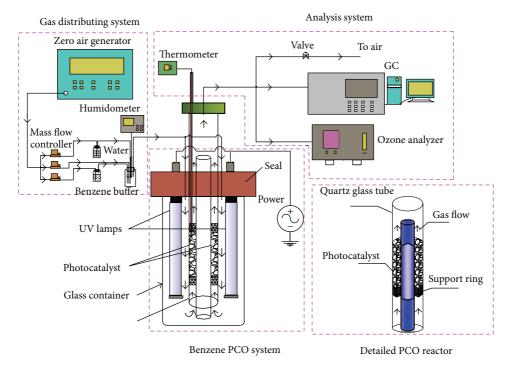


FIGURE 1: Schematic diagram of experimental setup.

agent. In this study, cobalt modified TiO<sub>2</sub> (Co-TiO<sub>2</sub>) was developed to improve the PCO activity and eliminate ozone generated from 185 nm irradiation. Benzene was selected as representative VOC and its oxidation performance is compared between 185-PCO and 254-PCO. Results show that Co-TiO<sub>2</sub> can simultaneously increase benzene removal and ozone decomposition in 185-PCO. 185-PCO presents an efficient, economic, simple, and stable process for benzene removal.

#### 2. Experimental Sections

2.1. Preparation of Photocatalysts. TiO<sub>2</sub> was prepared by solgel method using tetrabutyl titanate as the precursor, absolute alcohol as the solution, and HCl as the inhibitor, respectively. The preparation procedure is as follows: cobalt acetate was added into the mixture of 50 mL absolute alcohol and 17 mL tetrabutyl titanate and mixed for 30 min, forming solution A. Another mixture B containing 18 mL absolute alcohol, 1 mL HCl, and 3 mL deionized water was dropwise added into solution A under intensive stirring. The stirring was stopped till the gelatin was formed. The gelatin was aged for 12 h and then dried at 120°C for 6 h. The dry powder was followed by calcinations at 550°C for 4 h. Thus, cobalt doped TiO<sub>2</sub> was produced. Pure TiO<sub>2</sub> was fabricated by similar processes for the preparation of Co-TiO<sub>2</sub> except that no cobalt acetate was introduced during the synthesis. The catalysts were grinded into 40-60 mesh before use.

2.2. Catalytic Activity Test. The experimental setup and PCO reactor were shown in Figure 1. The catalytic activity test

system was composed of 3 parts: gas distribution, benzene PCO, and gas analysis system. The gas from zero air generator is dry air free of CO, CO<sub>2</sub>, and hydrocarbon. It was used for bubble water and benzene liquid to generate water and benzene vapor, respectively. The benzene concentration, humidity, and gas flow can be regulated by the mass flow controllers (S49, Horibametron). A 0.5 L/min gas flow of 50 ppm benzene concentration and 50% humidity was introduced into benzene PCO reactor. The reactor is a glass cylinder container with an effective volume of 0.5 L, in which a quartz glass tube was located in the centre and two UV lamps (4 W, Sungreen) were fixed in both sides of the tube with a distance of 8 mm. The detailed PCO reactor is shown in Figure 1. A solid rod of 8 mm diameter was placed in the center of the quartz glass tube with 1.3 cm i.d. and the photocatalysts was loaded in the space between the rod and glass tube. By this way, the photocatalysts have more chances to be irradiated by UV light. The UV lamps were turned on for 30 min for the warming-up of system before reaction and data recording. The gaseous benzene entered into the reactor from the bottom of glass tube and left from the top. The benzene and ozone concentrations of effluent were monitored by gas chromatography (GC) equipped with a FID (GC9790II, Fuli) and ozone analyzer (Model 202, 2B Technology) online, respectively.

2.3. Catalyst Characterization. BET surface areas of the samples were measured by  $N_2$  adsorption-desorption isotherms at 77 K using Quadrasorb SI instrument. Prior to the measurement, the samples were degassed at 573 K for 2 h. The morphology of photocatalysts was obtained with scanning electron microscopy (SEM) (JSM-6330F, JEOL) operated at

TABLE 1: BET surface area of photocatalysts.

Samples	BET surface area, m <sup>2</sup> /g	Particle size, nm
P25	55.4	29.0
${ m TiO_2}$	96.6	10.5
Co-TiO <sub>2</sub>	26.9	34.9

beam energy of 20.0 kV. XRD patterns were collected with a Panalytical Empyrean X-ray powder diffractometer operated at 35 kV and 25 mA, using Cu K  $\alpha$  ( $\lambda$  = 1.5418 Å) radiation. The intensity data were collected in a  $2\theta$  range from  $20^{\circ}$  to  $80^{\circ}$ .

#### 3. Results and Discussion

3.1. Characterization. Figure 2 shows the XRD spectra of the synthesized TiO2 and Co-TiO2 as well as the commercial TiO<sub>2</sub> (P25, Degussa). The nanocrystalline anatase structure was confirmed by (101), (004), (200), (105), and (204) diffraction peaks [20]. The XRD patterns of anatase have a main peak at  $2\theta = 25.2^{\circ}$  corresponding to the 101 plane (JCPDS 21-1272) while the main peaks of rutile and brookite phases are at  $2\theta = 27.4^{\circ}$  (110 plane) and  $2\theta = 30.8^{\circ}$  (121 plane), respectively. Therefore, rutile and brookite phases have not been detected on the synthesized TiO<sub>2</sub> and Co-TiO<sub>2</sub>. They exhibit very similar shape of diffractive peaks of the crystal planes. The XRD patterns did not show any Co phase, indicating that Co ions uniformly dispersed among the anatase crystallites. Unlike the synthesized TiO<sub>2</sub>, weak peaks of rutile phase can be observed on P25 (Figure 1). The average particle size of  $TiO_2$  was estimated by applying the Scherrer equation (D =  $K\lambda/\beta \cos \theta$ ) on the anatase and rutile diffraction peaks (the most intense peaks for each sample), where D is the crystal size of the catalyst,  $\lambda$  is the X-ray wavelength (1.54 Å),  $\beta$  is the full width at half maximum (FWHM) of the catalyst (radian), K = 0.89, and  $\theta$  is the diffraction angle [21]. The average crystal sizes of TiO2, 1% Co-TiO2, and P25 were calculated to be around 10.5 nm, 34.9 nm, and 29.0 nm, respectively, as shown in Table 1. Compared with P25, the synthesized TiO<sub>2</sub> can greatly reduce the particle size; however, the doping of cobalt triggered the aggregation of particle during the synthesis process, leading to the increase in particle size.

This observation is consistent with the results of BET surface area and the observation of SEM images. The BET surface area of  ${\rm TiO_2}$ , 1% Co- ${\rm TiO_2}$  and P25 is 96.6, 26.9 and 55.4 m<sup>2</sup>/g, respectively.  ${\rm TiO_2}$  with the smallest particle size has the largest BET surface area.

SEM micrograph of TiO<sub>2</sub>, 1% Co-TiO<sub>2</sub>, and P25 nanoparticles is shown in Figure 3. This image shows uniform small particles which are coherent together on the TiO<sub>2</sub> and P25; however, the particles of 1% Co-TiO<sub>2</sub> got aggregated. The results agree well with the results of XRD pattern and BET surface area.

3.2. Catalytic Activity Test. Figure 4 compared benzene removal efficiency in PCO processes with 185 nm and 254 nm UV irradiation. It can be found that it is very low in case

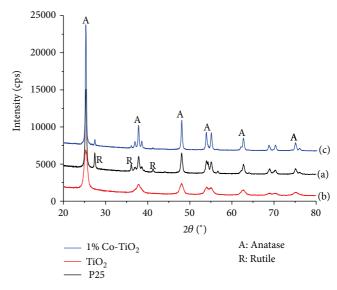


FIGURE 2: XRD spectra of photocatalysts: (a) P25, (b)  ${\rm TiO_2}$ , and (c) 1% Co-TiO<sub>2</sub>.

of 254-PCO process. Benzene removal efficiency is only about 2%. It is well known that benzene is very difficult to be destructed due to its stable  $\pi$ -bonding. Moreover, the intermediates from benzene PCO can lead to the serious deactivation of photocatalysts [22]. However, benzene conversion was greatly increased to about 50% under 185 nm UV irradiation and no obvious deactivation was observed after reaction for 3 h. Among 3 tested samples, Co-TiO<sub>2</sub> obtained the highest benzene removal efficiency of 51.5%, followed by P25 (50.2%) and TiO<sub>2</sub> (45.7%). Benzene removal efficiency of 185-PCO is over 20 times than that of 254-PCO. 185-PCO is a very complex process, in which 185 nm UV lamp not only acted as the irradiation light of photocatalysis but also generated reactive oxidants such as •O, •OH, and ozone. The reaction processes for the formation of reactive oxidants are as follows [23]:

$$H_2O + h\nu \longrightarrow \bullet H + \bullet OH$$

$$O_2 + h\nu \longrightarrow 2 \bullet O$$

$$\bullet O + H_2O \longrightarrow 2 \bullet OH$$

$$\bullet O + O_2 \longrightarrow O_3$$
(1)

In order to clarify the contribution of 185 nm irradiation, the photocatalysts were removed from the reactor. The new process is photolysis. It can be found that benzene removal efficiency reached 38% under 185 nm irradiation alone. 185 nm photolysis contributes much to benzene oxidation in the 185-PCO process. The sum of benzene removal efficiency due to PCO and 185 nm photolysis is about 40%, which is approximately 10% smaller than that of 185-PCO. This indicated that other factors were also involved in benzene oxidation in the 185-PCO process besides photolysis and PCO. As we know, ozone can be abundantly generated from 185 nm UV irradiation. The ozone concentration is 138 ppm in the absence of photocatalysts. Ozone is strong

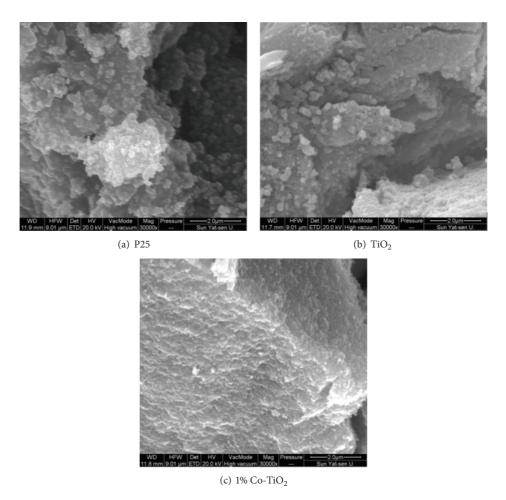


FIGURE 3: SEM images of photocatalysts: (a) P25, (b) TiO<sub>2</sub>, and (c) 1% Co-TiO<sub>2</sub>.

oxidant. Although it cannot directly oxidize benzene, it can be decomposed into more active oxygen species with the aid of catalysts [24]:

$$O_3 + * \longrightarrow O_2 + O^*$$

$$O^* + O_3 \longrightarrow O_2 + O_2^*$$

$$O_2^* \longrightarrow O_2 + *$$
(2)

3.3. Ozone Decomposition. 185-PCO exhibited more superior capacity for benzene oxidation than 254-PCO. However, ozone is another important concern besides benzene removal since it is a toxic byproduct. Although 3 tested samples had similar benzene removal efficiency since 185 nm UV photolysis contributed to a large proportion of benzene removal, they had entirely different activity toward ozone decomposition. As shown in Figure 5, the ozone concentration at outlet of 185-PCO reactor after reaction for 2.5 h was 119 ppm in case of the synthesized  ${\rm TiO_2}$ , and it was dropped to 58.4 ppm in case of P25. Although the synthesized  ${\rm TiO_2}$  had higher BET surface area than that of P25, its capacity for ozone decomposition is worse than that of the latter. It was reported

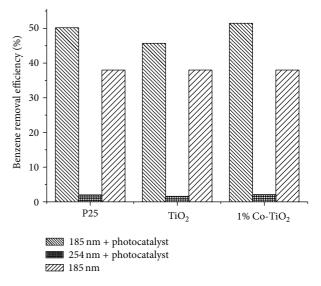


FIGURE 4: Benzene removal efficiency in different processes.

that higher BET surface area should be helpful for ozone decomposition [25]. The difference between synthesized  ${\rm TiO_2}$  and commercial P25 is that the former is pure anatase

<sup>\*</sup> represents the catalytic active sites.

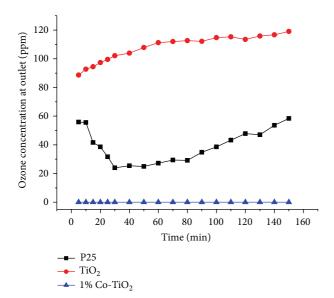


FIGURE 5: Ozone concentration at outlet of 185-PCO reactor with different photocatalysts.

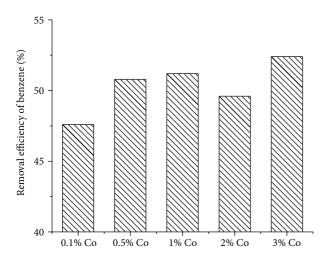


FIGURE 6: Effect of Co loading amount on benzene removal.

 ${
m TiO_2}$  while P25 contained some rutile  ${
m TiO_2}$  besides anatase one. A previous study showed that  ${
m TiO_2}$  with partial rutile had better capacity for ozone decomposition than that of pure anatase  ${
m TiO_2}$  [26]. As for Co-TiO<sub>2</sub>, ozone can be completely eliminated. Cobalt is a very active component for ozone decomposition. Co doped  ${
m TiO_2}$  exhibited superior activity toward ozone elimination. In comprehensive view of benzene removal and ozone decomposition, Co-TiO<sub>2</sub> exhibited the best performance among the 3 tested samples.

3.4. Effect of Co Doping. In order to study the effect of Co doping, 0.1%, 0.5%, 1%, 2%, and 3% Co-TiO $_2$  were prepared and tested in 185-PCO process. The results after reaction for 150 min are shown in Figure 6. Benzene removal efficiency is only 47.6% in case of 0.1% Co-TiO $_2$ . As the increase in Co loading, benzene removal efficiency was increased to 51.5% in case of 1% Co-TiO $_2$  and 52.4% in case of 3% Co-TiO $_2$ .

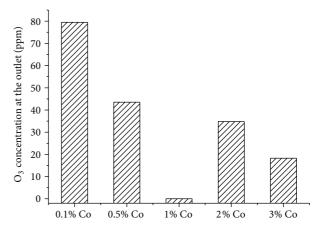


FIGURE 7: Effect of Co loading amount on ozone concentration at the outlet.

Figure 7 shows the effect of cobalt loading amount on ozone concentration at the outlet after reaction for 150 min. In case of Co doping amount lower than 1%, the ozone concentration at the outlet was dropped with the increase in Co loading. As for 0.1% Co doping, the ozone concentration is 79.5 ppm while it was decreased to nearly zero in case of 1% Co doping. The increase in Co doping can provide more catalytic active sites for ozone decomposition. However, the ozone concentration at the outlet was increased with further increase in Co doping. Too much Co doping is not beneficial to ozone decomposition since Co probably gets aggregated and blocks the micropore of TiO<sub>2</sub>. This will reduce the catalytic active sites and BET surface area, leading to worse activities toward ozone decomposition.

#### 4. Conclusion

To improve the efficiency and stability of PCO, 185-PCO was used to activate photocatalysts. Co-TiO<sub>2</sub> was developed to improve the PCO activity and eliminate the ozone generated from 185 nm UV irradiation. Results show that benzene removal efficiency of PCO with 254-PCO is only 2.1% while it was greatly increased to 51.5% in the 185-PCO process. 185 nm UV irradiation can generate much reactive oxygen species such as •O, •OH, and ozone, which can jointly enhance benzene oxidation together with PCO. In 185-PCO, much ozone is left in case of TiO<sub>2</sub> as photocatalysts while it can be completely eliminated by 1% Co-TiO<sub>2</sub>. 185-PCO is an efficient and promising process for benzene removal.

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#### Research Article

# A Cost-Effective Solid-State Approach to Synthesize $g-C_3N_4$ Coated $TiO_2$ Nanocomposites with Enhanced Visible Light Photocatalytic Activity

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Novel graphitic carbon nitride  $(g-C_3N_4)$  coated  $TiO_2$  nanocomposites were prepared by a facile and cost-effective solid-state method by thermal treatment of the mixture of urea and commercial  $TiO_2$ . Because the  $C_3N_4$  was dispersed and coated on the  $TiO_2$  nanoparticles, the as-prepared  $g-C_3N_4/TiO_2$  nanocomposites showed enhanced absorption and photocatalytic properties in visible light region. The as-prepared  $g-C_3N_4$  coated  $TiO_2$  nanocomposites under  $450^{\circ}C$  exhibited efficient visible light photocatalytic activity for degradation of aqueous MB due to the increased visible light absorption and enhanced MB adsorption. The  $g-C_3N_4$  coated  $TiO_2$  nanocomposites would have wide applications in both environmental remediation and solar energy conversion.

#### 1. Introduction

Visible light photocatalysis has attracted the worldwide attention due to its potential application in environmental remediation and solar energy conversion [1–7]. The photocatalyst  ${\rm TiO_2}$ , however, can only utilize the ultraviolet light (about 5% of natural solar light) because of its wide band gap (ca. 3.2 eV for anatase  ${\rm TiO_2}$ ). During the past 40 years, many efforts have been devoted to enhance the visible light photocatalytic activity of  ${\rm TiO_2}$ , including metal doping [8–10], nonmetal doping [11–14], surface modification [15], and heterojunction construction [16–19].

In recent years, polymeric g-C<sub>3</sub>N<sub>4</sub> materials have attracted much attention because of their similarity to graphene. Zhang et al. reported that the polymeric g-C<sub>3</sub>N<sub>4</sub> semiconductors exhibit high photocatalytic performance for water splitting under visible light irradiation [20]. Dong and coworkes reported that polymeric g-C<sub>3</sub>N<sub>4</sub> layered materials as novel efficient visible light photocatalyst, which can be synthesized facilely by directly heating urea or thiourea [21, 22].

Very recently, Zhou et al. reported a g-C<sub>3</sub>N<sub>4</sub>/TiO<sub>2</sub> nanotube array heterojunction with excellent visible light

photocatalytic activity [17]. Zhao et al. reported g- $\mathrm{C_3N_4/TiO_2}$  hybrids with wide absorption wavelength and effective photogenerated charge separation [18]. However, the precursors for g- $\mathrm{C_3N_4}$  (dicyandiamide and melamine) are poisonous and detrimental to the environment. The preparation processes were relatively tedious, which may prevent large-scale application [17, 18].

In the present work, g- $\mathrm{C_3N_4/TiO_2}$  nanocomposites were prepared by a facile and cost-effective solid-state method using urea and commercial  $\mathrm{TiO_2}$  as precursors. It was interesting to find that g- $\mathrm{C_3N_4}$  was in situ coated on the surface of  $\mathrm{TiO_2}$ . The precursors (urea and commercial  $\mathrm{TiO_2}$ ) are low cost and easily available. The as-prepared g- $\mathrm{C_3N_4}$  coated  $\mathrm{TiO_2}$  nanocomposites exhibited enhanced photocatalytic activity under visible light irradiation.

#### 2. Experimental

*2.1. Synthesis.* The g- $C_3N_4$  coated  $TiO_2$  nanocomposites were prepared by a facile and cost-effective solid-state method. In a typical synthesis, 2 g  $TiO_2$  and 6 g urea were immersed in 10 mL  $H_2O$  and dried at  $60^{\circ}C$  to completely remove the water.

The mixtures were put into an alumina crucible with a cover, and then heated to a certain temperature in the range of 400 and 600°C in a muffle furnace for 1h at a heating rate of 15°C min<sup>-1</sup>. The final samples were collected for use without further treatment.

2.2. Characterization. The crystal phases of the sample were analyzed by X-ray diffraction with Cu K $\alpha$  radiation (XRD: model D/max RA, Rigaku Co., Japan). The morphology and structure of the samples were examined by transmission electron microscopy (TEM: JEM-2010, Japan). The UV-vis diffuse reflection spectra were obtained for the dry-pressed disk samples using a Scan UV-Vis spectrophotometer (UV-Vis DRS: UV-2450, Shimadzu, Japan) equipped with an integrating sphere assembly, using BaSO<sub>4</sub> as reflectance sample. The spectra were recorded at room temperature in air range from 250 to 800 nm. X-ray photoelectron spectroscopy with Al K $\alpha$  X-rays ( $h\nu = 1486.6 \,\text{eV}$ ) radiation operated at 150 W (XPS: Thermo ESCALAB 250, USA) was used to investigate the surface properties. The shift of the binding energy due to relative surface charging was corrected using the C1s level at 284.8 eV as an internal standard. FT-IR spectra were recorded on a Nicolet Nexus spectrometer on samples embedded in KBr pellets. The nitrogen adsorption-desorption isotherms were determined by the BET method (BET-BJH: ASAP 2020, USA), from which the surface area, pore volume, and average pore diameter were calculated by using the BJH method. All the samples were degassed at 200°C prior to measurements.

2.3. Evaluation of Photocatalytic Activity. Photocatalytic activity of g-C<sub>3</sub>N<sub>4</sub>/TiO<sub>2</sub> for MB photodegradation was evaluated in a quartz glass reactor. 0.05 g of N-TiO2 was dispersed in MB aqueous solution (50 mL, 5 mg/L). The light irradiation system contains a 500 W Xe lamp with a jacket filled with flowing and thermostated aqueous NaNO2 solution (1 M) between the lamp and the reaction chamber as a filter to block UV light ( $\lambda$  < 400 nm) and eliminate the temperature effect. The suspension was first allowed to reach adsorptiondesorption equilibrium with continuous stirring for 60 min in the dark prior to irradiation. The degradation rate of MB was evaluated using the UV-Vis absorption spectra to measure the peak value of a maximum absorption of MB solution. During the irradiation, 5 mL of suspension was continually taken from the reaction cell at given time intervals for subsequent dye concentration analysis after centrifugation. The MB solution shows a similar pH value at 6.8, which does not affect the light absorption of MB. The maximum absorption of MB is at wavelength of 665 nm. The degradation rate  $\eta$  (%) can be calculated as

$$\eta(\%) = \frac{(C_0 - C)}{C_0} \times 100\%,$$
(1)

where  $C_0$  is the initial concentration of MB considering MB adsorption on the catalyst and C is the revised concentration after irradiation.

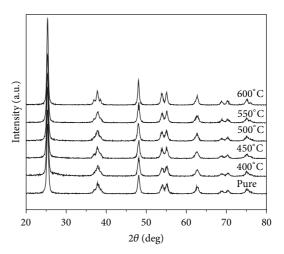


FIGURE 1: XRD patterns of the  $\rm C_3N_4/TiO_2$  nanocomposites obtained under different temperatures.

#### 3. Results and Discussion

Figure 1 shows the XRD patterns of the as-prepared g- $C_3N_4$  coated  $TiO_2$  nanocomposites at different temperatures. The peaks of all the samples can be indexed to the anatase phase of  $TiO_2$  (JCPDS file No. 21-1272). It can be seen that the peak intensity increases gradually under higher treatment temperature, which indicates that the crystal sizes of  $TiO_2$  nanocomposites increase under higher treatment temperature. No typical peaks of  $g-C_3N_4$  can be found for all the samples due to the fact that  $g-C_3N_4$  with layered structures on the surface of  $TiO_2$  is ultrathin (Figure 2) and the crystallinity is low [22].

The morphology of pure  $TiO_2$  and  $g-C_3N_4/TiO_2$  nano-composites were observed by TEM. As shown in Figure 2, both samples contain a number of monodispersed nanoparticles of  $TiO_2$  with a size of about 11 nm. The intra-aggregation of particles could form the mesoporous structure [23]. It can be seen from Figure 2(b) that the ultrathin  $g-C_3N_4$  with layered structures are dispersed and coated on the surface of  $TiO_2$  particles, which is consistent with absence of the peaks of  $g-C_3N_4$  in XRD (Figure 1).

The FT-IR spectra of pure  $TiO_2$  and  $g-C_3N_4$  coated  $TiO_2$  nanocomposites are shown in Figure 3(a). The absorption band around  $400-800~\rm cm^{-1}$  is attributed to Ti-O bonds [23]. Several bands in the range of  $1100-1650~\rm cm^{-1}$  correspond to the typical stretching vibration of CN heterocycles in  $g-C_3N_4$ . The characteristic vibration mode of triazine units can also be found at  $801~\rm cm^{-1}$  [22]. The peak at  $1630~\rm cm^{-1}$  is associated with the stretching vibration of water molecules for both samples, including molecular water and hydroxyl groups [23]. The FT-IR spectra further confirm the existence of  $g-C_3N_4$  on the surface of  $TiO_2$ .

The TG and DSC thermograms (Figure 3(b)) show that there are several phase transformations during heating. An endothermal peak at 135°C is the melting point of urea. The peak at 242°C indicates the reaction of urea into melamine. The weight loss during the two stages decreases rapidly by 36.1%. The sharp peak at 367°C implies that the thermal

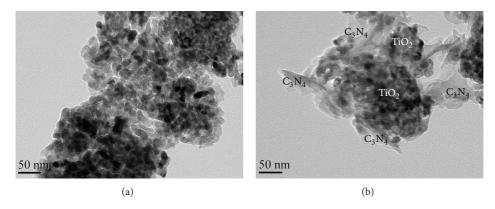


FIGURE 2: TEM images of pure TiO<sub>2</sub> (a) and g-C<sub>3</sub>N<sub>4</sub>/TiO<sub>2</sub> nanocomposites sample obtained under 450°C (b).

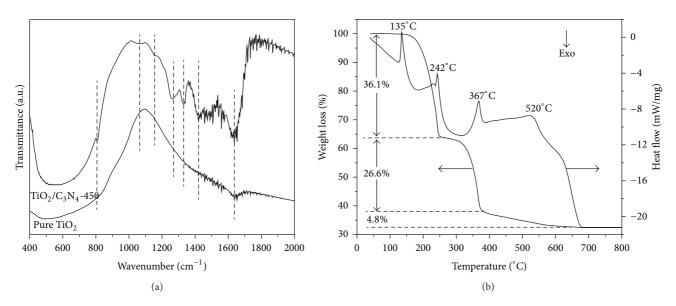


FIGURE 3: FTIR spectra of pure TiO<sub>2</sub> and g-C<sub>3</sub>N<sub>4</sub>/TiO<sub>2</sub> nanocomposites (a) and TG-DSC for heating the mixture of TiO<sub>2</sub> and urea (b).

condensation of melamine into g- $C_3N_4$  occurred in this temperature range. The weight loss in this stage is about 26.6%. The further weight loss of 4.8% with endothermal peak at 520°C can be attributed to the decomposition of g- $C_3N_4$ . The TG-DSC result implies that g- $C_3N_4$  can be *in situ* formed on the surface of  $TiO_2$ , which is consistent with Figure 2(b).

The Cls spectra in Figure 4(a) show that two main carbon species with binding energies of 284.9 and 288.1 eV, corresponding to C–C and C–N–C, respectively. Three binding energies in N1s region (Figure 4(b)) can be observed, which can be indexed to C–N–C (398.8 eV), N–(C) $_3$  (400.1 eV), and N–H groups (401.2 eV), respectively. The binding energy at 529.7 and 533.0 eV can be ascribed to Ti–O, surface hydroxyl groups, and adsorbed molecular water (Figures 4(c) and 4(d)) [22]. The XPS results are consistent with the FT-IR spectra. XPS results also indicate that no peak for Ti–C or Ti–N bond can be observed, which implies that there is no chemical bond connection between g-C $_3$ N $_4$  and TiO $_2$ .

The nitrogen adsorption-desorption isotherms of pure  ${\rm TiO_2}$  and  ${\rm g\text{-}C_3N_4/TiO_2}$  nanocomposites obtained under

450°C are shown in Figure 5(a). The two samples show a type IV adsorption isotherm with a  $\rm H_2$  hysteresis loop in the range  $(P/P_0)$  of 0.6–1.0, which indicates the presence of mesopores. The surface areas and pore volume of pure  $\rm TiO_2$  are  $78~\rm m^2/g$  and 0.281 cm³/g, higher than those of g- $\rm C_3N_4/\rm TiO_2$  nanocomposites ( $48~\rm m^2/g$  and 0.216 cm³/g). The pore size distribution curve (Figure 5(b)) indicates that the large mesopores of pure  $\rm TiO_2$  and g- $\rm C_3N_4/\rm TiO_2$  nanocomposites are about 37 and 48 nm, respectively. The presence of large mesopores can be ascribed to the aggregation of  $\rm TiO_2$  particles. It can be observed that the g- $\rm C_3N_4/\rm TiO_2$  nanocomposites have small mesopores of around 13.6 nm (inset in Figure 5(b)), which originates from the presence of layered g- $\rm C_3N_4$  on the  $\rm TiO_2$  surface. The small mesopore is advantageous for enhancing the adsorption for reactant.

Figure 6 shows the UV-Vis DRS spectra of pure  ${\rm TiO_2}$  and the as-prepared  ${\rm g-C_3N_4/TiO_2}$  nanocomposites. It is clear that the visible light absorption of  ${\rm g-C_3N_4/TiO_2}$  nanocomposites is enhanced with increased treatment temperatures until 450°C. Then the visible light absorption decreases when the temperature is higher than 450°C. This fact implies

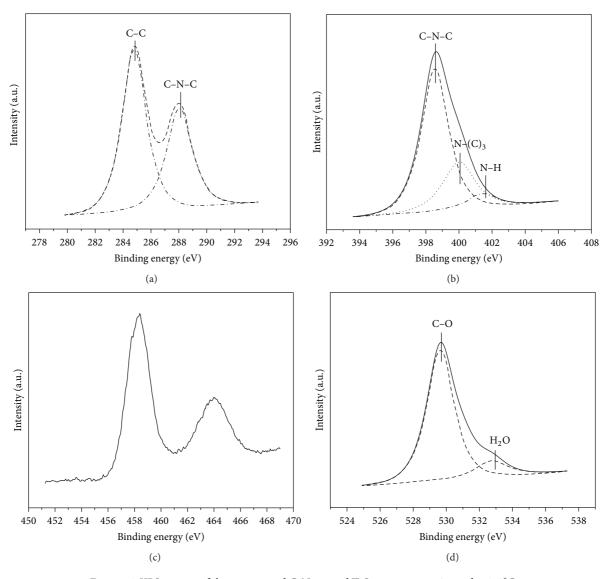


FIGURE 4: XPS spectra of the as-prepared C<sub>3</sub>N<sub>4</sub> coated TiO<sub>2</sub> nanocomposite under 450°C.

that the as-prepared g- $C_3N_4$  coated  $TiO_2$  nanocomposites under 450°C may exhibit excellent visible light photocatalytic activity. However, the decrease of visible light absorption intensity of coated  $TiO_2$  nanocomposites under higher treatment temperature can be attributed to the decomposition of g- $C_3N_4$ .

Figure 7 shows the adsorption and photocatalytic activity of pure  ${\rm TiO_2}$  and  ${\rm g-C_3N_4/TiO_2}$  nanocomposites for removal of MB. It can be seen that the  ${\rm g-C_3N_4/TiO_2}$  nanocomposites obtained under  ${\rm 450^{\circ}C}$  exhibit the highest adsorption capacity, which may be ascribed to presence of layered  ${\rm g-C_3N_4}$  and small mesopores of the nanocomposites sample. The photocatalytic activities of  ${\rm g-C_3N_4/TiO_2}$  nanocomposites first increase and then decrease with the increased treatment temperature. Pure  ${\rm TiO_2}$  shows low visible light activity due to its large band gap. The observed slight visible light activity for the pure  ${\rm TiO_2}$  sample can be ascribed to the photosensitization effect of the MB as MB can absorb visible light

[18]. During the visible light irradiation, the part of MB was self-decomposed due to the photosensitization. When TiO<sub>2</sub> was coated by g-C<sub>3</sub>N<sub>4</sub>, all the nanocomposite samples show decent visible light activity. Under visible light irradiation, g-C<sub>3</sub>N<sub>4</sub> with a band gap of 2.7 eV could be excited and the photogenerated electrons could transfer from the conduction band (CB) of g-C<sub>3</sub>N<sub>4</sub> to the CB of TiO<sub>2</sub> [17, 18, 24]. The holes in the valence band (VB) of g-C<sub>3</sub>N<sub>4</sub> and electrons on the CB of TiO<sub>2</sub> could initiate the following degradation reactions. The as-prepared g-C<sub>3</sub>N<sub>4</sub>/TiO<sub>2</sub> nanocomposites under 450°C exhibit the highest photocatalytic activity under visible light irradiation. Considering the fact that the surface area of g-C<sub>3</sub>N<sub>4</sub>/TiO<sub>2</sub> nanocomposites (48 m<sup>2</sup>/g) is lower than that of pure TiO<sub>2</sub> (78 m<sup>2</sup>/g), the surface area of g-C<sub>3</sub>N<sub>4</sub>/TiO<sub>2</sub> is not a positive factor. The enhanced visible light activity of g-C<sub>3</sub>N<sub>4</sub>/TiO<sub>2</sub> should be ascribed to the enhanced visible light adsorption because of the presence of g-C<sub>3</sub>N<sub>4</sub> (Figures 2(b) and 6) and the improved MB adsorption

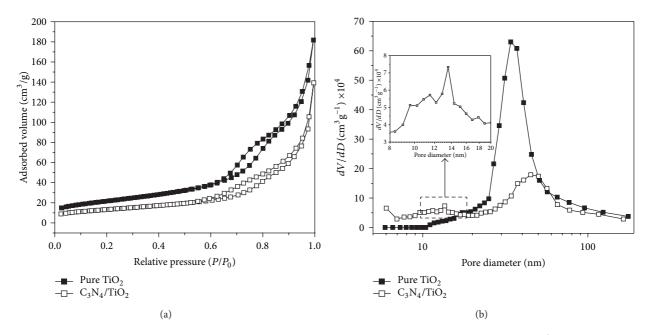


FIGURE 5: BET-BJH of the pure TiO<sub>2</sub> and C<sub>3</sub>N<sub>4</sub> coated TiO<sub>2</sub> nanocomposite obtained under 450°C.

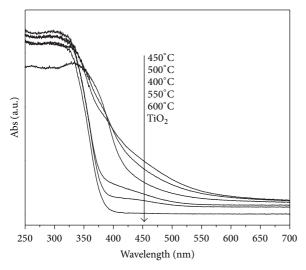


FIGURE 6: UV-Vis DRS of the pure  ${\rm TiO_2}$  and  ${\rm g\text{-}C_3N_4/TiO_2}$  samples obtained under different temperatures.

because of the small mesopores of the nanocomposites sample (Figure 5(b)). As the precursors (urea and commercial  ${\rm TiO_2}$ ) are cheap and preparation method is very simple, the as-prepared g-C<sub>3</sub>N<sub>4</sub> coated  ${\rm TiO_2}$  nanocomposites are ready for large-scale applications in environmental pollution control and solar energy conversion [25].

#### 4. Conclusion

The  $g-C_3N_4/TiO_2$  nanocomposites were synthesized by a cost-effective solid-state approach by thermal treatment of the mixture of urea and commercial  $TiO_2$ . It was found that the surface of  $TiO_2$  particles was coated by the *in* 

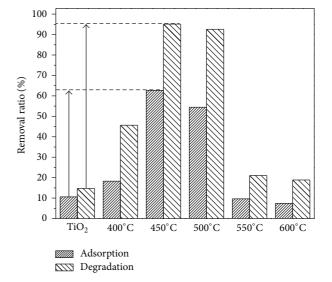


FIGURE 7: Adsorption and photocatalytic activity of the pure  ${\rm TiO_2}$  and  ${\rm g\text{-}C_3N_4/TiO_2}$  samples obtained under different temperatures for removal of MB.

situ formed thin layered g-C<sub>3</sub>N<sub>4</sub> from urea. The adsorption capacity and visible light photocatalytic activity were significantly enhanced. Under the optimized treatment temperature of 450°C, the g-C<sub>3</sub>N<sub>4</sub>/TiO<sub>2</sub> nanocomposites exhibited highest adsorption capacity and visible light photocatalytic activity toward removal of MB. The enhanced adsorption capacity can be ascribed to the presence of g-C<sub>3</sub>N<sub>4</sub> and small mesopores. The enhanced visible photocatalytic activity originated from the increased visible light adsorption and small mesopores of the nanocomposites sample. The novel

 $g-C_3N_4$  coated  $TiO_2$  nanocomposites prepared by the cost-effective solid-state approach would find wide application in environmental remediation.

#### **Conflict of Interests**

The authors declare no conflict of interests.

#### Acknowledgments

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#### Research Article

### Dynamic Hydrogen Production from Methanol/Water Photo-Splitting Using Core@Shell-Structured CuS@TiO<sub>2</sub> Catalyst Wrapped by High Concentrated TiO<sub>2</sub> Particles

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This study focused on the dynamic hydrogen production ability of a core@shell-structured  $CuS@TiO_2$  photocatalyst coated with a high concentration of  $TiO_2$  particles. The rectangular-shaped CuS particles, 100 nm in length and 60 nm in width, were surrounded by a high concentration of anatase  $TiO_2$  particles (>4~5 mol). The synthesized core@shell-structured  $CuS@TiO_2$  particles absorbed a long wavelength (a short band gap) above 700 nm compared to that pure  $TiO_2$ , which at approximately 300 nm, leading to easier electronic transitions, even at low energy. Hydrogen evolution from methanol/water photo-splitting over the core@shell-structured  $CuS@TiO_2$  photocatalyst increased approximately 10-fold compared to that over pure CuS. In particular, 1.9 mmol of hydrogen gas was produced after 10 hours when 0.5 g of  $1CuS@4TiO_2$  was used at pH = 7. This level of production was increased to more than 4-fold at higher pH. Cyclic voltammetry and UV-visible absorption spectroscopy confirmed that the CuS in  $CuS@TiO_2$  strongly withdraws the excited electrons from the valence band in  $TiO_2$  because of the higher reduction potential than  $TiO_2$ , resulting in a slower recombination rate between the electrons and holes and higher photoactivity.

#### 1. Introduction

In recent years, hydrogen has been highlighted as a next-generation energy source because of its environmentally friendly nature and high-energy efficiency. Therefore, hydrogen production has recently become the most active research topic globally. In particular, the technology for generating hydrogen by the splitting of water using a photocatalyst has attracted considerable attention. In the early days, the photocatalytic formation of hydrogen and oxygen focused extensively on metal-loaded or incorporated-TiO<sub>2</sub> semiconductors due to the low band gap and high corrosion resistance of these materials [1–5]. On the other hand, hydrogen production from water photo-splitting using TiO<sub>2</sub>-based photocatalysts is ineffective because the amount of hydrogen produced is limited by the rapid recombination of holes and electrons

over TiO<sub>2</sub>, resulting in the reformation of water [6]. In addition, more than 1.2 eV is needed to decompose water [7], which means that the photodecomposition of water should be performed at UV wavelengths of approximately 260 nm. Therefore, there is urgent need for the development of new and inexpensive photocatalysts that are both environmentally friendly and possess greater hydrogen-producing activity under visible light irradiation. Recently, studies of metal sulfide photocatalysts, such as ZnS- [8], CuS- [9, 10], FeS-[11], Bi<sub>2</sub>S<sub>3</sub>- [12], Sb<sub>2</sub>S<sub>3</sub>- [13], or CdS-loaded TiO<sub>2</sub> [14], have covered topics ranging from synthesis to applications in new photocatalytic reaction mechanisms. Narrow band gaps make it possible to absorb longer wavelengths compared to wide band gaps of conventional metal oxide semiconductor systems. A previous study reported high photocatalytic activity on the ZnS-loaded TiO<sub>2</sub> composite system for hydrogen

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production [15]. In that study, the evolution of H<sub>2</sub> from methanol/water (1:1) photo-splitting over the ZnS/TiO<sub>2</sub> composite was enhanced dramatically compared to that over pure TiO<sub>2</sub> and ZnS. In particular, 1.2 mmol of H<sub>2</sub> gas was produced after 10 h when 0.5 g of a 5.0 wt% ZnS-loaded TiO<sub>2</sub> composite was used. Recently, many studies began to focus their attention on bimetallic sulfides photocatalysts, such as CdZnS [16], CuZnS [17], ZnInS [18], and AgZnS [19]. These studies have been extended to trimetallic sulfide photocatalysts, such as CuAgInS [20], ZnCuCdS [21], CuInZnS [22], and AgGaInS [23]. On the other hand, most papers are based on metal sulfides loaded on the surface of TiO<sub>2</sub> particles. Few studies have examined TiO<sub>2</sub> nanoparticles loaded on the surface of large-sized metal sulfide particles.

This study focused on the CuS core material with a shorter band-gap of 1.56 eV and a higher reduction potential [24] than those of pure TiO<sub>2</sub>. Cu materials are widely used as catalysts for methanol steam reforming because of their excellent redox properties despite vulnerable to water. The potential ( $Cu^{2+} + 2e^{-} = Cu^{0}$ ,  $E^{\circ} = -0.224 \text{ V}$ ) is slightly lower than the conduction band (-0.26 V) of anatase TiO<sub>2</sub> but is higher than the reduction potential of  $H^+$  ( $2H^+ + 2e^- =$  $H_2$ ,  $E^{\circ} = -0.000 \text{ V}$ ), which favors electron transfer from the conduction band of TiO<sub>2</sub> to Cu<sup>2+</sup>, and the reduction of H<sup>+</sup>, thereby enhancing the photocatalytic H<sub>2</sub>-production activity [25, 26]. In this study, CuS was synthesized by a hydrothermal method with sodium sulfate as the sulfur source. A Ti precursor at a high concentrated molar ratio was then coated on the surface of the CuS like a core-shell structure. The relationship between the spectroscopic properties and the catalytic performance for the hydrogen production over the core@shell-structured CuS@TiO2 was examined by X-ray diffraction (XRD), transmission electron microscopy (TEM), UV-visible absorption spectroscopy, Brunauer, Emmett, and Teller (BET) surface areas, cyclic voltammetry (CV), and zeta potential measurements using an electrophoresis measurement apparatus.

#### 2. Experimental

2.1. Synthesis of CuS and Core@Shell-Structured CuS@TiO<sub>2</sub>. The TiO<sub>2</sub>, CuS, and core@shell-structured CuS@TiO<sub>2</sub> photocatalysts were prepared using hydrothermal and impregnation methods, respectively. In the first step for TiO<sub>2</sub>, titanium tetra-isopropoxide (TTIP, 99.99%, Junsei Chemical, Japan) as a titanium precursor was added dropwise to an aqueous solution and stirred homogeneously for 2h. The pH of the final solution was set to pH = 3.0 using acetic acid to induce mild hydrolysis, and the resulting solution was transferred to an autoclave for thermal treatment. The thermal treatment at 200°C was kept for 12 h, and the resulting precipitates were obtained, washed with distilled water, and dried at 80°C for 24 h. In the second step of CuS synthesis, CuSO<sub>4</sub>·5H<sub>2</sub>O (99.99%, Junsei Chemical, Japan) and Na<sub>2</sub>S<sub>2</sub>O<sub>3</sub>·5H<sub>2</sub>O (99.99%, Junsei Chemical, Japan) were used as the Cu and S precursors to prepare the sol mixture, respectively. Copper sulfate and sodium sulfate were dissolved sequentially in distilled water and stirred to homogeneity for 2h. The final solution was transferred to

an autoclave for thermal treatment. Cu ions were sulfurized during the thermal treatment at 180°C for 12 h. The resulting precipitates were obtained, washed with distilled water, and dried at 80°C for 24 h. Finally the dried powders were treated at 400°C for 4h to obtain crystallized CuS. Finally, 4.0 and 5.0 moles of TTIP (titanium tetraisopropoxide, 99.99%, Aldrich) for each 1.0 mole of CuS were added slowly to an ethanol solution containing the dispersed CuS particles during stirring to coat the CuS surface. The pH of the colloidal solution was kept at 4.0, and the solution was stirred homogeneously for 18 h. The final solution was evaporated at 80°C for 5 h and calcined at 400°C for 4 h to induce the anatase TiO2. Finally, three types of materials, CuS and the core@shell-structured 1CuS@4TiO2 and 1CuS@5TiO2, were examined. Three samples of pure TiO<sub>2</sub> (by hydrothermal method), CuS, and physically mixed TiO<sub>2</sub>/CuS were also prepared for comparison.

2.2. Characteristics of Synthesized CuS and Core@Shell-Structured CuS@TiO2. The synthesized CuS and core@shellstructured CuS@TiO2 photocatalysts were examined by XRD (X'Pert Pro MPD PANalytical 2-circle diffractometer) using nickel-filtered CuK $\alpha$  radiation (30 kV and 30 mA). The sizes and shapes of the CuS and core@shell-structured CuS@TiO<sub>2</sub> photocatalysts were examined by TEM (JEOL 2000EX). The BET surface areas of catalysts were measured using a Belsorp II instrument. All the catalysts were degassed under vacuum at 150°C for 30 min before the BET surface measurements. The catalysts were measured through the nitrogen gas adsorption using a continuous flow method with a mixture of nitrogen and helium as the carrier gas. The UVvisible absorption spectra of CuS and core@shell-structured CuS@TiO<sub>2</sub> powders were obtained using a Cary 500 spectrometer with a reflectance sphere. The CV measurements of the CuS and core@shell-structured CuS@TiO2 pellets were obtained using a BAS 100B potentiostat at room temperature in 0.1M KCl solution. A platinum wire as the counter electrode and Ag/AgCl as the reference electrode were used. The zeta potential of CuS and core@shell-structured CuS@TiO2 particles was determined by the electrophoretic mobility using an electrophoresis measurement apparatus (ELS 8000, Otsuka Electronics, Japan) with a plate sample cell. Electrophoretic light scattering (ELS) was performed in reference beam mode using a laser light source of 670 nm, a modular frequency of 250 Hz, and a scattering angle of 15°. The standard error of the zeta potential, converted from the experimentally determined electrophoretic mobility, was typically <1.5%, and the percentage error was <5%. To measure the zeta potentials, 0.1 wt% of each sample was dispersed in deionized water, and the pH of the solution was adjusted with HCl or NaOH. The relative molecular diameter size distributions of the various solutions were also measured using this equipment.

2.3. Hydrogen Production from Photo-Splitting of Methanol/Water over CuS and Core@Shell-Structured CuS@TiO<sub>2</sub>. Photo-splitting in methanol/water using CuS and core@shell-structured CuS@TiO<sub>2</sub> photocatalysts was carried out using a liquid photoreactor designed in house, as shown in Figure 1.

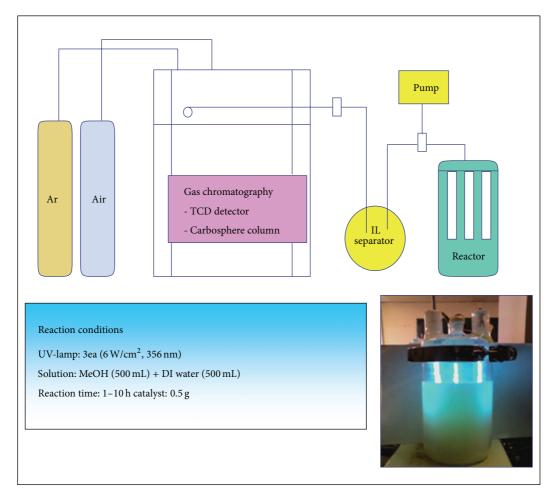


FIGURE 1: Apparatus of a liquid photoreactor for the methanol/water photo-splitting using CuS and core@shell-structured CuS@TiO<sub>2</sub> photocatalysts.

For methanol/water photo-splitting, 0.5 g of a photocatalyst was added to 1.0 L distilled water in a 2.0 L Pyrex reactor. UV-lamps  $(6 \times 3 \text{ W cm}^{-2} = 18 \text{ W cm}^{-2}, 30 \text{ cm length} \times 2.0 \text{ cm}$ diameter; Shinan Co.) emitting radiation with a wavelength of 365 nm were used. Methanol/water photo-splitting was carried out for 10 h with constant stirring, and the level of hydrogen evolution was measured at 1h intervals. The hydrogen gas (H2) produced during methanol/water photosplitting was analyzed by TCD-type gas chromatography (GC, model DS 6200; Donam Instruments Inc., Republic of Korea). To determine the products and intermediates, the GC was connected directly to the methanol/water photo-splitting reactor. The following GC conditions were used: TCD detector; Carbosphere column (Alltech, Deerfield, IL, USA); and an injection, initial, final, and detector temperature of 413 K, 393 K, 393 K, and 423 K, respectively.

#### 3. Results and Discussion

3.1. Properties of Synthesized CuS and Core@Shell-Structured CuS@TiO<sub>2</sub>. Figure 2 shows XRD patterns of the TiO<sub>2</sub>, CuS,

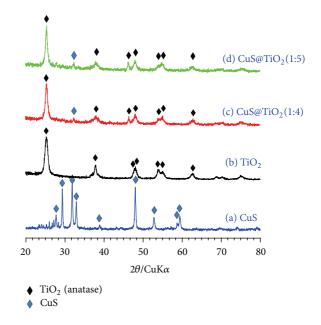


FIGURE 2: XRD patterns of the CuS and CuS@TiO<sub>2</sub> photocatalysts.

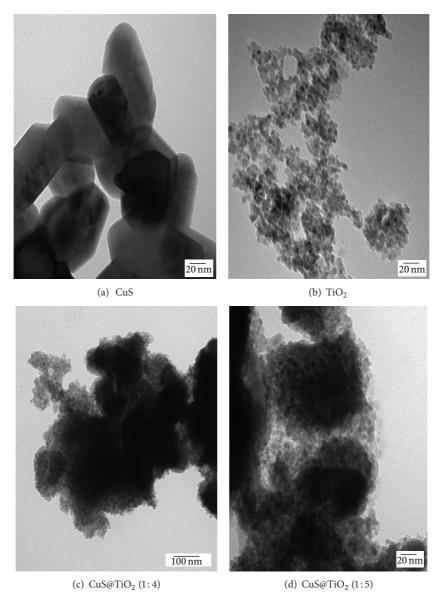


FIGURE 3: TEM images of the CuS and CuS@TiO2 photocatalysts.

and CuS@TiO<sub>2</sub> photocatalysts. All the peaks in CuS were indexed to the hexagonal phase CuS (P63/mmc space, cell constants  $a=3.8\,\text{Å}$ ,  $b=3.8\,\text{Å}$ , and  $c=16.43\,\text{Å}$ ; JCPDS Card no. 02-0820). The XRD patterns showed the main peaks at 26.75, 27.51, 29.36, 31.82, 33.03, 38.96, 43.04, 44.60, 52.88, 59.18, 63.69, 67.86, 69.58, 74.00, and 79.08° 2 $\theta$ , which were assigned to the (100), (101), (102), (103), (006), (105), (106), (008), (110), (114), (116), (1010), (0012), (207), (208), and (213) planes, respectively. In the case of CuS@TiO<sub>2</sub>, the peaks for crystalline CuS almost disappeared except for a very small peak at 33.03° 2 $\theta$  (006). This result coincides with the fact that in general if the core-shell structure formed completely in a core-shell material, the XRD peaks for the core do not appear; only the diffraction patterns for the shell are observed [27]. Otherwise, the XRD patterns for

crystalline TiO<sub>2</sub> (anatase, tetragonal crystal system, I41/amd space, JCPDS Card no. 02-0387) in CuS@TiO<sub>2</sub> were observed at 25.35, 37.93, 48.10, 53.89, 55.30, 68.99, 70.18, and 75.37° 2 $\theta$ , which were assigned to the (101), (004), (200), (105), (211), (116), (220), and (215) planes, respectively. The locations were the same as the hydrothermally prepared pure TiO<sub>2</sub> in (b). The peaks in CuS@TiO<sub>2</sub> were slightly larger according to the loaded Ti concentration. The XRD peak intensities that were assigned to anatase TiO<sub>2</sub> in 1CuS@5TiO<sub>2</sub> were slightly sharper than those of CuS@TiO<sub>2</sub> loaded with 4.0 mol-concentrated Ti. Generally, the line widths of the XRD peaks were broad, which indicated a smaller crystallite size. The Scherrer equation,  $t = 0.9 \lambda/\beta \cos \theta$ , where  $\lambda$  is the wavelength of incident X-rays,  $\beta$  is the full width at half maximum (FWHM) in radians, and  $\theta$  is the diffraction angle,

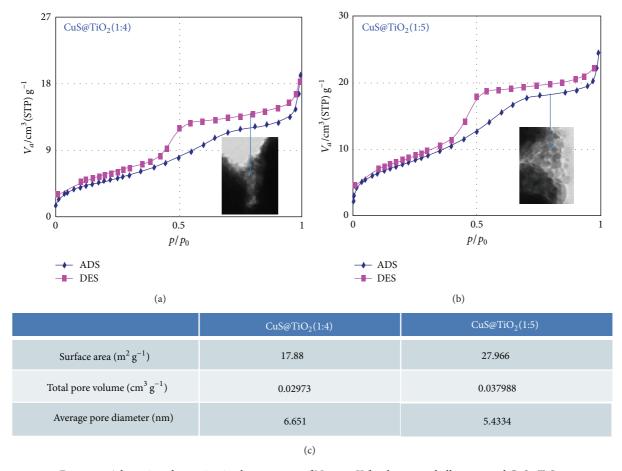


Figure 4: Adsorption-desorption isotherm curves of  $N_2$  at 77 K for the core@shell-structured CuS@TiO2.

was used to determine the crystallite size. The loaded  ${\rm TiO_2}$  crystallite sizes of  ${\rm 1CuS@4TiO_2}$  and  ${\rm 1CuS@5TiO_2}$  based on the 25.35°  $2\theta$  peak were 17.50 and 17.90 nm, respectively.

Figure 3 shows TEM images of the CuS and CuS@TiO2 powders. Rectangular-shaped particles with 100 nm long and 60 nm wide sides were observed in the CuS sample, and 10 nm sized TiO2 particles were also observed in TiO2 samples. Here, the nanosized TiO2 particles were synthesized hydrothermally for comparison. Interestingly, the huge CuS particles were surrounded by nanosized TiO2 particles with high concentrations (4~5 moles compared to 1 mole of core CuS). This is in good agreement with the XRD patterns. This is a reliable result in that, when the loaded TiO2 amounts increased, the shell composed of TiO2 particles was thicker. TEM confirmed that the obtained CuS@TiO2 sample had a core@shell structure.

Figure 4 shows the adsorption-desorption isotherm curves of  $\rm N_2$  at 77 K for the fresh powder samples and core@shell-structured  $\rm CuS@TiO_2$ . The isotherms belonged to the IV type in the IUPAC classification [28]. Generally, this hysteresis slope has been observed in the presence of large mesopores. Here, the mesopores are considered to be bulk pores formed between  $\rm TiO_2$  particles in the shell. This suggests that the reaction of the catalyst with a high surface area facilitates adsorption, which can improve the catalytic

activity. Therefore, it is expected that the methanol or water molecules are adsorbed more easily on the surfaces of the core@shell-structured CuS@TiO $_2$  than those of pure TiO $_2$  or CuS particles during methanol/water photo-splitting. The surface area increased from 17.88 to 27.97  $\rm m^2~g^{-1}$  according to the change in TiO $_2$  concentration from 4.0 to 5.0 mol. Generally, the specific surface area increases with decreasing particle size. Here, the loaded TiO $_2$  particle sizes in the two samples were similar. Therefore, the surface area in this study possibly depends on the bulk pores formed by aggregation between the TiO $_2$  particles in the shell. The total bulk-pore volumes increased from 0.029 (4 mol TiO $_2$  loading) to 0.038 (5 mol TiO $_2$  loading) cm $^3~g^{-1}$ . Eventually, the specific surface area increased with increasing pore volume.

Figure 5 shows the UV-visible absorption spectra of the CuS and core@shell-structured CuS@TiO<sub>2</sub> powders. The absorption edges of Ti<sup>4+</sup> and Cu<sup>2+</sup> with octahedral symmetries normally appear at a maximum of approximately 300 and 700 nm in pure TiO<sub>2</sub> and CuS, respectively [29, 30]. The band gap in a semiconductor material is closely related to the wavelength range absorbed, where the band gap decreases with increasing absorption wavelength. Consequently, a material with a narrow band gap can be extended readily to utilize visible light, whereas a narrow band gap can reduce photocatalytic activity by increasing the recombination rate

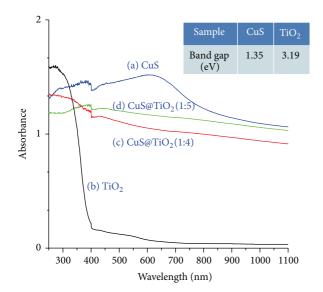


FIGURE 5: UV-visible absorption spectra of the CuS and core@shell-structured CuS@TiO<sub>2</sub> powders.

between the electrons and holes. Based on the Tauc equation [31], the band gaps obtained by extrapolation at the cross-section point of the two tangents were approximately 1.35 and 3.19 eV for pure CuS and  $\text{TiO}_2$ , respectively.

Figure 6 presents the CV measurements of CuS and the core@shell-structured CuS@TiO<sub>2</sub>, indicating high dependence on the analytic conditions being studied, which must be redox active within the experimental potential window. A reversible wave that provides the following information is desirable: reversible reactions will show a ratio of the peak currents passed at reduction ( $E_{pc}$ ) and oxidation ( $E_{pa}$ ). When such reversible peaks are observed, thermodynamic information in the form of a half cell potential  $E_{1/2}^{\circ}(E_{pc} +$  $E_{\rm pa}/2$ ) can be determined. In particular, when the waves are semireversible, such as when  $E_{pa}/E_{pc} \ge 1$ , it can be possible to induce even more information, particularly in kinetic processes. Recently, some studies reported a useful equation that can determine the energy levels of the HOMO and LUMO using a CV method [32]. In the synthesized CuS, the Cu(II)  $\rightarrow$  Cu(0) redox process appeared to be a reversible reaction, and the absolute potential in the reduction  $(E_{pc})$  was observed at -0.732 V. The onset potentials in the core@shell-structured CuS@TiO2 samples might be used to determine the thermodynamic  $E_{1/2}^{\circ}$  as -1.255 and -2.59 V in 1CuS@4TiO<sub>2</sub> and 1CuS@5TiO<sub>2</sub>, respectively. The CV curves were observed at two locations, and there might be two factors from TiO<sub>2</sub> (front) and CuS (back), -1.79 and -0.712 V, respectively. Therefore, the corresponding LUMO energy levels were calculated to be -3.65 (for CuS), -3.12 (for 1CuS@4TiO<sub>2</sub>), and -3.668 (for 1CuS@5TiO<sub>2</sub>) eV, respectively.

Figure 7 summarizes the hydrogen evolution from methanol/water photo-splitting over the CuS, TiO<sub>2</sub>, and two types of core@shell-structured CuS@TiO<sub>2</sub> photocatalysts in a batch-type liquid photosystem, and the catalytic performance of a physically mixed CuS+TiO<sub>2</sub> sample was also evaluated

for comparison. The catalytic activities of the core@shellstructured CuS@TiO2 photocatalysts were enhanced considerably compared to the pure CuS or TiO<sub>2</sub>. In Figure 7(a), a very small amount of hydrogen was collected over CuS (0.2 mmol) and TiO<sub>2</sub> (0.09 mmol) after methanol/water photo-splitting for 10 h. A significant amount of hydrogen gas was collected over CuS@TiO<sub>2</sub>, and the amount of hydrogen produced reached 1.9 mmol over 0.5 g 1CuS@4TiO<sub>2</sub>. On the other hand, the amount produced was significantly lower on the core@shell-structured 1CuS@5TiO<sub>2</sub> catalyst with higher Ti incorporation. Here, CuS absorbs longer wavelengths easily, but recombination between the excited electrons and the holes also causes rapid catalytic deactivation. In contrast, the core@shell-structured CuS@TiO<sub>2</sub> has stronger oxidationreduction ability than pure CuS. Here, the CuS core acts as a good electron collector excited from TiO<sub>2</sub> and transporter, resulting in the retardation of electron-hole recombination, leading to an increase in photocatalytic performance. On the other hand, the collected hydrogen did not increase significantly over the physically mixed CuS+TiO<sub>2</sub> sample. The catalytic performance of methanol/water destruction over the core@shell-structured 1CuS@4TiO2 was enhanced more under the alkali electrolytes solution, as shown in Figure 7(b). When OH<sup>-</sup> ions are present in the alkali solution, the subsequent reaction occurs:  $OH^- + hole \rightarrow OH$  in the valence band. Therefore, a large number of OH radicals are generated in the alkali solution, resulting in an increase in hydrogen evolution. Hydrogen production was increased dramatically in the alkali solution by generating more OH ions, reaching up to 8.0 mmol after 10 h in a KOH (pH = 11) solution. In an acidic solution, however, the level of production was decreased due to  ${\rm SO_4}^{2-}$  ions formed after the reaction. The S ions inside the CuS catalyst appear to dissolve in the acidic solution, followed by a reaction with O ions in water to form  $SO_4^{2-}$  ions. Eventually, the sulfate ions combine with the hydrogen ions generated during the methanol/water photo-splitting process, which occurs during the formation of  $H_2SO_4$ .

Figure 8 shows the influence of pH on the zeta potential distribution in the CuS,  ${\rm TiO_2}$ , and two types of core@shell-structured  ${\rm CuS@TiO_2}$ . The adjacent table summarizes the aggregated particle sizes in the aqueous solution. The zeta potential of the  ${\rm 1CuS@4TiO_2}$  suspensions decreased significantly with increasing pH. The surface charges in all samples changed from a positive value in an acidic solution to a larger negative value in an alkali solution. The isoelectric points, meaning the large aggregation of particles, were different: 5.8, 7.9, 7.0, and 7.7 for  ${\rm CuS}$ ,  ${\rm TiO_2}$ ,  ${\rm 1CuS@4TiO_2}$ , and  ${\rm 1CuS@5TiO_2}$ , respectively. At pH = 11.0, the surface charges in all samples showed the highest absolute value. This suggests that the colloidal samples were stable [33] with high mobility, which is closely related to the reaction sites over the photocatalyst surface. This result matches the results in Figure 6 well.

The CV curves, UV-visible absorption spectra, and their photocatalytic performance suggest a photocatalysis model over the core@shell-structured CuS@TiO<sub>2</sub>, as shown in Scheme 1. The TiO<sub>2</sub> shells covered the core CuS completely, which means that the electrons on the valence band of

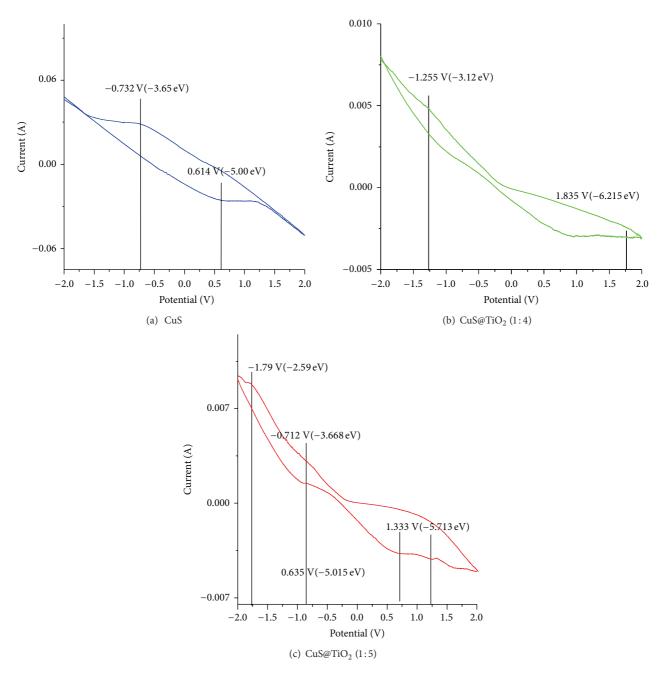


FIGURE 6: Cyclic voltammetry for the CuS and core@shell-structured CuS@TiO<sub>2</sub>.

TiO<sub>2</sub> will be transferred to the conduction band. The excited electrons are moved to the valence band in CuS because of its higher reduction potential than TiO<sub>2</sub>. In this study the core CuS acted as a good electron collector and transporter, similar to reduced graphene oxide reported in another paper [34]. Therefore, the recombination of electrons and holes was reduced, and finally more OH radicals were generated easily at the holes in the valence band of TiO<sub>2</sub>. Radicals with strong oxidative power attack CH<sub>3</sub>OH molecules, and CO<sub>2</sub>, H<sub>2</sub>, and H<sub>2</sub>O are produced by the complete oxidation of methanol. In addition, if the core CuS also absorbs the radiation (if it does not have a complete core@shell structure),

the electrons would be excited more easily from the valence band of CuS. Overall, the catalytic activity of  $CuS@TiO_2$  is performed more effectively in the methanol/water photosplitting reaction. This also means that the electrons excited from the valence band over  $CuS@TiO_2$  recombine slowly with the holes during photocatalysis. Therefore, the hole effect at the valence band continues for a longer time than those in pure CuS or  $TiO_2$ . In addition, according to the UV-visible spectra, the  $CuS@TiO_2$  samples exhibited enhanced absorbance over the entire visible-light region. Therefore, the CuS core can also absorb visible radiation compared to the  $TiO_2$  shell, which can only absorb UV light. Consequently,

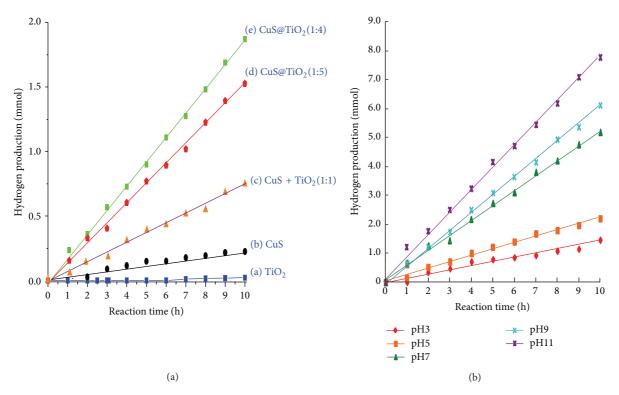
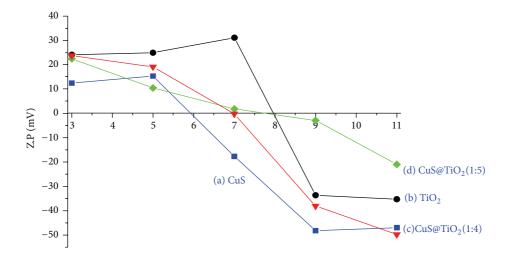
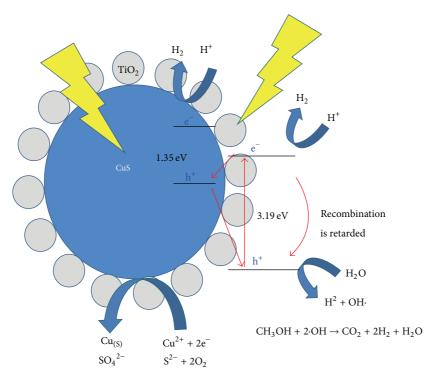


Figure 7: Evolution of  $\rm H_2$  from methanol/water photo-splitting over the CuS,  $\rm TiO_2$ , and two types of core@shell-structured  $\rm CuS@TiO_2$  photocatalysts in a batch-type liquid photosystem. (a) Hydrogen production according to the catalysts and (b) hydrogen production according to the pH for  $\rm 1CuS@4TiO_2$ .



	(a) CuS		(b) TiO <sub>2</sub>		(c)CuS@TiO <sub>2</sub> (1:4)		(d) CuS@TiO <sub>2</sub> (1:5)	
pН	Zeta potential (mV)	Mobility (cm <sup>2</sup> /Vs)	Zeta potential (mV)	Mobility (cm <sup>2</sup> /Vs)	Zeta potential (mV)	Mobility (cm <sup>2</sup> /Vs)	Zeta potential (mV)	Mobility (cm <sup>2</sup> /Vs)
3	12.47	9.739e(-4)	24.06	1.944e(-4)	23.76	1.853e(-4)	22.42	1.749e(-4)
5	15.34	1.199e(-5)	24.89	1.944e(-4)	19.13	1.492e(-4)	10.5	8.189 <i>e</i> (-5)
7	-17.65	-1.377e(-4)	31.13	4.478e(-4)	-0.23	-1.802e(-6)	1.84	1.435e(-5)
9	-48.24	-3.775e(-4)	-33.61	-2.752e(-4)	-38.08	-2.970e(-4)	-2.88	-2.246e(-4)
11	-47.01	-3.673e(-4)	-35.29	-2.752e(-4)	-49.78	-3.887e(-4)	-20.94	-1.636e(-4)

Figure 8: Zeta potential distributions of the CuS,  $TiO_2$ , and two types of core@shell-structured  $CuS@TiO_2$  according to the pH.



SCHEME 1: Supposed photocatalysis model over the core@shell-structured CuS@TiO<sub>2</sub>.

the photocatalytic activity is enhanced over the core@shell-structured CuS@TiO<sub>2</sub> photocatalysts.

#### 4. Conclusions

Core@shell-structured CuS@TiO2 was synthesized using hydrothermal/impregnation methods. Based on the UVvisible absorption and CV results, the band gap of the pure CuS was estimated to be approximately 1.35 eV, respectively, and the corresponding LUMO energy level was -3.65 eV. ELS showed that the core@shell-structured 1CuS@4TiO<sub>2</sub> particles were stable in an alkali solution. A significant amount of hydrogen gas was collected over 0.5 g of the core@shell-structured 1CuS@4TiO2 photocatalyst, and the amount reached 1.9 mmol with a maximum yield of 8.0 mmol after 10 h in a KOH solution. This was due most likely to the slower recombination between the electrons and a hole, which enables higher catalytic performance over the core@shell-structured 1CuS@4TiO2. These results are expected to play a significant role in the development of new photocatalysts with a core@shell structure for dramatic hydrogen production.

#### Acknowledgment

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#### Research Article

# **H<sub>2</sub>** Fuels from Photocatalytic Splitting of Seawater Affected by Nano-TiO<sub>2</sub> Promoted with CuO and NiO

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To enhance  $H_2$  yields from the photocatalytic splitting of seawater, better photocatalysts such as nanostructured  $TiO_2$  promoted with NiO (2.5%) and CuO (2.5%) have been studied in the present work. The accumulated  $H_2$  yielded from the photocatalytic splitting of seawater containing oxalic acid (50 mM) as the sacrificial reagents on CuO/nano- $TiO_2$  is 8.53  $\mu$ mol/ $g_{cat}$  after the 5 h radiation. On the NiO/nano- $TiO_2$  photocatalyst, the  $H_2$  yield is relatively low (i.e., 1.46  $\mu$ mol/ $g_{cat}$ ). Note that the hole scavenging with chlorides in seawater may be associated with the less  $H_2$  yielded from the seawater photocatalysis (on CuO/nano- $TiO_2$ ) if compared with that from water (42.4  $\mu$ mol/ $g_{cat}$ ).

#### 1. Introduction

Utilization of fossil energy which may cause air pollution or global warming has negative impacts on the human health and environment. Today's world is also facing an urgency need in developing alternative fuels. Renewable hydrogen energy ( $\rm H_2$ ) is becoming one of the better alternatives. Combustion of  $\rm H_2$  for energy does not emit pollutant gases such as  $\rm CO$ ,  $\rm NO_x$ , or  $\rm SO_x$ .  $\rm H_2$  has also been widely used in many sectors such as food, metallurgical, electronic, chemical, petroleum, and refinery industries.  $\rm H_2$  has been technically demonstrated for transportation, heating, and power generation [1].

 $\rm H_2$  yielded from the photocatalytic splitting of water has extensively received attention recently [2–4]. Since the  $\rm H_2$  generation by the water electrochemical method was demonstrated, splitting of water photocatalyzed by  $\rm TiO_2$  for the  $\rm H_2$  fuel has been considered to be one of the alternates [5]. The  $\rm TiO_2$ -based photocatalysts for  $\rm H_2$  generation could be promoted by codoping of antimony and chromium [6],

nickel and either tantalum or niobium [7], cobalt [8], Pt [9], and nitrogen [10]. During photocatalysis, photo-excited holes can irreversibly oxidize electron donor compounds, and thus facilitate water reduction by conduction band electrons if the bottom of the conduction band of the photocatalyst is located at a more negative redox potential than the reduction potential of water [11]. Inorganic reagents such as  $Na_2S$  and  $Na_2SO_3$  are generally used as the sacrificial compounds [12, 13].

In the present work, CuO and NiO were used as the promoters on the nanosize  ${\rm TiO_2}$  to enhance catalytic splitting of water and seawater. Oxalic acid which may be formed from the photocatalytic reduction of  ${\rm CO_2}$  in  ${\rm H_2O}$  was used as the sacrificial reagent during photocatalysis.

#### 2. Materials and Methods

The CuO (2.5%) and NiO (2.5%) supported on nanosize  ${\rm TiO_2}$  (P25) (UR, ITIT001) were prepared by the impregnation method. The samples were dried and calcined at 673 K for two

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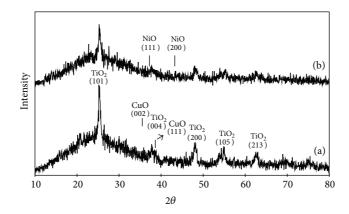


FIGURE 1: XRD patterns of (a) CuO and (b) NiO promoted nano-TiO<sub>2</sub>.

hours to form CuO and NiO dispersed on TiO<sub>2</sub> (CuO/nano-TiO<sub>2</sub> and NiO/nano-TiO<sub>2</sub>), respectively. The X-ray diffraction (XRD) patterns of the photocatalysts were recorded on a XRD spectrometer using Cu K $\alpha$  radiation ( $\lambda$  = 1.5418 Å) ranged from 10° to 80° (2 $\theta$ ) at the scanning speed of 5°/min.

The XANES spectra of the  ${\rm TiO_2}$  photocatalysts were also recorded on the Wigler 17C beam line at the Taiwan National Synchrotron Radiation Research Center (NSRRC). The electron storage ring was operated at the energy of 1.5 GeV (ring current = 120–200 mA). A Si(111) double crystal monochromator was used for selection of energy at an energy resolution ( $\Delta E/E$  (eV/eV)) of  $1.9 \times 10^{-4}$ . The absorption spectra were collected in ion chambers that were filled with helium and nitrogen mixed gases. Beam energy was calibrated by the adsorption edges of nickel and copper foils at the energy of 8335 and 8979 eV, respectively.

The photocatalytic splitting of water and seawater experiments was carried out in a quartz reactor (45 mL) having a total reflection mirror system. About 100 mg of the catalyst samples were dispersed in the simulated seawater (about 35 g of NaCl in the 1L of pure water) under magnetic stirring for five hours. A 300 W Xenon arc lamp (Oriel Instruments, Model 6259) equipped with a water filter was used as the photocatalytic light source. The  $\rm H_2$  gas generated from the photocatalytic splitting of water and seawater was analyzed by a gas chromatography (Varian 430-GC) equipped with a thermal conductivity detector. The apparent quantum efficiency (QE) of the photocatalysts was obtained by the equation QE (%) = (number of reacted electrons)/(number of incident photons) × 100 = (number of evolved  $\rm H_2$  molecules × 2)/(number of incident photons) × 100.

#### 3. Results and Discussion

The XRD patterns of the CuO/nano-TiO $_2$  and NiO/nano-TiO $_2$  photocatalysts are shown in Figure 1. The main diffraction peaks of the photocatalysts at (101), (200), (004), and (105) are observed, suggesting that the photocatalysts have mainly anatase crystallites. The XRD peaks of CuO and NiO are barely observed in the CuO/nano-TiO $_2$  and NiO/nano-TiO $_2$ , which may be due to the existence of

subnanosize CuO and NiO crystallites that are well dispersed on the nano-TiO<sub>2</sub>.

The XANES spectra of nickel and copper in the photocatalysts are shown in Figure 2. Metallic nickel (Ni) and copper (Cu) are not found. The absorption features observed at 8335 and 8979 eV suggest that NiO and CuO are the main nickel and copper species on the TiO<sub>2</sub>, respectively.

Figure 3 presents the photocatalytic splitting of water and seawater containing 0.05 M oxalic acid as the sacrificial reagent. On the nano-TiO2 photocatalyst, a very small amount of H2 is formed from the photocatalytic splitting of water and seawater. Notably, the accumulated H<sub>2</sub> yielded from the photocatalytic splitting of water on CuO/nano-TiO<sub>2</sub> and NiO/nano-TiO<sub>2</sub> is about 32.4 and 3.07  $\mu$ mol/g<sub>cat</sub> after the 5h radiation, respectively. Compared to the photocatalytic splitting of seawater on CuO/nano-TiO2 and NiO/nano-TiO<sub>2</sub>, the accumulated H<sub>2</sub> yields are less than those from water by 3.8 and 2.1 times, respectively. Hole scavenging with chlorides may occur during photocatalysis [14, 15]. Many hydroxyl groups such as TiOH<sub>2</sub>, TiOH on TiO<sub>2</sub> may absorb Cl<sup>-</sup> to form TiCl, which may decrease the H<sub>2</sub> yield in the photocatalysis [16, 17]. Generally, CuO on TiO<sub>2</sub> can be reduced to  $Cu^{+}$  ( $E_0 = 0.16 \, V$ ) or  $Cu^{0}$  ( $E_0 = 0.34 \, V$ ) by attracting the excited electrons from the valence band of  ${\rm TiO_2}$ during photooxidizing [18-21]. The reduction potential of NiO ( $E_0 = -0.25 \text{ V}$ ) is slightly less than the TiO<sub>2</sub> conduction band gap ( $E_0 = -0.26 \text{ V}$ ) [22, 23]. Additionally, the reduction potential of  $H^+/H_2$  ( $E_0 = -0.00 \text{ V}$ ) is less than that of CuO or NiO. CuO and NiO can thus promote TiO2 in the photocatalytic H<sub>2</sub> formation.

In the separate experiments, oxalic acid was formed from simultaneously photocatalytic reduction of  $\rm H_2O$  and  $\rm CO_2$ . It is of great interest to study the behavior of acetic acid as the sacrificial compound for photocatalytic splitting of water and seawater for the  $\rm H_2$  fuel. Note that addition of sacrificial reagents in water or seawater may cause water pollution.

Effects of the oxalic acid sacrificial reagent concentrations on the photocatalytic splitting of water and seawater on  $\text{CuO/nano-TiO}_2$  are shown in Figure 4. Without oxalic acid,  $\text{H}_2$  may not be formed in the photocatalysis. A small amount of oxalic acid can enhance the  $\text{H}_2$  generation. Note that

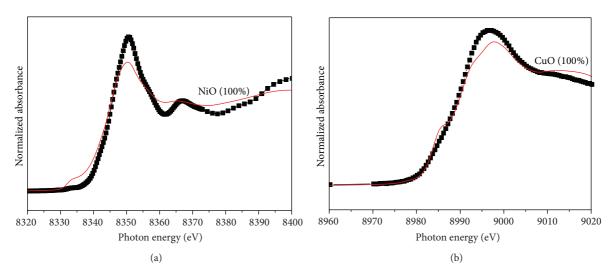


FIGURE 2: Component-fitted XANES spectra of (a) nickel and (b) copper in the NiO/nano-TiO<sub>2</sub> and CuO/nano-TiO<sub>2</sub> photocatalysts, respectively.

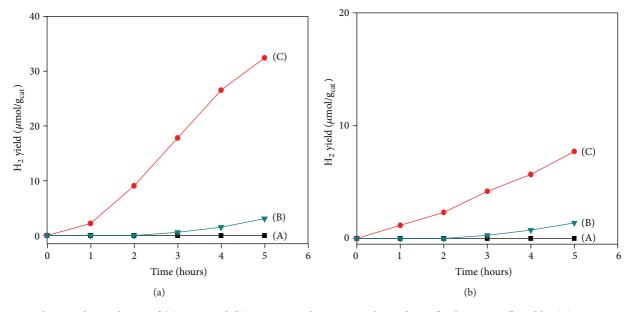


FIGURE 3: Photocatalytic splitting of (a) water and (b) seawater with 50 mM oxalic acid sacrificial reagent affected by (A) nano-TiO<sub>2</sub>, (B) NiO/nano-TiO<sub>2</sub>, and (C) CuO/nano-TiO<sub>2</sub>.

oxalic acid is a strong reductive reagent which may consume the photogenerated holes. After a 5 h UV-Vis irradiation, a better  $\rm H_2$  yield from the photocatalytic splitting of water is about 42.4  $\mu$ mol/g<sub>cat</sub> when the initial concentration of oxalic acid is 12.5 mM. However, the photocatalytic  $\rm H_2$  formation from water and seawater affected by CuO and NiO promoted  $\rm TiO_2$  was less than that of related studies, mainly due to the fact of the much less amount of the sacrificial reagents used in the photocatalysis. With an increase of the initial oxalic acid concentration by two times, the photocatalytic  $\rm H_2$  generation is slightly decreased. As the initial concentration of oxalic acid is increased by four times, the  $\rm H_2$  yields from the photocatalytic splitting of water are decreased by 24%. It seems that excessive oxalic acid sacrificial reagent may

not have a positive effect on the photocatalytic splitting of water.

#### 4. Conclusions

Photocatalytic splitting of seawater for  $\rm H_2$  formation on CuO/nano-TiO<sub>2</sub> and NiO/nano-TiO<sub>2</sub> is feasible experimentally. The sacrificial reagent (oxalic acid) can enhance the  $\rm H_2$  yields in the photocatalytic splitting of seawater. However, the excessive sacrificial reagent may not favor the photocatalysis. It is worth noting that a better  $\rm H_2$  can be yielded from the photocatalytic splitting of seawater affected by CuO/nano-TiO<sub>2</sub> (8.53  $\mu$ mol/g<sub>cat</sub>) than that by NiO/nano-TiO<sub>2</sub> (1.46  $\mu$ mol/g<sub>cat</sub>). In particular, the hole scavenging with

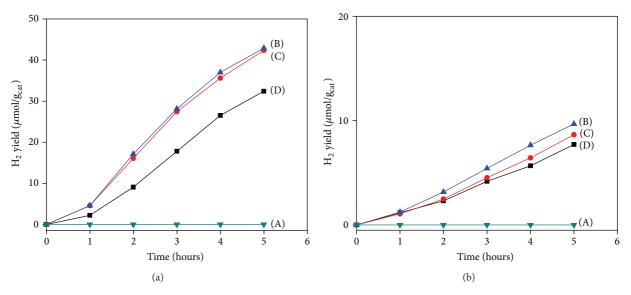


FIGURE 4: Photocatalytic splitting of (a) water and (b) seawater affected by  $CuO/nano-TiO_2$  with (A) 0, (B) 12.5, (C) 25, and (D) 50 mM of the oxalic acid sacrificial reagent.

chlorides in seawater may be associated with the less  $H_2$  yielded from the seawater photocatalysis (on CuO/nano-TiO<sub>2</sub>) if compared with that from water (42.4  $\mu$ mol/g<sub>cat</sub>).

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#### Research Article

# Removal of Formaldehyde Using Highly Active Pt/TiO<sub>2</sub> Catalysts without Irradiation

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Formaldehyde (HCHO) is one of the major indoor air pollutants.  $TiO_2$  supported Pt catalysts were prepared by sol-gel method and used to eliminate HCHO at room temperature without irradiation. The reduced Pt/ $TiO_2$  catalyst (denoted as Pt/ $TiO_2$ -H<sub>2</sub>) showed much higher activity than that calcined in air (denoted as Pt/ $TiO_2$ -air). More than 96% of the conversion of HCHO was obtained over 0.5 wt% Pt/ $TiO_2$ -H<sub>2</sub>, on which highly dispersed metallic Pt nanoparticles with very small size (~2 nm) were identified. Metallic Pt rather than cationic Pt nanoparticles provide the active sites for HCHO oxidation. Negatively charged metallic Pt nanoparticles facilitate the transfer of charge and oxygen species and the activation of oxygen.

#### 1. Introduction

Gaseous formaldehyde (HCHO) may cause adverse effects on both air quality and human health [1-3]. Great efforts have been made to eliminate indoor HCHO to satisfy the stringent environmental regulations and improve air quality. Physical adsorption with porous materials or the combined physical adsorption and chemical reaction by impregnating the chemical reagents (such as potassium permanganate and organic amine) on the adsorption materials was found to be effective for eliminating HCHO emission but only for a short period before saturation. The overall efficiency of these adsorbent materials is not so promising due to their limited removal capacities [4, 5]. Catalytic oxidation is recognized as the most promising HCHO removal technology [6-8]. Nevertheless, HCHO oxidation can only occur under irradiation (UV or visible light) or at high temperature over most of the reported catalysts [9-11]. In these cases, an extra irradiation or heating apparatus is needed, causing higher operating cost and more severe reaction conditions, which is not suitable for the control of indoor air pollution [10]. For air cleaning, low energy demand and low concentration of HCHO strongly require a catalyst to exhibit high activity for complete oxidation of HCHO. HCHO purification at room temperature is highly desirable due to its environment-friendly reaction conditions and energy saving consideration [6, 7, 12]. Moreover, indoor air is often enriched with water vapor, which frequently leads to severe catalytic deactivation through the strong adsorption of water on the active sites, especially at low temperatures [10]. The development of effective catalysts for complete oxidation of low-concentration HCHO at ambient temperature is a challenging subject for scientists [4, 7].

Recently, several studies related to HCHO removal at low temperature have been carried out using supported noble metal (Pt, Rh, Au, and Pd) [6, 7, 13, 14] and nonnoble metal catalysts [15, 16]. Among them, Pt/TiO<sub>2</sub> is the most active [6, 14]. Peng and Wang [5] found that HCHO conversion for 1 wt% Pt/TiO<sub>2</sub> is only 14.3% at 20°C and it increased to 97% at 120°C. However, the oxidation state of active component may be changed due to HCHO reduction at high temperature, which may cause confusion to mechanistic study although supported Pt catalysts have been proved to be effective for HCHO oxidation at low temperature, even at room temperature in some cases. However, high loading of Pt is generally needed for effective oxidation of HCHO, which greatly limits its widespread application due to the expensive cost [10]. One

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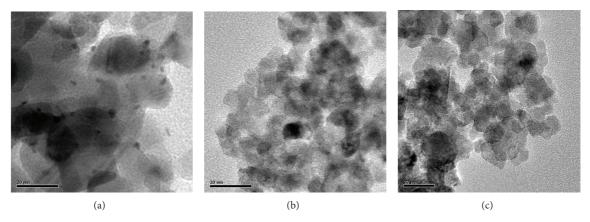


FIGURE 1: TEM micrographs for (a) Pt/TiO<sub>2</sub>-H<sub>2</sub>, (b) Pt/TiO<sub>2</sub>-air, and (c) TiO<sub>2</sub>.

alternative is to improve the catalytic activity by optimizing catalysts with lower Pt loading. In addition, several hundred ppm of HCHO concentration used for the performance test is much higher than the normal HCHO concentration in indoor environments, which generally ranges from dozens of ppb to ppm. Furthermore, the Pt catalysts were generally pretreated in air at high temperature [4, 6, 7, 14], which result in the formation of PtOx. As known, oxidation state of Pt is one of the most important factors controlling the catalytic activity [17]. The effect of metallic Pt on catalytic activity and the mechanism leading to high activity for HCHO oxidation at room temperature has not well demonstrated yet.

Herein, we present an effective catalyst with low Pt loading for the purification of indoor HCHO at room temperature without any irradiation. Efficient elimination of low-concentration HCHO was obtained over a reduced 0.5 wt% Pt/TiO $_2$  catalyst prepared by sol-gel method. Structural analysis of the catalysts used was performed and subsequently correlated with their catalytic performances to investigate the mechanism leading to the high activity over the reduced Pt nanoparticles.

#### 2. Experimental Sections

2.1. Preparation and Characterization of Pt/TiO<sub>2</sub> Catalysts. The Pt-doped TiO<sub>2</sub> catalysts were prepared by the sol-gel method. A mixture solution containing 34 mL of ethanol, 1.7 mL of water, and 1.7 mL of hydrochloric acid was added dropwise under vigorous stirring to another mixture solution containing 17 mL of tetrabutyl titanate, 5.1 mL of 0.02 mol/L chloroplatinic acid ( $\rm H_2PtCl_6\cdot 6H_2O$ ), and 45 mL of absolute ethanol. The resulting transparent colloidal suspension was stirred for 5 h and aged until the formation of gel. The gel was dried at 353 K for 12 h and then calcined at 673 K for 4 h in air and hydrogen flow, obtaining the oxidized and reduced Pt catalysts, respectively. They were referred to as Pt/TiO<sub>2</sub>-air and Pt/TiO<sub>2</sub>-H<sub>2</sub>, respectively. The Pt loading is 0.5 wt% on both catalysts. The catalysts were crushed and then sieved through 40–60 meshes.

Transmission electron microscopy (TEM) images were recorded by a Tecnai G2 20 microscope operated at 200 kV.

BET surface areas of the samples were measured by N<sub>2</sub> adsorption-desorption isotherms at 77 K using a Micromeritics ASAP 2020 instrument. Prior to the measurement, the samples were degassed at 573 K for 2 h. X-ray powder diffraction (XRD) patterns were collected with a Bruker D8 Advance X-ray powder diffractometer, using Cu K $\alpha$  ( $\lambda$  = 1.5418 Å) radiation. The working voltage of the instrument was 40 kV, and the current was 40 mA. The intensity data were collected in a  $2\theta$  range from  $20^{\circ}$  to  $90^{\circ}$ . The average crystal size was determined from the anatase peak broadening (101) crystal plane for anatase with Scherrer's formula. X-ray photoelectron spectroscopy (XPS) measurements of the catalysts were performed with a PHI 5000 VersaProbe system using a monochromatic Al K $\alpha$  source. The binding energies (BEs) were determined by utilizing C1s line as a reference with energy of 284.8 eV.

2.2. Measurement of Catalytic Activity. The oxidation of HCHO was performed in a quartz tubular (i.d. = 6 mm) fixed-bed reactor in a dark environment at ambient temperature (25  $\pm$  1°C). Also, 0.5 g of the catalyst in 40–60 mesh was loaded in the reactor. Gaseous HCHO was generated by zero air flowing through an HCHO solution in an incubator. An air mixture containing 10 ppm HCHO and water vapor (50% relative humidity) was introduced as the reactants. The total flow rate was 1 L/min, corresponding to a gas hourly space velocity (GHSV) of 120,000 mL/g<sub>cat</sub>·h. The HCHO and CO<sub>2</sub> in the air stream were analyzed by an HCHO monitor (Formaldemeter 400, PPM Technology) and a CO<sub>2</sub> monitor (HAL-HCO<sub>2</sub>01, Chinaway), respectively.

#### 3. Results and Discussion

#### 3.1. Catalyst Characterization

3.1.1. TEM. Representative TEM micrographs of the  $TiO_2$  and  $Pt/TiO_2$  are presented in Figure 1. The TEM micrograph for the  $Pt/TiO_2$ -air catalyst was similar to that of  $TiO_2$ . No distinguishable Pt particles are observed over the  $Pt/TiO_2$ -air catalyst, indicating that their sizes were probably very small and could not be detected by TEM. Pt nanoparticles prepared

TABLE 1: BET surface area of Pt/TiO<sub>2</sub> and TiO<sub>2</sub>.

Sample	$Pt/TiO_2-H_2$	Pt/TiO <sub>2</sub> -air	$TiO_2$	P-25
BET surface area (m <sup>2</sup> /g)	74.1	84.5	74.9	50 [18]

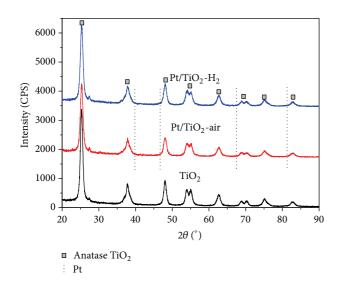


FIGURE 2: XRD patterns of the Pt/TiO<sub>2</sub> and TiO<sub>2</sub> catalysts.

by different methods existed with different crystal structure. Pt nanoparticles with very small and homogeneous size ( $\sim$ 2 nm) present uniformly on the surface of the Pt/TiO<sub>2</sub>-H<sub>2</sub> catalyst. Hence, the H<sub>2</sub> reduction promoted the formation of Pt clusters.

3.1.2. BET Surface Areas. Table 1 shows the BET surface area of the tested catalysts. TiO<sub>2</sub> prepared by sol-gel method obtained a BET surface area of 74.9 m<sup>2</sup>/g, which is much larger than that of commercially available P-25 TiO<sub>2</sub> (Degussa, Germany) with a BET surface area of 50 m<sup>2</sup>/g [18]. It is worth noting that the BET surface area of Pt/TiO<sub>2</sub>-air is increased to 84.5 m<sup>2</sup>/g, which is larger than that of Pt/TiO<sub>2</sub>-H<sub>2</sub> (74.1 m<sup>2</sup>/g). This is probably because Pt nanoparticles on Pt/TiO<sub>2</sub>-H<sub>2</sub> cover the surface of TiO<sub>2</sub> and block its pores. As observed in TEM, small Pt nanoparticles were highly dispersed on the support, which may cause the loss of surface area. Pt/TiO<sub>2</sub> prepared by sol-gel method possesses much higher surface area, which can provide more absorption sites for HCHO.

3.1.3. XRD. As shown in Figure 2, XRD patterns for pure  $TiO_2$  exhibited strong diffraction peaks at  $25.2^{\circ}$  and  $48.1^{\circ}$  indicating  $TiO_2$  in the anatase phase. The peaks of the  $Pt/TiO_2$ - $H_2$  and  $Pt/TiO_2$ -air catalyst are essentially the same as pure  $TiO_2$ , and no significant Pt peaks are observed, suggesting that Pt particles are very small, as observed by the TEM (Figure 1). The average particle sizes as calculated with the Scherrer formula were 14.1, 12.8, and 12.9 nm for the samples of  $TiO_2$ ,  $Pt/TiO_2$ - $H_2$ , and  $Pt/TiO_2$ -air, respectively. They are much smaller than P-25 with an average crystal sizes of about 30 nm [18]. The particle sizes for the  $Pt/TiO_2$ - $H_2$  and

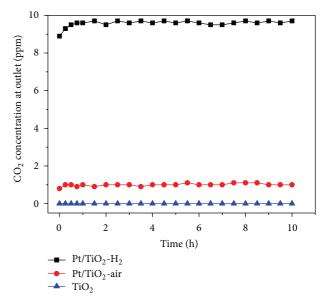


FIGURE 3: CO<sub>2</sub> concentration at the outlet of reactor.

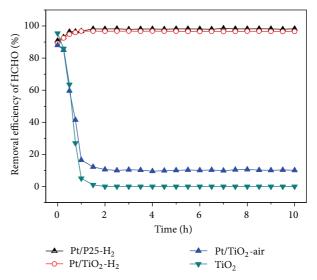


Figure 4: HCHO removal efficiency over the  $\mathrm{Pt/TiO_2}$  and  $\mathrm{TiO_2}$  catalysts.

Pt/TiO<sub>2</sub>-air are smaller than TiO<sub>2</sub>, indicating that the deposition of Pt can inhibit the growth of TiO<sub>2</sub> crystal. The doping of Pt probably changed the surface character of TiO<sub>2</sub> and avoided the sintering and conglobation during thermal treatment hence inhibiting its growth. It can be found that the average particle size of the Pt/TiO<sub>2</sub>-H<sub>2</sub> catalyst is almost the same as that of the Pt/TiO<sub>2</sub>-air catalyst. The small TiO<sub>2</sub> crystal accounts for the high BET surface area of the Pt/TiO<sub>2</sub>, as shown in Table 1.

3.2. Catalytic Activity Test. HCHO oxidation by pure TiO<sub>2</sub> can be excluded from the discussion since no CO<sub>2</sub> was identified during the reaction, as shown in Figure 3. However, CO<sub>2</sub> concentration was increased to about 1 ppm and 9.6 ppm over Pt/TiO<sub>2</sub>-air and Pt/TiO<sub>2</sub>-H<sub>2</sub>, respectively. Figure 4 shows

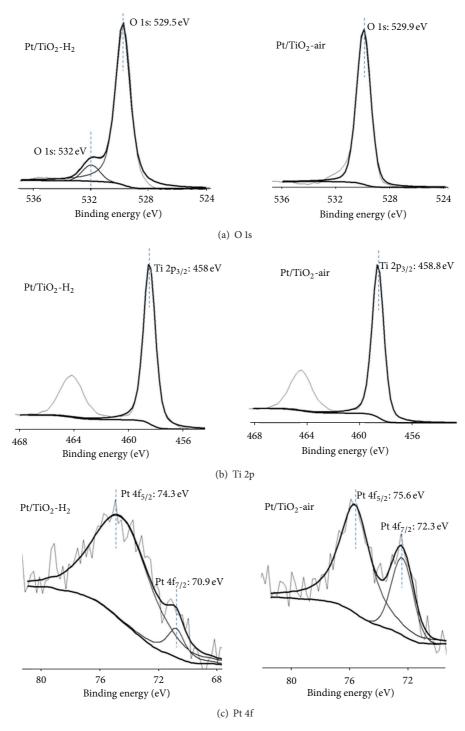


FIGURE 5: XPS spectra of the Pt/TiO<sub>2</sub>-H<sub>2</sub> and Pt/TiO<sub>2</sub>-air catalyst.

the time dependence of HCHO removal efficiency for Pt/TiO $_2$  together with TiO $_2$  at ambient temperature. The removal of HCHO at initial stage over pure TiO $_2$  and Pt/TiO $_2$ -air was mainly ascribed to the adsorption by TiO $_2$ . Only about 10% HCHO conversion was obtained over the Pt/TiO $_2$ -air catalyst at the stable stage, whereas it was notably increased to 96.6% over the Pt/TiO $_2$ -H $_2$  catalyst. HCHO removal efficiency was significantly improved over the Pt/TiO $_2$ -H $_2$  catalyst.

The results showed that the catalytic activities were greatly influenced by the catalyst's preparation methods.

The most important factors controlling the catalytic activity of nanoscale noble metal catalysts appear to be the particle size, nature of support, and noble metal oxidation state [19]. The smaller the size of nanoparticles is, the more active centers are formed, leading to better catalytic activity [20]. As described previously, the unreduced catalyst possesses higher

surface area and smaller Pt particles than the reduced one, which can provide more active sites for the adsorption and oxidation of HCHO. Therefore, the Pt/TiO<sub>2</sub>-air catalyst is expected to be more active for HCHO oxidation than the Pt/TiO<sub>2</sub>-H<sub>2</sub> catalyst. On the contrary, the former showed much poorer activity for HCHO oxidation than the latter, as shown in Figure 4. Therefore, Pt oxidation state should be the most important factors controlling the catalytic activity in this reaction. Reduced Pt supported on commercial TiO<sub>2</sub> (P25, Degussa) (Pt/P25-H2) also confirmed this. HCHO removal efficiency reached 98% over 0.5% Pt/P25-H<sub>2</sub>. Pt oxidation state was analyzed by XPS, as shown in Figure 5(a). The binding energy of Pt  $4f_{7/2}$  is 72.3 and 70.9 eV on the Pt/TiO<sub>2</sub>-air and Pt/TiO<sub>2</sub>-H<sub>2</sub> catalyst, corresponding to Pt<sup>2+</sup> and Pt<sup>0</sup> [21], respectively. Pt was reduced into metallic state on the Pt/TiO<sub>2</sub>-H<sub>2</sub> catalyst. Figure 4 clearly showed that the reduced Pt/TiO<sub>2</sub> with metallic Pt achieved much higher HCHO removal efficiency than the oxidized one with Pt<sup>2+</sup>, suggesting that metallic Pt is the active site for HCHO oxidation. Similar conclusions were made for active centers of Pd [22-25] and Au [26-28] in oxidation reaction. It is worth noting that Pt 4f<sub>7/2</sub> of Pt/TiO<sub>2</sub>-H<sub>2</sub> was shifted to lower BE by approximately 0.3 eV compared with bulk metallic Pt with typical Pt 4f<sub>7/2</sub> BE around 71.2 eV, indicating that nanoparticles are negatively charged on the Pt/TiO<sub>2</sub>-H<sub>2</sub> catalyst. The electron transfer was proposed to be responsible for this negative shift [21]. It can be observed from Figure 5(b) that Ti  $2p_{3/2}$ on the  $Pt/TiO_2$ -air catalyst is located at 458.8 eV, corresponding to Ti<sup>4+</sup> of TiO<sub>2</sub>. However, it was slightly shifted to 458.4 eV on the Pt/TiO<sub>2</sub>-H<sub>2</sub> catalyst, suggesting that Ti<sup>4+</sup> is partially reduced. The electron transfer can be expected from the reduced TiO<sub>2</sub> to Pt nanoparticles [29]. Oxygen vacancies on the reduced TiO<sub>2</sub> and the negative charged Pt showed enhanced capacity of O<sub>2</sub> adsorption. The charge was further transferred from negative charged Pt to the adsorbed O<sub>2</sub>, leading to negative charge of adsorbed O<sub>2</sub>. This was confirmed by the change of O 1s BE after reduction, as shown in Figure 5(c). The O 1s core level peak on the Pt/TiO<sub>2</sub>-air catalyst appears at 529.9 eV, which is ascribed to the lattice oxygen in TiO<sub>2</sub> [30]. However, it was negatively shifted to 529.5 eV on the Pt/TiO<sub>2</sub>-H<sub>2</sub> catalyst. Charge transfer from Pt particles to oxygen in the meanwhile activates the oxygen. Activated oxygen may exist in the form of Pt-O complex. It was confirmed by a significant shoulder peak of O 1s at 532.0 eV on the Pt/TiO<sub>2</sub>-H<sub>2</sub> catalyst, as shown in Figure 5(c). This shoulder peak of O 1s should belong to O of OH groups on the surface of the catalyst [31]. It is probably highly active and responsible for the HCHO oxidation. Thus, the transfer of charge and oxygen species and the activation of oxygen can efficiently occur at room temperature, which may account for the high activity of the Pt/TiO<sub>2</sub>-H<sub>2</sub> catalyst for HCHO oxidation.

HCHO in indoor air is often enriched with water vapor, which frequently leads to severe catalytic deactivation through the strong adsorption on the active sites, especially at low temperatures [10]. The Pt/TiO $_2$ -H $_2$  catalyst can keep active in moist air (50% relative humidity) at room temperature, and no deactivation was observed after reaction for 10 h. Thus, the activity of Pt/TiO $_2$  is stable and resistant to water.

#### 4. Conclusions

Purification of indoor HCHO at room temperature was investigated using  ${\rm TiO_2}$  supported Pt catalysts without irradiation. The  ${\rm H_2}$  reduced  ${\rm Pt/TiO_2}$  catalysts showed much higher removal efficiency than the unreduced one. More than 96% HCHO conversion was obtained over the reduced 0.5 wt%  ${\rm Pt/TiO_2}$  catalyst, on which highly dispersed metallic Pt nanoparticles with very small size (~2 nm) were identified. Oxidation state of Pt is the most important factor controlling the catalytic activity. Metallic Pt rather than cationic Pt nanoparticles provide the active sites for HCHO oxidation. Efficient purification of indoor HCHO was successfully achieved over a low Pt-loading catalyst at room temperature without any heating or illumination. It is a very efficient and promising technology for the removal of indoor HCHO.

#### **Conflict of Interests**

The authors declare that there is no conflict of interests regarding the publication of this paper.

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### Research Article

# Photocatalytic Degradation of Organic Dyes by $H_4SiW_6Mo_6O_{40}/SiO_2$ Sensitized by $H_2O_2$

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 $H_4SiW_6Mo_6O_{40}/SiO_2$  was sensitized by  $H_2O_2$  solution that significantly improved its catalytic activity under simulated natural light. Degradation of basic fuchsin was used as a probe reaction to explore the influencing factors on the photodegradation reaction. The results showed that the optimal conditions were as follows: initial concentration of basic fuchsin 8 mg/L, pH 2.5, catalyst dosage 4 g/L, and light irradiation time 4 h. Under these conditions, the degradation rate of basic fuchsin is 98%. The reaction of photocatalysis for basic fuchsin can be expressed as the first-order kinetic model. After being used continuously for four times, the catalyst kept the inherent photocatalytic activity for degradation of dyes. The photodegradation of malachite green, methyl orange, methylene blue, and rhodamine B were also tested, and the degradation rate of dyes can reach 90%–98%.

#### 1. Introduction

In the past few years, a great deal of attention has been paid to water-treatment technology [1]. A lot of water treatment techniques including condensation, ultrafiltration, membrane separation, and adsorption have been adopted to remove persistent organic compounds and microorganisms in water [2, 3]. Especially, advanced oxidation processes (AOPs), which have the potential to completely mineralize organic compounds to CO<sub>2</sub> and H<sub>2</sub>O, have shown a great potential as a low-cost and high efficiency water treatment technology [4]. Semiconductor photocatalytic process have played an important role in many advanced oxidation processes. Semiconductor materials including Ag<sub>2</sub>O [5], Ag-loaded Bi<sub>2</sub>WO<sub>6</sub> [6], TiO<sub>2</sub> [7, 8], bismuth tungstate [9], ZnO [10], and TiO<sub>2</sub>rGO [11] have been found to exhibit high photocatalytic activity. Although TiO2 has been investigated widely in photocatalytic degradation of organic chemicals in water under ultraviolet (UV) light, constituting only 4% of the solar light, it cannot be effectively activated under solar light irradiation due to its wide intrinsic band gap. Because the light wavelength of light sources is one of the few parameters that affects the overall photocatalytic rate, it is essential to

use solar light efficiently to achieve a high photocatalytic reaction rate. Visible-light responsive photocatalysts have been investigated quite intensively in recent years, including modified  ${\rm TiO_2}$  [12–15].

Heteropoly acid (HPA) has been extensively studied as acid or oxidation catalyst for a wide range of reactions [16, 17]. In recent years, HPA has also attracted much attention as photocatalysts owing to its photophysics and photochemical properties, analogous to these of semiconductors [18, 19]. Upon absorbing UV-near visible light irradiation, HPA will be excited to generate electron-hole pairs. The electron and hole will initiate reductive and oxidative reactions to decomposition of organic pollutants. However, several reports related to the photocatalysis of HPAs are concentrated on UV irradiation. In order to overcome their disadvantages, such as low surface area (1–10 m<sup>2</sup>/g), highly soluble in polar media, and difficulty in separation, HPAs should be immobilized on a support like montmorillonite clay [20], MCM-41 [21], and TiO<sub>2</sub> [22] to obtain insoluble catalysts. Moreover, some support materials seem to improve the catalytic performance of the combined catalysts because of a synergistic catalytic effect [23].

In this paper, it was attempted to improve photocatalytic activity of  $\rm H_4SiW_6Mo_6O_{40}/SiO_2$  according to sensitization by  $\rm H_2O_2$  solution. The photocatalytic degradation of some dyes having different chemical structures with the catalyst under simulated natural light irradiation was investigated.

#### 2. Experimental

2.1. Preparation of Samples.  $H_4SiW_6Mo_6O_{40}/SiO_2$  was synthesized according to reference [24, 25] by a sol-gel technique. An amount of  $H_4SiW_6Mo_6O_{40}$  was dissolved in 26 mL of  $H_2O$ , and a stoichiometric amount of TEOS was mixed with 1-BuOH. The latter was added dropwise to the aqueous solution. The resultant was allowed to be stirred at room temperature for 1 h, at 45°C for 1 h, and then at 80°C until a uniform gel was formed. The hydrogel obtained was dehydrated slowly at 45°C for 16 h in vacuum and then at 90°C for 3.5 h. Thus, the silica network was fastened, and the removal of the  $H_4SiW_6Mo_6O_{40}$  molecules from it was avoided. The particulate gel was washed with hot water for several times until the filtrate was neutral, and then the products were calcined for the required duration.

 $\rm H_4SiW_6Mo_6O_{40}/SiO_2$  was treated by  $\rm H_2O_2$  as follows [26]: 1g  $\rm H_4SiW_6Mo_6O_{40}/SiO_2$  was added into 15 mL 30%  $\rm H_2O_2$  solution and sonicated the mixture for 20 min. The slurry mixture was filtrated and dried at room temperature. This catalyst is denoted by  $\rm H_4SiW_6Mo_6O_{40}/SiO_2(x)$ .

2.2. Characterization. The FT-IR spectra of the samples in KBr matrix were recorded on a Nicolet 5700 FT-IR spectrometer in the range  $400{\sim}4000\,\mathrm{cm}^{-1}$ . The X-ray powder diffraction pattern of the samples was measured by a Bruker AXS D8-Advanced diffractometer (Bruker, Germany) employing Cu  $\mathrm{K}_{\alpha}$  radiation. Scanning electron micrographs (SEM) were obtained on a Hitachi S-3400N scanning electron microscope.

2.3. Photocatalytic Activity Measurement. The photocatalytic activities of the samples were determined by measuring the degradation of dyes in an aqueous solution under simulated sunlight irradiation. Simulated sunlight irradiation was provided by a 500 W xenon lamp (Nanjing Xujiang Electromechanical Factory), and the intensity of the lamp was 1200  $\mu$ mol·m<sup>-2</sup>·s<sup>-1</sup>. Solution pH was adjusted with dilute aqueous HCl and NaOH solutions. The system was cooled by circulating water and maintained at room temperature. Before irradiation, the suspension was vigorously stirred in the dark for 30 min to reach the adsorption-desorption equilibrium of dyes on the catalyst surface. At given time intervals, about 3 mL suspension was continually taken out from the photoreactor and centrifuged. The change of the basic fuchsin concentrations was analyzed by the UV-vis spectrophotometer (Hitachi U-3010).

#### 3. Results and Discussion

3.1. Characterization of the  $H_4SiW_6Mo_6O_{40}/SiO_2$  Catalyst. The IR spectra of  $H_4SiW_6Mo_6O_{40}$  and  $H_4SiW_6Mo_6O_{40}/SiO_2$ 

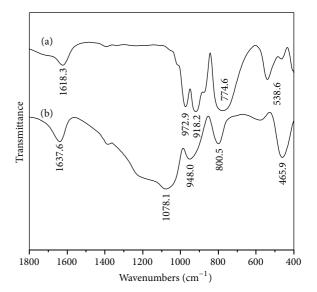


FIGURE 1: FT-IR spectra of  $\rm H_4SiW_6Mo_6O_{40}$  (a) and  $\rm H_4SiW_6Mo_6O_{40}/SiO_2$  (b).

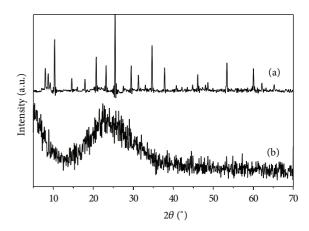


FIGURE 2: The XRD patterns of  $\rm H_4SiW_6Mo_6O_{40}$  (a) and  $\rm H_4SiW_6Mo_6O_{40}/SiO_2$  (b).

are shown in Figure 1. As shown in Figure 1, the characteristic bands of  $\rm H_4SiW_6Mo_6O_{40}$  Keggin anion at 972.9, 918.2, 774.6, and  $\rm 538.6\,cm^{-1}$  are observed for pure  $\rm H_4SiW_6Mo_6O_{40}$ . In addition, the band at  $\rm 1618.3\,cm^{-1}$ , which is the bending mode of the water, indicates the presence of the water. When  $\rm H_4SiW_6Mo_6O_{40}$  is bonded to the Si-OH group of  $\rm SiO_2$ , these bands have changed. However, the characteristic bands for the Keggin anion could be observed for  $\rm H_4SiW_6Mo_6O_{40}/SiO_2$ . The shifts indicate that a strong chemical interaction, not simple physical adsorption, exists between the  $\rm H_4SiW_6Mo_6O_{40}$  and the support.

Figure 2 shows the XRD patterns of  $H_4SiW_6Mo_6O_{40}$  and  $H_4SiW_6Mo_6O_{40}/SiO_2$ . The characteristic diffraction peaks of  $H_4SiW_6Mo_6O_{40}$  that were explored at 8.0, 10.4, 20.7, 25.5, 29.2, 34.5, and 37.8° can be assigned to the diffraction characteristic peaks of crystalline  $H_4SiW_6Mo_6O_{40}$  Keggin structure. For  $H_4SiW_6Mo_6O_{40}/SiO_2$ , only a broad band at  $2\theta=22.4^\circ$  that can be assigned to the diffraction peaks of

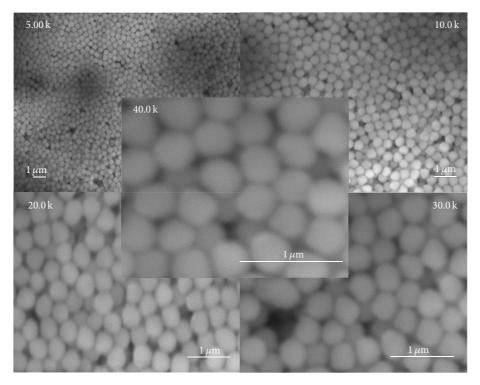


FIGURE 3: SEM images of SiO<sub>2</sub> particles at different multiples.

amorphous silica appears, but no signals of  $H_4SiW_6Mo_6O_{40}$  are displayed. Thus, it can be proposed that  $H_4SiW_6Mo_6O_{40}$  is well dispersed on the surface of silica support.

Figure 3 shows the SEM images of  ${\rm SiO_2}$  particles at different multiples. As can be seen from the figure, surface morphology of  ${\rm SiO_2}$  is spherical and massive. Silicon sphere is dispersed evenly in the whole system, and its diameter is about 4.5  $\mu$ m.

Figure 4 shows the SEM patterns of SiO<sub>2</sub>,  $H_4SiW_6Mo_6O_{40}$ , and  $H_4SiW_6Mo_6O_{40}/SiO_2$  at 5000 times. Surface morphology of  $SiO_2$  is massive, dispersed evenly in the whole system. Surface morphology of  $H_4SiW_6Mo_6O_{40}$  is net-like, and its specific surface area is relatively small. The results show that the catalyst not only uniformly dispersed in the system, but also the specific surface area is bigger than before.

#### 3.2. Investigation of Photocatalytic Activity of Catalysts

3.2.1. Comparison of Photocatalytic Activity of Catalysts. In order to detect the catalytic activity of catalysts, the degradation of model basic fuchsin aqueous over the samples was carried out at the basic fuchsin concentration of 16 mg/L, pH 2.5 and 4 g/L of catalyst, and the results are shown in Figure 5.

As shown in Figure 5, direct photolysis of an aqueous basic fuchsin under simulated natural light irradiation for 3.5 h did not cause any changes of its concentration. In addition, the degradation rate of basic fuchsin over  $\rm H_4SiW_6Mo_6O_{40}/SiO_2$  is only 31.0%, while the degradation rate over  $\rm H_4SiW_6Mo_6O_{40}/SiO_2(\it{x})$  is as high as 98%. The photocatalytic performance of  $\rm H_4SiW_6Mo_6O_{40}/SiO_2(\it{x})$  is much higher than that of  $\rm H_4SiW_6Mo_6O_{40}/SiO_2$ . So, the peroxo complexes formed from the decomposition of  $\rm H_4SiW_6Mo_6O_{40}$  in hydrogen peroxide have played an important role in the photodegradation of dyes. Therefore, it is concluded that the sensitizing effect has a remarkable influence on the photocatalytic activity of catalyst.

3.2.2. Effect of the Initial Concentration of Dye. To investigate the effects of initial concentration on the photocatalytic degradation of basic fuchsin, this was varied from 8 mg/L to 40 mg/L, and the results are presented in Figure 6.

From Figure 6, it can be seen that the photocatalytic degradation rate of basic fuchsin decreases with an increase in the initial concentration of basic fuchsin. This phenomenon could be attributed to the excessive absorption of the basic fuchsin molecules on the surface of catalyst and a diminishing of light penetration through the solution at high initial concentration of basic fuchsin, which inhibits the process of activated catalyst. Then, the optimum of the initial concentration is 8 mg/L.

3.2.3. Effect of Catalyst Dosage. We have also investigated the effects of catalyst dosage on the degradation rate of basic fuchsin, and the results were shown in Figure 7.

It was found that the degradation rate of basic fuchsin increases with an increase in the amount of catalyst from  $1\,\text{g/L}$  to  $4\,\text{g/L}$ , then decreases when the catalyst dosage is higher

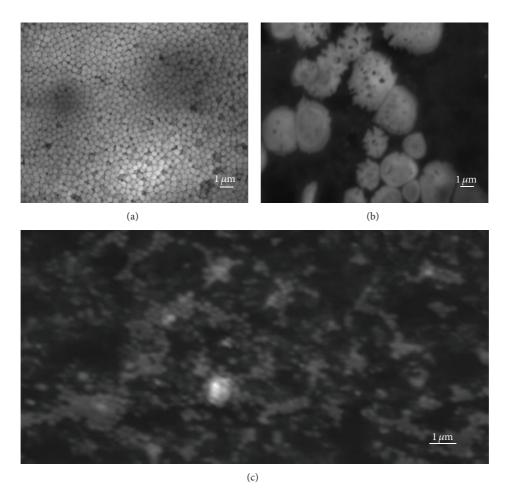


FIGURE 4: SEM images of SiO<sub>2</sub> (a), H<sub>4</sub>SiW<sub>6</sub>Mo<sub>6</sub>O<sub>40</sub> (b), and H<sub>4</sub>SiW<sub>6</sub>Mo<sub>6</sub>O<sub>40</sub>/SiO<sub>2</sub> (c).

than 4 g/L. This may be attributed to the scattering effect. The high turbidity of catalyst decreased the penetration depth of solar radiation [22]. So, the optimum amount of catalyst is 4 g/L.

3.2.4. Effect of pH. The pH value is one of the most important parameters in the photodegradation of organic compounds. The effect of pH on the photodegradation rate of basic fuchsin was also investigated at different pH. The results are shown in Figure 8.

From Figure 8, it can be seen that the degradation rate increased with decreasing pH of the solution, then decreases when pH of the solution is lower than 2.5. This is mainly ascribed to the variations of surface charge properties of the photocatalyst.

3.2.5. Effect of HPA. The effect of the kind of HPA on photocatalytic degradation of organic compounds was examined, and the results were shown in Figure 9.

From Figure 9, it can be seen that the kind of HPA plays an important role in the photocatalytic reaction. After 3.5 h irradiation under simulated natural light

irradiation, the degradation rate of basic fuchsin over  $\rm H_4SiW_6Mo_6O_{40}/SiO_2(x),~H_3PW_{12}O_{40}/SiO_2(x),~H_4SiW_{12}O_{40}/SiO_2(x),~H_4SiW_{12}O_{40}/SiO_2(x),~H_4SiW_6Mo_6O_{40}~is 98\%,~96\%,~68\%,~82\%,~and~68\%,~respectively. The activity of various HPA in the reaction follows the order <math display="inline">\rm H_4SiW_6Mo_6O_{40}/SiO_2(x) > H_3PW_{12}O_{40}/SiO_2(x) > H_3PW_6Mo_6O_{40}/SiO_2(x) > H_4SiW_{12}O_{40}/SiO_2(x) > H_4SiW_6Mo_6O_{40}.$ 

- 3.3. Photocatalytic Degradation of Various Dyes. In order to determine the feasibility of the catalyst in treatment of some dyes having different chemical structures, we attempted to choose other dyes such as methyl orange, rhodamine B, malachite green, and methylene blue as reactants. The results are shown in Figure 10. The degradation rate of dyes can reach 90%~98% at the optimized conditions. Therefore, the catalysts have good prospects of application in treatment of organic pollutants.
- 3.4. Reuse of the Catalyst. Reusability of the catalyst was also studied under the optimized conditions. After the reaction finished, the catalyst was recovered and washed with distilled

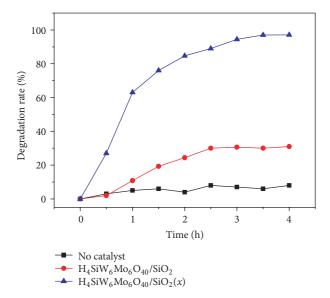


FIGURE 5: Comparison of photocatalytic activity of catalysts.

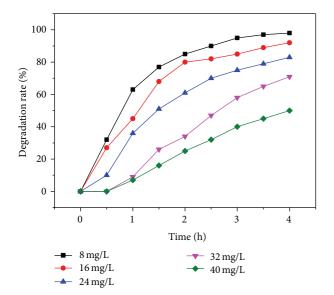


FIGURE 6: Effects of initial dye concentration on photocatalytic activity of catalyst.

water and ethyl alcohol. The recovered catalyst was treated again by  $H_2O_2$  for the next degradation run.

The results are shown in Figure 11. It was observed that a decrease in catalytic activity is observed with its subsequent reuse. However, the degradation rate of basic fuchsin can reach 87% in the fifth run. So, it can be concluded that the high catalytic activity is retained in a next run.

3.5. Kinetic Analysis. The kinetics of photocatalytic degradation of basic fuchsin by  $H_4SiW_6Mo_6O_{40}/SiO_2(x)$ ,  $H_3PW_{12}O_{40}/SiO_2(x)$ ,  $H_4SiW_{12}O_{40}/SiO_2(x)$ , and  $H_3PW_6Mo_6O_{40}/SiO_2(x)$  was studied under optimized conditions. The results are shown in Figure 12.

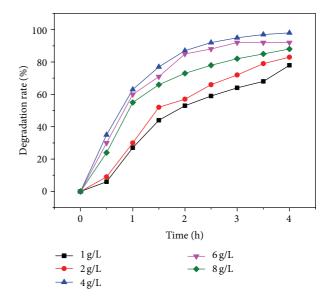


FIGURE 7: Effect of catalyst dosage on photocatalytic activity of catalyst.

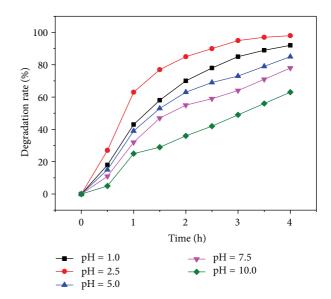


FIGURE 8: Effects of the solution pH on photocatalytic activity of catalyst.

The results show that a plot of  $\ln(C_0/C_t)$  versus "time" exhibits a nearly straight line, and the linear correlation coefficients (R) are ca. 0.985, 0.991, 0.994, 0.986, and 0.997, respectively. It can be concluded that the photodegradation reactions follow the first-order kinetics, which follow Langmuir-Hinshelwood kinetics. The rate constants were calculated to be 0.85, 0.45, 0.29, 0.15, and 0.99 h<sup>-1</sup>.

#### 4. Conclusion

 $\rm H_4SiW_6Mo_6O_{40}/SiO_2$  was prepared by a sol-gel method and sensitized by  $\rm H_2O_2$  solution. Degradation of basic fuchsin was used as a probe reaction to explore the influencing factors

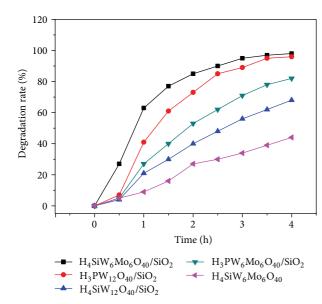


FIGURE 9: Effect of HPA on photocatalytic activity of catalyst.

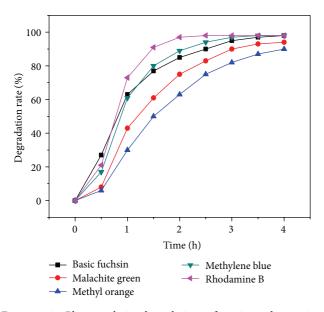


FIGURE 10: Photocatalytic degradation of various dyes using  $\rm H_4SiW_6Mo_6O_{40}/SiO_2(\it x)$  as a catalyst.

on the photodegradation reaction. The results showed the optimal conditions were as follows: initial concentration of basic fuchsin 8 mg/L, pH 2.5, catalyst dosage 4 g/L, and light irradiation time 4 h. Under these conditions, the degradation rate of basic fuchsin is 98%. The photodegradation of other dyes such as malachite green, methyl orange, methylene blue, and rhodamine B were also tested, and the degradation rate of dyes can reach 90%–98%. The high activity and stability of the catalyst is well retained after 5 runs. The reaction of photocatalysis for basic fuchsin can be expressed as the first-order kinetic model.

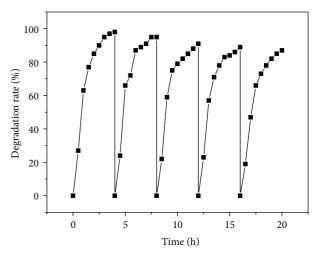


FIGURE 11: Recycling of the catalyst.

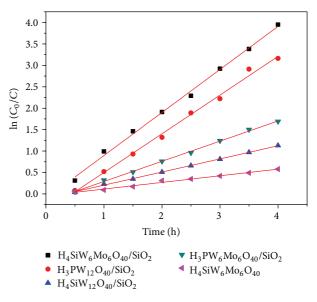


FIGURE 12: Relation curve of  $ln(C_0/C)$  and time (*t*).

#### Acknowledgment

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## Research Article

## Bactericidal Activity of TiO<sub>2</sub> on Cells of Pseudomonas aeruginosa ATCC 27853

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The photocatalytic activity of semiconductors is increasingly being used to disinfect water, air, soils, and surfaces. Titanium dioxide  $(TiO_2)$  is widely used as a photocatalyst in thin films, powder, and in mixtures with other semiconductors or metals. This work presents the antibacterial effects of  $TiO_2$  and light exposure (at 365 nm) on *Pseudomonas aeruginosa* ATCC 27853.  $TiO_2$  powder was prepared from a mixture of titanium isopropoxide, ethanol, and nitric acid using a green and short time sol-gel technique. The obtained gel annealed at 450°C was characterized by X-ray diffraction, Raman spectroscopy, ultraviolet-visible spectroscopy, diffuse reflectance, scanning electron microscopy, and transmission electron microscopy. The nanocomposite effectively catalyzed the inactivation of *Pseudomonas aeruginosa*. Following 90 minutes exposure to  $TiO_2$  and UV light, logarithm of cell density was reduced from 6 to 3. These results were confirmed by a factorial design incorporating two experimental replicates and two independent factors.

#### 1. Introduction

The gram-negative bacterium *Pseudomonas aeruginosa* (PA) is considered an opportunistic pathogen because it requires minimal nutrients to survive, can tolerate a wide variety of physicochemical conditions, and possesses one of the largest and most complex known prokaryotic genomes (conferring strong resistance to antibiotics). In addition, a high proportion of its proteins is involved in regulation, virulence functions, and transport. PA is a major cause of nosocomial infections, cystic fibrosis, ulcer-like keratitis, lung infections, and fatal diseases in immunocompromised individuals. Selfproduced antibiotic-inactivating enzymes cause high antibiotic resistance, low outer membrane permeability, and the expression of genes encoding various efflux pumps [1-3]. One area of continuing study is the type of surfaces likely to harbor pathogens, as reservoirs of contamination present a significant health hazard. Common sources of infection are hospitals, food, both consumption and production centers, and public places.

In 1972, Fujishima and Honda demonstrated that titanium dioxide TiO<sub>2</sub> (TD) exhibits strong bactericidal activity

in the presence of light ( $\lambda \le 385$  nm) [4]. To date, there have been several reports which tested the antibacterial activity of both powder in solution and surfaces coated with TD on clinically relevant microorganisms such as *Escherichia coli*, *Staphylococcus aureus*, *Listeria monocytogenes*, and *Pseudomonas aeruginosa* [5, 6].

At the cellular level, some researchers have found different modes of action of bactericidal activity on TD, between which there are two commonly accepted mechanisms that have been proposed for the bactericidal action of TD (i) direct oxidation of intracellular coenzyme A, leading to respiratory inhibition [7], and (ii) loss of potassium ions and the slow release of pathogenic proteins and RNA, resulting in death by intracellular disorder and cell wall decomposition [8]. Conversely, photocatalysis has been shown to promote destruction of the cell membrane [9]. Some studies have identified the most resistant pathogens as those with both complex gene expression systems and thickened cell walls [9–11]. The bactericidal activity of PA has been reported. Others researchers have found variable results, 100% inhibition in 25 minutes using TD solutions (1 mg/mL) [6] until reports

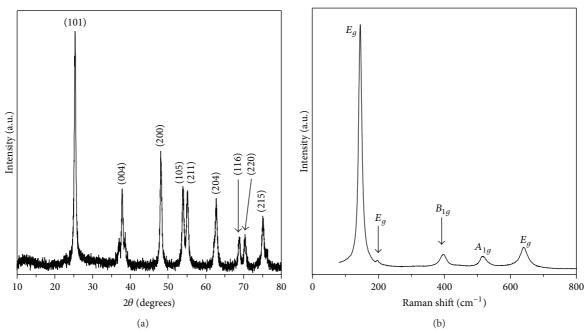


FIGURE 1: (a) Powder XRD of TiO<sub>2</sub> synthesized by sol-gel at 450°C. (b) Raman spectrum of TiO<sub>2</sub> powder obtained at 450°C.

indicate that the use of concentrations of 10 mg/mL of Ag doped TD with similar inhibition values reached in 120 minutes [12] and tests on films of TD. The nature of the materials used due to the synthesis and thermal treatment are some of the factors that have an influence on the antibacterial ability. Our group has obtained the synthesis of TD in thin film by the sol-gel method, according to the method reported in [13], obtaining good results in the degradation of methylene blue; however, antimicrobial activity was unknown in TD powder. So in this research paper we carried out the characterization and evaluated the antimicrobial effect of the TD powder on *Pseudomonas aeruginosa* ATCC 27853.

#### 2. Experimental Methods

2.1. Powder of Titanium Dioxide. The titanium dioxide TiO<sub>2</sub> powder was prepared by the sol-gel technique from a precursor solution containing titanium isopropoxide, ethanol, deionized water, and nitric acid (molar ratio 2:72:6:1 [13]). The preparation of this solution requires an inert atmosphere. The precursor solution, thus prepared, was removed from the inert atmosphere and dried at 80°C until all solvents had evaporated. The powder obtained was annealed at 100°C for 1 hour and 450°C for another hour in an open atmosphere, after which, pure titanium dioxide powder was obtained. The characterization of the TD powders was carried out by XRD patterns and was registered using a Rigaku Miniflex<sup>+</sup> Diffractometer (CuK $\alpha_1$  radiation, 1.54 Å). For the Raman measurements a Dilor Labram II microRaman was employed. The diffuse reflectance of the samples was measured using an Ocean Optic Spectrometer. The SEM and TEM images were obtained by a JEOL JSM-6060LV and JEOL JEM1010 microscopies, respectively.

2.2. Bactericidal Activity. Pseudomonas aeruginosa ATCC 27853 was grown in a 30 mL nutrient broth at 37°C for 16 h. The bacterial suspension was then centrifuged at 3,000 rpm for 10 min. and washed twice with saline solution (NaCl 0.85%). The resulting cell pellet was resuspended in 1 mL of saline solution, and cell density was determined using a Neubauer counting chamber. Prior to testing the antimicrobial properties of TiO<sub>2</sub>, the cell count was adjusted to 10<sup>6</sup> cells mL<sup>-1</sup>. The test itself was performed in glass vessels in which 10<sup>6</sup> cells were mixed with 0.5 and 1 mg (final volume 1 mL). A vessel without TiO<sub>2</sub> was prepared as a control.

The mixed solutions were irradiated with UVA (365 nm) from a black-light bulb (9 W). Exposure times were 30, 60, 90, and 120 min. Following exposure, the solution was sampled to determine the cell viable counts using the most probable number method (MPN). Decimal dilutions of samples were inoculated in quintuplicate in tubes containing nutrient broth and incubated at 37°C for 24 h. Tubes in which the solution had become turbid during incubation were considered positive for bacterial growth. Data from these tubes were used to calculate cell numbers and cell viability (as a percentage of all cells). The Degussa P25 (P25) was used in order to compare the TD synthesized for our experimental method. The characteristics of the P25 are nanopowder with 21 nm particle size (TEM), >99.5%.

#### 3. Results and Discussion

X-ray diffraction (XRD) was performed on the TD powders to determine their phase and crystallinity. Figure 1(a) shows the XRD patterns with peaks at  $2\theta = 25.32$ , 37.82, 48.12, 53.94, 55.11, 62.76, 68.8, 70.38, and 75.14°, corresponding to the planes (101), (004), (200), (105), (211), (204), (116), (220), and (215), respectively. These planes closely match

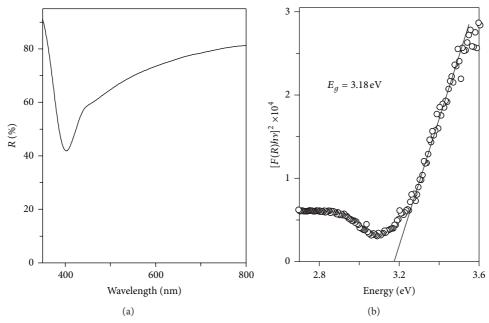


FIGURE 2: (a) Uv-Vis diffuse reflectance spectra of  $TiO_2$  obtained at 450°C. (b) Band gap of the  $TiO_2$  computed by Kubelka-Munk function, where  $E_a$  is the band gap energy, R is the reflectance of the TD, h is Planck's constants, and  $\nu$  is the frequency of the radiation.

those of PDF number 78-2486, corresponding to the pure tetragonal anatase TD phase. The grain size, calculated from the XRD pattern using the Scherer formula, is 25.27±0.11 nm. The anatase phase in TD is one of the most important metal oxides in terms of potential applications to photonic crystals, sensors, smart surfaces coatings, photovoltaic cells, photocatalysis, and bactericidal agents and as such has been extensively studied [9, 14-17]. The phase of bactericidal TD powder was determined by Raman spectroscopy. The TD displays six Raman active modes of anatase phase, with symmetries of 3 vibrating modes for  $E_q$ , and 2 for  $B_{1q}$  and  $A_{1q}$ , corresponding to 144, 197, 399, 515, 519, and 639 cm<sup>-1</sup> [18– 20]. Figure 1(b) displays the Raman spectra of TD obtained at 450°C in an open atmosphere, in which the vibrating modes occur at 144, 196, 396, 516, and 638 cm<sup>-1</sup>, consistent with those reported previously for the anatase phase [18-20].

Figure 2 shows the Uv-Vis diffuse reflectance spectra of TD powder annealed in an open atmosphere at 450°C. The maximum of the reflection edge can be estimated as 390 nm. From the plot of the Kubelka-Munk function versus the energy of the incoming radiation and supposing that the anatase phase of TD is an indirect band gap semiconductor, a band gap of 3.18 eV was obtained (Figure 2(b)).

The superficial structure of the TD annealing at 450°C was characterized by scanning electron microscopy (SEM) imaging (Figures 3(a) and 3(b)). The sample contains a range of particle sizes (diameter 30 to 1 micron). The larger particles comprise aggregates of smaller particles. Under transmission electron microscopy (TEM), the nanocrystalline form of the TD powder is revealed (Figures 3(c) to 3(e)). The TEM images display tetragonal nanocrystals with facets (001) and (101) of anatase phase. The space group is I4(1)/amd. Recently, it has been revealed that the reactivity of TD depends

not only on its superficial separation properties but also on low recombination of bulk charge carriers and/or the ability of TD to tune its reaction preferences during reaction [21, 22]. Conversely, materials with structures such as (001) facets of anatase exhibited enhanced photocatalytic activity, because they efficiently generate OH\* radicals that promote the chemical destruction. In the context of our study, such radicals can penetrate the bacterial cell wall, leading to death of the bacterium.

The predominance of the facet is {001}, {101}, and {010} [23–25]. Figures 3(d) and 3(e) show the different morphologies obtained in the anatase TD nanocrystals. Similar results of the TEM images were found by Hao et al. [22] and Jiao et al. [24]. To control the crystal morphology, the exposed (001) and (101) facets (see insets) were synthesized via a green and short time sol-gel method in the absence of fluorine compounds, which are hazardous to both environment and health. Being the most electronegative element in the periodic table, fluorine is extremely reactive (corrosive and poisonous) and requires care in handling.

Figure 4 displays photocatalytic activity of the TD and commercial P25 (exposed to light at 365 nm) versus time, for concentrations 0.5 mg mL<sup>-1</sup> (Figure 4(a)) and 1 mg mL<sup>-1</sup> (Figure 4(b)). The black squares in both plots represent the effect of the light source only (control without TD and P25).

As revealed in Figure 4(a) the viability of cells exposed to 0.5 mg mL<sup>-1</sup> TD was affected significantly at 60, 90, and 120 minutes after which 99, 99.92, and 100% and for P25 99.38, 99.996, and 100% of the microorganism, respectively, were killed. Similar results were obtained at 1 mg mL<sup>-1</sup>, where cell viability was reduced by 99.7, 99.99, and 100% after 60, 90, and 120 min exposure, respectively, and the P25 99.997 and 100% for 60 and 90 min. With commercial P25 exposure

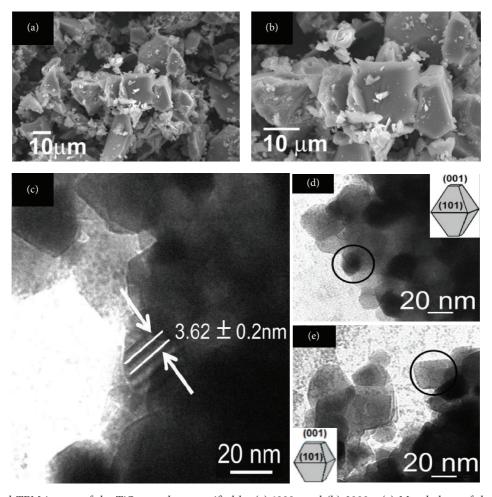


FIGURE 3: SEM and TEM images of the  $TiO_2$  powder, magnified by (a) 1000x and (b) 2000x. (c) Morphology of the anatase (distance between marks is 3.8 nm). (d) 2D tetragons showing highly absorbing (001) facets and (e) images of TD synthetized in the absence of fluorine compounds. Insets of Figures (d) and (e) are representative sketches of the faceted nanoparticles.

to the same times, we can observe better results with 1% (times ≥ 60 minutes), see Figures 4(a) and 4(b). As a control, a solution with  $1.7 \times 10^6$  and  $9 \times 10^5$  cells mL<sup>-1</sup> for 0.5 and 1 mg mL<sup>-1</sup>, respectively, was utilized. They were exposed to UV light (365 nm), showing no change in the density population; this was maintained in the order of 10°, so it discarded any inhibitory effect of UV light. The main difference between our TD and P25 is the crystal size. Currently in our laboratory, is underway additional work in order to find a new synthesis to obtain crystal size of the order of 21 nm, we probably get comparable results (closer) since it is well known that nanoparticles significantly increase the surface area. Ibáñez et al., 2003 [26], using Degussa P25 in a concentration of  $0.1\,\mathrm{mg\,mL^{-1}}$  on PA ATCC, starting with a cell density of 10<sup>6</sup> to 10<sup>7</sup>, after 40 min it observed that there is a decrease of 3 log. This is very comparable to the present study. Amézaga et al. 2003 [27] conducted a similar test on TiO<sub>2</sub> thin films (anatase phase) prepared on glass slides by the sol-gel process, in which it was found that Pseudomonas aeruginosa ATTC 27853 was inhibited by 32 to 72%, over a range of irradiation times (40 to 120 min). Under TEM they observed abnormal cell division after

40 min exposure to TiO<sub>2</sub>/UV. At 240 min, wavy structures and bubble-like protuberances appeared, and intracellular material was expelled [22]. Some biochemical mechanisms have been proposed for the powerful bactericidal action of photocatalytic anatase TD powder in the presence of an illumination source. Illumination encourages the generation of highly reactive chemical oxidative species (OH\*) that promote the peroxidation of phospholipid components in the lipid membrane and the oxidation of intracellular coenzymes, resulting in the inhibition of respiratory activity and subsequent cell death [7, 8, 26]. The intensity of the radiation used during the tests could have an effect on microbial inhibition. Robertson et al., 2005 [28], using Degussa P25 material at a concentration of 1 mg mL<sup>-1</sup>, obtained a 3 log reduction of PA in a time of 2 h, which is comparable to the test performed in this study; however, it was found that they used a 480 W lamp with a 330 to 450 nm wavelength range, which had a bactericidal activity confirmed in the controls when the test was performed in the absence of Degussa P25, obtained for exposing the cells to UV light; higher percentages of inhibition were reached. In the present research work no inhibition was observed by UV light lamp in the controls.

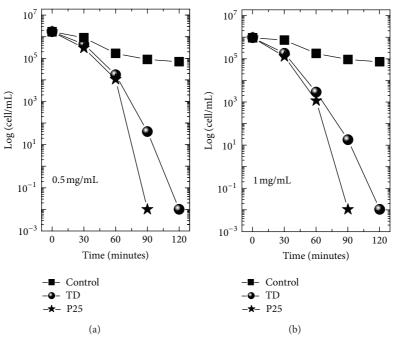


FIGURE 4: Effect of light and  $TiO_2$  concentration on viability of the *Pseudomonas aeruginosa* ATCC 27853 exposed to (a) 0.5 mg mL<sup>-1</sup> TD and P25 and (b) 1 mg mL<sup>-1</sup> TD and P25. In both plots, the control data (light exposure without TD and P25) are displayed as black squares.

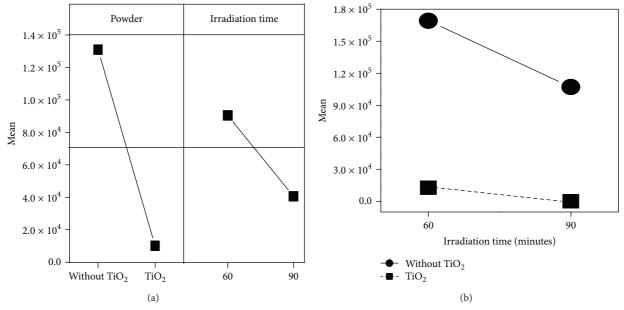


FIGURE 5: Principal effects and interaction between light and TD on the *Pseudomonas aeruginosa* survival at TD concentration 0.5 mg mL<sup>-1</sup>.

The grain size could also be related to bactericidal activity due to the increase in the reaction surface. Ubonchonlakate et al. conducted a test in 2012 [29] with porous film with grain size of 15 to 25 nm, and they obtained close to 100% at 60 minutes for a cell density of PA  $1 \times 10^3$  cells/mL. They also found that the use of porous materials and Ag particles reached almost 100% inhibition for 45 and 10 min, respectively. Similar results were obtained by Hitkova et al. 2012 [6] with thin films of TD, and they found efficiencies of 100% inhibition ( $10^5$  cells/mL) in a 25 min. The particle size

employed was 20 nm, the preparation time of the material was 340 h, and the thermal treatment was 500°C. In addition to particle size, the presence of Ag could influence the rapid reduction of cell viability, since it has been reported that this metal has bactericidal activity.

To assess the bactericidal effect of the anatase TD on *Pseudomonas aeruginosa*, the results were input to the Minitab program as an experimental design with two factors and two levels (results were analyzed at 60 and 90 minutes only). The computation was performed using full factorial design

StdOrder	RunOrder	CenterPt	Blocks	Powder	t/min	Y <sub>1</sub> (0.5 mg/mL)	Y <sub>2</sub> (1 mg/mL)
5	1	1	1	WTD	60	$1.690 \times 10^{5}$	$1.69 \times 10^{5}$
4	2	1	1	TD	90	$4.700 \times 10^{1}$	$1.30 \times 10^{1}$
1	3	1	1	WTD	60	$1.690 \times 10^{5}$	$1.69 \times 10^{5}$
7	4	1	1	WTD	90	$6.915 \times 10^4$	$6.91 \times 10^{4}$
2	5	1	1	TD	60	$1.275 \times 10^4$	$2.16 \times 10^{3}$
6	6	1	1	TD	60	$2.159 \times 10^4$	$3.28 \times 10^{3}$
3	7	1	1	WTD	90	$1.070 \times 10^{5}$	$1.07 \times 10^{5}$
8	8	1	1	TD	90	$3.300 \times 10^{1}$	$2.10 \times 10^{1}$

TABLE 1: Experimental data entered for the experimental design run.

TABLE 2: ANOVA factorial fit:  $Y_1$  (0.5 mg mL<sup>-1</sup>) versus TD powder and irradiation time.

Estimated effects and coefficients for $Y_1$ (0.5 mg/mL) (coded units)						
Term	Effect	Coeff	SE Coeff	T	P	
Constant		68581	4861	14.11	0.000	
TD	-119951	-59976	4861	-12.34	0.000	
Irradiation time	-9037	-24518	4861	-5.04	0.007	
$TD \times Irrad \ time$	31906	15953	4861	3.28	0.030	
S = 13750.1		PRESS = 3025065282				
$R^2 = 97.92\%$		$R^2 = 91.68\%$		$R^2$ (adj) = 96.36%		

with TD and WTD as the two factors and two replicates (see Table 1, where WTD is without  ${\rm TiO_2}$ ). To analyze the significance of factors, TD concentrations of  $0.5~{\rm mg~mL}^{-1}$  and  $1~{\rm mg~mL}^{-1}$  were considered separately, for two separate observations of the cell viability ( $Y_1$  and  $Y_2$ ), representing independent experiments.

The results of the factorial fit for  $0.5 \text{ mg mL}^{-1}$  powdered TD are presented in Table 2. We observe that the selected factors are significant at the 95% confidence level, because all of the P values are less than 0.05. The presence of TD powder, the exposure time, and the interaction between these two variables are similarly significant. The model further shows that the factorial design can account for 96.36% of the data behavior, confirming the bactericidal activity of the TD. At 1 mg mL<sup>-1</sup> TD (data not shown) similar P values are obtained and the model fits 96.86% of the data.

Figure 5 presents the principal effects of light irradiation (at 365 nm), TD presence, and irradiation time, as well as their combined effects, on *Pseudomonas aeruginosa*. The presence of TD and exposure to light independently decrease the estimated bacterial population significantly. The interaction between exposure time and the presence of TD powder is also significant, and their combined impact is greater than that of either factor alone.

#### 4. Conclusions

Powdered titanium dioxide in anatase phase with possible facets (001) and (010) was synthesized by the sol-gel technique from a simple, green, and short time route. The bactericidal properties of the synthesized compound were confirmed in aqueous solution. Titanium dioxide combined with illumination (at 365 nm) exerted significant antibactericidal activity.

The efficacy of this activity was confirmed by factorial design, which demonstrated that the mortality of *Pseudomonas aeruginosa* ATCC 27853 exposed for 90 minutes to 0.5 and 1 mg mL<sup>-1</sup> TD was 99.92 and 99.99%, respectively. The results consolidate previous reports of the unique physical and chemical properties of synthesized TiO<sub>2</sub> powder (namely, strong oxidizing and photocatalytic activity) that render it an effective bactericidal material.

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### Research Article

## The Multiple Effects of Precursors on the Properties of Polymeric Carbon Nitride

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Polymeric graphitic carbon nitride (g- $C_3N_4$ ) materials were prepared by direct pyrolysis of thiourea, dicyandiamide, melamine, and urea under the same conditions, respectively. In order to investigate the effects of precursors on the intrinsic physicochemical properties of g- $C_3N_4$ , a variety of characterization tools were employed to analyze the samples. The photocatalytic activity of the samples was evaluated by the removal of NO in gas phase under visible light irradiation. The results showed that the as-prepared CN-T (from thiourea), CN-D (from dicyandiamide), CN-M (from melamine), and CN-U (from urea) exhibited significantly different morphologies and microstructures. The band gaps of CN-T, CN-D, CN-M, and CN-U were 2.51, 2.58, 2.56, and 2.88 eV, respectively. Both thermal stability and yield are in the following order: CN-M > CN-D > CN-T > CN-U. The photoactivity of CN-U (31.9%) is higher than that of CN-T (29.6%), CN-D (22.2%), and CN-M (26.8%). Considering the cost, toxicity, and yield of the precursors and the properties of g- $C_3N_4$ , the best precursor for preparation of g- $C_3N_4$  was melamine. The present work could provide new insights into the selection of suitable precursor for g- $C_3N_4$  synthesis and in-depth understanding of the microstructure-dependent photocatalytic activity of g- $C_3N_4$ .

#### 1. Introduction

Visible-light-active photocatalysts are attracting increasing interests for their potential application in the areas of environmental protection, material science, and solar energy conversion by directly utilizing nature sunlight and artificial indoor illumination [1–3]. During the past few decades, many efforts have been devoted to develop novel and efficient visible light photocatalytic systems, including inorganic photocatalysts (e.g., Fe<sub>2</sub>O<sub>3</sub>, (BiO)<sub>2</sub>CO<sub>3</sub>, Cu<sub>2</sub>SnS<sub>3</sub>, SrTiO<sub>3</sub>, and WO<sub>3</sub>/BiOCl) [4–7], organic photocatalysts (e.g., graphitic carbon nitride, g-C<sub>3</sub>N<sub>4</sub>), and elemental photocatalysts (e.g., Si, P, S, and Se) [8–10].

In particular,  $g-C_3N_4$  material as a novel mental-free organic photocatalyst has triggered great attention in the fundamental and applied scientific researches due to its suitable electronic band structure, nontoxic nature, biocompatibility,

high thermal and chemical stability, easily available at low cost, and amenability to chemical modification [11–16]. Properties mentioned previously make it a promising organic photocatalyst for solar energy converting, organic photosynthesis, drug delivery, and environment remediation under visible light irradiation [17–19].

g- $C_3N_4$  can be prepared by the direct pyrolysis of various organic precursors. Dong et al. prepared g- $C_3N_4$  from thiourea and urea at 550°C for 2 h [20, 21], respectively. Yan et al. obtained g- $C_3N_4$  from melamine at 550°C for 4 h [22]. Xu et al. prepared g- $C_3N_4$  by directly heating dicyandiamide first at 350°C for 2 h and then 550°C for another 2 h [23], respectively. The different pyrolysis conditions for g- $C_3N_4$  synthesis made the comparison of the precursors difficult. Until now, little information is known about the effects of precursors on intrinsic physicochemical properties of g- $C_3N_4$  under the same pyrolysis conditions, including morphology, band gap,

TABLE 1: The cost, acute toxicity, and melting point of thiourea,
dicyandiamide, melamine, and urea [16].

Precursors	Cost (\$/t)	Acute toxicity LD <sub>50</sub> (oral, rat)	Melting point (°C)
Thiourea	3906	125 mg/kg	182
Dicyandiamide	1538	4000 mg/kg	209
Melamine	2025	3248 mg/kg	345
Urea	450	8500 mg/kg	133

thermal stability, surface area, pore volume, and yield and visible light photocatalytic activity. It is thus highly desirable to solve this issue in order to screen the most suitable precursors for synthesis of g- $C_3N_4$ .

In this paper,  $g-C_3N_4$  materials were prepared by directly treating thiourea, dicyandiamide, melamine, and urea under the same condition (550°C for 3 h in air), respectively. The precursors are easily available in the chemical industry at low cost (see Table 1). Various characterization tools were utilized to analyze the effects of precursors on the intrinsic physicochemical properties and photocatalytic activity of  $g-C_3N_4$ . The results showed that the precursors had significant effect on the properties of  $g-C_3N_4$ . Considering the cost, toxicity, and yield of the precursors and the properties of  $g-C_3N_4$ , the best precursor was confirmed.

#### 2. Experimental

2.1. Synthesis of g- $C_3N_4$ . In a typical synthesis, 12 g of thiourea was put into a semiclosed alumina crucible with a cover and then heated to 550°C in a muffle furnace for 3 h at a heating rate of  $10^{\circ}$ C min $^{-1}$ . Following the same procedure, g- $C_3N_4$  samples were prepared by directly treating dicyandiamide, melamine, and urea, respectively. After the reaction, the alumina crucible was cooled to room temperature. The resultant g- $C_3N_4$  were collected and ground into powder, respectively. The different g- $C_3N_4$  prepared from thiourea, dicyandiamide, melamine, and urea were labeled as CN-T, CN-D, CN-M, and CN-U, respectively.

2.2. Characterization. The crystal phases of the samples were analyzed by X-ray diffraction with Cu K $\alpha$  radiation (XRD: model D/max RA, Rigaku Co., Japan). FT-IR spectra were recorded on a Nicolet Nexus spectrometer on samples embedded in KBr pellets. The morphology and structure of the samples were further examined by transmission electron microscopy (TEM: JEM-2010, Japan). The UV-vis diffuse reflection spectra were obtained for the dry-pressed disk samples using a Scan UV-vis spectrophotometer (UV-vis DRS: UV-2450, Shimadzu, Japan) equipped with an integrating sphere assembly, using  ${\rm BaSO_4}$  as the reflectance sample. Nitrogen adsorption-desorption was conducted on a nitrogen adsorption apparatus (ASAP 2020, USA). The thermal stability was detected by using thermogravimetry analysis (TG-DSC, Netsch STA 449F3) under N<sub>2</sub> gas atmosphere. All the samples were degassed at 150°C prior to measurements.

2.3. Visible Light Photocatalytic Performance. The photocatalytic activity was investigated by removal of NO at ppb levels in a continuous flow reactor at ambient temperature. The volume of the rectangular reactor, which was made of polymethyl methacrylate plastics and covered with quartz-glass, was  $4.5\,L\,(30\,cm\times15\,cm\times10\,cm)$ . A  $100\,W$  commercial tungsten halogen lamp (General Electric) was vertically placed outside and above the reactor. Four minifans were used to cool the flow system. Adequate distance was also kept from the lamp to the reactor for the same purpose to keep the temperature at a constant level. For the visible light photocatalytic activity test experiment, a UV cut-off filter (420 nm) was adopted to remove UV light in the light beam.

For each photocatalytic activity test, two sample dishes (with a diameter of 12.0 cm) containing photocatalyst powder were placed in the center of the reactor. The weight of the photocatalyst used for each dish was kept at 0.1 g. g-C $_3$ N $_4$  sample was added into 30 mL of  $\rm H_2O$  and sonicated for 10 min, and then photocatalyst samples were prepared by coating aqueous suspension of the samples onto the glass dishes. The coated dish was pretreated at 60°C to remove water in the suspension and then cooled to room temperature before photocatalytic testing.

The NO gas was acquired from a compressed gas cylinder at a concentration of 100 ppm of NO (N<sub>2</sub> balance, BOC gas) with the National Institute of Standards and Technology (NIST) standard. The initial concentration of NO was diluted to about 600 ppb by the air stream supplied by a zero air generator (Thermo Environmental Inc., model 111). The relative humidity at indoor environmental condition is 40%-80%. The desired relative humidity in the present system is controlled at 50% in the gas flow which could simulate the indoor environmental conditions. The desired relative humidity (RH) level of the NO flow was controlled at 50% by passing the zero air streams through a humidification chamber. The gas streams were premixed completely by a gas blender, and the flow rate was controlled at 2.4 L min<sup>-1</sup> by a mass flow controller. After the adsorption-desorption equilibrium was achieved, the lamp was turned on. The concentration of NO was continuously measured by a chemiluminescence NO analyzer (Thermo Environmental Instruments Inc., model 42c), which monitors NO, NO2, and NOx (NOx represents  $NO + NO_2$ ) with a sampling rate of 0.7 L min<sup>-1</sup>. The removal ratio ( $\eta$ ) of NO was calculated as  $\eta$  (%) =  $(1 - C/C_0) \times 100\%$ , where C and  $C_0$  are concentrations of NO in the outlet steam and the feeding stream, respectively. The kinetics of photocatalytic NO removal reaction is a pseudofirst order reaction at low NO concentration as  $ln(C_0/C) = kt$ , where k is the apparent rate constant.

#### 3. Result and Discussion

The XRD patterns (Figure 1(a)) of the samples prepared from thiourea, dicyandiamide, melamine, and urea can be indexed to g- $C_3N_4$  [24–26]. The strongest interplanar stacking peaks of the conjugated aromatic systems at around 27.6° are indexed to graphitic materials as the (002) peak. The small angle peaks at around 13.0° can be indexed to (100) peak

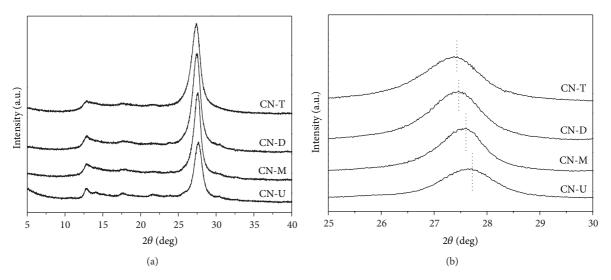


FIGURE 1: XRD patterns of the CN-T, CN-D, CN-M, and CN-U (a) and enlarged view of the (002) peak (b).

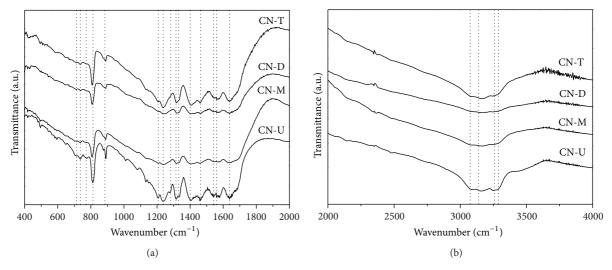


FIGURE 2: FT-IR spectra for CN-T, CN-D, CN-M, and CN-U.

of graphitic materials, corresponding to the in-plane tri-striazine units which formed one-dimensional (1D) melon strands. Further observation implies (Figure 1(b)) that the typical (002) peak is 27.43° for CN-T, 27.47° for CN-D, 27.60° for CN-M, and 27.72° for CN-U, respectively, indicating that the interplanar distance tends to decrease and g- $G_3N_4$  structure becomes more compact. The dense structure can be ascribed to the localization of the electrons and stronger binding between the layers [27, 28]. The dominant (002) diffraction peaks shifted toward higher diffraction angles for CN-U compared with CN-T, indicating that O-containing precursors (urea) could improve the polycondensation of g- $G_3N_4$ . In addition, the intensity and breadth of the XRD patterns (Figure 1) are different, due to the presence of different nanostructures and morphologies of the as-prepared g- $G_3N_4$  [29].

The chemical structures of dicyandiamide and melamine contain C=N bond which plays a key role in the formation of  $g-C_3N_4$ . However, both the S-containing thiourea and

O-containing urea do not containa C=N bond. The fact indicates that the formation mechanisms and condensation degrees of thiourea and urea are different from that of dicyandiamide and melamine [20–22, 30].

Figure 2(a) shows that the weak absorption at the 700–800 cm $^{-1}$  region is assigned to the bending vibration mode of CN heterocycles and the characteristic out of plane bending vibration mode of the triazine units at 810 cm $^{-1}$  for all the samples [31]. All the samples reveal several bands in the 1200–1650 cm $^{-1}$  region, which corresponds to the typical stretching vibration modes of the heptazine heterocyclic ring ( $C_6N_7$ ) units [32].

The stretching vibration modes of N–H and O–H at  $3000-3500\,\mathrm{cm}^{-1}$  are also observed (Figure 2(b)), indicating the existence of uncondensed amino groups and absorbed  $\mathrm{H_2O}$  molecules in all the samples [33]. It can be seen that the peak intensity of CN-U at  $400-4000\,\mathrm{cm}^{-1}$  is stronger than that of CN-T, CN-D, and CN-M, indicating that O-containing

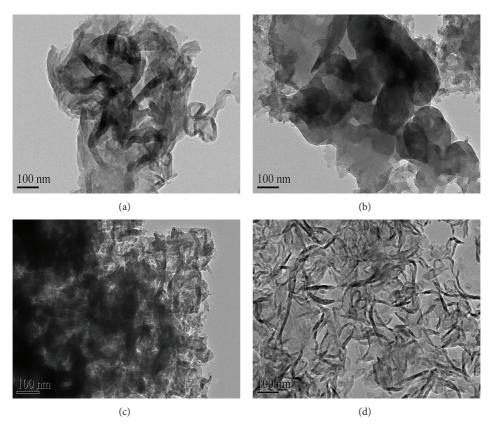


FIGURE 3: TEM images of CN-T (a), CN-D (b), CN-M (c), and CN-U (d).

precursors could improve the polycondensation of  $g-C_3N_4$  [34].

The morphologies and microstructures of CN-T, CN-D, CN-M, and CN-U were observed by TEM. As shown in Figure 3, all the samples consist of large amounts of packing layers with different sizes of nanosheets and nanoparticles, which exhibit obviously wrinkles and irregular shapes. Figure 3(a) shows that CN-T is composed of smooth and flat layers. Numerous large buckle nanosheets with aggregated structures which formed smooth layers in the CN-D sample can be seen in Figure 3(b). By observing carefully for CN-M (Figure 3(c)), the layers consist of dense and thick nanosheets with irregular shape. Figure 3(d) shows that CN-U is composed of smooth and thin layers with typical porous morphology and loose structure. The result clearly shows that CN-U prepared from urea favors the formation of typical porous structure. The fact indicates that the morphologies and microstructures of the resultant g-C<sub>3</sub>N<sub>4</sub> strongly depend on the different heteroatom-containing precursors.

As shown in Figure 4(a), all the samples exhibit excellent visible light absorption, and the absorption edges of the samples shift apparently to longer wavelengths from CN-U to CN-T. The band energies  $(E_g)$  which can be estimated from the intercept of the tangents to the plots of  $(Ahv)^{1/2}$  versus photo energy (Figure 4(b)) are 2.51, 2.58, 2.56, and 2.88 eV for CN-T, CN-D, CN-M, and CN-U, respectively. The fact indicates that the precursors could affect the band gap and

absorption edge of g-C<sub>3</sub>N<sub>4</sub>, which may be caused by the different local structures, defects, and degrees of condensation during the pyrolysis [8, 11].

Figure 5 shows the nitrogen adsorption-desorption isotherms and corresponding curves of the pore size distribution for CN-T, CN-D, CN-M, and CN-U. The isotherms of CN-T (Figure 5(a)), CN-D (Figure 5(c)), and CN-M (Figure 5(e)) can be classified to type IV, which indicates the presence of mesopores. The CN-U exhibits type III behavior (Figure 5(g)), which can be ascribed to the weak adsorbent-adsorbent interaction [35]. The specific surface areas and pore volumes of CN-T (23 m<sup>2</sup>/g and 0.14 cm<sup>3</sup>/g) and CN-U (153 m<sup>2</sup>/g and 0.40 cm<sup>3</sup>/g) are significantly higher than that of CN-D (18 m<sup>2</sup>/g and 0.09 cm<sup>3</sup>/g) and CN-M (14 m<sup>2</sup>/g and 0.06 cm<sup>3</sup>/g). The data illustrates that the heteroatoms of sulfur and oxygen play a key role in increasing the specific surface area and enlarging the pore volume during the condensation. The formation of H<sub>2</sub>S and CO<sub>2</sub>, release of NH<sub>3</sub>, and generation of additional H<sub>2</sub>O vapor during the pyrolysis of thiourea and urea favor the expansion of the packing layers and porous structure [32, 35]. Further observation implies that all the samples have micropores and mesopores. The interconnected porous network could mainly contribute to the formation of micropores and mesopores of CN-T (Figure 5(b)) and CN-U (Figure 5(h)), the aggregation of nanosheets and nanoparticles could result in the formation of the micropores and mesopores of CN-D (Figure 5(d)) and CN-M (Figure 5(f)) [19, 20].

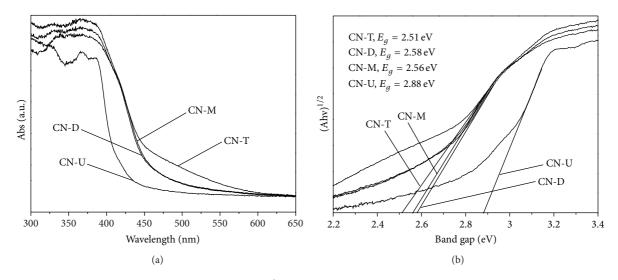


FIGURE 4: UV-vis DRS (a) and plots of  $(Ahv)^{1/2}$  versus photo energy (b) of CN-T, CN-D, CN-M, and CN-U.

Table 2: The  $S_{\text{BET}}$ , pore volume, band gap, removal ration, initial rate constant k, yield, and thermal stability of CN-T, CN-D, CN-M, and CN-U.

Samples	$S_{\rm BET}~({\rm m}^2/{\rm g})$	Pore volume (cm³/g)	Band gap (eV)	Removal ratio η (%)	k (min <sup>-1</sup> )	Yield (g)	Thermal stability (°C)
CN-T	23	0.14	2.51	29.6	0.310	1.46	<550°C
CN-D	18	0.09	2.58	22.2	0.079	3.73	<563°C
CN-M	14	0.06	2.56	26.8	0.298	5.32	<575°C
CN-U	153	0.40	2.88	31.9	0.384	0.12	<530°C

In order to understand the thermal stability of CN-T, CN-D, CN-M, and CN-U, the thermal analysis was carried out by using TG-DSC and the heating rate of 20°C/min under N<sub>2</sub> gas atmosphere. It can be found that the CN-T (Figure 6(a)), CN-D (Figure 6(b)), and CN-M (Figure 6(c)) became unstable when the heating temperature was above 550, 563, and 575°C, respectively. The exothermic peaks can be seen at 672.4 for CN-T, 683.1 for CN-D, and 649.5°C for CN-U, which should be attributed to the decomposition for the samples. Figure 6(d) shows that no significant weight loss of CN-U is recorded when the temperature is below 530°C, and complete decomposition of CN-U occurred at 750°C. Further observation reveals that there are two strong exothermic peaks at 550.1 and 682.4°C of CN-U, which can be ascribed to the sublimation and thermal decomposition [36], respectively. It should be noted that the thermal stability of the samples is different, due to the different degrees of condensation and the packing between the layers during the polymerization [37, 38].

The photocatalytic performance of the as-prepared samples was further evaluated by removal of NO in gas phase in order to demonstrate their potential ability for indoor air purification under visible light irradiation at room temperature (Figure 7). There are four reactions of the photocatalytic materials, which involved that NO reacted with the

photo-generated reactive radicals and produced HNO<sub>2</sub> and HNO<sub>3</sub> displayed in the following [39]:

$$NO + 2^{\bullet}OH \longrightarrow NO_{2} + H_{2}O$$

$$NO_{2} + {^{\bullet}OH} \longrightarrow NO_{3}^{-} + H^{+}$$

$$NO + NO_{2} + H_{2}O \longrightarrow 2HNO_{2}$$

$$NO + {^{\bullet}O_{2}^{-}} \longrightarrow NO_{3}^{-}$$

$$(1)$$

Figure 7(a) shows the variation of NO concentration  $(C/C_0\%)$  with irradiation time over the samples under visible light irradiation ( $\lambda > 420$  nm). Here,  $C_0$  is the initial concentration of NO, and C is the concentration of NO after photocatalytic reaction for time t.

As shown in Figure 7(a), the concentration of NO for all samples decreased rapidly due to the photocatalytic degradation in 5 min. However, the reaction intermediates, and final products generated during irradiation may occupy the active sites of photocatalyst, which result in the decrease in activity. After 40 min irradiation, the removal rates and apparent rate constants of CN-T (29.2% and 0.310 min<sup>-1</sup>) and CN-U (32.2% and 0.384 min<sup>-1</sup>) are higher than that of CN-D (22.2% and 0.079 min<sup>-1</sup>) and CN-M (26.2% and

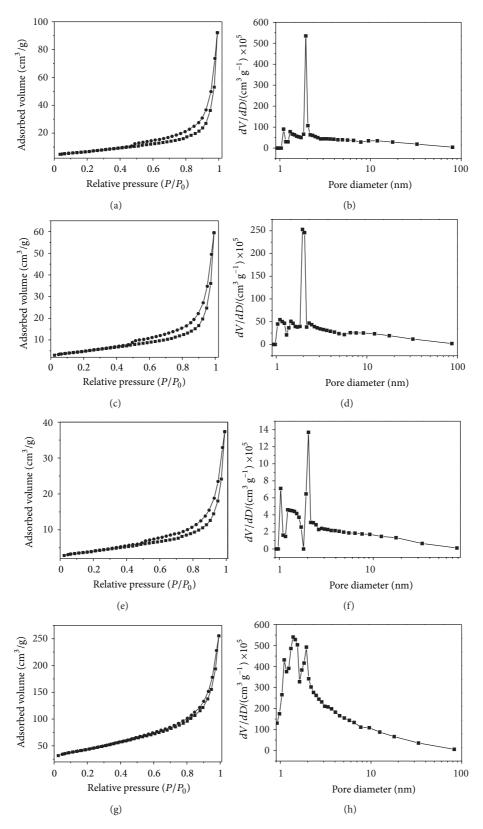


FIGURE 5:  $N_2$  adsorption-desorption isotherms of CN-T (a), CN-D (c), CN-M (e), and CN-U (g) and the corresponding pore size distribution curves of CN-T (b), CN-D (d), CN-M (f), and CN-U (h).

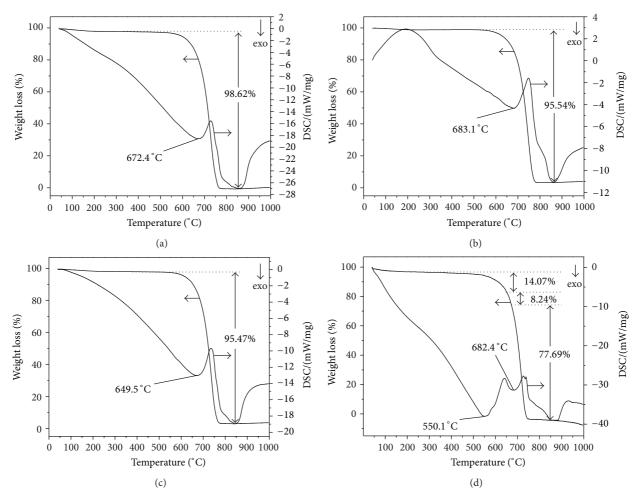


FIGURE 6: TG-DSC thermalgrams for CN-T (a), CN-D (b), CN-M (c), and CN-U (d).

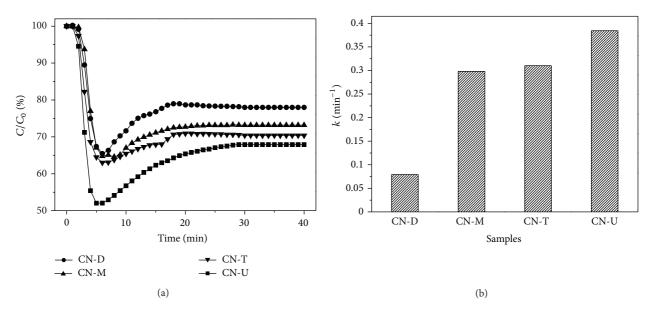


FIGURE 7: Photocatalytic activity (a) and initial rate constants (b) of CN-T, CN-D, CN-M, and CN-U for removal of NO under visible light irradiation ( $\lambda > 420$  nm) at room temperature.

0.298 min<sup>-1</sup>), respectively. Generally, CN-T, CN-D, and CN-M with narrower band gaps than CN-U (see Table 2) are favorable for photocatalytic reaction, due to the enhanced visible light absorption with more available photogenerated electron hole. In fact, the high surface areas and large pore volumes can enhance the adsorption of reactants and diffusion of the reaction products and provide more efficient active sites for photochemical reaction [40, 41]. Thus, the surface area and pore volume of CN-U play a more significant role in NO degradation than the electronic properties. However, it is interesting to find that the CN-M exhibits higher photocatalytic activity than that of CN-D. Figure 4(b) shows that the band energy of CN-M is narrower than that of CN-D, which can enhance visible light absorption in CN-M sample. On the other hand, the enhanced condensation of CN-M can effectively reduce the number of structure defects (e.g., uncondensation groups of -NH<sub>2</sub> and –NH) which always capture the electrons or holes to prevent the following photoredox reaction [8]. The fact indicates that the photocatalytic efficiency strongly depends on the surface area, pore volume, band energy, and the degree of condensation of g-C<sub>3</sub>N<sub>4</sub>.

To ensure the large-scale application, four evaluation indicators were proposed for screening the most suitable precursors, including the cost, toxicity, and yield of the precursors and the removal rate for the contaminant. As shown in Tables 1 and 2, melamine exhibits the middle cost, toxicity, and removal ratio for the degradation of NO. However, it possesses the highest yield among the four precursors. Based on the advantages analysis previously mentioned, the best precursor is melamine.

#### 4. Conclusions

In summary, g- $C_3N_4$  samples were prepared by a simple pyrolysis of thiourea, dicyandiamide, melamine, and urea under the same procedures, respectively. The systematic research results confirmed that the precursors have significant effect on the morphology, band gap, surface area, pore volume, thermal stability, and visible light photocatalytic activity of g- $C_3N_4$ . Considering the cost, toxicity, and yield of the precursors and the properties of g- $C_3N_4$ , the best precursor for preparation of g- $C_3N_4$  is melamine. The present work could provide new insights into appropriate selection of precursors for g- $C_3N_4$  synthesis as visible light photocatalyst in environmental protection.

#### **Conflict of Interests**

The authors declare that they have no conflict of interests.

#### Acknowledgments

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### Research Article

## Enhanced Visible Light Photocatalytic Activity for TiO<sub>2</sub> Nanotube Array Films by Codoping with Tungsten and Nitrogen

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A series of W, N codoped  $TiO_2$  nanotube arrays with different dopant contents were fabricated by anodizing in association with hydrothermal treatment. The samples were characterized by scanning electron microscopy, X-ray diffraction, X-ray photoelectron spectroscopy, and ultraviolet-visible light diffuse reflection spectroscopy. Moreover, the photocatalytic activity of W and N codoped  $TiO_2$  nanotube arrays was evaluated by degradation of methylene blue under visible light irradiation. It was found that N in codoped TNAs exists in the forms of Ti-N-O, while W exists as  $W^{6+}$  by substituting Ti in the lattice of  $TiO_2$ . In the meantime, W and N codoping successfully extends the absorption of TNAs into the whole visible light region and results in remarkably enhanced photocatalytic activity under visible light irradiation. The mechanism of the enhanced photocatalytic activity could be attributed to (i) increasing number of hydroxyl groups on the surface of TNAs after the hydrothermal treatment, (ii) a strong W-N synergistic interaction leads to produce new states, narrow the band gap which decrease the recombination effectively, and then greatly increase the visible light absorption and photocatalytic activity; (iii) W ions with changing valences in all codoped samples which are considered to act as trapping sites, effectively decrease the recombination rate of electrons and holes, and improve the photocatalytic activity.

#### 1. Introduction

Nowadays, photocatalysis has attracted lively interest due to its potential applications in environmental remediation and clean energy production. Among various photocatalysts, TiO<sub>2</sub> is most frequently employed owing to the advantages of earth abundance, low toxicity, and thermal and chemical stability. However, because of the wide band gap of titanium dioxide, only a small UV fraction of solar light (3-5%) can be utilized [1-3]. Many investigations have been conducted to extend optical absorption of TiO<sub>2</sub>-based materials to the visible light region and to improve visible light photocatalytic activity by nonmetal doping using N [4], C [5, 6], S [7] or multielemental-doped materials [8-11]. In particular, TiO<sub>2</sub> photocatalysts codoped with N and another metal had attracted many attentions in recent years [12, 13]. For example, Yang et al. prepared C- and V-doped TiO2 photocatalysts by a sol-gel method with high photocatalytic activity for the degradation of acetaldehyde both under visible light irradiation (>420 nm) and in the dark [14]. Liu et al. prepared a series of  ${\rm Ti}_{1-x}{\rm Mo}_x{\rm O}_{2-y}{\rm N}_y$  samples using sol-gel method and found that Mo + N codoping can increase the up-limit of dopant concentration and create more impurity bands in the band gap of  ${\rm TiO}_2$  by first-principles band structure calculations [15]. It reveals that Mo + N codoped  ${\rm TiO}_2$  material is a promising photocatalyst with high photocatalytic activity under visible light.

Recently, many reports have focused on the W, N codoped TiO<sub>2</sub> nanoparticles to increase photocatalytic activity under visible light irradiation. Shen et al. fabricated the W, N codoped TiO<sub>2</sub> nanopowders using sol-gel and mechanical alloying methods. The samples exhibited strong absorbance in the visible range and enhanced photocatalytic activities under visible light irradiation from the results of photodegradation experiments and chemical oxygen demand analysis [16]. Li et al. prepared W, N codoped TiO<sub>2</sub> nanophotocatalysts with twist-like helix structure by a facile and templatefree one-pot method, which showed higher visible light

response compared with pure  ${\rm TiO_2}$  and P25 [17]. Kubacka et al. synthesized W- and N-doped  ${\rm TiO_2}$  anatase-based materials with both unprecedented high activity and selectivity in the gas-phase partial oxidation of aromatic hydrocarbons using sunlight as excitation energy and molecular oxygen as oxidant [18–20]. The doped tungsten and nitrogen species plays a key role in narrowing the band gap and then in expanding the photoactivity to visible light region and also in decreasing the recombination rate of excited electron and holes. However, most of the reported W- and N-doped  ${\rm TiO_2}$  photocatalysts were typically present in powders which usually display low surface area due to the closed packing and limit their industrial applications as photocatalysts.

Highly ordered TiO<sub>2</sub> nanotube arrays (TNAs) fabricated via electrochemical anodization of high purity Ti foils have attracted extensive interests in recent years. Owing to the presence of unique structural features such as large surface area, high porosity, and ordered pore channels facilitating reactant diffusion and adsorption, TiO<sub>2</sub> nanotube arrays are more attractive for use in the applications of photocatalysis [21], gas sensing [22], solar cells [23], photoelectrochemistry [24], and so on. However, full technological applications of TiO<sub>2</sub> nanotube arrays are hampered by the wide band gap of TiO<sub>2</sub> and the activation only under ultraviolet light irradiation. Although nonmetal doping of TiO2 nanotube arrays has been confirmed as an effective method to enhance the photocatalytic activity under visible light irradiation [22, 23]; to our knowledge, there is little work about the fabrication and visible light photocatalytic activity of the W and N codoped TiO<sub>2</sub> nanotube arrays. In this work, we successfully prepared W, N codoped TiO<sub>2</sub> nanotube arrays by anodization and hydrothermal synthesis. The photocatalytic activity of as-prepared samples was studied based on methylene blue dye degradation under visible light irradiation. The results demonstrated that the W and N codoped TiO<sub>2</sub> nanotube arrays exhibited a higher photocatalytic activity than the single N-doped sample under visible light irradiation. The mechanism of visible light photocatalytic activity enhancement was also discussed.

#### 2. Experimental Sections

2.1. Synthesis of W and N Codoped TiO<sub>2</sub> Nanotube Arrays. Self-organized and well-aligned TNAs were fabricated by two-step electrochemical anodization process [25]. Briefly, commercial titanium sheets (20 mm × 40 mm, purity > 99.6%) with a thickness of 0.25 mm were sequentially sonicated in acetone, isopropanol, and methanol for 10 min, followed by etching in the mixture of HF/HNO<sub>3</sub>/H<sub>2</sub>O for 20 s, rinsing with deionized water, and drying under a  $N_2$ stream. Resultant rectangular Ti sheet was used as an anode to couple with Pt meshwork as a cathode in the anodic oxidation test setup. A direct current power supply and a mixed electrolyte solution of ethylene glycol containing 0.25 wt% NH<sub>4</sub>F and 2 vol% deionized water were used in the electrochemical processes. The first oxidation step was conducted at 60 V for 1h, with which the oxidized surface films were removed by sonication in distilled water before the oxidized samples were dried under high purity N2 stream at

room temperature. As-dried Ti substrates were subsequently oxidized in the original electrolyte at 60 V for 2 h, followed by sonication in ethanol for 7 min to remove the surface cover and drying under high purity  $\rm N_2$  stream to afford as-prepared TNAs. Magnetic stirring was adopted throughout the oxidation processes, while a circulation pump was performed at a low temperature of about 20°C. After electrochemical anodization, as-prepared TNAs were calcinated at 500°C for 3 h in a furnace. Interstitial nitrogen species were formed in the TNAs due to the electrolyte containing NH $_4\rm F$  [26]. We denoted these single N-doped TiO $_2$  nanotube arrays samples fabricated by two-step oxidization as N-TiO $_2$ .

W and N codoped TNAs with different dopant concentration (0.01%, 0.05%, 0.5%, 1.00%, and 3.00%, referring to different concentration of W and N source) were then prepared by hydrothermally treating the anodized N-TiO<sub>2</sub> in a teflon-lined autoclave (120 mL, Parr Instrument) containing approximately 60 mL of ammonium tungstate  $((NH_4)_{10}H_2(W_2O_7)_6)$  as the source of both W and N. The hydrothermal synthesis was conducted at 180°C for 5 h in a box oven, and then the autoclave was naturally cooled down to room temperature affording target products denoted as W-N-TiO<sub>2</sub>-water, W-N-TiO<sub>2</sub>-0.01, W-N-TiO<sub>2</sub>-0.05, W-N-TiO<sub>2</sub>-0.5, W-N-TiO<sub>2</sub>-1, and W-N-TiO<sub>2</sub>-3 (numeral suffixes water, 0.01, 0.05, 0.5, 1 and 3 refer to pure water and ammonium tungstate solution concentration of 0.01%, 0.05%, 0.50%, 1.00%, and 3.00%). All samples were rinsed with distilled water and dried under high purity N<sub>2</sub> stream at room temperature.

- 2.2. Characterization. Surface morphologies of TNAs were observed using a field emission scanning electron microscopy (FESEM, Nova NanoSEM 230). A Philips X'Pert Pro PW3040/ 60 X-ray diffractometer (XRD, Philips Corporation, Holland) was used to determine the crystal structure of as-prepared samples. Chemical state analysis was conducted with an Axis Ultra X-ray photoelectron spectroscopy (XPS, Kratos, UK; a monochromatic Al source operating at 36 W with a pass energy of 40 eV and a step of 0.1 eV was used). All XPS spectra were corrected using the C 1s line at 284.8 eV. A Cary-5000 scanning ultraviolet-visible light diffuse reflection spectrophotometer (denoted as UV-vis DRS; Varian, USA) equipped with a labsphere diffuse reflectance accessory was performed to collect the UV-vis diffuse reflectance spectra. The adsorption spectra of N-TiO<sub>2</sub> and W + N codoped TNAs in the range of 300~800 nm were recorded with the UV-vis DRS facility at a scan rate of 600 nm min<sup>-1</sup>.
- 2.3. Photocatalytic Activity Measurements. Photocatalytic activity of all samples was evaluated by monitoring the photocatalytic degradation of methylene blue (denoted as MB) in aqueous solution under visible light with vertical irradiation as light source. Briefly, to-be-tested N-TiO $_2$  and W-N-TiO $_2$ -X (X = water, 0.01, 0.05, 0.5, 1, and 3) samples were dipped into 25 mL of MB solution with an initial concentration of 10 mg L $^{-1}$ . The effective photocatalytic reaction area of all samples was 4 cm $^2$ . A 300 W Xenon lamp (PLS-SEX300, Beijing Changtuo) was used as the light source. A cut-off filter was used to remove any radiation below 420 nm to ensure

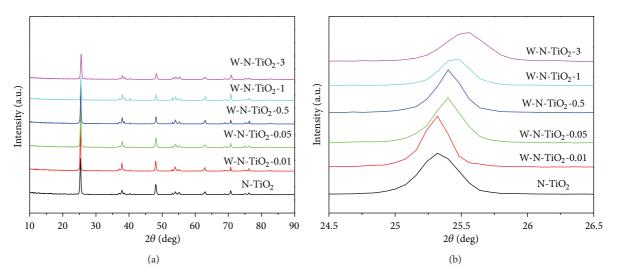


FIGURE 1: XRD patterns of N-TiO<sub>2</sub> and W-N-TiO<sub>2</sub>-X (a), the enlarged XRD peaks of crystal plane (101) (b).

visible light irradiation only. The light intensity was measured by a photodetector, and the value is about  $30\,\mathrm{mW/cm^2}$  at 420 nm. Prior to irradiation, the MB solution containing to-be-tested sample was magnetically stirred in the dark for 30 min to establish adsorption-desorption equilibrium. During the photocatalytic reaction, the absorbance of MB solution at 664 nm was measured using an SP-2000 spectrophotometer at a time interval of 30 min. The decoloration rate of MB solution is calculated as  $(C_0-C)/C_0\times 100\%$ , where  $C_0$  is the concentration of MB at adsorption–desorption equilibrium in the dark and C is the concentration of MB upon completion of the photocatalytic reaction under visible light irradiation. In this way, the influence of adsorption amount of MB on its solution decoloration rate is excluded (different photocatalyst samples adsorb different amount of MB).

#### 3. Results and Discussion

The phase structure, crystallite size, and crystallinity of TiO<sub>2</sub> play important roles in photocatalytic activity and photochemical properties. Many studies have confirmed that the anatase phase of TiO2 exhibits higher photocatalytic activity than brookite or rutile phases [27]. Herein, XRD measurements were performed to investigate the changes of phase structure of TiO2 nanotube arrays codoped with different ammonium tungstate addition. XRD patterns of various samples are shown in Figure 1. It can be seen that all the diffraction peaks of N-TiO2 and W-N-TiO2-X can be ascribed to anatase TiO<sub>2</sub>, which indicates that W and N codoping has no effect on the crystal structure and phase composition of TNAs. It is worth noting that no WO<sub>3</sub> phase could be observed in all the XRD patterns, even in that of the sample with the W doping amount reaching 3%. Accordingly, we propose that tungsten ions may be incorporated into the titania lattice and replaced titanium ions to form W-O-Ti bonds.

From the enlarged image in Figure 1(b), it is interesting to note that W and N codoping causes the diffraction peak of anatase TiO<sub>2</sub> along (101) plane to shift towards higher

values of  $2\theta$ . Moreover, slight enhancement of crystallinity properties can be observed when comparing the (101) peak intensities of the TNAs samples before and after the hydrothermal treatments. The XRD results imply that the Ti atoms in the anatase lattice of codoped TNAs samples may be substituted by W atoms, since W<sup>6+</sup> ions with a radius close to that of Ti<sup>4+</sup> are easy to enter into the lattices of TiO<sub>2</sub> and displace Ti<sup>4+</sup> ions, while nitrogen and tungsten have a synergistic doping effect [17, 21].

Figure 2 presents typical FESEM top view images of the N-TiO<sub>2</sub> and W-N-TiO<sub>2</sub>-1 photocatalysts. Both images show the similar morphology of highly ordered nanotube arrays grown on the Ti substrate. SEM observation indicates that there is no apparent structural transformation of the TNAs samples after hydrothermal codoping process. The nanotubes of N-TiO<sub>2</sub> samples are open at the top end with an average diameter of 70 nm (Figure 2(a)). However, the diameter of nanotube in W-N-TiO2-1 sample is found to be slightly increased to 80 nm. This difference of pore size is due to the enhanced crystallinity of the anatase nanotube walls after hydrothermal treatments in agreement with the XRD results. Yu et al. had reported that the nanotube array structures were completely destroyed after 180°C hydrothermal treatments with as-prepared TNAs samples due to the strongly enhanced anatase crystallinity and phase transformation from amorphous to anatase [28]. In our work, the as-prepared TNAs samples were calcinated at 500°C to realize the phase transformation from amorphous to anatase before subsequently hydrothermal process. The reported hydrothermally induced collapse was prevented with the simple calcination method. The calcined TNAs samples show better crystallinity with no apparent morphology change after hydrothermal codoping process.

XPS measurements are used to investigate the chemical states of W, N, Ti, and O in N-TiO $_2$  and W-N-TiO $_2$ -1 samples. Figure 3(a) shows the high resolution XPS spectra for the N 1s region of N-TiO $_2$  and W-N-TiO $_2$ -1. The N 1s binding energy peaks are broad, extending from 396 to 403 eV. The centre

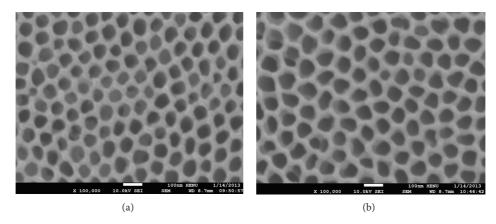


FIGURE 2: FESEM cross-sectional views of W and N codoped TiO<sub>2</sub> nanotube arrays: (a) N-TiO<sub>2</sub>, (b) W-N-TiO<sub>2</sub>-1.

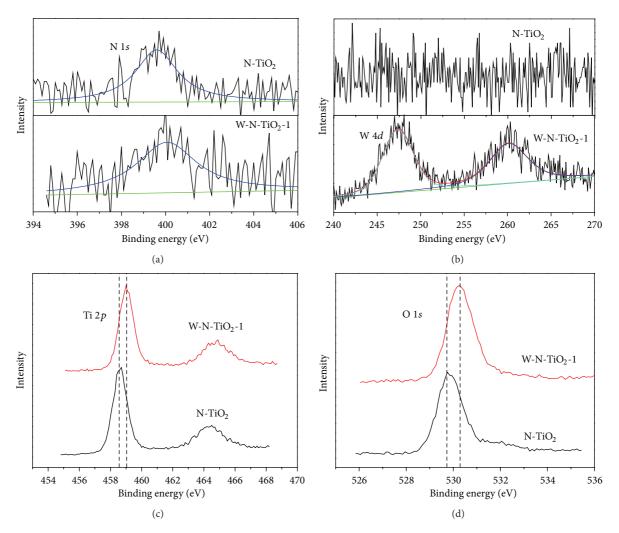


FIGURE 3: High resolution XPS spectra of (a) N 1s, (b) W 4d, (c) Ti 2p, and (d) O 1s for N-TiO<sub>2</sub> and W-N-TiO<sub>2</sub>-1 samples.

of the N 1s peak locates at ca. 399.8 eV and  $400.1 \, \text{eV}$  for N-TiO<sub>2</sub> and W-N-TiO<sub>2</sub>-1 sample, respectively. These two peaks are much higher than that of typical binding energy of N 1s (396.9 eV) in TiN [29], indicating that the N atoms in N-TiO<sub>2</sub> and W-N-TiO<sub>2</sub>-1 interact strongly with O atoms

[30]. The binding energy of 399.8 eV and 400.1 eV here is attributed to the oxidized nitrogen similar to  $NO_x$  species, meaning Ti-N-O linkage possibly formed on the surface of N-TiO<sub>2</sub> and W-N-TiO<sub>2</sub>-1 [13, 31, 32]. The N 1s peak of N-TiO<sub>2</sub> at 399.8 eV is assigned to interstitial nitrogen species

according to the previous report of Varghese et al. [26]. They suggested that the nitrogen incorporated within  ${\rm TiO_2}$  nanotubes during anodization is primarily supplied by  ${\rm NH_4F}$  or low extent of atmospheric nitrogen dissolved into the electrolyte. Furthermore, it is highly possible that some N-O species coordinate with W to form the W-N-O linkage on the surface of W-N- ${\rm TiO_2}$ -1. For the latter case, the electron density of N atoms in W-N-O is lower than that in  ${\rm Ti-N-O}$  since the electronegativity of W is larger than that of  ${\rm Ti}$  [13, 33]. It may explain why the binding energy of nitrogen surface species for W-N- ${\rm TiO_2}$ -1 (400.1 eV) is higher than that for N- ${\rm TiO_2}$  (399.8 eV). High resolution W 4*d* spectra of N- ${\rm TiO_2}$  and W-N- ${\rm TiO_2}$ -1 are presented in Figure 3(b). The W 4*d* peaks of W-N- ${\rm TiO_2}$ -1 at about 247.5 eV and 260.2 eV are assigned to  ${\rm 4d_{5/2}}$  and  ${\rm 4d_{3/2}}$  electronic states of W<sup>6+</sup>, respectively [19, 20].

Figures 3(c) and 3(d) show high-resolution spectra of Ti 2p, O 1s of N-TiO<sub>2</sub>, and W-N-TiO<sub>2</sub>-1. For N-TiO<sub>2</sub> sample, two peaks at 458.6 and 464.3 eV correspond to the Ti  $2p_{3/2}$ and Ti2  $p_{1/2}$  states, indicating that Ti is 4+ valence. A strong peak centered at 529.8 eV is observed in the O 1s XPS spectra of N-TiO<sub>2</sub>, attributing to bulk oxygen bonded to titanium. For the W and N codoped TiO<sub>2</sub> sample, both the Ti 2p and O 1s peaks are slightly shifted toward higher binding energy due to the doping of W in the TiO<sub>2</sub> lattice, which is in agreement with the result reported by Gong et al. [34]. All XPS results indicate that the W<sup>6+</sup> ions were doped into the bulk TiO<sub>2</sub> lattice by displacing Ti<sup>4+</sup> ions and forming the W-O-Ti bonding, which is in accordance with relevant XRD analytical results. According to the previous XPS and XRD results, it indicates that nitrogen is present as interstitial nitrogen in codoped TNAs samples, and W incorporates into TiO<sub>2</sub> lattice in substitutional mode.

The exact amounts of surface elements in all doped samples were studied by XPS analysis. The surface N/Ti and W/Ti ratio of all samples are calculated and listed in Table 1. It is found that the surfaces N/Ti and W/Ti ratio increased with the concentration of ammonium tungsten solution. Then, both the surfaces N/Ti and W/Ti ratio reaches their maximum value with the concentration of ammonium tungsten solution to 1% (theoretical doping concentration). However, the N/Ti and W/Ti ratio decreased clearly with further increasing the ammonium tungsten concentration to 3%. It indicates that the dopant concentration has an optimal value of about 1%. Above this optimal concentration, excess W and N ions cannot be doped in TiO<sub>2</sub> and show no contribution to the visible light absorption and subsequent photocatalytic activity. Moreover, the concentration of doped N increases with the codoping of W, which demonstrates that W and N codoping is in favor of enhancing the dopant solubility.

Figure 4 presents the UV-vis diffuse reflectance spectra of all samples. A relatively weak visible light absorption can be observed for the oxidized N-TiO $_2$  sample, which corresponds to a typical reported absorption feature of nitrogen-doped TiO $_2$  arising from the electron transition from surface state of NO $_x$  species to the conduction band of TiO $_2$  [13, 35]. Compared with that of N-TiO $_2$  sample, UV-vis spectra of all W and N codoped TNAs samples present red-shifted absorption edge and a strong absorption in the visible light

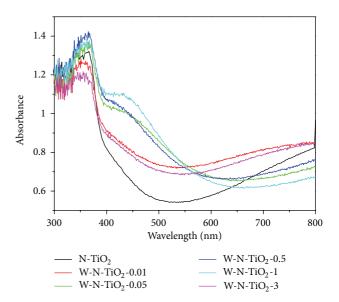


FIGURE 4: UV-vis diffuse reflectance spectra of N-TiO $_2$  and W-N-TiO $_2$ -X samples.

region with typical extended absorption tail of about 600 nm. Moreover, for W and N codoped TNAs samples, the intensity of visible light absorption is enhanced with the increase of W and N concentration (the ammonium tungsten solution concentration from 0.01% to 1%). We consider that this absorption enhancement is due to the contribution of both interstitially doped N and substitutionally doped W. W and N incorporated in the lattice of TNAs show synergistic doping effect which favors to increase the solubility limits of W and N thereby greatly enhancing the visible light absorption along with the increase of the up-limits of W and N concentration [15, 36]. For the W-N-TiO<sub>2</sub>-3 sample, the absorption edge is decreased because the superfluous W and N atoms cannot be doped into the lattice of TiO<sub>2</sub>. Overall, the UV-vis DRS results indicate that nitrogen and tungsten codoped TiO<sub>2</sub> nanotube arrays are more sensitive to the visible light than N-TiO2 samples.

The photocatalytic activities of N-TiO<sub>2</sub> and hydrothermal treated W-N-TiO2-X samples were evaluated by monitoring the degradation of MB under visible light irradiation. To investigate the effect of hydrothermal treatment on the photocatalytic activity, the oxidized N-TiO<sub>2</sub> was firstly hydrothermally treated in pure water, and the obtained sample was denoted as W-N-TiO<sub>2</sub> water. An obviously enhanced photocatalytic activity was found for the W-N-TiO2 water sample after hydrothermal treatment as shown in Figure 5. Many reports have shown that the photocatalytic activity of TiO<sub>2</sub> samples strongly depends on the preparing methods and posttreatments [36, 37]. Yu et al. had demonstrated an obvious increase of photocatalytic activity after thermal treatment of TiO<sub>2</sub> (P25) in pure water [36]. Recently, Dai et al. reported the enhanced photoelectrocatalytic activity of the TiO<sub>2</sub> nanotube arrays by hydrothermal modification [37]. They suggested that the enhanced photocatalytic activity was attributed to the formation of increasing number of hydroxyl groups on the surface of TiO<sub>2</sub> nanotube arrays

Sample	$N-TiO_2$	$W-N-TiO_2-0.01$	$W-N-TiO_2-0.05$	$W-N-TiO_2-0.5$	W-N-TiO <sub>2</sub> -1	W-N-TiO <sub>2</sub> -3
W/Ti	0	0.11	0.11	0.12	0.16	0.12
N/Ti	0.02	0.13	0.16	0.19	0.22	0.14

TABLE 1: W/Ti and N/Ti ratio of W-N-TiO<sub>2</sub>-X samples determined by XPS analysis.

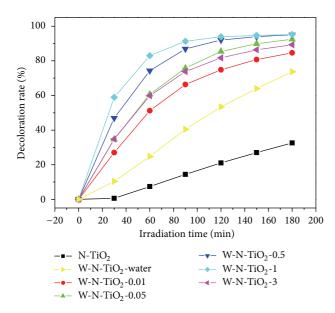


FIGURE 5: Photocatalytic degradation rate of MB in the presence of N-TiO $_2$  and W-N-TiO $_2$ -X photocatalysts under visible light irradiation.

after hydrothermal treatment. The increased hydroxyl groups would react with photoexcited holes on the surface of TiO<sub>2</sub> and produce hydroxyl radicals, which in turn are powerful oxidants in the photocatalytic reaction. In our work, before codoping, the number of hydroxyl groups on the surface of N-TiO<sub>2</sub> decreases due to the dehydration reaction during the higher temperature calcination process of oxidized TiO<sub>2</sub> nanotube arrays. When N-TiO<sub>2</sub> was codoped with W and N by hydrothermal treatment, Ti-OH leading to an enhanced photocatalytic activity can be regenerated on the surface of W-N-TiO<sub>2</sub>-X samples due to the rupture of Ti-O-Ti bond.

W and N codoping of N-TiO<sub>2</sub> samples was performed by the hydrothermal treatment in a series of concentrations of ammonium tungstate solution (concentration from 0.01% to 3%). As shown in Figure 5, W and N codoped TNAs possess much higher photocatalytic activity under visible light irradiation than N-TiO<sub>2</sub> sample and the W-N-TiO<sub>2</sub>-water sample hydrothermal treated in pure water. Besides, the decoloration rate of MB for W and N codoped TNAs increases under visible light irradiation with the increase of dopant concentration. The decoloration rate reaches a maximum value for W-N-TiO<sub>2</sub>-1, and it allows nearly complete elimination of MB within 3 h. Then, the photocatalytic activity for W-N-TiO<sub>2</sub>-3 shows clear decrease due to its visible light absorption as discussed before.

The origin of the visible light photocatalytic activity of W and N codoped TNAs can be attributed to the interactions

between N doping and W doping in the preparation processes. For the single N-doped sample (N-TiO<sub>2</sub>) prepared by electrochemical anodization, isolated N 2p states above the top of valence band are responsible for the red shifts in the optical absorption edge. After hydrothermal codoping with W and N, a hybridized state (composed of N 2p orbitals and W 5d states) is formed; in particular, the hybridized states are located mainly at the edge of the valence band, whereas other W 5d states are at the edge of the conduction band. W 5d states may contribute to the lowering of the energy levels of the N 2p states, bringing the N states closer to the valence band and therefore enhancing mixing of N 2p and O 2p states in the valence band. Therefore, the addition of W to N-TiO<sub>2</sub> changes the character of N 2p orbitals from isolated midgap states to N 2p states mixed with O 2p states [38]. At the same time, W 5d states were located at the conduction band edge. Moreover, as electrons move from occupied W 5d states to empty lower energy N 2p states, a strong N-W bond forms in N and W codoped TNAs. This synergistic effect is beneficial for the increased doping amount of W and N in TiO<sub>2</sub> nanotube arrays. Consequently, the band gap energy of TiO2 is significantly reduced, and its absorption in the visible light region is considerably increased due to modified conduction and valence band edges simultaneously. The band gap narrowing effect makes it feasible for W and N codoped TNAs to be activated by visible light with more electrons and holes being generated to participate in the photocatalytic reactions.

Moreover, W ions with changing valences in all codoped samples are considered to act as a temporary photogenerated electron or hole-trapping site thereby inhibiting the recombination of photogenerated charge carriers, prolonging their lifetime and improving the photocatalytic activity [17]. The detailed reaction steps are as follows:

$$TiO_{2} + hv \longrightarrow e^{-} + h^{+},$$

$$W^{6+} + e^{-} \longrightarrow W^{5+},$$

$$W^{5+} + O_{2} \longrightarrow W^{6+} + O_{2}^{-\bullet},$$

$$W^{6+} + h^{+} \longrightarrow W^{7+},$$

$$W^{7+} + OH^{-} \longrightarrow W^{6+} + OH^{\bullet}.$$

$$(1)$$

When  $W^{6+}$  ( $d^5$ ) trap an electron, its electronic configuration is transferred to  $d^6$ , and if it traps a hole, its electronic configuration will be transferred to  $d^4$  which is highly unstable. Therefore, to restore the stable electronic configuration, the trapped charge carrier tends to be transferred from  $W^{5+}$  or  $W^{7+}$  to the adsorbed  $O_2$  or surface hydroxyl (OH $^-$ ) thereby regenerating  $W^{6+}$ . These newly produced active species (such

as  $OH^{\bullet}$  and  $O_2^{-\bullet}$ ) are able to initiate the photocatalytic reactions.

#### 4. Conclusions

W and N codoped TiO<sub>2</sub> nanotube arrays have been successfully synthesized by combining anodizing technique with hydrothermal method. W and N codoped TNAs samples show better crystallinity with no apparent morphology change after hydrothermal codoping process. XPS data reveal that, in as-prepared W and N codoped TNAs, nitrogen is present in the forms of Ti-N-O and W incorporates into TiO<sub>2</sub> lattice in substitutional mode. UV-vis DRS data show that W and N codoping was found to successfully extend the absorption of TiO2 nanotube arrays into the whole visible light region. Increased number of hydroxyl groups produced by hydrothermal treatment shows an important role for the enhancement of photocatalytic activity. The synergetic doping effect between W and N plays a key role in producing new states, narrowing the band gap, and reducing the recombination effectively thereby greatly improving the visible light absorption and photocatalytic activity of TNAs. Besides, W ions with multiple valences in W-N-TiO<sub>2</sub>-X samples can act as trapping sites to effectively decrease the recombination rate of electrons and holes, also resulting in improved photocatalytic activity of TNAs. Therefore, W and N codoped TiO2 nanotube arrays with higher visible light absorption and photocatalytic activity are promising materials for visible light photocatalysts.

#### **Conflict of Interests**

The authors declare that they do not have any commercial or associative interests that represents a conflict of interest in connection with the work submitted.

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## Research Article

## Synthesis and Characterization of Pyrochlore Bi<sub>2</sub>Sn<sub>2</sub>O<sub>7</sub> Doping with Praseodymium by Hydrothermal Method and Its Photocatalytic Activity Study

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Praseodymium doped  $\mathrm{Bi_2Sn_2O_7}$  (BSO), as a visible-light responsive photocatalyst, was prepared by a hydrothermal method with different dopant contents. The as-prepared photocatalysts were investigated by X-ray diffraction (XRD), scanning electron microscope (SEM), transmission electron microscope (TEM),  $\mathrm{N_2}$  adsorption-desorption isotherm, X-ray photoelectron spectroscopy analysis (XPS), and UV-Vis diffuse reflectance spectroscopy (DRS). The photocatalytic activity of prepared catalysts was evaluated by the degradation of Rhodamine Bextra (RhB) and 2,4-dichlorophenol (2,4-DCP) in aqueous solution under visible light irradiation. It was found that Pr doping inhibited the growth of crystalline size and the as-prepared materials were small in size (10–20 nm). In our experiments, Pr-doped BSO samples exhibited enhanced visible-light photocatalytic activity compared to the undoped BSO, and the optimal dopant amount of Pr was 1.0 mol% for the best photocatalytic activity. On the basis of the calculated PL spectra, the mechanism of enhanced photocatalytic activity has been discussed.

#### 1. Introduction

Semiconductor photocatalysis has been a very attractive research topic since its potential in the treatment of biorecalcitrant components in wastewaters [1, 2]. Among the semiconductors, TiO2 has been widely discussed as a photocatalyst to purify air and water polluted with various hazardous chemicals due to its high photocatalytic activity, low cost, nontoxicity, and good stability [3, 4]. However, low quantum yields and the lack of visible-light utilization blocked its practical application. Therefore, much effort has been done in order to enhance the photocatalytic efficiency and visible-light utilization of TiO<sub>2</sub>, such as metal ion doping [5-7], nonmetal doping [8, 9], and coupling with other semiconductors [10]. In addition, the development of novel visible-light respond photocatalysts has been put forward and drawn great attention, such as Bi<sub>2</sub>Ti<sub>2</sub>O<sub>7</sub> [11, 12], La<sub>2</sub>Zr<sub>2</sub>O<sub>7</sub> [13], and Bi<sub>1.5</sub>MgNb<sub>1.5</sub>O<sub>7</sub> [14].

As a kind of pyrochlore-type composite oxides, bismuth pyrostannate (Bi<sub>2</sub>Sn<sub>2</sub>O<sub>7</sub>) has received considerable attention by a number of groups due mainly to its demonstrated applications in catalysis and gas sensing [15-18]. Moens et al. [19] used Bi<sub>2</sub>Sn<sub>2</sub>O<sub>7</sub> (BSO) mechanically mixed with MoO<sub>3</sub> to evidence a cooperation catalytic effect between BSO and Bi<sub>2</sub>Mo<sub>3</sub>O<sub>12</sub>. Kim et al. [20] utilized a novel method to prepare SnO<sub>2</sub> nanowires with BSO nanoparticles and investigated its oxygen sensing properties. Wu et al. [21] explored band engineering to improve visible light photocatalysis of nano-BSO. All previous research studies showed that it was necessary to take steps to promote the photocatalytic efficiency of pure BSO. Doping with rare earth ions also could reduce the recombination rate of electron-hole pairs and enhance the interfacial charge transfer efficiency [22], such as La-TiO<sub>2</sub> [23], Nd-TiO<sub>2</sub> [24], and Ce-Bi<sub>2</sub>O<sub>3</sub> [25]. However, rare-earth doped BSO and its corresponding photocatalytic activity have been rarely investigated.

In the present work, in order to expand its absorption in visible light, the Pr-doping within the BSO photocatalyst was carried out by hydrothermal method. Furthermore, the effects of different Pr-doping amounts and the reasons accounting for the photocatalytic results were discussed. Meanwhile, the model pollutants of RhB and 2,4-CP were chosen to evaluate the photocatalytic activity of as-prepared photocatalysts under visible light irradiation.

#### 2. Experimental

2.1. Synthesis. All chemicals were obtained commercially and used without further purification. Bi(NO<sub>3</sub>)<sub>3</sub>·5H<sub>2</sub>O and K<sub>2</sub>SnO<sub>3</sub>·3H<sub>2</sub>O were used as the starting materials for the syntheses. Pr-doped BSO was synthesized by hydrothermal method, and in every aqueous phase, dosage of 1.46 g of Bi(NO<sub>3</sub>)<sub>3</sub>·5H<sub>2</sub>O (3 mmol) and 0.9 g of K<sub>2</sub>SnO<sub>3</sub>·3H<sub>2</sub>O (3 mmol) was added to 80.0 mL of deionized water and then mixed with Pr(NO<sub>3</sub>)<sub>3</sub>·6H<sub>2</sub>O according to the doping ratio of Pr/BSO of 0, 0.5, 1.0, 2.0, and 3.0 mol%, respectively. Under vigorous stirring, the pH value of the mixture was adjusted to 12 by using 2 mol/L KOH. After the solids were completely dissolved in the solution at room temperature, the autoclave was sealed, heated under autogenerous pressure at 180°C for 24 h, and then cooled down to room temperature naturally. The resultant precipitates were filtered, washed with deionized water and anhydrous ethanol, and then dried in a vacuum oven at 60°C for 12 h. The final products were milled using an agate mortar before characterization. The samples were labeled as x%-Pr-BSO, where x% was the molar ratio of Pr to BSO.

2.2. Characterization. The as-prepared samples were characterized by powder X-ray diffraction (XRD) instrument (Bruker D8 ADVANCE). The scanning electron microscopy (SEM) images were obtained on a JEOL JSM 6700F instrument with an accelerating voltage of 20 kV. Transmission electron micrographs (TEM) images were recorded using a JEM-2100HR (JEOL, Japan) microscope at an accelerating voltage of 200 kV. X-ray photoelectron spectroscopy (XPS) analysis was performed on an ESCALAB 250 photoelectron spectroscopy (Thermo-VG Scientific) at  $2.0 \times 10^{-10}$  mbar using Al Kα X-ray beam (1486.6 eV). UV-Vis diffuse reflectance spectrum (DRS) was determined on a Hitachi U-3010 UV-Vis spectrophotometer with BaSO<sub>4</sub> as the background between 250 and 800 nm. The BET surface area and pore volume of samples were measured by a Micromeritics ASAP 2010 nitrogen adsorption apparatus. The photoluminescence (PL) spectra of photocatalysts were recorded by a fluorescence spectrophotometer (Shimadzu Rf-540, Japan) using a 150 W xenon lamp as light source.

2.3. Photocatalytic Activity Measurement. RhB and 2,4-DCP were adopted as a representative organic pollutant to evaluate the photocatalytic activity of as-prepared samples under visible light irradiation. All photocatalytic experiments were conducted at room temperature. The catalyst (0.1g) was immersed in a 250 mL Pyrex beaker with 100 mL of RhB

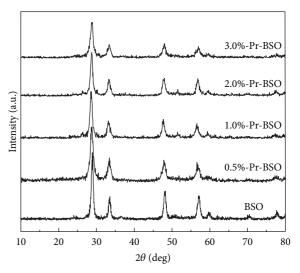


FIGURE 1: XRD analysis of different Pr-doped photocatalysts.

solution (5 mg/L) or 2,4-DCP solution (20 mg/L). The suspensions were magnetically stirred in the dark for 40 min prior to irradiation to achieve adsorption-desorption equilibrium on the catalysts surface at room temperature. As for the photocatalytic reactions, a 300 W Xe arc lamp (LTIC 300BF, BoYi Ltd., China), with a 420 nm cut-off filter, was provided about 10 cm from the top surface of the suspensions, and the concentration of pollutants during photocatalysis was monitored by pulling out about 5.0 mL suspension periodically from the reactor and centrifuging for analysis. A UV-vis 8500 spectrophotometer (Shanghai Tianmei Science Apparatus Ltd., Co., China) was used to analyse the RhB and the high performance liquid chromatography (HPLC, Shimadzu) was assisted to determine the degradation of 2,4-DCP.

#### 3. Results and Discussion

3.1. Phase Structure and Morphology of the As-Prepared Samples. BSO has three polymorphs (monoclinic  $\alpha$ , facecentered cubic  $\beta$ , and cubic pyrochlore  $\gamma$ ) [17], and the thermodynamically stable phase is  $\alpha$ -BSO. In this paper,  $\gamma$ -BSO is obtained by a hydrothermal method. The powder XRD patterns of different Pr-doped BSO photocatalysts are presented in Figure 1. The XRD of samples shows several strong peaks at  $2\theta = 28.8^{\circ}$ ,  $33.4^{\circ}$ ,  $47.9^{\circ}$ , and  $56.9^{\circ}$ , which represent the formation of pyrochlore structure. The diffraction peaks of pure BSO and the doped samples are similar and are found to be in a good agreement with the standard XRD patterns of cubic pyrochlore (JCPDS no. 87-0284). In terms of Pr-doped BSO, the peak at 28.8° corresponding to characteristic peak of the crystal plane (222) becomes broader and the relative intensity decreases with increasing Pr ion dosage. On the basis of the Scherrer equation, the average size of crystallite is calculated from the (222) peak of pyrochlore BSO. The results are summarized in Table 1, and the crystallite size decreased with increasing the amount of praseodymium. It can be attributed to the segregation of the praseodymium cations at the grain boundary, which inhibited the grain growth by restricting direct contact of grains [26].

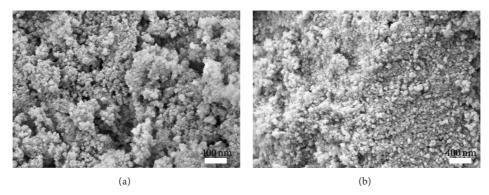


FIGURE 2: SEM images of as-prepared samples: (a) BSO sample and (b) 1%-Pr-BSO sample.

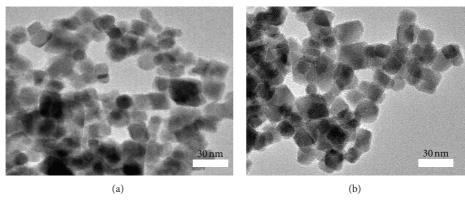


FIGURE 3: TEM images of (a) BSO sample and (b) 1%-Pr-BSO sample.

Table 1: Crystallite size, BET surface areas, and pore size of different photocatalysts.

Sample	Crystallite size <i>D</i> (222)/(nm)	$S_{\rm BET}~({\rm m}^2/{\rm g})$	Pore size (nm)
Pure BSO	13.5	45.3	9.4
0.5%-Pr-BSO	12.5	52.4	9.1
1.0%-Pr-BSO	11.3	61.6	8.1
2.0%-Pr-BSO	10.6	59.3	8.5
3.0%-Pr-BSO	9.8	54.7	8.8

Figure 2 shows the typical SEM images of pure BSO and 1.0%-Pr-BSO. As seen from the SEM micrograph, a large number of small particles are presented in Figure 2(a) (BSO) and Figure 2(b) (1.0%-Pr-BSO), demonstrating that high yield of products can be readily achieved through this approach. The diameters of particles that consisted of spherical clusters are around 8–20 nm.

Figures 3(a) and 3(b) show the TEM photograph of BSO and 1.0%-Pr-BSO, respectively. From Figure 3(a), it can be seen that BSO nanoparticles have irregular lump-like and spherical-like morphology, and the diameter is about 8–20 nm. However, 1.0%-Pr-BSO with a thin layer of about 2 nm in thickness has smaller grain size than BSO, which is consistent well with that calculated from the XRD data (Table 1).

3.2.  $N_2$  Adsorption/Desorption Isotherm Analysis. The specific surface areas and pore size distributions of the BSO

and 1.0%-Pr-BSO are measured using nitrogen gas sorption. The nitrogen adsorption-desorption isotherms of BSO (Figure 4(a)) and 1.0%-Pr-BSO (Figure 4(b)) exhibit stepwise adsorption and desorption (type-IV isotherm), indicating that the samples have mesoporous structure [26]. The specific surface area of BSO is 45.3 m<sup>2</sup>/g, but after Pr coating, the BET surface area of 1.0%-Pr-BSO is increased to 61.6 m<sup>2</sup>/g. High specific surface area of 1.0%-Pr-BSO will provide more active site for the photocatalytic reaction and enhance the interfacial reaction process. The pore size distribution plots of as-prepared samples calculated using the BJH equation from the absorption branch of the isotherm are shown in the inset of Figure 4. The result suggests that the spherical BSO sample has pronounced mesoporosity of narrow pore size distribution with average pore diameter around 12 nm. The specific surface area and pore diameter are calculated and also listed in Table 1.

3.3. X-Ray Photoelectron Spectroscopy Analysis. 1.0%-Pr-BSO is analyzed by XPS to discuss the elemental composition and chemical state on the BSO surface. The XPS survey spectrum is shown in Figure 5(a). It can be seen that 1.0%-Pr-BSO contains only five elements, namely, Bi, Sn, O, Pr, and C. Carbon probably originates from the calcinations residue of the precursor and adventitious hydrocarbon from the XPS instrument itself. In Bi 4f XPS spectrum (Figure 5(b)), two symmetric peaks at 164.3 eV and 159.1 eV, assigned to Bi4  $\rm f_{5/2}$  and Bi4  $\rm f_{7/2}$ , correspond to Bi<sup>4+</sup> and Bi<sup>3+</sup>, respectively [27].

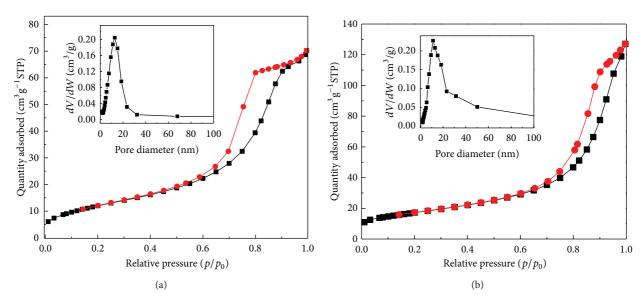


FIGURE 4: The  $N_2$  sorption isotherms and pore size distribution of (a) BSO and (b) 1%-Pr-BSO.

TABLE 2: Maximum absorption and band gap of as-prepared samples.

Sample	Maximum absorption (nm)	Band gap (eV)
BSO	450	2.76
0.5%-Pr-BSO	436	2.84
1.0%-Pr-BSO	460	2.70
2.0%-Pr-BSO	422	2.94
3.0%-Pr-BSO	436	2.84

From the high resolution XPS spectra, it can be observed that the binding energies of Sn  $3d_{5/2}$  and O 1s are 486.8 eV and 530.4 eV, respectively. Moreover, the binding energies of Sn  $3d_{5/2}$  and O 1s are consistent with the literature values for Sn<sup>4+</sup> and O<sup>-</sup> in BSO [28, 29]. Figure 5(e) shows that the peaks of Pr  $3d_{5/2}$  and Pr  $3d_{3/2}$  are located at 933.7 eV and 953.5 eV. The results mean that the Pr oxidation state shows the presence of Pr<sup>3+</sup> [21].

3.4. UV-Vis Diffuse Reflectance Spectra. Figure 6 displays UV-Vis diffuse reflection spectrum (DRS) of BSO precursors and Pr-BSO samples with different Pr contents. Figure 6(a) shows a phenomenon that the maximum absorptions of Pr-BSO photocatalysts, except the 1.0%-Pr-BSO sample, are slightly shifted to a shorter wavelength compared to those of pure BSO. The red shift of the absorption edge in 1.0%-Pr-BSO has been attributed to the charge-transfer transition between Pr ion f electrons and the BSO conduction or valence band [24]. As it is shown in Figure 6(b), the band gap achieved by extrapolation in 1.0%-Pr-BSO (460 nm) at the meeting point of the two tangents is about 2.70 eV. The maximum absorption wavelength and band gap of other photocatalysts are displayed in Table 2.

3.5. Photocatalytic Activity. To evaluate the photocatalytic activity of BSO and Pr-BSO with different molar ratios,

the photodegradation of RhB and 2,4-DCP is carried out in aqueous dispersions under visible light illumination (Figure 7). In order to ensure adsorption/desorption equilibrium, adsorption experiments are carried out on all samples in the dark for 40 min. From Figure 7, it can be observed that the doped samples have a higher absorbtion rate compared with that of the undoped BSO. So it is obvious that Pr ions benefit the adsorption processes. When the BSO nanoparticles are modified by Pr ions, the Pr-BSO photocatalysts show an obvious enhanced photocatalytic activity and model pollutants (RhB and 2,4-DCP) are quickly decomposed with increasing irradiation time. After visible-light irradiation for 4h, the degradation of RhB and 2,4-DCP over pure BSO reaches 52.0% and 50.2%, respectively. However, 90.8% of RhB and 87.6% of 2,4-DCP are degraded in 4 h irradiation over 1.0%-Pr-BSO. In this experiment, 1.0 mol% praseodymium is the optimal dopant content. It is found that the photocatalytic activity increased with increasing Pr loading to the optimum value and then decreased with further increase of Pr content. This result can be attributed to the influence of the space charge layer thickness [30]. As the doped contents are low, the surface barrier becomes higher and the space charge region becomes narrower, and at last the electron-hole pairs are efficiently separated before recombination. However, when the doped content is above its optimum, the space charge region becomes very narrow and the penetration depth of light into photocatalysts greatly exceeds the space charge layer, so that the electron and hole pairs recombine easily. Consequently, there is an optimum concentration of Pr ions.

3.6. Visible Light Photodegradation Mechanism. According to many previous investigations on the mechanism of photocatalytic degradation, it is widely confirmed that hydroxyl radicals (\*OH) are a key active species in the photocatalytic process [31, 32]. It can attack the adsorbed toxic organic molecules to produce oxidized species and/or

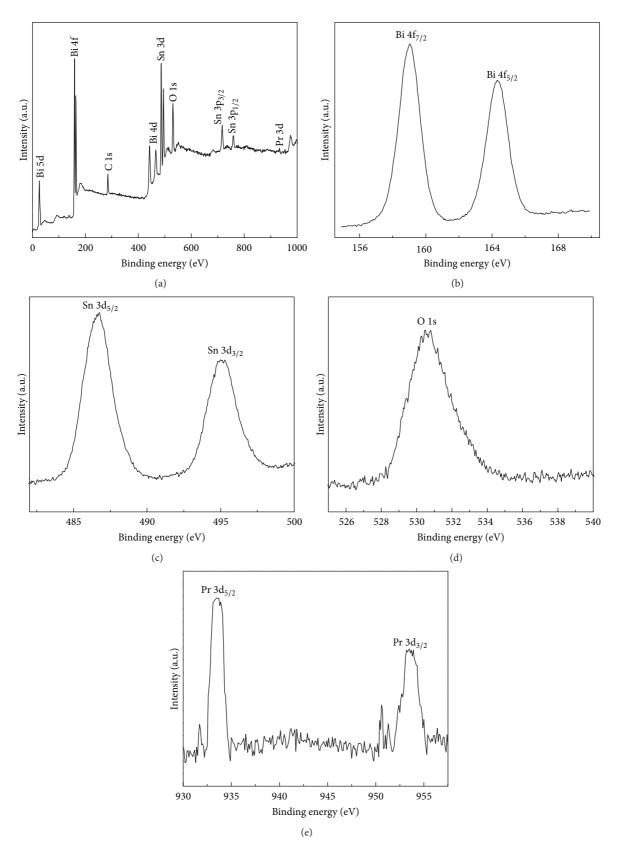


Figure 5: XPS spectra of 1%-Pr-BSO sample: (a) survey spectrum, (b) Bi 4f, (c) Sn 3d, (d) O 1s, and (e) Pr 3d.

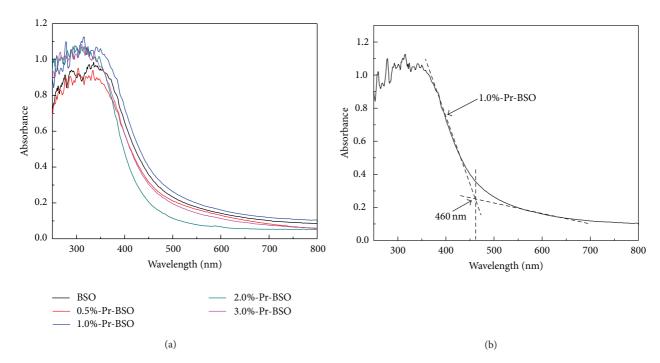


FIGURE 6: UV-Vis diffuse reflectance spectra of (a) different Pr-doped BSOs and (b) 1%-Pr-BSO.

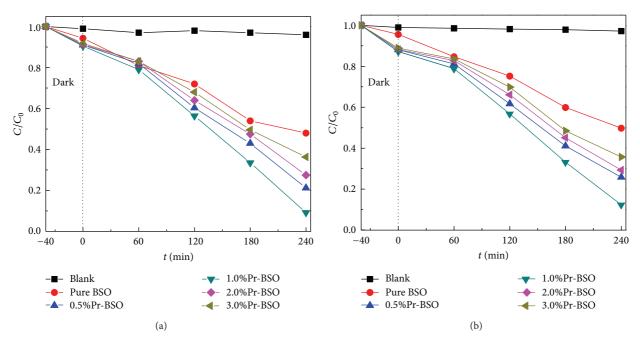


FIGURE 7: Degradation curves of (a) RhB and (b) 2,4-DCP.

decomposed products [33]. The analysis of \*OH radical is performed by fluorescence technique using terephthalic acid, which can react with \*OH radical in basic solution and generate 2-hydroxy terephthalic acid (TAOH) [34]. TAOH emits a strong fluorescence signal at around 426 nm on the excitation of its own 312 nm absorption band. Therefore, the formation of \*OH radicals at the photocatalytic system was detected by PL technique using terephthalic acid as a probe molecule. Figure 8(a) shows the fluorescence spectra

of 1%-Pr-BSO catalyst recorded at the same interval of irradiation time. It was obvious that the photoluminescence emission peak at about 426 nm was continuously enhanced. However, no fluorescence emission was observed in the absence of visible light. Figure 8(b) shows the plot of increase in fluorescence intensity against illumination time at 426 nm. The fluorescence intensity by visible light illumination in terephthalic acid solutions increased linearly against time. Based on the results, we could conclude that the large amount

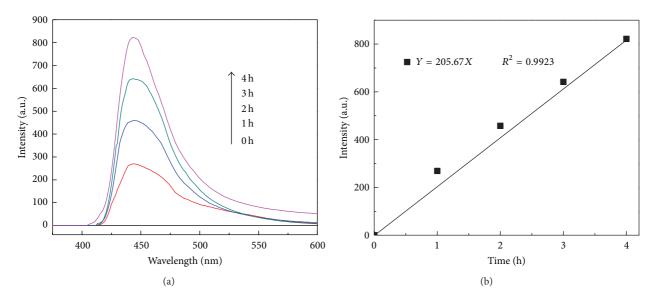


FIGURE 8: (a) \*OH-trapping photoluminescence spectra of 1%-Pr-BSO in solution of terephthalic acid at room temperature (ex, 312 nm; em, 426 nm) and (b) plots of the induced PL intensities of 1%-Pr-BSO at 426 nm on the irradiation time.

of \*OH was generated in the 1%-Pr-BSO photocatalytic system under visible light irradiation. The generation of \*OH radicals was the main active specials in the photocatalytic system.

3.7. Discussion on Photocatalysis Process of Pr-BSO. Generally, the photoexcited state of Pr cations is generated by the absorption of light, corresponding to the transition of the electrons situated in the inner 4f orbital to the 4s orbital [35]. The excited state ions have the capability of transferring their excited energy to other adsorbed molecules (f-f transition) [36]. The transitions of 4f electrons can lead to the enforcement of the optical adsorption of catalysts [24]. Reddy et al. [37] reported that rare earth elements could be used as good electron acceptors, and it could capture excited electron and facilitate the separation of electron-hole pairs. As we all know, photons from visible irradiation are used to generate electrons and holes. The holes react with H2O or OH to form hydroxyl radicals (OH) and the electronhole separation process is improved because BSO sample transfers photoelectrons to Pr when praseodymium appears on BSO surface [22, 30]. Subsequently, the electrons migrate from Pr to the adsorbed  $O_2$  to form  $O_2^{\bullet-}$ . OH and  $O_2^{\bullet-}$  are important species which posses strong capability of oxidizing and breaking RhB and 2,4-DCP in aqueous solution [25]. The photocatalytic procedure is presented in Figure 9.

### 4. Conclusions

Pr-doped BSO materials prepared by a facile hydrothermal method were successfully used in the photocatalytic conversion of RhB and 2,4-DCP under visible light. The nanostructured Pr-BSO samples possessed high photocatalytic activity, fine-grained distribution and large surface area. The praseodymium doping effectively shifted the BSO

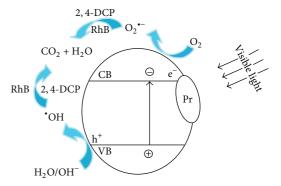


FIGURE 9: Photocatalysis process of Pr-doped BSO photocatalyst under visible light irradiation.

absorption edge and retarded the growth of crystallite. The as-prepared Pr-BSO photocatalysts displayed approximately the spherical shape and owned the mesoporous surface. An optimal Pr doping concentration existed and was 1.0 mol%, and superfluous Pr would make negative influence on photodegradation efficiency.

### Acknowledgment

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### Research Article

### Solar Photocatalytic Degradation of Bisphenol A on Immobilized ZnO or TiO<sub>2</sub>

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The removal of bisphenol A (BPA) under simulated solar irradiation and in the presence of either TiO $_2$  or ZnO catalysts immobilized onto glass plates was investigated. The effect of various operating conditions on degradation was assessed including the amount of the immobilized catalyst (36.1–150.7 mg/cm $^2$  for TiO $_2$  and 0.5–6.8 mg/cm $^2$  for ZnO), initial BPA concentration (50–200  $\mu$ g/L), treatment time (up to 90 min), water matrix (wastewater, drinking water, and pure water), the addition of H $_2$ O $_2$  (25–100 mg/L), and the presence of other endocrine disruptors in the reaction mixture. Specifically, it was observed that increasing the amount of immobilized catalyst increases BPA conversion and so does the addition of H $_2$ O $_2$  up to 100 mg/L. Moreover, BPA degradation follows first-order reaction kinetics indicating that the final removal is not practically affected by the initial BPA concentration. Degradation in wastewater is slower than that in pure water up to five times, implying the scavenging behavior of effluent's constituents against hydroxyl radicals. Finally, the presence of other endocrine disruptors, such as  $17\alpha$ -ethynylestradiol, spiked in the reaction mixture at low concentrations usually found in environmental samples (i.e.,  $100 \mu$ g/L), neither affects BPA degradation nor alters its kinetics to a considerable extent.

### 1. Introduction

Endocrine disrupting compounds (EDCs) constitute an important class of emerging environmental contaminants, which pose an increasing threat to aquatic organisms, as well as to human health [1]. In particular, the exposure to EDCs has been linked with altering functions of the endocrine system in male fish such as vitellogenin induction and feminized reproductive organs [2]. Moreover, the increasing incidence of cancer and the hypothesis of a decreasing reproductive fitness of men are thought to be attributed to endocrine disruptors. Among various EDCs, bisphenol A (BPA) is well-known for its interference with the endocrine system of living beings [3, 4]. BPA is widely used in the manufacturing of numerous chemical products, such as CDs, DVDs, drink containers, electrical and electronic equipment, and protective

coatings [1, 5]. These substances enter municipal wastewater treatment plants (WWTPs) through either human excretion or their direct disposal in the sewage system. Currently, when EDCs enter conventional biological WWTP, only a small amount of these chemicals are removed via biodegradation processes because most of them are xenobiotics and thus nonbiodegradable [6]. Therefore, the majority of EDCs remain soluble in the effluent, and they are discharged to aquatic bodies. In the last decade, several studies have confirmed the occurrence of EDCs at the level of ng/L- $\mu$ g/L in inland waters (rivers and streams) and wastewaters (outlets of municipal and industrial WWTPs) worldwide [7-11]. Not only this, but it has been found that these compounds can pose a potential danger to fish and other aquatic organisms, even at low concentrations of 0.1-10 ng/L [12]. Thus, it is necessary to look further on the removal mechanisms, in order to improve

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the efficiency of the existing treatment systems and to develop new and reliable treatment strategies to remove EDCs from wastewaters.

Semiconductor photocatalysis using solar radiation as the source of photons for the activation of the catalyst has received considerable attention over the past several years. Several heterogeneous photocatalysts have been investigated, and, amongst them, the use of TiO<sub>2</sub> under ultraviolet and/or visible light has extensively been researched. Another photocatalyst that absorbs over a large fraction of the solar spectrum is ZnO with a gap energy of 3.2 eV. The photocatalytic mechanism of ZnO is similar to that of TiO<sub>2</sub> [13]. Moreover, solar photocatalysis is considered as a cost-effective and sustainable treatment technique due to the utilization of solar energy (an abundant source of energy). However, the biggest problem with slurry photocatalysis has been recognized to be the need for a posttreatment recovery step [14, 15]. Therefore, research has been conducted to produce catalysts on supports that would keep the catalyst powder out of the treated water and sufficiently reduce even more the cost of the photocatalytic process, since there will be no need for catalyst aftertreatment. So far, few studies have dealt with the treatment of EDCs by means of TiO<sub>2</sub> or ZnO catalysts immobilized onto supports, such as glass [4, 16], PTFE mesh sheets [17], titanium substrates [18, 19], and polyurethane foam cubes [20].

Hence, in this work, the efficacy of solar photocatalytic process to remove BPA from aqueous environmental samples was investigated. For this purpose, two different photocatalytic materials, namely, ZnO and  ${\rm TiO_2}$ , were immobilized onto appropriate glass substrate by means of a heat attachment technique. The effect of various operating parameters, such as the immobilized catalyst amount, the initial BPA concentration, the treatment time, the water matrix, the addition of  ${\rm H_2O_2}$ , and the presence of other organic substances, on process efficiency, was investigated.

### 2. Materials and Methods

2.1. Materials. BPA and  $17\alpha$ -ethynylestradiol (EE2) were purchased from Sigma-Aldrich, while ZnO (≥99%, particle size < 100 nm, 15– $25\,\text{m}^2/\text{g}$  BET surface area) and TiO<sub>2</sub>-P25 (anatase: rutile 75: 25, 21 nm primary crystallite particle size,  $50\,\text{m}^2/\text{g}$  BET surface area) were purchased from Fluka and Degussa-Evonik Corp., respectively. The water matrix was either of the following three: (i) wastewater (WW) collected from the outlet of the secondary treatment of the municipal WWTP of Chania, W. Crete, Greece; (ii) commercially available bottled water, which will be referred to in the text as drinking water (DW); and (iii) ultrapure water (UPW) at pH = 6.1 taken from a water purification system (EASYpureRF-Barnstead/Thermolyne, USA). The main properties of WW and DW are given in Table 1.

2.2. Catalyst Preparation. The ZnO or  $TiO_2$  catalyst powders were immobilized on glass plates (1.5 cm  $\times$  1.5 cm) by a heat attachment method. Analytically, the glass plates were first treated with a 38% HF solution and then washed with

Table 1: Properties of wastewater and drinking water matrices used in this study.

Parameter	Wastewater	Drinking water	
pH	8	7.7	
TOC (mg/L)	7.8	0.3	
COD (mg/L)	24 ND		
Conductivity (µs/cm)	820	329	
$HCO_3^-$ (mg/L)	190	188	
Cl <sup>-</sup> (mg/L)	220	<5	
$NO_2^-$ (mg/L)	57	< 0.09	
$NO_3^-$ (mg/L)	26	<5	

ND: not determined.

0.01 M NaOH in order to increase the number of OH groups and achieve better contact of the catalyst on glass plates [14]. Moreover, a suspension of 8 g/L catalyst in distilled water was prepared. This suspension was sonicated at 80 kHz for 120 min in order to improve the dispersion of the solid catalyst in water. Afterwards, the sonicated catalyst solution was poured on the glass plates at various volumes, ranging from some  $\mu$ L to about 10 mL and then placed in an oven at 120°C for 60 min. After drying, the glass plates were calcined at 500°C for 180 min. Finally, the glass plates were washed with distilled water to remove the loosely attached catalytic particles.

2.3. Catalyst Characterization Techniques. The crystal structure, particle size, and morphology were examined with a powder X-ray diffraction (XRD) system and scanning electron microscopy (SEM), respectively. XRD patterns were collected on a Rigaku D/MAX-2000H rotating anode diffractometer (Cuk $\alpha$  radiation) equipped with a secondary pyrolytic graphite monochromator operating at 40 kV and 80 mA over the 2 $\theta$  collection range of 10–80°. The scan rate was 0.05/min with a step size of 0.01. Surface morphology of the catalytic plates was carried out on a JEOL JSM-6400V SEM instrument.

2.4. Photocatalytic Experiments. Photocatalytic experiments were performed using a solar simulator (Newport, model 96000) equipped with a 150 W xenon ozone-free lamp and an Air Mass 1.5 Global Filter (Newport, model 81094), simulating solar radiation reaching the surface of the earth at a zenith angle of 48.2°.

The incident radiation intensity on the photochemical reactor in the UV region of the electromagnetic spectrum was measured actinometrically using 2-nitrobenzaldehyde (purchased from Sigma-Aldrich) as the chemical actinometer [21], and it was found to be 16.5 10<sup>-5</sup> einstein/m<sup>2</sup>. In a typical photocatalytic run, 64 mL of the water matrix spiked with the appropriate amount of the organic substance was fed in a cylindrical pyrex cell and the ZnO or TiO<sub>2</sub> catalytic plate was added, while the cell was open to the atmosphere. The solar simulator was placed on top of the liquid surface, while the catalytic glass plate was held by a Ti support dipped into

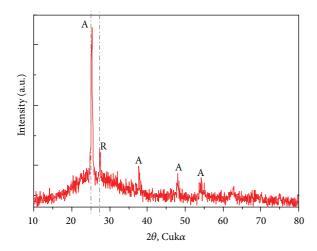


FIGURE 1: XRD pattern of the  ${\rm TiO_2}$  immobilized particles on glass plate (A: anatase; R: rutile).

the reaction mixture. Samples of about 1 mL were periodically taken from the cell and analyzed as follows.

2.5. Analytical Techniques. High-performance liquid chromatography (Alliance 2690, Waters) was employed to monitor the concentrations of BPA and EE2. Separation was achieved on a Luna C-18(2) column (5  $\mu$ m, 250 mm  $\times$ 4.6 mm) and a security guard column (4 mm  $\times$  3 mm), both purchased from Phenomenex. The mobile phase consists of 35:65 UPW: acetonitrile eluted isocratically at 1 mL/min and 30°C, while the injection volume was 100  $\mu$ L. Detection was achieved through a fluorescence detector (Waters 474), in which the excitation wavelength was 280 nm and the emission wavelength was 305 nm. Under these conditions, the retention time for BPA was 4.3 min, the limit of detection was 0.68  $\mu$ g/L, and the limit of quantitation was 2.32  $\mu$ g/L; the respective values for EE2 were 5.1 min, 0.63  $\mu$ g/L, and  $2.11 \,\mu g/L$ . Residual  $H_2O_2$  concentration was monitored using Merck peroxide test strips in the range 0–100 mg/L. Changes in effluent pH during photocatalytic treatment were checked using a Toledo 225 pH meter.

### 3. Results and Discussion

3.1.  $TiO_2$  Catalyst Plates. Figure 1 shows XRD pattern of the  $TiO_2$  immobilized particles on glass plate subjected to heat treatment at 500°C for 3 h. Peaks at  $2\theta$  values of  $25^\circ$  and  $27^\circ$  correspond to the anatase (101) and rutile (110) planes, respectively. The crystalline size (*D*) was calculated at 17 nm using the Scherrer equation:

$$D = \frac{k\lambda}{\beta\cos\theta},\tag{1}$$

where k is a constant equal to 0.9,  $\lambda$  is the wavelength of characteristics X-ray applied (0.15418 nm),  $\beta$  is the full width at half maximum of the anatase (101) peak obtained by XRD, and  $\theta$  is the Bragg angle.

The phase content of  ${\rm TiO_2}$  particles can be calculated as follows:

$$f_A = \frac{1}{1 + I_R/0.79I_A},\tag{2}$$

where  $f_A$  is the content of anatase, and  $I_A$  and  $I_R$  are the integrated intensities of the anatase (101) and rutile (110) peaks, respectively. The  $TiO_2$  catalytic plate mainly consists of the anatase phase with mirror rutile phase (70:30).

Figure 2 shows SEM images of the immobilized catalytic particles on glass plates with different amounts of  ${\rm TiO_2}$  in the range 81.3–339.2 mg (36.1–150.7 mg/cm²). The  ${\rm TiO_2}$  layer is homogeneous with a porous surface, while the morphology of  ${\rm TiO_2}$  particles is amorphous. As the amount of  ${\rm TiO_2}$  increases the homogeneity increases and so does the film thickness in the range 2–6  $\mu$ m.

The effect of increasing the amount of immobilized TiO<sub>2</sub> on BPA removal is shown in Figure 3; the 90 min conversion increases from 60% to 80% as TiO2 increases from 36.1 to 150.7 mg/cm<sup>2</sup>, and this is expected since more catalyst surface sites are available for reaction at higher catalyst loadings. An additional run was performed in the absence of catalyst yielding only 15% photolytic removal after 90 min. Since TiO<sub>2</sub> in slurry has extensively been used for photocatalytic purposes, an extra run was carried out to compare the efficiencies of slurry and immobilized catalysts. Hence, 0.65 mg TiO<sub>2</sub> powder was added to the reaction mixture, and complete removal of 100  $\mu$ g/L BPA could be achieved after 35 min of reaction (data not shown). This shows that slurry catalysts, even at extremely low concentrations, yield higher reaction rates than the immobilized systems, presumably due to lower mass transfer limitations.

3.2. ZnO Catalyst Plates. Figure 4 shows XRD pattern of the ZnO immobilized particles on glass plate subjected to heat treatment at 500°C for 3 h. The sharp intense peaks of ZnO confirm the good crystalline nature of ZnO and form (100), (002), (101), (102), (110), (103), (200), and (112) reflections of hexagonal ZnO. The size of the particles was calculated at 47 nm using (1).

Figure 5 shows SEM images of the immobilized catalytic particles for the fresh and used ZnO. Moreover, the initial glass plate, as well as the HF-treated surface, is shown. It is evident that the glass surface becomes rough after acid treatment (Figure 5(b)), thus facilitating catalyst attachment. Figure 5(c) shows the dispersion of fresh ZnO onto the glass surface, where agglomeration of the particles takes place to some extent. Conversely, Figure 5(d) shows the SEM image of a plate that has been employed for more than 30 h of photocatalytic experiments under various conditions (including runs with wastewater). It is observed that particles dispersion is more homogeneous than that of the fresh plate and this is probably due to the presence of several organic and/or inorganic impurities accumulated onto the surface during its photocatalytic use. The film thickness is in the range  $2-4 \mu m$ .

The effect of increasing ZnO loading in the range 1.2–15.3 mg (0.5–6.8 mg/cm<sup>2</sup>) on BPA removal is shown in

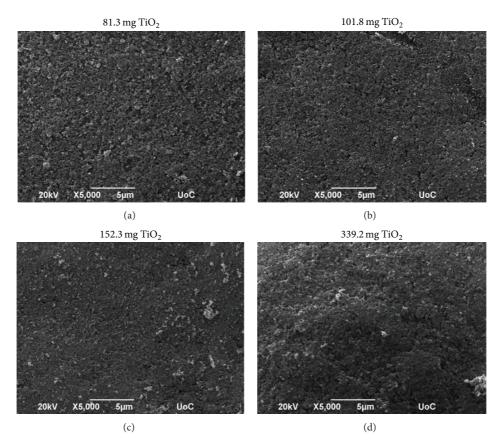


FIGURE 2: SEM images of  $TiO_2$  immobilized particles on glass plate with increasing amount of catalyst from 81.3 to 339.2 mg (36.1 to  $150.7 \text{ mg/cm}^2$ ).

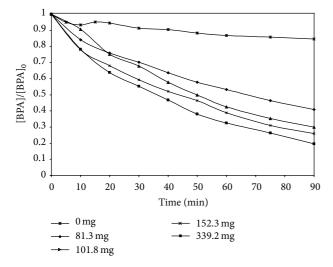
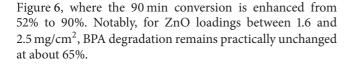


FIGURE 3: Effect of TiO  $_2$  loading on the conversion of 100  $\mu g/L$  BPA in UPW.



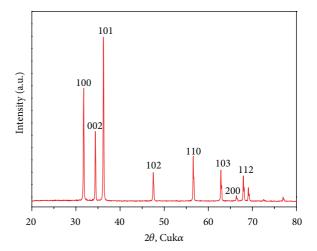


Figure 4: XRD pattern of the ZnO immobilized particles on glass plate.

Another interesting finding is that for the same volume of the catalyst aqueous suspension (i.e., from 200  $\mu$ L to 10 mL), the quantity of ZnO attached onto the glass support is 1-2 orders of magnitude lower than that of TiO<sub>2</sub>. This is due to the fact that TiO<sub>2</sub> is known to have more hydroxyl anions on its surface than ZnO, thus enhancing the adhesion of

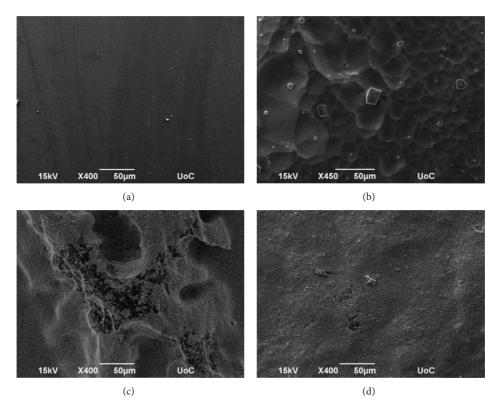


FIGURE 5: SEM images of (a) glass plates; (b) glass plates treated with HF solution; (c) 3.7 mg fresh ZnO (1.6 mg/cm<sup>2</sup>) immobilized onto the plate; and (d) 3.7 mg used ZnO (1.6 mg/cm<sup>2</sup>) immobilized onto the plate.

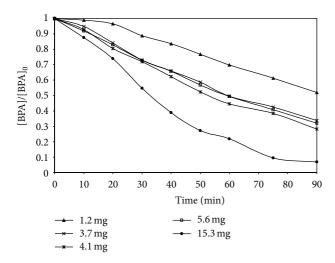


FIGURE 6: Effect of ZnO loading on the conversion of 100  $\mu$ g/L BPA in UPW.

powder onto the appropriate substrate. Nevertheless, this does not seem to affect the catalytic activity of ZnO which, on a catalyst-loading basis, is more efficient than  ${\rm TiO_2}$ ; for example, a common BPA conversion can be achieved after 90 min at 1.8 mg/cm<sup>2</sup> ZnO or 45.2 mg/cm<sup>2</sup> TiO<sub>2</sub>, as can be observed from Figures 3 and 6.

3.3. Effect of Initial BPA Concentration. The effect of initial BPA concentration (50, 100, and 200  $\mu$ g/L) on its degradation over 150.7 mg/ cm<sup>2</sup> TiO<sub>2</sub> was investigated and concentration-time profiles were followed (data not shown). The 90 min BPA removal was 77  $\pm$  3% irrespective of the initial BPA concentration, thus implying first-order kinetics, that is,

$$-\frac{d \text{ [BPA]}}{dt} = k_{\text{app}} \text{ [BPA]} \iff \ln \frac{\text{[BPA]}_o}{\text{[BPA]}}$$
$$= k_{\text{app}} t \iff \ln (1 - X) = -k_{\text{app}} t,$$
(3)

where  $k_{app}$  is an apparent reaction rate constant and X is BPA conversion independent of its initial concentration [BPA]<sub>o</sub>.

Figure 7(a) confirms that the reaction approaches, indeed, first-order kinetics. Plotting the logarithm of normalized BPA concentration against time results in straight lines (the coefficient of linear regression of data fitting,  $r^2$ , is between 99.3% and 99.6%) with a nearly common slope, which corresponds to the apparent reaction rate constant; this is 15  $\pm 1\,10^{-3}\,\mathrm{min}^{-1}$ .

The effect of initial BPA concentration was also studied at  $1.6 \text{ mg/cm}^2$  ZnO; the 90 min removal was  $64\pm2\%$  irrespective of the initial concentration. Figure 7(b) shows the respective first-order degradation kinetics, from which the apparent rate constant is computed at  $11\pm1~10^{-3}~\text{min}^{-1}$  (the coefficient of linear regression of data fitting,  $r^2$ , is between 99.4% and 99.6%).

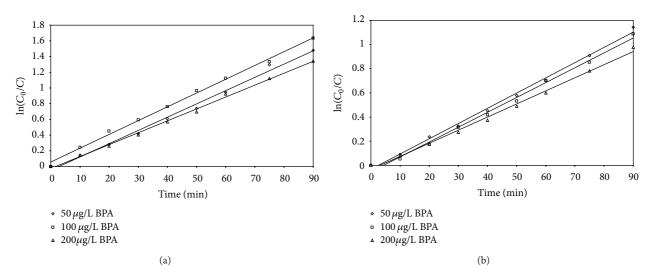


FIGURE 7: Effect of initial BPA concentration on its degradation in UPW at (a) 150.7 mg/cm<sup>2</sup> TiO<sub>2</sub> and (b) 1.6 mg/cm<sup>2</sup> ZnO. Plot of (3).

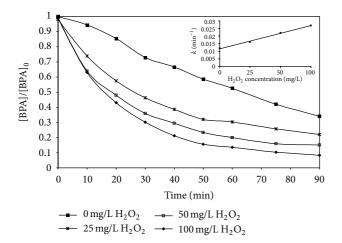


FIGURE 8: Effect of  $\rm H_2O_2$  on the conversion of 100  $\mu$ g/L BPA in UPW at 1.6 mg/cm² ZnO. Inset graph: change of  $k_{\rm app}$  with  $\rm H_2O_2$  concentration.

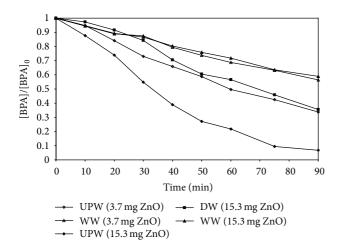


FIGURE 9: Effect of water matrix on the conversion of 100  $\mu$ g/L BPA at two ZnO loadings.

From the results presented so far, it is evident that both catalysts exhibit a similar performance for BPA degradation through first-order kinetics. We decided to expand experimentation with ZnO since (a) TiO<sub>2</sub> has extensively been studied in the literature for several environmental applications and (b) ZnO has the potential to achieve improved photocatalytic performance as it absorbs over a wide region of the UV-A spectrum [22]. It should be mentioned here that ZnO is generally more susceptible to photo corrosion and/or chemical corrosion (i.e., leaching) than TiO<sub>2</sub> and this is a point of concern; nonetheless, our previous studies [13] showed that ZnO was remarkably stable during the photocatalytic oxidation of slightly alkaline, wastewater matrices.

3.4. Effect of Hydrogen Peroxide. The addition of oxidizing species increases the efficiency of the photocatalytic process because  $\rm H_2O_2$  is an electron acceptor and reacts with the electrons of the photo-activated surface of the catalyst:

$$H_2O_2 + e^- \longrightarrow {}^{\bullet}OH + OH^-$$
 (4)

Thus, the addition of peroxide constitutes an extra source of hydroxyl radicals and increases the photoreactivity of ZnO during the photocatalytic degradation [23].

According to our findings (Figure 8), increasing hydrogen peroxide concentration from 0 to 100 mg/L results in increased removal; for example, the 90 min conversion is 66%, 78%, 85%, and 92% at 0, 25, 50, and 100 mg/L  $\rm H_2O_2$ , respectively. The inset of Figure 8 shows that the respective apparent rate constants increase almost linearly with the amount of  $\rm H_2O_2$  added up to 100 mg/L.

It should be noted here that  $H_2O_2$  was only partly consumed during the previous photocatalytic runs as confirmed with the peroxide test strips; unfortunately, precise determination of residual peroxide was not possible with this method.

3.5. Effect of Water Matrix. Figure 9 clearly shows that BPA degradation is impeded in complex water matrices

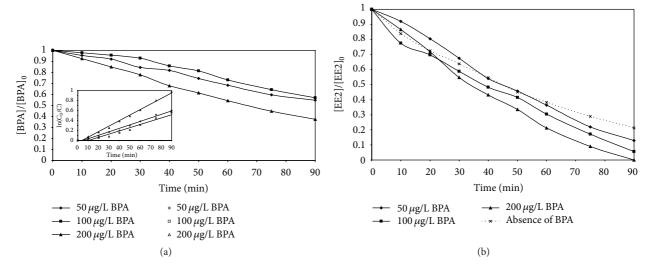


FIGURE 10: Degradation of a mixture of BPA and EE2 in UPW at 1.6 mg/cm $^2$  ZnO. Effect of (a) 100  $\mu$ g/L EE2 on 50, 100 and 200  $\mu$ g/L BPA; (b) 50, 100 and 200  $\mu$ g/L BPA on 100  $\mu$ g/L EE2. Inset graph: plot of (3).

containing organic and inorganic constituents; for instance the 90 min conversion is 93%, 65%, and 41% in UPW, DW, and WW, respectively, at 15.3 mg (6.8 mg/cm<sup>2</sup>) ZnO. The respective apparent kinetic constants are computed equal to  $0.342 \ (r^2 = 0.955), \ 0.128 \ (r^2 = 0.95), \ \text{and} \ 0.064 \, \text{min}^{-1}$  $(r^2 = 0.979)$ . The discrepancy by an order of magnitude between kinetics in UPW and WW can be explained taking into account that (a) the oxidizing agents are competitively consumed in reactions involving the residual organic fraction present in treated WW (i.e., COD = 24 mg/L) but not in UPW. Since this is known to be refractory to biological or chemical oxidation [24] and constitutes most of the matrix's total organic content, nonselective oxidizing agents will partly be wasted attacking this fraction; (b) hydroxyl radicals may be scavenged by bicarbonates and chlorides present in WW and/or DW to form the respective radicals, whose oxidation potential is lower than that of hydroxyl radicals [25, 26].

The experiments were repeated at a reduced ZnO loading of 3.7 mg (1.6 mg/cm²). In this case, the 90 min BPA conversion is 60% in UPW and decreases to 44% in WW with the respective rate constants being 12  $10^{-3}$  min<sup>-1</sup> ( $r^2 = 0.994$ ) and 6  $10^{-3}$  min<sup>-1</sup> ( $r^2 = 0.992$ ); the ratio  $k_{\rm UPW}/k_{\rm ww}$  is 5.3 and 2 at 6.8 and 1.6 mg/cm² ZnO, respectively. These results clearly indicate that the degree of deceleration of the photocatalytic process due to the complexity of the water matrix strongly depends on the catalyst-loading.

3.6. Degradation of EDCs Mixture. Experiments were carried out to investigate the possible interactions of BPA with EE2, a synthetic hormone typically found in the contraceptive pill and well-known for its interference with the endocrine system of living beings [27].

Figure 10(a) shows BPA concentration-time profiles (50–200  $\mu$ g/L initial concentration) in UPW and in the presence

of 100 µg/L EE2, while Figure 10(b) shows EE2 concentrationtime profiles (100  $\mu$ g/L initial concentration) in UPW and in the presence of different BPA concentrations in the range 0-200 µg/L. Comparing Figures 7(b) and 10(a) (inset graph), it is deduced that BPA degradation is slightly impeded by the presence of EE2, especially at 50 and 100 µg/L BPA initial concentrations. On the other hand, Figure 10(b) shows an enhancement of EE2 degradation from 79% in the absence of BPA to 87%, 94.5%, and 99% in the presence of 50, 100, and 200 µg/L BPA, respectively. These results are consistent with our previous work [16], where the photocatalytic EE2 degradation was studied in the presence of BPA. Possible explanations of this observation would involve the following (a) differences in BPA and EE2 chemical structures; EE2 has a longer molecular chain with more complicated structure than BPA and this could render it more readily susceptible to oxidative attack; (b) the simultaneous BPA-EE2 degradation may create active radicals that would also attack firstly EE2, facilitating thus its degradation; and (c) EE2, due to its longer and more complex molecule chain, may act as a shield to BPA molecule preventing its diffusion to the catalyst surface, thus decreasing its degradability.

The experiments were then performed in WW and the results are shown in Figure 11. The previous phenomenon is far less pronounced in this case, and this is possibly due to the fact that the WW matrix has already had a strong adverse impact (see Section 3.5), thus masking any interactions between BPA and EE2.

A kinetic simulation of BPA degradation in the presence of EE2 was performed for both UPW and WW matrices. Based on the experimental data shown in Figures 10(a) and 11(a), BPA degradation seems to follow near first-order kinetics as its degradation rate does not depend strongly on its initial concentration. The apparent rate constant for degradation in UPW is  $9 \pm 2~10^{-3}~\text{min}^{-1}$  (computed from the

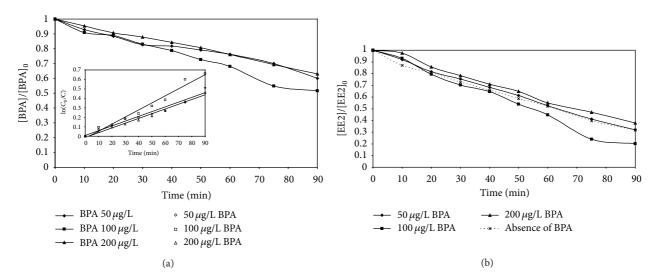


FIGURE 11: Degradation of a mixture of BPA and EE2 in WW at 1.6 mg/cm<sup>2</sup> ZnO. Effect of (a)  $100 \mu g/L$  EE2 on 50, 100, and  $200 \mu g/L$  BPA and (b) 50, 100 and  $200 \mu g/L$  BPA on  $100 \mu g/L$  EE2. Inset graph: plot of (3).

slope of the straight lines shown in inset Figure 10(a)) and decreases to  $6 \pm 1 \cdot 10^{-3} \text{ min}^{-1}$  in WW (inset Figure 11(a)).

### 4. Conclusions

Overall, the removal of BPA under simulated solar irradiation and in the presence of either TiO2 or ZnO catalysts immobilized onto glass plates was investigated. It was observed that the amount of catalyst attached onto the glass plate can affect process efficiency, which generally increases at increased catalyst loadings under the conditions tested. BPA removal follows a first-order reaction rate indicating that the removal is not practically affected by the initial BPA concentration, in the presence of either TiO<sub>2</sub> or ZnO catalyst. At the conditions employed in this study, apparent reaction rates increase with (a) increasing  $H_2O_2$  concentration in a proportional fashion and (b) decreasing complexity of the water matrix (i.e., from wastewater to drinking water to ultrapure water). The presence of other EDCs, such as EE2, spiked in the reaction mixture does not seem to obstruct BPA degradation.

Hence, solar photocatalytic treatment using immobilized  ${\rm TiO_2}$  or ZnO photocatalysts can be a promising, with low energy requirements and efficient process to remove endocrine disrupting compounds, found at low concentrations, from aqueous matrices. The key advantage of the proposed setup is that there is no need for catalyst aftertreatment and separation in train with the photocatalytic process, thus decreasing the overall cost of a large-scale treatment plant.

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### Research Article

# CTAB-Assisted Hydrothermal Synthesis of Bi<sub>2</sub>Sn<sub>2</sub>O<sub>7</sub> Photocatalyst and Its Highly Efficient Degradation of Organic Dye under Visible-Light Irradiation

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Pyrochlore-type  $\mathrm{Bi_2Sn_2O_7}$  (BSO) nanoparticles have been prepared by a hydrothermal method assisted with a cationic surfactant cetyltrimethylammonium bromide (CTAB). These BSO products were characterized by powder X-ray diffraction (XRD), infrared spectroscopy (IR), scanning electron microscopy (SEM), transmission electron microscopy (TEM), Brunauer-Emmett-Teller (BET), and UV-visible diffuse reflectance spectroscopy (DRS). The results indicated that CTAB alters the surface parameters and the morphology and enhances the photoinduced charge separation rate of BSO. The photocatalytic degradation test using rhodamine B as a model pollutant showed that the photocatalytic activity of the BSO assisted with CTAB was two times that of the reference BSO. Close investigation revealed that the size, the band gap, the structure, and the existence of impurity level played an important role in the photocatalytic activities.

### 1. Introduction

Synthetic textile dyes and other industrial dyestuffs are important organic pollutants and produced all over the world. Their release as wastewater in the ecosystem will cause serious consequences, such as esthetic pollution, eutrophication, and perturbations in aquatic life [1, 2]. Many treatments have been developed and photocatalytic oxidation is regarded as a "green" technology for the decomposition of the soluble dyes in wastewater [3]. Nanosized TiO<sub>2</sub> semiconductor has been considered as one of the most promising photocatalysts in practical applications due to its high photocatalytic activity, chemical stability, low cost, and nontoxicity [4, 5]. However, the TiO2 photocatalyst has no visible-light response due to its large band gap of 3.2 eV [6]. As a result, there are two strategies to develop the visible-light-driven photocatalysts: modification of TiO<sub>2</sub> [7-11] and exploitation of novel semiconductor materials [12-15]. Recently, many investigations have been undertaken on the latter strategy. A great deal

of effort has been devoted to developing photocatalysts containing bismuth with high activities for environmental applications and/or water splitting, such as  $\alpha\text{-Bi}_2\text{O}_3$  [14],  $\text{Bi}_2\text{WO}_6$  [15],  $\text{BiVO}_4$  [12],  $\text{CaBi}_2\text{O}_4$  [16] and  $\text{Bi}_2\text{O}_2\text{CO}_3$  [17]. Zhou et al. [7] have synthesized mesoporous Au-TiO2 nanocomposite with high visible-light photocatalytic activity. Chen et al. [6] reported that some dyes could be degraded under visible-light irradiation over TiO2 by a self-photosensitized process. However, its photoefficiency was rather low due to the much slower interfacial electron transfer to the oxidize sensitizer. Therefore, the development of efficient visible-light-induced bismuth-based oxides photocatalysts through new synthetic routes has been an urgent issue.

Bi<sub>2</sub>Sn<sub>2</sub>O<sub>7</sub>, a novel important semiconducting material with a typical pyrochlore structure and a band gap of 2.88 eV [18], has received considerable attention in catalysis and gas sensors [19–23]. However, the photocatalytic performance of bismuth stannate should be further improved for practical use. In order to overcome the defect, some researches have

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shown that properties of the matter were limited by its size, shape, and specific surface area. Therefore, recently, in order to explore some photocatalysts with specific morphologies and unique properties, surfactant containing system has been employed to the preparation of nanosized photocatalysts. Liu et al. achieved nanocrystalline TiO<sub>2</sub> in microemulsions by using CTAB as surfactant [24]. Yin et al. have synthetized highly efficient monoclinic BiVO<sub>4</sub> with the assistance of CTAB [25]. Shen et al. found that the photocatalytic activities of ZnIn<sub>2</sub>S<sub>4</sub> photocatalysts improved with the amounts of CTAB increasing [26]. CTAB can make the surface of photocatalysts hydrophobic, which is beneficial to the adsorption of nonionic organic compounds onto the photocatalyst and will improve the photocatalytic efficiency. Moreover, synthetic method also played an important role in preparing samples. Solid-state reaction technique had been a common method for the synthesis of pyrochlore BSO [12, 16, 17]. Compared with solid-state reaction, hydrothermal route [18] provided a milder environment for the pyrochlore BSO and the reaction parameters could be easily tuned. However, to the best of our knowledge, the synthesis of BSO by hydrothermal method with surfactant CTAB as the template has not been reported.

In this paper, we developed a facile surfactant (CTAB)-assisted hydrothermal method to prepare BSO photocatalyst at 180°C and the sample was labeled as C-BSO. A model dye of rhodamine B (RhB) was used to evaluate its photocatalytic efficiency under visible-light irradiation. Furthermore, the effects of CTAB on the crystal structure, morphology, and photocatalytic activity were discussed in detail.

### 2. Experimental

2.1. Synthesis. All the reagents were of analytical purity and used without further purification. In a typical reaction, K<sub>2</sub>SnO<sub>3</sub>·3H<sub>2</sub>O (3 mmol) and Bi(NO<sub>3</sub>)<sub>3</sub>·5H<sub>2</sub>O (3 mmol) were added by stoichiometric ratio, and 0.3 mmol CTAB was dissolved in a Teflon liner with 100 mL capacity containing 80 mL of deionized water. Under vigorous stirring, the pH value of the mixture was adjusted to 12 by using 2 mol/L KOH, and then the Teflon liner was sealed in the stainless steel autoclave and maintained at 180°C for 24 h. The asprepared products were obtained by filtration and washed with deionized water and absolute ethanol several times. Finally, the products were dried in hot air oven at 80°C for 12 h. BSO was also prepared by the same procedure mentioned previously without the presence of CTAB.

2.2. Characterization. Samples were characterized by using X-ray diffraction (XRD) with a Bruker D8 Advance diffractometer using Cu KR ( $\lambda=1.5406\,\mathrm{nm}$ ) and operating at 40 kV and 40 mA. FT-IR spectra were taken in a Shimadzu IR Prestige-21 Fourier transform spectrometer. A scanning electron microscopy (SEM) images were obtained on a JEOL JSM-6700F instrument. Transmission electron microscopy (TEM) images were obtained with a JEOL JEM-2100HR field-emission electron microscope. The Brunauer-Emmett-Teller (BET) specific surface areas of the materials were detected by Micromeritics ASAP 2010 nitrogen adsorption

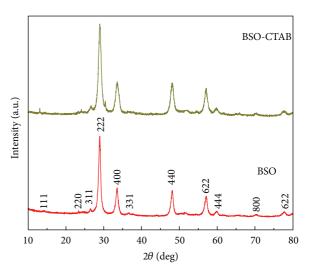


FIGURE 1: XRD patterns of BSO and C-BSO photocatalysts.

apparatus. UV-visible absorption spectra of the samples were determined on a Hitachi U-3010 UV-Vis spectrophotometer with  ${\rm BaSO_4}$  as the reference.

2.3. Photocatalytic Test. The photocatalytic efficiencies of BSO were evaluated by the degradation of RhB under visible-light irradiation. A 300 W Xe arc lamp (LTIC 300BF, Boyi Ltd, China) was used as the light source with a 420 nm cutoff filter. In every experiment, 0.1g of catalyst was immersed in a 250 mL Pyrex beaker with 100 mL of RhB solution (5 mg/L). In order to ensure adsorption/desorption equilibrium between RhB and the photocatalyst, the suspension was stirred in the dark for 1h. As for the photocatalytic reactions, 3 mL of the suspensions was taken out at given time intervals and centrifuged to remove the photocatalyst particles. The concentrations of the centrifuged RhB solutions were monitored using a UV-Vis 8500 spectrophoto-meter (Shanghai Tianmei Science Apparatus Ltd. Co. China).

### 3. Results and Discussion

3.1. Structural and Morphological Characterization. The XRD patterns of as-prepared samples are shown in Figure 1. All strong peaks can be indexed to a pure cubic phase of BSO (JCPDS no. 87-0284). No other peaks can be observed, indicating high purity of the final products. The average sizes of the crystallite estimated using the Scherrer equation from (222) crystal plane of pyrochlore phase at  $2\theta = 28.8^{\circ}$  are 13.5 and 10.2 nm for BSO and C-BSO, respectively. Compared with the BSO sample, the diffraction peak intensity of the C-BSO nanoparticles is weak and broad. This implies that the crystallite size of C-BSO catalyst is smaller than that of the BSO catalyst.

The IR spectrum of the BSO and C-BSO samples, recorded in the range  $400-4000\,\mathrm{cm}^{-1}$ , is shown in Figure 2. Subramanian et al. have reported the infrared spectra of the pyrochlore oxides and demonstrated that the band at about  $600\,\mathrm{cm}^{-1}$  was from the B-O stretching vibration in the BO<sub>6</sub>

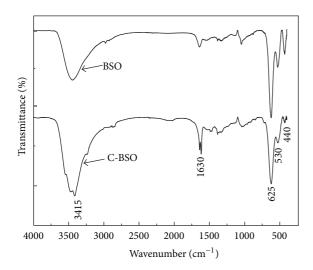


FIGURE 2: IR spectrum of the as-prepared BSO and C-BSO samples.

octahedron and the A-O stretching vibration of pyrochlore  $A_2B_2O_7$  centered at about  $500\,\mathrm{cm}^{-1}$  [27]. Similar results are obtained by the previous present work. It can be seen clearly that the main band at about  $625\,\mathrm{cm}^{-1}$  is assigned to the Sn-O stretching vibration while the weak bands of  $440\,\mathrm{cm}^{-1}$  and  $530\,\mathrm{cm}^{-1}$  are ascribed to Bi-O-Bi bonds vibrations [28]. The bands centered at about  $3415\,\mathrm{cm}^{-1}$  and  $1630\,\mathrm{cm}^{-1}$  are assigned to O-H stretching and bending modes of water, respectively [29].

The morphology of BSO and C-BSO is characterized by SEM as shown in Figure 3. Figure 3(a) shows the BSO samples which consist of a large number of microspheres, indicating that highlield of products can be readily achieved through this approach. Figure 3(b) shows the SEM image of the C-BSO photocatalyst; it can be seen that the irregular lumps and particles are relatively dispersed. The size of the as-prepared BSO nanoparticles is in the range of 8–20 nm (Figure 3(a)). After modification by CTAB, the size of the C-BSO sample has slightly changed. The mean mesopore size is about 10–15 nm, which is consistent with the pore size calculated from N2 isotherms.

The high-magnification TEM images of the BSO and C-BSO samples are shown in Figure 4. Figure 4(a) displays various specifications block-like morphology with sizes of 8–20 nm. Figure 4(b) shows irregular spherical-like morphology of C-BSO, and the sizes of C-BSO are only slightly smaller than BSO sample. Clearly, the size of the assynthesized C-BSO is smaller than BSO. This phenomenon is consistent with the typical crystallite sizes calculated from XRD results.

 $3.2.\ N_2$  Adsorption/Desorption Isotherm Analysis. The  $N_2$  adsorption-desorption isotherms and pore size distributions of BSO and C-BSO are determined by BET and BJH methods (shown in Figure 5). The isotherms of all the two samples are of classical type IV, characteristic of mesoporous materials according to the IUPAC. The result indicates that the BET surface area of nanosized BSO samples increased, from 45.3

to 71.9  $\rm m^2/g$ , accompanied with the increase of pore volumes from 0.11 to 0.18  $\rm m^2/g$ . The pore size distribution curves of BSO and C-BSO determined by BJH method from the absorption branch of the isotherms exhibit one single narrow peak centered at 12.7 nm, indicating the good homogeneity of the pores.

3.3. UV-Vis Diffuse Reflectance Spectra. Figure 6 shows the diffuse reflectance spectra of the BSO and C-BSO samples. It is clearly visible from the spectra that the absorption edge of C-BSO gets further shifted to the visible region comparing to the BSO sample. The band gap absorption edges of the BSO and C-BSO are measured to be 450 nm (2.76 eV) and 464 nm (2.67 eV), respectively. Such differences may be ascribed to the changes of crystallite phase and the size of coupled oxides, defects, and so on [30]. In this work, we believe that C-BSO photocatalyst, with its long wavelength absorption band, is an attractive photocatalyst for pollutant. The narrower band gap of C-BSO photocatalyst not only benefits the absorption of more photons in sunlight, but also promotes the excitation of photogenerated electrons from the valence band (VB) to the conduction band (CB), which may make the photocatalyst with high photocatalytic activity.

3.4. Photocatalytic Activity of BSO and C-BSO Nanocomposites under Visible Conditions. The photocatalytic performance of BSO and C-BSO is compared and presented in Figure 7, where C and  $C_0$  represent the time-dependent concentration and the initial concentration of pollutants solution, respectively. The blank test exhibits extremely low photodegradation efficiency in the absence of a photocatalyst under visible-light irradiation. The decrease of RhB concentration in the presence of BSO under visible light is about 51.0% after six hours of illumination. It can be found that the photodegradation efficiency of BSO assisted with CTAB decreases with the increase of CTAB amounts. However, their photocatalytic efficiency can be significantly improved compared with the sample without CTAB. 0.3 mmol C-BSO product exhibits better photodegradation activity than 1.5 mmol C-BSO photocatalyst, with the RhB concentration reduced as much as 97.8% under the same condition.

3.5. Effect of CTAB Assistance. As an efficient sorbent material, supramolecular assemblies (hemimicelles/admicelles) are formed from adsorption of surfactants on the surface of metal oxides. Attractive electrostatic interactions between the head group of ionic surfactants and oppositely charged groups on the oxide lead to the formation of monolayers of adsorbed surfactant termed hemimicelles. After saturation of the oxide surface, hydrophobic interactions between hydrocarbon chains of surfactant molecules lead to the formation of admicelles [31]. In term of hemimicelles, the hydrophobic tails are exposed to aqueous solution, so that the surfactantcoated oxide surface will become hydrophobic, which contributes to the adsorption of nonionic organic compounds onto the adsorbents [32]. Owing to the possession of higher special areas and more ion-exchangeable OH groups on surface, BSO materials have obvious advantage for the sorption

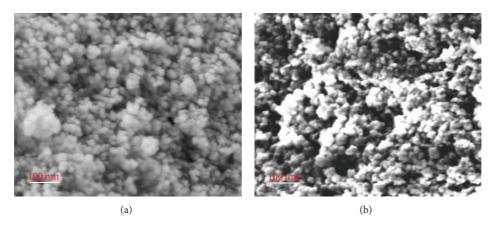


FIGURE 3: SEM images of as-prepared samples, (a) BSO sample and (b) C-BSO sample.

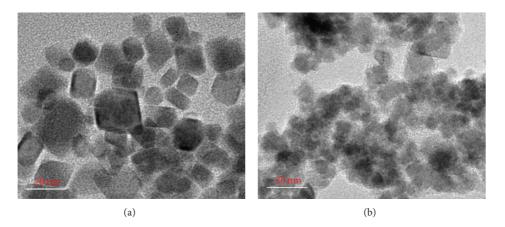
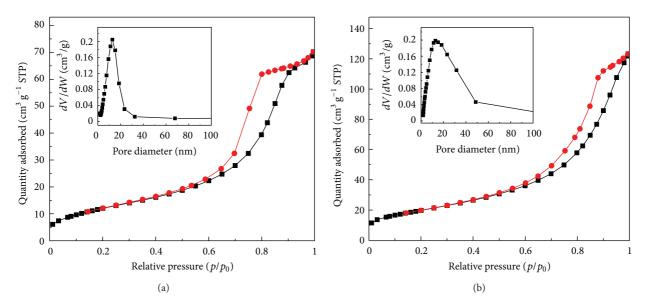


FIGURE 4: TEM images of (a) BSO sample and (b) C-BSO sample.



 $FIGURE \ 5: The \ N_2 \ sorption \ is otherms \ and \ pore \ width \ distribution \ of \ as-synthesized \ samples \ and \ (a) \ BSO, \ (b) \ C-BSO \ sample.$ 

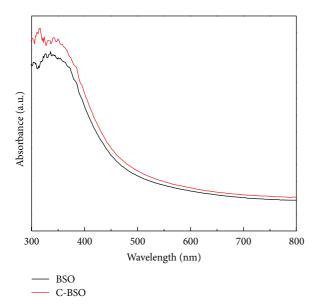


FIGURE 6: UV-Vis diffuse reflectance spectra of BSO and C-BSO samples.

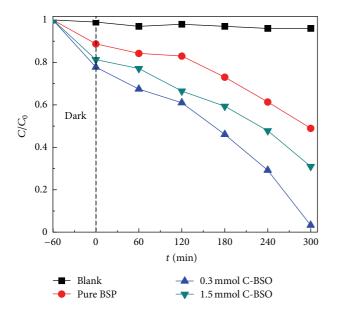
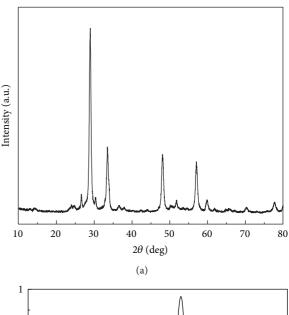


FIGURE 7: Degradation curves of RhB over as-prepared nanoparticles.

of ionic surfactant and have remarkable adsorption capability to organic compounds correspondingly [33]. Therefore, as shown in Figure 7, the nanomaterials BSO prepared by using CTAB are advantageous in photocatalytic reaction.

3.6. Reasons for Enhanced Efficiency of Photocatalysts. The photocatalytic activity of pyrochlore BSO is strongly influenced by its phase structure, crystallite size, and specific surface area [25]. From the XRD results, the phase structure of BSO did not change before and after using CTAB and retained the good crystallization. The crystallite size of BSO decreased from 13.5 nm to 10.2 nm after using CTAB, which



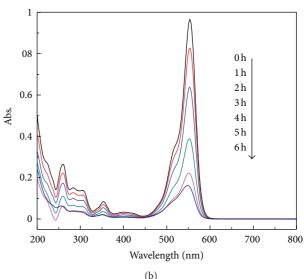


FIGURE 8: (a) XRD patterns of C-BSO-cal; (b) photocatalytic activities of RhB of C-BSO-cal product.

may be good for the enhancement of their photocatalytic performance. Moreover, the sample prepared with CTAB exhibited larger surface area (71.9 m²/g) than the reference BSO (45.3 m²/g). As the specific surface area and pore volume increased, it could result in the transition of band electron indirectly and the enhancement of the generation rate of photogenerated carriers [34]. Therefore, it also can be concluded that the surface area and pore structure of this sample played an important role in its degradation efficiency for wastewater. Moreover, another factor may be the existence of impurity level which could give rise to the shift of absorption edge to the long wavelength side and thus improves photocatalytic efficiency.

In order to test the previous assertion, the C-BSO is calcined at 600°C for 2 h to remove the impurity level (labelled as C-BSO-cal). The XRD pattern of C-BSO-cal (Figure 8(a)) reveals that the C-BSO-cal has the same phase as the C-BSO. The BET surface area of the C-BSO-cal is much smaller

than that of the C-BSO, which can respond for the decline of photocatalytic efficiency of the C-BSO-cal. The photocatalytic efficiency of the C-BSO-cal is presented in Figure 8(b). Obviously, only about 85.1% of RhB is degraded after 6 h of irradiation. It can be attributed to the elimination of impurity level by calcination that affects the removal efficiency of RhB.

### 4. Conclusions

In conclusion, nanoscale BSO could be conveniently synthesized by a CTAB assisted hydrothermal process at the temperature 180°C for 24 h. The experimental results show that adding CTAB into the synthesis system resulted in excellent dispersivity of lumps blocks and particles spheres with irregular shapes. BET surface area and pore volume of C-BSO are higher than those of BSO sample. Moreover, the photocatalytic activity of C-BSO is two times that of the reference BSO. The results demonstrate that the excellent photocatalytic activity of C-BSO stems from the efficiency of electron-hole pairs separation rate and the existence of impurity levels in C-BSO crystals.

### Acknowledgment

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### Research Article

### Enhancement of Photocatalytic Activity on TiO<sub>2</sub>-Nitrogen-Doped Carbon Nanotubes Nanocomposites

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 ${
m TiO_2}$ -nitrogen-doped carbon nanotubes ( ${
m TiO_2}$ -CNx) nanocomposites are successfully synthesized via a facile hydrothermal method. The prepared photocatalysts were systematically characterized by X-ray diffraction (XRD), scanning electron microscopy (SEM), transmission electron microscopy (TEM), and thermogravimetric and differential scanning calorimetry analyses (TGA-DSC). The results show that the  ${
m TiO_2}$  nanoparticles with a narrow size of 7 nm are uniformly deposited on CNx. The photocatalytic activity of the nanocomposite was studied using methyl orange (MO) as a model organic pollutant. The experimental results revealed that the strong linkage between the CNx and  ${
m TiO_2}$  played a significant role in improving photocatalytic activity. However, the mechanical process for CNx and  ${
m TiO_2}$  mixtures showed lower activity than neat  ${
m TiO_2}$ . Moreover,  ${
m TiO_2}$ -CNx nanocomposites exhibit much higher photocatalytic activity than that of neat  ${
m TiO_2}$  and  ${
m TiO_2}$ -CNTs nanocomposites. The improved photodegradation performances are attributed to the suppressed recombination of electrons and holes caused by the effective transfer of photogenerated electrons from  ${
m TiO_2}$  to CNx.

### 1. Introduction

Photocatalysis has been widely applied as a technique of destruction of organic pollutants due to its high performance, low cost, nontoxicity, stability, and availability [1, 2]. Titanium dioxide ( $\mathrm{TiO}_2$ ), a semiconductor with direct bandgap of 3.2 eV, has excellent photocatalytic properties and chemical stability, and it is an environmentally friendly and abundant substance [3, 4]. However, a major limitation to achieve high photocatalytic efficiency is the quick recombination of photogenerated charge carries [5]. Recombination has faster kinetics than surface redox reactions and greatly reduces the quantum efficiency of photocatalysis. Therefore, currently a particularly attractive option is to design and develop hybrid materials based on  $\mathrm{TiO}_2$  to solve this problem.

Recently, carbon-based nanomaterials, such as carbon nanotubes (CNTs) and graphene, have been reported as the hybrid component to be incorporated into  ${\rm TiO_2}$  due to their unique electrical properties, superior chemical stability,

and good conductivity. The common approaches to synthesize  ${\rm TiO_2}$ -CNTs composites include sol-gel method [6, 7], chemical vapor deposition (CVD) [8, 9], and electrospinning [10]. Various structural forms of titania-carbon nanotubes photocatalysts have been prepared, such as  ${\rm TiO_2}$  nanoparticles on CNTs [11],  ${\rm TiO_2}$  layer coating on aligned CNTs arrays [12], CNTs incorporating into the  ${\rm TiO_2}$  film [13],  ${\rm TiO_2}$  layer coating on CNTs [14], and low loading amounts of CNTs embedded inside mesoporous  ${\rm TiO_2}$  aggregates [15]. Cong et al. [16] have prepared uniform and fine well-dispersed carbon-doped  ${\rm TiO_2}$  coating on multiwalled carbon nanotubes by oxidation of titanium-carbide-(TiC-) coated CNTs, and the prepared carbon-doped  ${\rm TiO_2}$  coating on CNTs shows a higher visible light photocatalytic activity.

However, to fabricate the  $TiO_2$ -CNTs composites, the CNTs required a pretreatment process to modify their inert surface nature via harsh processes for activation by refluxing in concentrated acids, which destroys the  $\pi$  conjugation and reduces the conductance of the CNTs base [17]. Unfavorably,

the harsh process would risk CNTs to some damages in their inherent properties. To bypass the drawbacks suffered by CNTs, employing CNx without requiring any pretreatment to composite with the functional materials directly is a promising method because the nitrogen atoms on the surface of the CNTs modify the adsorption strength of the nanotubes towards foreign elements. Moreover, nitrogen atoms in the framework of CNx will form chemically active points which are available for metal or metallic oxide nanoparticles anchoring. Ghosh and coworkers [17] prepared ZnO/CNx composites via a simple wet-chemical method and studied their field emission performance. CNx decorated with CeO<sub>2</sub> and SnO<sub>2</sub> nanoparticles showed greater activity and sensitivity than the conventional CNT-based composites for NO electrooxidation [18].

In this work, according to the unique properties of CNx, we have synthesized  ${\rm TiO_2}$ -CNx nanocomposites with different weight ratios via a facile hydrothermal method. The resulting materials were well characterized for their physicochemical properties, structural features, as well as potential applications to the photodegradation of MO.

### 2. Experimental

2.1. Synthesis of  $TiO_2$ -CNx. Following the procedures reported previously [19], CNx was synthesized using diethylamine as the carbon and nitrogen source. The purification process for CNx was as follows: CNx was firstly washed three times by 20% HF solution, then soaked in 20% HF solution overnight, gathered by filtration, and finally dried at 80°C for 2 h

TiO2-CNx nanocomposites were prepared using a hydrothermal synthesis method. CNx was added to provide a weight ratio of TiO<sub>2</sub> over CNx in the range from 5% to 20%, indicated with X wt% TiO<sub>2</sub>-CNx. CNx was initially dispersed into a 30 mL solution containing 2.7 mL water and 27.3 mL isopropanol, and the suspension was treated by sonication overnight. Then the titanium precursor solution, 3.41 mL titanium isopropoxide in 18 mL isopropanol was added dropwise into the CNx suspension under vigorous stirring. The mixture was left at room temperature under stirring for 2 h to complete the hydrolysis reaction. The mixed solution was then transferred into a teflon-lined stainless-steel autoclave (50 mL capacity). The autoclave was maintained at 140°C for 24 h and then cooled down to room temperature. The resulting solid was washed with ethanol and deionized water, gathered by filtration, and subsequently dried at 80°C overnight. The TiO2-CNx solids were ground into powder and stored in a dessicator for further usage. For comparison, TiO<sub>2</sub>-CNTs composites were synthesized using the similar procedures besides CNTs pretreated in concentrated HNO<sub>3</sub> at 140°C for 14 h, and neat TiO2 sample was synthesized without adding CNTs.

2.2. Characterization. The bare CNx and the composites were characterized by a wide range of analytical techniques. The degree of crystallinity of the  $TiO_2$ -CNx composites was characterized by powder X-ray diffraction (XRD). The XRD patterns with diffraction intensity versus  $2\theta$  were recorded

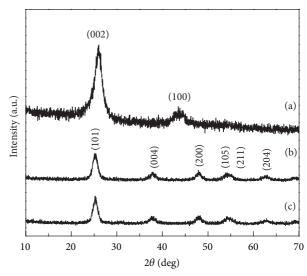


FIGURE 1: XRD patterns of bare CNx (a) and TiO<sub>2</sub>-CNx composites with different weight ratio of TiO<sub>2</sub> over CNx 5% (b) and 20% (c).

in a Bruker D8 ADVANCE instrument with Cu-Ka radiation ( $\lambda=1.5418~\text{Å}$ ) from 20° to 70° at a scanning speed of 2°/min. X-ray tube voltage and current were set at 40 kV and 40 mA, respectively. Thermogravimetric and differential scanning calorimetry analyses (TGA-DSC) were performed by a Netzsch STA-449C analyzer with a heating rate of 10° C/min and an air flow rate of 100 mL/min. Scanning electron microscopy (SEM) was carried out on Hitachi S-4800 with an acceleration voltage of 5 kV. Transmission electron microscopy (TEM) was carried out on JEOL-JEM-1005 at 200 kV. The specimens for SEM and TEM imaging were prepared by suspending solid samples in ethanol with 15 min ultrasonication and placing a drop of this mixture on a 3.05 mm diameter copper mesh, which was then dried in air.

2.3. Photodegradation of MO. The photoreactor was designed with a cylindrical quartz cell configuration and an internal light source surrounded by a quartz jacket, where MO aqueous solution completely surrounded the light source. An external cycled cooling flow of water was used to maintain the reaction temperature constant.

Photocatalytic experiments were carried out by adding  $0.01\,\mathrm{g\,TiO_2}$  or  $\mathrm{TiO_2}$ -CNTs composites or  $\mathrm{TiO_2}$ -CNx composites into photoreactor containing 30 mL MO solution with an initial concentration of 15 mg/L. The mixture was stirred for 30 min in the dark to favor the adsorption equilibration, and then the stirred suspensions were illuminated with a 300 W high-pressure mercury lamp 10 cm high over the solution. The solution was stirred continuously during the photocatalytic reaction. The concentration of MO was analyzed by recording the absorption band maximum at 464 nm in the absorption spectra, using Shimadzu UV-2550 spectrophotometer

### 3. Results and Discussion

The XRD patterns of the bare CNx and  ${\rm TiO_2}$ -CNx nanocomposites are shown in Figure 1. The main peaks at 26.1° and

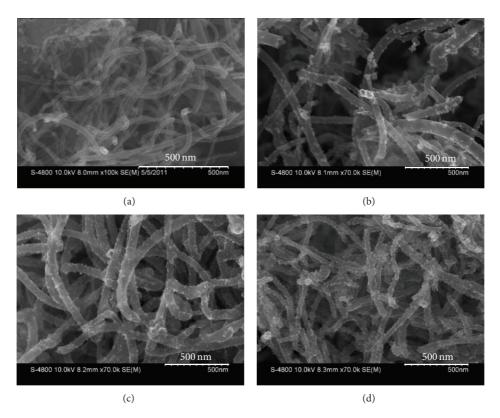


FIGURE 2: SEM images of bare CNx (a), TiO<sub>2</sub>-CNx composites with different weight ratio of TiO<sub>2</sub> over CNx 5% (b), 10% (c), and 20% (d).

42.6° corresponded to the (002) and (100) reflections of CNx, respectively, (JCPDS 41-1487), which indicated that the employed CNx was highly graphitized (Figure 1(a)). It is obvious that the  $\rm TiO_2$ -CNx nanocomposites show the same characteristic diffraction peaks referred to as anatase  $\rm TiO_2$  (JCPDS number 21-1272). The characteristic peaks at  $2\theta$  of 25.3, 37.8, 48.0, 53.9, 55.1, and 62.7° can be indexed to (101), (004), (200), (105), (211), and (204) crystal planes of anatase  $\rm TiO_2$ , respectively. Notably, no typical diffraction peaks belonging to the separate CNx are observed in the  $\rm TiO_2$ -CNx nanocomposites. The reason can be ascribed to the fact that the main characteristic peak of CNx at 26.1° might be shielded by the main peak of anatase  $\rm TiO_2$  at 25.3°.

Figures 2 and 3 show the SEM and TEM images of bare CNx and TiO<sub>2</sub>-CNx composites. CNx with relatively outer diameter (30~60 nm) was obtained, and the nanomaterial has a bamboo-like morphology with a clear, smooth surface. It is clearly seen that, for TiO<sub>2</sub>-CNx nanocomposites, the TiO<sub>2</sub> nanoparticles are almost uniformly deposited on the surface of CNx. The more weight ratio of TiO<sub>2</sub> over CNx, the more visible nanoparticles observed (Figures 2(b), 2(c), and 2(d)). Figure 3(b) is TEM image of an individual CNx fully coated with TiO<sub>2</sub> nanoparticles. The bamboo-like morphology of CNx can be also clearly observed, and its surface is entirely and homogeneously covered by TiO2 nanoparticles. There are no clear boundary and vacant space between the TiO2 coating and CNx substrate. The nanoparticles covered on the CNx show clear crystal lattice fringes (Figure 3(c)). The intimate contact between CNx and TiO<sub>2</sub> favors the formation

of junctions between the two materials, as a result, being helpful for improving the charge separation and thus the photocatalytic activity. As estimated from the TEM images, the size of TiO<sub>2</sub> nanoparticles is about 7 nm. EDX spectrum presented in Figure 3(d) further determined the existence of Ti and O atoms.

TGA-DSC analysis was carried out to estimate the carbon nanotube content of the nanocomposite. The results of weight loss and heat flow as a function of temperature for TiO2-CNx nanocomposites are shown in Figure 4. For the 5 wt% and 15 wt% TiO<sub>2</sub>-CNx nanocomposites, the weight loss due to the combustion of the CNx was 93.5% and 83.8%, respectively, indicating that TiO<sub>2</sub>/CNx ratios estimated from the synthesis precursors of the nanocomposites were in close agreement with the results obtained from TGA-DSC analyses. Therefore, negligible losses of CNx occurred during the composite preparation procedure. The combustion point of CNx in the 15 wt% TiO<sub>2</sub>-CNx composite was found to be 544.3°C, whereas CNx in 5 wt% TiO2-CNx composite could not be combusted until approximately 647.6°C. The combustion temperature shift between different TiO<sub>2</sub>/CNx ratios may be ascribed to the following two reasons: (i) more amount of TiO<sub>2</sub> grafted on the sidewall of CNx may provide more oxygen required by the combustion of CNx and (ii) more amount of TiO<sub>2</sub> restrains the heat transfer creating localized hot spots, facilitating the oxidation of carbon.

Figure 5 shows the results of the decomposition of MO under irradiation, in the presence of neat TiO<sub>2</sub>, TiO<sub>2</sub>-CNTs, and TiO<sub>2</sub>-CNx nanocomposites with different weight

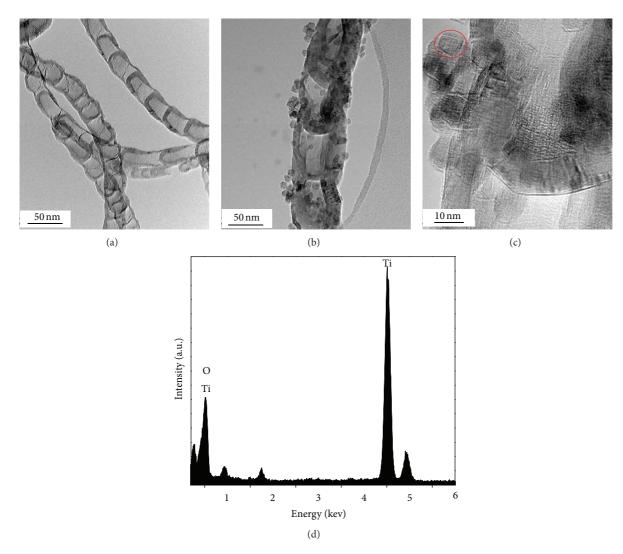


FIGURE 3: TEM images of bare CNx (a), low-magnification TEM image (b), high-magnification TEM image (c), and EDS spectrum of 10 wt%  ${\rm TiO_2}$ -CNx composites (d).

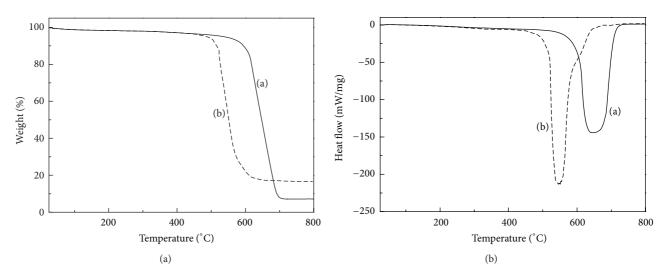


Figure 4: TG and DSC curves of  $TiO_2$ -CNx composites with different weight ratio of  $TiO_2$  over CNx 5% (a) and 15% (b).

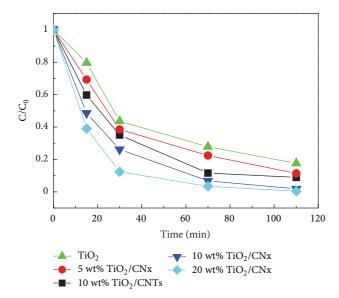


FIGURE 5: Comparison of photocatalytic activity between different photocatalysts.

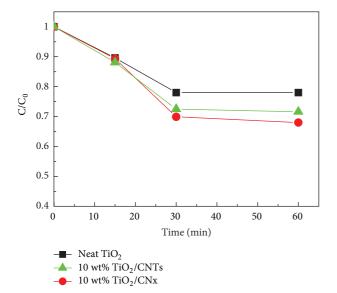


FIGURE 6: Influence of adsorption time on the remaining fraction of MO ( $C/C_0$ ) by neat  $TiO_2$ , 10 wt%  $TiO_2$ -CNTs composites, and 10 wt%  $TiO_2$ -CNx composites.

ratios. Control experiments showed that UV irradiation with no catalyst and catalyst (composite or bare CNx) without irradiation could not degrade MO dye solutions. When  ${\rm TiO_2}$  photocatalyst is used, the degradation efficiency is calculated to be 82.4% at 110 min. When CNTs is introduced, the degradation efficiency is increased to 91.1% for 10 wt%  ${\rm TiO_2}$ -CNTs composites and reaches the maximum value of 99.6% for 20 wt%  ${\rm TiO_2}$ -CNx composites at 110 min. It is noteworthy that  ${\rm TiO_2}$ -CNx composites show superior activity to  ${\rm TiO_2}$ -CNTs composites with the same  ${\rm TiO_2}$  weight ratio. With the reaction time at 110 min, the MO degradation efficiency of 10 wt%  ${\rm TiO_2}$ -CNTs catalysts is about 91.1%. However, the

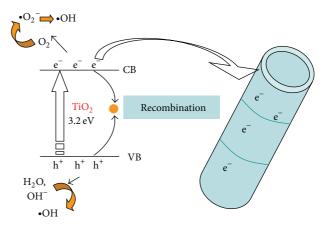


FIGURE 7: Schematic diagram showing band configuration and electron-hole separation at interface of  ${\rm TiO_2}$ -CNx nanocomposites under UV irradiation (CB: the bottom of conduction band, VB: the top of valence band).

value of 10 wt% TiO<sub>2</sub>-CNx is 98.2%. Hence, TiO<sub>2</sub>-CNx is an excellent photocatalyst in our experiment.

It has been reported that high adsorption capacities of photocatalysts can lead to the rapid diffusion of MO molecules from solution to the surface of photocatalysts and thus improve photocatalytic performances [20]. Figure 6 shows the remaining fraction of MO  $(C/C_0)$  in solution during adsorption for 60 min in dark by neat TiO2, TiO2-CNTs composites and TiO<sub>2</sub>-CNx composites. It is obvious that three photocatalysts exhibited adsorption capacities for MO molecules in the following order: 10 wt% TiO<sub>2</sub>-CNx >  $10 \text{ wt}\% \text{ TiO}_2\text{-CNTs} > \text{TiO}_2$ . The improved adsorption capacity of 10 wt% TiO2-CNx is attributed to its larger specific surface area of 150.25 m<sup>2</sup>/g than these of 10 wt% TiO<sub>2</sub>-CNTs  $(128.26 \text{ m}^2/\text{g})$  and neat  $\text{TiO}_2$   $(85.49 \text{ m}^2/\text{g})$ . It is noteworthy that the concentration of MO molecules shows negligible change after 30 min, indicating the adsorption equilibration. So the adsorption is not the main reason for the improvement of photocatalytic activity in our experiment because the mixture was stirred for 30 min in advance. The enhancement of the photocatalytic performance should be mainly ascribed to the promotion of separation rate of photogenerated electron and hole by the formation of heterostructure, as shown in Figure 7.

Under UV irradiation, the valence band electrons of TiO<sub>2</sub> can be excited to its conduction bands, giving rise to high-energy electron-hole pairs. Compared with CNTs, CNx has a high degree of defects introduced by nitrogen doping [21]. When the electrons generated by TiO<sub>2</sub> transfer into CNx, it could be used as a larger capacity container of electron in comparison with the usual CNTs. So the separation efficiency of electron-hole pairs improved, leading to the dramatically enhanced photoactivity. Moreover, compared to carbon, nitrogen has an extra electron, and from an electronic point of view it is natural to expect an excess of donors in the N-rich areas of the CNTs upon doping [22, 23]. That is to say, impurities significantly enhanced the CNx metallic/conductive character [24]. Hence, the rapid transferring of

electron enhanced separation rate of photogenerated electron and hole.

In order to further explore the effect of the interphase linkage, a mechanical mixture of CNx and TiO<sub>2</sub> was prepared. The composition of the mixture was prepared with the same ratio as that in 10 wt% TiO<sub>2</sub>-CNx nanocomposites. The photocatalytic activity of the mixture photocatalyst was 76.4% at 110 min, much lower than that of 10 wt% TiO<sub>2</sub>-CNx nanocomposites (98.2%). The low activity is ascribed to CNx in the photocatalyst not being effective in trapping electrons. This lack of effectiveness prevents a decrease in recombination rate. In the mechanical mixture, it is possible that the mechanical mixture process cannot form a strong interphase between the TiO2 and the CNx. In contrast, a strong interphase was formed in TiO<sub>2</sub>-CNx composites, as evidenced by the previous analysis. Therefore, TiO2-CNx composites showed high activity. Moreover, CNx was almost inactive during MO degradation by UV light irradiation. Once CNx became incapable of bonding strongly with TiO<sub>2</sub>, they simply occupied the active sites and scattered the incident light. Therefore, the hydrothermal synthesis procedure is a critical factor in forming high-activity TiO2-CNx nanocomposites photocatalysts.

### 4. Conclusions

In this work, we have synthesized uniformly dispersed  $TiO_2$  on the surface of CNx via a hydrothermal synthesis method. The nanocomposites showed excellent photocatalytic activity compared with neat  $TiO_2$  and  $TiO_2$ -CNTs. The rapid transferring of electron and high separation efficiency of electronhole pairs lead to the dramatically enhanced photocatalytic activity. According to the activity and characterization results, the interphase linkage of  $TiO_2$  and CNx is a critical factor for promoting photocatalysis. A mechanical mixture cannot provide strong binding between  $TiO_2$  and CNx, thus showing decreased activity.

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### Research Article

## Effect of Different Calcination Temperatures on the Structural and Photocatalytic Performance of Bi-TiO<sub>2</sub>/SBA-15

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The new novel material Bi-TiO<sub>2</sub>/SBA-15 was synthesized by an easy wet impregnation method. A combination of XRD, XPS, Raman,  $N_2$  adsorption-desorption isotherm measurement, TEM, and solid state UV-Vis spectroscopy has been used to characterize the Bi-TiO<sub>2</sub>/SBA-15 material. It was found that SBA-15 retained the ordered hexagonal mesostructure after incorporation of TiO<sub>2</sub> and Bi. The photodecomposition of rhodamine B (RhB) in aqueous medium was selected to evaluate the photocatalytic performance of Bi-TiO<sub>2</sub>/SBA-15 under visible light irradiation ( $\lambda \ge 420$  nm). The experiment results indicated that Bi-TiO<sub>2</sub>/SBA-15 exhibited higher photocatalytic activities than pure TiO<sub>2</sub> and Bi<sub>2</sub>O<sub>3</sub>. The influences of calcination temperature were studied. It strongly influenced the activity of the samples. The sample calcined at 550°C shows the highest photocatalytic activity in the decomposition of RhB under visible light. The catalyst preserved almost its initial photocatalytic activity after six reuses.

### 1. Introduction

The photocatalytic properties of TiO<sub>2</sub> have been exploited in various applications since Fujishima and Honda reported a TiO<sub>2</sub> photochemical electrode for splitting water in 1972 [1]. TiO<sub>2</sub> is regarded as the most promising one for its high photocatalytic activity, chemical/photocorrosion stability, low cost, and environmental friendiness. However, the large band gap of TiO<sub>2</sub> (3.20 eV) and low quantum efficiency restricts its wide application [2]. This factor can be minimized by doping of semiconductors such as WO<sub>3</sub>, Bi<sub>2</sub>O<sub>3</sub>, and CdS, which could change the electronic properties of TiO<sub>2</sub> [3–5]. Among them, Bi-based photocatalysts (Bi<sub>2</sub>O<sub>3</sub> or its related compounds) have attracted much attention. Bi<sub>2</sub>O<sub>3</sub> (2.8 eV) exhibits good charge carrier mobility, in which species with lone electron pair forming Bi-O polyhedra can act as electron trapping centers and hinder electron-hole pair recombination to improve the photoabsorptivity and photocatalytic activity

Recently, there are several works on the photocatalytic properties of Bi-doped  $TiO_2$  materials under visible light irradiation [8–10]. Hou et al. used  $Bi_2O_3$  quantum dots to

enhance the photoactivity of TiO<sub>2</sub> nanosheets with exposed (001) facets [11]. Di Camillo et al. reported that Bi-doped TiO<sub>2</sub> NFs have been deposited by electrospinning and showed very interesting photocatalytic properties [12]. Su et al. synthesized a new TiO2-based photocatalyst with both B doping and Bi<sub>2</sub>O<sub>3</sub> coupling (Bi<sub>2</sub>O<sub>3</sub>/TiO<sub>2-x</sub>B<sub>x</sub>). The catalyst was used in degrading pentachlorophenol under visible light ( $\lambda$  > 420 nm) irradiation [13]. Li et al. reported the preparation of highly monodisperse spherical Bi-doped TiO<sub>2</sub>. Their hybrid showed enhanced photocatalytic activity under visible light [14]. Shamaila et al. demonstrated an approach for the preparation of a mesoporous nanocrystalline TiO2 based on EISA method [15]. The catalyst showed the superior activity as compared to M-TiO2 (M refers to metal ion), Degussa P25, and impregnated Degussa P25 for the photodegradation of Methyl Orange (MO) and 2,4-dichlorophenol (2,4-DCP). Rengaraj and coworkers synthesized a Bi3+-doped TiO<sub>2</sub> nanocatalyst. According to their results, the presence of Bi species in TiO2 catalysts substantially enhanced the photocatalytic degradation of methyl parathion under UV irradiation [16].

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Generally, the present  $\rm Bi_2O_3$ - $\rm TiO_2$  composite photocatalysts were limited by the low adsorption ability. To address this issue, much effort has been focused on enhancing the adsorption ability of the catalysts to improve their photocatalytic performance. Well-ordered mesoporous silica materials such as MCM-41 and SBA-15 have been widely used for adsorption, separation and catalysis [17–20]. SBA-15 is a type of uniform hexagonal pores and high surface area mesoporous material. Such type of highly interconnected mesostructured porous material is expected to allow the guest species to access the opened porous host easily. Design of photocatalysts modified by SBA-15 is a promising way to enhance high photocatalytic activity. However, no studies have attempted to establish a system consisting of a  $\rm Bi_2O_3$ - $\rm TiO_2$  hybrid incorporated into mesoporous silica.

Herein, the aim of the present paper is to investigate the synthesis of size controlled Bi<sub>2</sub>O<sub>3</sub> and TiO<sub>2</sub> supported on mesostructured SBA-15. The photodegradation of RhB was employed to evaluate the photocatalytic activities of the Bi-TiO<sub>2</sub>/SBA-15, with a 300 W Xe lamp ( $\lambda \geq$  420 nm) as the light source.

Rhodamine B (RhB, N,N,N',N'-tetraethylrhodamine) has moderate wash and light fastness properties. It is a useful analytical reagent for the detection and determination of metals. However, the use of RhB as a food color has been discontinued for a number of years on account of its suspected carcinogenic nature. Therefore, the removal of these dyes from wastewater is of great concern. Based on these considerations, the photodecomposition of RhB in aqueous medium was selected to evaluate the photocatalysis performance of Bi-TiO<sub>2</sub>/SBA-15.

Considering the different calcination temperatures having an influence on the photocatalytic performance, the activities on different calcination temperatures were tested and discussed. Moreover, the recycle ability of Bi-TiO $_2$ /SBA-15 was also evaluated.

#### 2. Experimental

2.1. Catalyst Preparations. The SBA-15 was prepared according to the previous procedure by reaction from a solution of triblock copolymer P123 (EO<sub>20</sub>PO<sub>70</sub>EO<sub>20</sub>, Aldrich) and tetraethoxysilane (TEOS) [21, 22]. P123 was used as a structure directing agent. In a typical process, 2 g of P123 was added to 75 mL of aqueous HCl under stirring at 40°C for 2 h. 4.17 mL of TEOS was then added to the solution which was stirred for another 24 h. The suspension was transferred into a steel autoclave and kept at 100°C for 72 h. After cooling to room temperature, the precipitate in the bottom of Teflon vessel was collected, filtered, thoroughly washed with water to remove any unreacted chemicals, and dried at room temperature. Calcinations were performed by heating in air at 550°C for 6 h to remove the template.

 ${
m TiO_2/SBA-15}$  material was first prepared by internal hydrolysis method with little modification [23]. In this case, the calculated amount of tetrabutyl titanate (TBT) was dissolved in ethanol in a volume ratio of 1:5 (the amount of TBT is 0.92 mL). 0.5 g SBA-15 was then added to the solution containing TBT and stirred for 1 h to make the TBT adsorb

completely on the SBA-15. The condensation reaction was started by dropwise addition of water and then the stirring was continued for 2 h to hydrolyze TBT completely. The solid product was recovered by filtration, washed with ethanol to remove any unanchored titanium species, dried at  $80^{\circ}\mathrm{C}$  overnight, and calcined in air at  $550^{\circ}\mathrm{C}$  for 3 h. The calcined samples were designated as  $\mathrm{TiO_2/SBA-15}$ .

For Bi-doping  $TiO_2/SBA-15$  supports, samples containing Bi were prepared by an easy wet impregnation method.  $TiO_2/SBA-15$  and  $Bi(NO_3)_3 \cdot 5H_2O$  were mixed in an ethanol solution with a drop of  $HNO_3$  and stirred for 5 h, where the Bi/Ti molar ratio is 2.0%. The suspension was dried and calcined in air at different temperatures. The samples were designated as  $Bi-TiO_2/SBA-15(x)$ , where x refers to the calcination temperatures, which are  $400^{\circ}$ C,  $550^{\circ}$ C,  $700^{\circ}$ C, and  $850^{\circ}$ C, respectively.

2.2. Characterization Techniques. Small-angle X-ray diffraction (SAXRD) measurements were performed on a Siemens D5005 instrument with CuK $\alpha$  ( $\lambda = 0.154$  nm) radiation. The diffractograms were recorded in the  $2\theta$  range of  $0.5-5^{\circ}$  with a 29 step size of 0.01°. Wide-angle X-ray diffraction (WAXRD) measurements were carried out on an XRD-6000 X-ray diffractometer (Shimadzu) CuK $\alpha$  ( $\lambda = 0.154$  nm) radiation. The diffractograms were recorded in the 29 range of 10-80° with a 29 step size of 0.2°. Raman spectra were measured with JOBIN YVON HR800 Raman spectrophotometer (France) in the range of  $100-1400 \,\mathrm{cm}^{-1}$ , using an Ar ion laser. N<sub>2</sub> adsorption-desorption isotherms were measured at 77 K in a Quantachrome Autosorb-1 sorption analyzer. Samples were outgassed at 300°C for 10 h before the measurement. TEM was performed by an FEI Tecnai G2 S-Twin electron microscope with an acceleration voltage of 200 kV. XPS was obtained using a physical electronics model PHI5700 X-ray photoelectron spectrometer with MgK $\alpha$  X-rays as the excitation source. The binding energies were calibrated with reference to Cls at 285 eV. UV-V is absorption spectra scans were performed on a Shimadzu UV-2550 spectrometer in the range from 300 to 600 nm. BaSO<sub>4</sub> was used as a reflectance standard material during the experiment. Photoluminescence (PL) spectra were performed on JASCO FP-6500 fluorescence spectrometer.

2.3. Photocatalytic Activity Measurement. The photocatalytic activities were investigated for the photodegradation of RhB in aqueous solution under visible light in a photolysis glass reactor. The pH of solution was 7 during the reaction. The visible light source was a 300 W Xe lamp ( $\lambda \geq 420\,\mathrm{nm}$  to provide visible light irradiation) with a double wall jacket in which water was circulated to prevent overheating of the reaction mixture. 50 mg of Bi-TiO₂/SBA-15(x) was added to rhodamine B (RhB) (100 mL, 1 × 10<sup>-5</sup> M) and stirred for 30 min without visible light irradiation in order to establish an adsorption-desorption equilibrium between RhB and the catalyst. Next, the solution was illuminated by visible light. At a given time interval, 4 mL of the suspension was withdrawn. After centrifugation at 5000 rpm for 5 min, the filtrate was monitored by UV-Vis spectrophotometer (UV-5200).

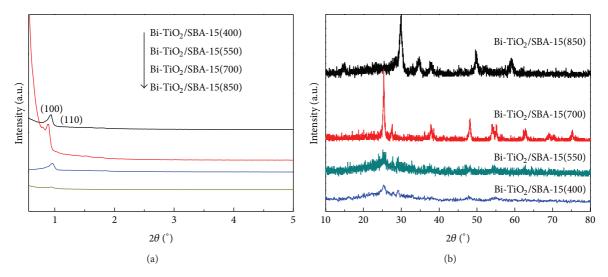


FIGURE 1: Small-angle (a) and wide-angle (b) XRD patterns of Bi-TiO<sub>2</sub>/SBA-15(x).

TABLE 1: Textural properties of Bi-TiO<sub>2</sub>/SBA-15(x).

Samples	Bi/Ti <sup>a</sup>	BET area (m <sup>2</sup> ·g <sup>-1</sup> )	$V_{\rm tot}^{}  ({\rm cm}^3 {\cdot} {\rm g}^{-1})$	D <sup>c</sup> (nm)
SBA-15	0	590.3	0.961	7.224
Bi-TiO <sub>2</sub> /SBA-15(400)	2.01%	540.1	0.544	5.936
Bi-TiO <sub>2</sub> /SBA-15(550)	1.95%	527.7	0.518	5.882
Bi-TiO <sub>2</sub> /SBA-15(700)	1.89%	299.5	0.307	5.767
Bi-TiO <sub>2</sub> /SBA-15(850)	1.62%	182.7	0.221	4.061
TiO <sub>2</sub> /SBA-15(550)	0	568.3	0.924	6.818

 $<sup>^{</sup>a}$ Bi/Ti was measured by ICP,  $^{b}V_{\text{tot}}$ : the total pore volume,  $^{c}D$ : average pore diameter.

### 3. Results and Discussions

3.1. Textural Properties and Characterization Typical. Small-angle XRD patterns of calcined Bi-TiO<sub>2</sub>/SBA-15(x) samples in the range of 0.5–5° were shown in Figure 1(a). All samples exhibit well-resolved diffraction peak at  $2\theta = 0.8$ -0.9° corresponding to the (100) diffraction peak of the hexagonal features of the SBA-15, indicating that their ordered pore structure is maintained well. The position of the diffraction peak shifted to a higher angle indicating a small decrease of the pore size and unit cell. It is seen that SBA-15 has a good thermal stability. The diffraction intensity gradually decreased with increasing the calcination temperature.

Figure 1(b) shows the wide-angle XRD pattern of the Bi-TiO $_2$ /SBA-15(x) calcined at different calcination temperatures. The XRD patterns of the samples evidenced that when the temperature is 400 and 550°C, a typical broad diffraction peak centered at 2 $\theta$  of 25°, which is typical characteristic of amorphous silica. No clear characteristic peaks of crystalline TiO $_2$  and Bi $_2$ O $_3$  were observed in XRD patterns of sample, which indicated that the small nanoparticle sizes of TiO $_2$  and Bi $_2$ O $_3$  were successfully incorporated into the silica framework. However, sample calcined at 700°C shows the appearance of anatase phase. It is observed that, with increase of calcination temperature, TiO $_2$  grain size increases. With further increase of calcination temperature to 850°C, a new

diffraction peak at  $2\theta = 30^{\circ}$  was observed in the XRD pattern, which might be due to the formation a new phase of Bi<sub>4</sub>Ti<sub>3</sub>O<sub>12</sub> at 850°C. It is indicated that the new phase gradually dominates the composition of the samples. So it is feasible to control the ratio of the anatase phases by varying the calcination temperatures. In addition, no significant diffraction peak of Bi species was observed regardless of the calcination temperature because of the higher dispersion of Bi and the low content of Bi.

The adsorption-desorption isotherms for Bi-TiO $_2$ /SBA-15 are shown in Figure 2(a). The samples exhibit isotherms of typical type IV with a H2 hysteresis loop due to the capillary condensation steps at relative pressure of 0.5 <  $p/p_0$  < 0.8, which is characteristic of a mesopores material [24, 25]. It can be clearly observed that the amount of N $_2$  adsorption decreases upon Bi $_2$ O $_3$  and TiO $_2$  addition. Such a decrease of N $_2$  adsorption for samples is reasonable, considering the formation of Bi $_2$ O $_3$  and TiO $_2$  nanoparticles inside the mesopores of SBA-15. When the calcination temperature increases to 850°C, the isotherm changes to H1 hysteresis loop. The hysteresis loop in the isotherms is obviously shifted to the high relative pressure, indicating that pore sizes of the samples decrease with the calcination temperature.

The BET specific area and the pore size of  $TiO_2/SBA$ -15 and  $Bi-TiO_2/SBA-15(x)$  were summarized in Table 1. The specific surface area, pore size, and volume decrease

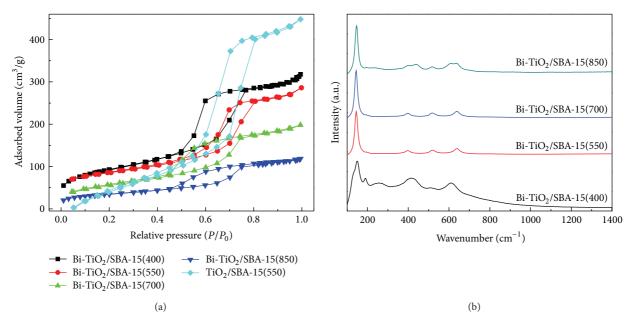


FIGURE 2: (a) N<sub>2</sub> adsorption-desorption isotherms of Bi-TiO<sub>2</sub>/SBA-15(x). (b) Raman spectra of Bi-TiO<sub>2</sub>/SBA-15(x).

with the calcination temperature increasing. Based on the observations, with the calcination temperature increasing, total pore volume and BET surface area were decreased 16.0% and 5.9% at least, respectively. It is clear that the increasing calcination temperature leads to decrease pore volume, specific surface area, and the porosity of the samples. Meanwhile, the increasing calcination temperature helps to increase the  ${\rm TiO}_2$  nanoparticles crystallization degree. We also noted that, when the temperature increased to 850°C, there was a mutation of the specific surface area, which was attributed to the new phase, obstructing the pores of the SBA-15.

Raman spectroscopy further verified the  ${\rm TiO_2}$  transformation for  ${\rm Bi\text{-}TiO_2/SBA\text{-}15}(x)$ , as shown in Figure 2(b). The Raman bands appear at 147, 400, 520, and 641 cm<sup>-1</sup> and can be assigned to the  ${\rm E_g}$ ,  ${\rm B_{1g}}$ ,  ${\rm A_{1g}}$ , and  ${\rm B_{1g}}$  vibration modes of anatase  ${\rm TiO_2}$  [26]. The results indicate that the doping of Bi has not influenced the anatase type of  ${\rm TiO_2}$ . A new peak appears at 200 cm<sup>-1</sup> when the calcination temperature was 400°C, which is attributed to the brookite phase. When the temperature is higher, the  ${\rm TiO_2}$  in brookite phase has been full conversion to anatase with improving the crystalline. When the calcination temperature is up to 850°C,  ${\rm TiO_2}$  is still in anatase phase in the samples with partial conversion to a new phase of  ${\rm Bi_4Ti_3O_{12}}$ . It is indicated that the introduction of Bi can inhibit the transformation of  ${\rm TiO_2}$  phase in the high temperature.

Figure 3 shows that it retains a regular hexagonal array of uniform channels characteristic of SBA-15 with Bi and  $\mathrm{TiO}_2$ . It displays highly ordered hexagonal regularity mesopores, where nanoparticles are embedded in the pore walls with random orientation. When the calcination temperature is up to 850°C, the nanocrystals structures do not change and slightly increased the nanoparticles size derived from XRD data. After the same treatment (up to 850°C), the crystal domain size of  $\mathrm{TiO}_2$  increased with partial conversion to

 ${\rm Bi_4Ti_3O_{12}}$  and that of  ${\rm Bi_2O_3}$  crystals increased with partial conversion to monoclinic modification.

HRTEM image (Figure 3(e)) reveals that the materials were well crystallized, as evidenced by well-defined lattice fringes. The lattice fringes of 0.35 nm match the (101) plane of anatase  ${\rm TiO_2}$ , while that of 0.325 nm match the (120) plane of  ${\rm Bi_2O_3}$  nanoparticles, respectively. The HRTEM analysis confirmed that  ${\rm Bi_2O_3}$  and  ${\rm TiO_2}$  coexisted in the resulting samples.

In order to analyze the chemical composition and purity of the prepared particles, the XPS survey spectrum of Bi-TiO<sub>2</sub>/SBA-15 is shown in Figure 4. Figure 4(a) shows that Bi-TiO<sub>2</sub>/SBA-15 contains only Ti, O, Bi, Si, and C elements. The C element can be ascribed to the residual carbon from our characterization. The high-resolution XPS spectra of Bi4f are shown in Figure 4(b). The peaks of Bi 4f7/2 and Bi 4f5/2 are centered at 159.3 and 164.5 eV, which is in agreement with Bi<sub>2</sub>O<sub>3</sub> values of other observations [27, 28]. After calcinations at higher temperature, these two peaks move a little to lower energies, hinting that bismuth element brings more effective positive charge and tends to convert to its stable oxidation state from +3 to 0. The Bi species would segregate from the shallow surface and move onto the photocatalyst surface, and some Bi<sup>0</sup> species are oxidized into Bi<sup>3+</sup> species. This means that calcination may lead to more Bi<sub>2</sub>O<sub>3</sub> species formed and to segregation on photocatalyst surface. A weak signal centred at 157.2 eV indicated the existence of Bi<sup>0</sup> [29].

The XPS spectra of O Is are shown in Figure 4(c). The O Is peak is broad and complicated due to the nonequivalence of oxygen ions. The peak shape suggests that it is composed of multiple peaks that arise due to the overlapping contributions of oxide ions. The strong peak at 529.8 eV is ascribed to Ti–O bond in  ${\rm TiO_2}$ , the peak at 531.4 eV, which is assigned to the oxygen attached to bismuth (Bi–O bond), and

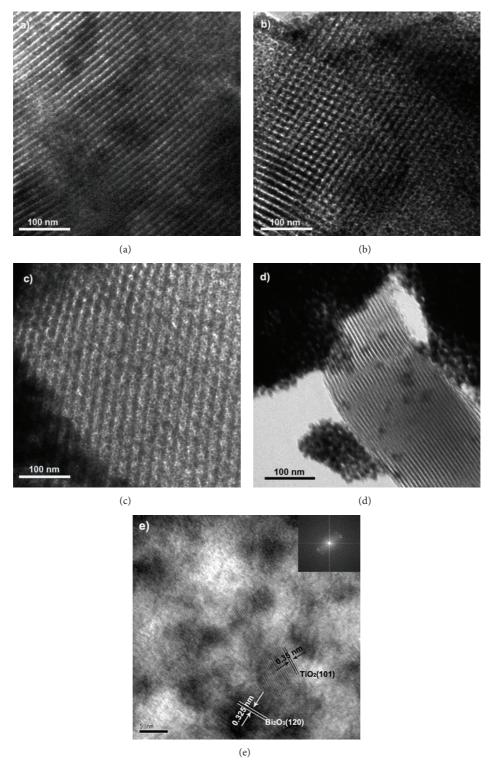


FIGURE 3: TEM images of Bi-TiO<sub>2</sub>/SBA-15: (a) Bi-TiO<sub>2</sub>/SBA-15(400), (b) Bi-TiO<sub>2</sub>/SBA-15(550), (c) Bi-TiO<sub>2</sub>/SBA-15(700), (d) Bi-TiO<sub>2</sub>/SBA-15(850), and (e) HRTEM image of Bi-TiO<sub>2</sub>/SBA-15(550) (inset is the corresponding FFT pattern).

the shoulder at  $533.6\,\mathrm{eV}$  is attributed to the OH<sup>-</sup> group absorbed on the surface. The Ti 2p of Bi-TiO<sub>2</sub>/SBA-15 is shown in Figure 4(d). The peaks of Ti2p3/2 and Ti2p1/2 were centered at  $458.2\,\mathrm{and}\,464.7\,\mathrm{eV}$ , which showed that the

main valence of Ti in the prepared catalysts is +4 and Ti<sup>4+</sup> is in tetrahedral coordination with oxygen in the catalysts. Meanwhile, there was no significant influence on the spectra in either Ti 2p or O 1s in the presence of  $Bi_2O_3$ .

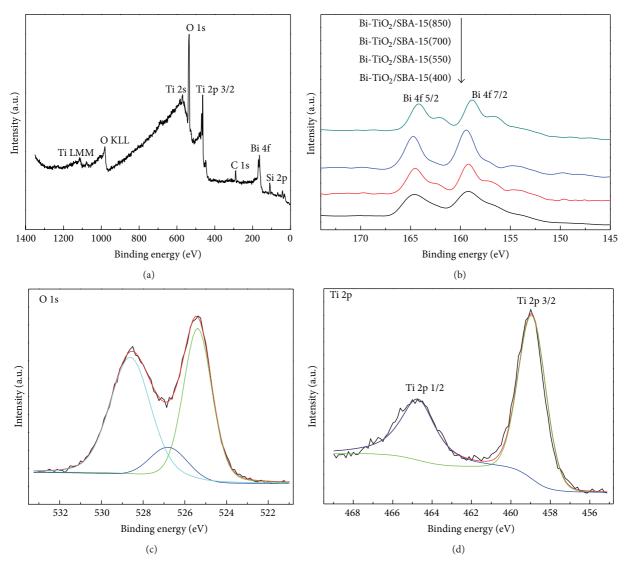


FIGURE 4: XPS survey spectrum of Bi-TiO<sub>2</sub>/SBA-15 (a), the high-resolution XPS spectra of Bi 4f region (b), O 1s (c), and Ti 2p (d).

The UV-Vis absorption spectra of the Bi-TiO<sub>2</sub>/SBA-15 were presented in Figure 5(a). There a red shift for Bi-TiO<sub>2</sub>/SBA-15 in the visible region. The results show that the doping of Bi can increase the absorbance of visible light and extend the absorption edge to longer wavelengths. It can be seen that the Bi-TiO<sub>2</sub>/SBA-15 calcined at 400-700°C displayed similar absorbance for visible lights, suggesting that, in the composite, Bi<sub>2</sub>O<sub>3</sub> mainly resulted in the spectral response in the visible region. However, with the increase of calcination temperature to 850°C, the Bi-TiO<sub>2</sub>/SBA-15 showed an obviously stronger absorption in the visible light region than that of calcined at other temperatures, which might be due to the formation of a new phase of Bi<sub>4</sub>Ti<sub>3</sub>O<sub>12</sub> at 850°C. Moreover, the plot of  $(\alpha h \nu)^{1/2}$  versus the energy of light afforded band gap energy of 2.81 eV for Bi-TiO<sub>2</sub>/SBA-15 (see the inset in Figure 5(a)), which could be easily induced photoelectrons and holes by visible lights.

PL emission spectra have been used to investigate the efficiency of charge carrier trapping, immigration,

transfer and to understand the fate of electron-hole pairs in semiconductor particles [30]. Figure 5(b) showed the PL spectra of  ${\rm TiO_2}$  and  ${\rm Bi\text{-}TiO_2/SBA\text{-}15}$  in the range of 400–525 nm. The PL intensity of the samples decreases as follows:  ${\rm TiO_2} > {\rm Bi\text{-}TiO_2/SBA\text{-}15(400)} > {\rm Bi\text{-}TiO_2/SBA\text{-}15(700)} > {\rm Bi\text{-}TiO_2/SBA\text{-}15(850)} > {\rm Bi\text{-}TiO_2/SBA\text{-}15(550)}$ . It indicated that, when increasing the calcination temperature, the decrease in trap states on samples surface may slow the recombination process of photogenerated electrons and holes in  ${\rm TiO_2}$ , which benefit the photocatalytic reaction.

3.2. The Photocatalytic Activity of Bi-TiO<sub>2</sub>/SBA-15. The UV-Vis absorption spectra clearly reveal that the visible light absorption of Bi-TiO<sub>2</sub>/SBA-15 is higher than that of TiO<sub>2</sub>. Therefore, it is reasonable to expect higher photocatalytic activity when the Bi species and TiO<sub>2</sub> deposited on the SBA-15 mesostructure. We evaluated the Bi-TiO<sub>2</sub>/SBA-15(x) samples for degradation of RhB under visible light irradiation and compared the catalytic efficiency of Bi-TiO<sub>2</sub>/SBA-15(x) with

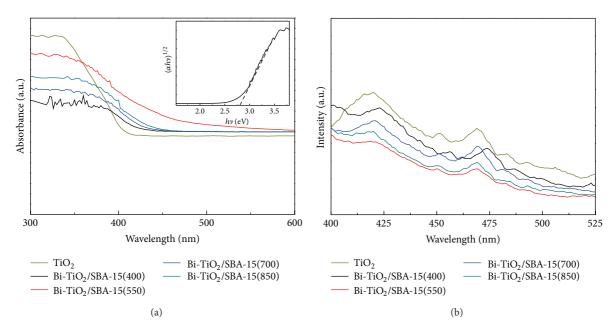


FIGURE 5: UV-Vis absorption spectra (a) and PL spectra of Bi-TiO<sub>2</sub>/SBA-15 (b).

that of TiO<sub>2</sub>. The photoactivities for RhB in dark in the presence of the photocatalyst under visible light irradiation in the absence of the photocatalyst are evaluated. It is found that there was no degradation for the RhB in the dark and in the presence of the photocatalyst. There is no degradation observed for RhB when the solution is placed under visible light radiation without the addition of photocatalysts.

Figure 6(a) displayed the effect of the calcination temperature on the photocatalytic activity. The activities decrease showed in the following order:  $Bi-TiO_2/SBA-15$  (550) >  $Bi-TiO_2/SBA-15$ (850) >  $Bi-TiO_2/SBA-15$ (700) >  $Bi-TiO_2/SBA-15$ (400) >  $Bi_2O_3/SBA-15$  >  $TiO_2/SBA-15$ (550) >  $Bi_2O_3$  >  $TiO_2$ .

It is well known that pure  $TiO_2$  and  $TiO_2/SBA-15$  have no photocatalytic activity under visible light irradiation. However, in Figure 6(a), the experiment results show a little decomposition ability of RhB, which is due to the small size of  $TiO_2$  nanoparticles improving the photocatalytic activity. The degradation efficiency by  $Bi_2O_3/SBA-15$  and  $Bi_2O_3$  is also low.

The Bi-TiO<sub>2</sub>/SBA-15(x) almost decomposed the RhB solution within 90 min, compared to the TiO<sub>2</sub> sample, which implies that the doped Bi is essential as a cocatalyst for the efficient degradation. That is to say, the Bi doping on TiO<sub>2</sub>/SBA-15 is accorded to the higher photodegradation, which resulted from the formation of Bi species enhancing the electron and hole separation by capturing the photoinduced charges efficiently. There are two reasons for the superior photocatalytic performance. Firstly, valence band (VB) composed of hybridized Bi 6s, Ti 3d, and O 2p orbitals has a strong oxidizing ability and can effectively degrade organic pollutants. And the hybridization of the Bi 6s, Ti 3d, and O 2p levels makes the VB largely dispersed, which favors the mobility of photoholes in the VB and is beneficial for the oxidation reaction. Secondly, the assembled Bi<sub>2</sub>O<sub>3</sub> increases the mobility of the photogenerated carriers, and good crystallization may lead to the enhancement of photocatalytic activity for the decomposition of the organic compounds. It is allowing more opportunities for electrons to participate in the reduction reaction to form active oxygen species. The transfer of the photoexcited electrons from the surface of  $\mathrm{Bi_2O_3}$  to  $\mathrm{TiO_2}$  occurs due to the small  $\mathrm{Bi_2O_3}$  band gap and its higher conduction band potential compared to that of  $\mathrm{TiO_2}$ .

It is known that photodegradation kinetics follow Langmuir-Hinshelwood kinetics model [31]. The reaction can be represented as follows (1):

$$\ln \frac{C_0}{C} = k_{\rm app}t,$$
(1)

where  $k_{app}$  is the apparent first-order reaction constant and  $C_0$  is the initial concentration of the RhB solution. A kinetic linear simulation curve of RhB photocatalytic degradation using Bi-TiO<sub>2</sub>/SBA-15(x) is shown in Figure 6(b). The fact that the curve showed good linearity indicating that the photo catalytic degradation of RhB using Bi-TiO<sub>2</sub>/SBA-15(x) as catalyst fits well with the first-order reaction kinetics. The rate constant of Bi-TiO<sub>2</sub>/SBA-15(x) for RhB photodegradation is shown in Table 2.  $k_{\rm app}$  value of the Bi-TiO $_2$ /SBA-15(550) is 0.0212 min<sup>-1</sup>, which is higher than that of TiO<sub>2</sub> and other samples of Bi-TiO<sub>2</sub>/SBA-15. It suggested that  $k_{app}$  improved by Bi doping. It is widely accepted that the high calcination temperature usually results in smaller specific surface area and particle size, as illustrated in Table 1. The calcination temperature strongly influenced the activity of the samples. Though the sample calcined at 400°C has the largest BET surface area and particle size, its crystalline is worse than that of the calcined at higher temperature, leading to lower photoactivity. Meanwhile, the effect of the photocatalytic activity is decreased when the calcination temperature is up to 700-850°C. It can be explained that the high calcination

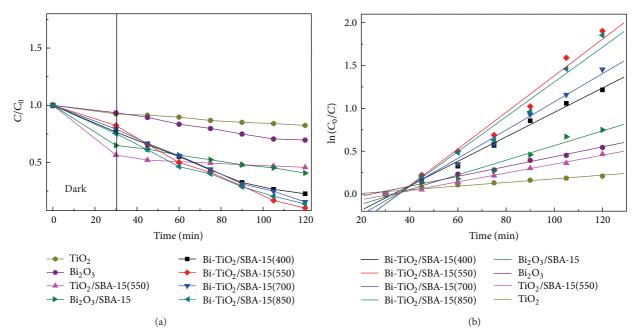


FIGURE 6: Photocatalytic activity (a) and kinetic linear simulation curve (b) of photocatalytic degradation by  $Bi-TiO_2/SBA-15(x)$  under visible light.

Table 2: The rate constant of  $Bi-TiO_2/SBA-15(x)$  for RhB photodegradation.

Samples	$k_{\rm app}~({\rm min}^{-1})$
Bi-TiO <sub>2</sub> /SBA-15(400)	0.0135
Bi-TiO <sub>2</sub> /SBA-15(550)	0.0212
Bi-TiO <sub>2</sub> /SBA-15(700)	0.0162
Bi-TiO <sub>2</sub> /SBA-15(850)	0.0206
Bi <sub>2</sub> O <sub>3</sub> /SBA-15	0.00818
TiO <sub>2</sub> /SBA-15(550)	0.00553
$Bi_2O_3$	0.00755
TiO <sub>2</sub>	0.00540

temperature destructed pore structure and caused loss in surface area to some extent, reducing the oxygen vacancies. The samples at 850°C show better photocatalytic activity than samples at 700°C, which might be due to the formation of a new phase of  $\rm Bi_4Ti_3O_{12}$  having higher photocatalytic activity. The sample calcined at 550°C shows the highest photocatalytic activity in the decomposition of RhB under visible light. Furthermore, the doping of Bi could effectively limit the phase transformation, preventing the overgrowth of crystallites and enhancing the visible light absorption in comparison with TiO<sub>2</sub> and TiO<sub>2</sub>/SBA-15.

In addition, the Bi-TiO<sub>2</sub>/SBA-15 obtained at 550°C presents the highest photocatalytic activity. However, as an excellent catalyst, it should not only show higher activity but also present stability in recycle process. As shown in Figure 7, Bi-TiO<sub>2</sub>/SBA-15 can preserve most of its catalytic activity after six cycles and this confirms that the as-prepared Bi-TiO<sub>2</sub>/SBA-15 is stable under irradiation for photocatalytic decomposition of organic pollutants.

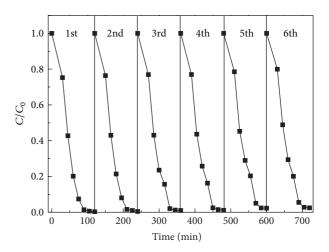


FIGURE 7: Recycling photocatalytic test of Bi-TiO $_2/{\rm SBA}{\text -}15$  calcined at 550°C.

#### 4. Conclusions

In conclusion, we have fabricated a visible photocatalyst Bi-TiO<sub>2</sub>/SBA-15 material. The photocatalytic activity of the prepared photocatalysts was investigated by the photodegradation of RhB. A combination of XRD, XPS, Raman, nitrogen adsorption-desorption isotherm measurement, TEM, and UV-Vis absorption spectra has been used to characterize the Bi-TiO<sub>2</sub>/SBA-15 material. The experiment results indicated that the Bi doping could enhance the photocatalytic activities than TiO<sub>2</sub>. The calcination temperature strongly influenced the activity of the samples. The sample calcined at 550°C shows the highest photocatalytic activity in the decomposition of RhB under visible light. This work provides a new

pathway to design and fabricate novel photoactive materials for practical application in environmental cleaning.

### **Conflict of Interests**

The authors declare that they do not have any commercial or associative interests that represents a conflict of interest directly or indirectly in connection with our work.

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